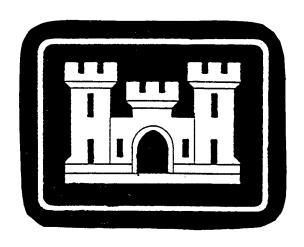


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FY95 LIMITED ENERGY STUDY FOR THE AREA "A" PACKAGE BOILER

HOLSTON ARMY AMMUNITION PLANT KINGSPORT, TENNESSEE



U.S. ARMY CORPS OF ENGINEERS MOBILE DISTRICT

CONTRACT NO.: DACA01-94-D-0007

DELIVERY ORDER NO.: 003

FINAL REPORT

Approved the public release:

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AESE PROJECT NO.: 95046-00

3 NOVEMBER 1995

DEPARTMENT OF THE ARMY

CONSTRUCTION ENGINEERING RESEARCH LABORATORIES, CORPS OF ENGINEERS
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ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

FINAL REPORT

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Prepared For:

Mobile District
U.S. Army Corps of Engineers
Mobile, Alabama

DTIC QUALITY INSPECTED 2

Prepared By:

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I. Executive Summary

Introduction

In March 1995, Affiliated Engineers SE, Inc. (AESE) was retained by the Mobile District U.S. Army Corps of Engineers to perform a Limited Energy Study for Holston Army Ammunition Plant, Kingsport, Tennessee.

The field survey of existing conditions was completed in May 1995. The results of this field survey were subsequently tabulated and used to generate single line building drawings on Autocad.

This report summarizes the results obtained from this field investigation and the analysis of various alternative Energy Conservation Opportunities (ECO's). To develop the field data into various alternative ECO concepts or models, we utilized an "Excel" spreadsheet to tabulate and compare energy consumption, installation and operating costs for various ECO's.

These ECO's were then analyzed for suitability for the Energy Conservation Investment Program (ECIP) using the government's software package called Life Cycle Cost in Design (LCCID).

Scope of Work

The Scope of Work developed by the U.S. Army Corps of Engineers gave the following tasks:

- 1. Perform a field survey to gather information on existing operating conditions and equipment at Holston Army Ammunition Plant, Area "A".
- 2. Perform a field survey to gather information on existing boilers laid away at Volunteer Army Ammunition Plant in Chattanooga, Tennessee.
- Provide a list of suggested ECO's.
- 4. Analyze ECO's using the LCCID program.
- 5. Perform savings to investment ratio (SIR) calculation.
- 6. Rank ECO's per SIR's.

- 7. Provide information on study assumptions and document equations used in calculations.
- 8. Perform Life Cycle Cost Analysis.
- Perform Synergism Analysis.
- 10. Calculate Energy/Cost Ratios.
- 11. Calculate Benefit/Cost Ratios.
- 12. Provide documentation in the form of Project Development Brochures (PDB's) and DD Form 1391.
- 13. Provide recommendations for implementation of ECO's into projects by ECIP priority.
- 14. Prepare a report to document the work performed, results, and recommendations.

Buildings examined for Energy Conservation Opportunities were as follows:

Area "A" Building 8-A Steam Plant

Area "A" Building 7-A Acetic Anhydride Manufacture

Description of ECO's

Six alternate methods (ECO's) of providing and/or utilizing thermal energy, in the form of steam, in the acetic anhydride production processes at Area "A" were studied. One ECO addressed operating procedure change only, with no associated first cost. Two ECO's addressed operation using boilers relocated from Volunteer Army Ammunition Plant (VAAP), Chattanooga, Tennessee; these ECO's differed in system operating procedures, but had identical estimated first cost. A final ECO addressed the provision of a new 100 psig, natural gas fired, 30,000 lb/hr capacity boiler and the layup of the existing 400 psig boiler system.

The six ECO's were each compared to baseline conditions which were developed from historical data, with data extrapolated to represent the anticipated 1996 production of 2 million lbs equivalent RDX explosive.

The following description for Case 1 represents baseline system configuration.

Case 1

Existing stoker operated, coal fired boilers producing 400 psig, 575°F steam utilized at non-condensing turbines driving boiler feedwater pumps, boiler ID/FD fans, and 1,000 hp river water pumps. The river water pump backpressure turbine exhaust steam at 100 psig, augmented by steam from a pressure reducing station, is utilized for thermal requirements of the acetic anhydride chemical processes, as well as building and storage tank heating and pipeline steam tracing. Other turbine exhaust at 5 psig is used within the boiler room, primarily for feedwater heating in the deaerator. In addition, the case simulation includes manual discharge of steam so as to preclude boiler operation below 40,000 lbs/hr output, below which it has been found to be impossible to avoid boiler stack emissions limit violations.

Energy conservation opportunities studied in depth are further defined in Case 2 through Case 7 hereinafter.

Case 2

The system configuration is identical to the baseline, but existing electric driven feedwater and river water pumps are utilized in lieu of the turbine driven units.

Case 3

The Case 2 scenario is modified by retrofit of one of the six stoker operated, coal fired boilers with a natural gas burner installed in place of an existing (abandoned) producer-gas-tar burner on the furnace wall opposite the stoker drives. A nominal 50,000 mbh burner is considered, giving output modulation capability down to 20,000 #/hr steam output or below.

Case 4

Dual fuel boilers relocated from VAAP, producing 350 psig saturated steam, serve the pumps and thermal processes of the baseline (Case I) system configuration. Turbine driven ID/FD fans of the baseline system are not utilized, and electric driven forced draft fans relocated from VAAP are included. Existing deaerating heater systems and other water treatment equipment are retained.

Case 5

The system configuration is identical to Case 4 (with relocated VAÁP boilers), but existing electric driven feedwater pumps and riverwater pumps are utilized in lieu of the turbine driven units.

Case 6

Building 8A is "Layed Away" for future reactivation when required, and 100 psig steam demands are accommodated by a new packaged 850 bhp water tube boiler, natural gas fired, with light oil burning capability for standby purposes. The new boiler and feedwater/condensate conditioning and pumping equipment are proposed to be installed at the ground floor of Building 7 to the east of the existing heat recovery boiler. Natural gas is delivered to Building 7 at the northeast corner through an existing 6 inch supply pipe. Building 7 contains 32 cracking furnaces fired by natural gas from the 6 inch supply pipe, but at anticipated near future production levels, a limited number of furnaces will be active, leaving ample gasline capacity for boiler fuel.

Case 7

All conditions of the steam system of Case 6 are identical in Case 7. Because there is considerable uncertainty in estimating reduced fixed maintenance and overhead costs realized by deactivating boiler plant Building 8, the assumed Case 6 fixed maintenance cost of \$3,750 per month is increase to \$6,250 and the Case 6 fixed overhead cost of \$35,000 per month is increased to \$50,000. In effect, Case 7 provides a sensitivity indicator for evaluation of assumptions.

Case 8

All conditions of the steam system of Cases 6 and 7 are identical, but non-recurring savings (maintenance and overhead) was adjusted interactively within the LCCID program until the resultant SIR value was below the ECIP limiting criteria of 1.25. This minimum non-recurring savings amount was \$665,000.

It represents variable maintenance and overhead costs identical to Cases 6 and Case 7 (\$326,105); derived as follows:

	Case 7	Case 8
Total Non-Recur. Savings:	\$ 1,001,105	\$ 791,106
Less Fixed Savings: Case 6 - 12 (\$6,250 + \$50,000)	675,000	
Case 7 - 12 (\$3,750 + \$35,000) Variable Non-Recurring	\$ 326,105	465,000 \$ 326,106

The Case 8 calculated fixed monthly maintenance and overhead savings is as follows:

Savings =
$$\underline{$665,000 - $326,105}$$
 = \$28,250 per month 12

This value compares to the baseline case assumption of \$56,250 per month (\$37,500 fixed maintenance + \$18,750 fixed overhead).

Other Alternatives

An additional ECO was considered to retrofit existing 100 psig firetube heat recovery boilers at the Acetic Anhydride Manufacturing Facilities in Building 7-A with supplemental natural gas burners. It was abandoned after partial analysis indicated its system control complexity required to accommodate variations in the sequencing and operation of the 32 cracking furnaces, representing the waste heat source, rendered this ECO infeasible.

As an alternative to purchasing a new 100 psig boiler, AESE was requested to provide a cursory evaluation of costs and conditions for rental or lease of a new boiler system equivalent to the case 6, 7 and 8 proposed boiler three firms advertising in trade magazines as having boilers for rent/lease were contacted. Indeck Power Equipment Co. provide a proposal for an 800 hp boiler and deaerator at \$3,800 per month, minimum 3 year term. Their written proposal is presented in Appendix 9. An LCCID analysis was performed for reference, identified as Case 9, described as follows:

Case 9

The energy related data of Case 8 are duplicated for leased equipment on a 3 year lease. Because a 3 year life is used, this data is for information only and cannot be directly compared to other cases.

FINDINGS, ANALYSIS AND RESULTS

It was determined that significant fossil fuel energy savings could be realized by utilizing natural gas fuel in lieu of coal at the extremely low explosives production rate projected for 1996, with moderate increase in electrical energy consumption. Quantified values are as follows:

CASE NO.	FOSSIL FUEL ENERGY REDUCTION
	BASELINE
2	(46338 - 46338) (12) = 0 MMBtu/yr
3	(46338 - 25504) (12) = 250,008 MMBtu/yr
4	(46338 - 25173) (12) = 255,180 MMBtu/yr
5	(46338 - 25173) (12) = 255,180 MMBtu/yr
6	(46338 - 23238) (12) = 277,200 MMBtu/yr
7	(46338 - 23238) (12) = 277,200 MMBtu/yr
8	(46338 - 23238) (12) = 277,200 MMBtu/yr
9	(46338 - 23238) (12) = 277,200 MMBtu/yr

CASE NO.	ELECTRICAL INCREASE
	BASELINE COMPARISON
2	3350 - 28857 = -25507 MMBtu/yr
3	3350 - 26037 = -22687 MMBtu/yr
4	3350 - 5534 = -2184 MMBtu/yr
5	3350 - 35372 = -32022 MMBtu/yr
6	3350 - 32587 = -29237 MMBtu/yr
7	3350 - 32587 = -29237 MMBtu/yr
8	3350 - 32587 = -29237 MMBtu/yr
9	3350 - 32587 = -29237 MMBtu/yr

Results of the LCCID analysis, prioritized by descending SIR, are as follows:

Priority No.	Case No.	SIR	Tota	l Investment	Simple Payback
1	6	10.70	\$	420,000	0.68
2	7	4.78	\$	420,000	1.03
3	8	1.22	\$	420,000	1.49
4	4	-2.74	\$	350,000	2.53
5	5	-10.75	\$	350,000	-4.09
6	3	-87.22	\$	65,000	-0.27
7	2		\$	0.00	

The two analysis runs producing ECIP qualifying results (Construction Cost >\$300,000, SIR>1.25 and simple payback <10 years) are both for a new 100 psig firetube boiler proposed for installation in Building 7-A, and represent "sensitivity analyses" of assumed savings.

Operation with the new boiler saves fossil fuel energy at the expense of increased electrical consumption. The net result is reduced total energy consumption of 247,963 million Btu/yr.

Results of cursory analysis of a 3 year lease of the proposed new boiler (Case 9), compared to Case 8 purchased boiler at 15 year life cycle are as follows:

Case No.	SIR	Construction Cost		Simple Payback
8	1.22	\$	595,000	1.40
9	1.26	\$	375,00	1.26

II. Detailed Narrative

History

Holston Army Ammunition Plant (HSAAP) in Holston, Tennessee, manufactures explosives from raw materials. The facility comprises two separate areas designated Area "A" and Area "B". Each area is served by a steam plant which produces steam for production processes, equipment operation, space heating, domestic water heating, steam tracing, and product storage heating requirements.

Construction of the steam plant serving Area "A" (Building 8-A) was completed in 1943. The majority of the equipment in the plant is the original design with relatively minor changes since the original installation. Seven boilers, each having a full-load capacity of at least 100,000 pounds per hour (lb/hr), are located in the building. Six of the boilers are coal-fired spreader stoker dump grate type. The seventh boiler is a pulverized coal-fired type. The pulverized coal fired boiler and one of the stoker type boilers are currently layed away (not operational). Only two of the five remaining stoker type boilers are currently operated, with one active and the other on stand-by. Operation is rotated on a weekly schedule.

Problem Statement

Demand for explosives has declined in the last few years and is expected to continue to decline in the near future. As production levels drop and production lines are taken out of service, the demand for steam in Area "A" has fallen.

Present steam demand averages 35 to 40,000 lb/hr. The one active boiler cannot be reduced in capacity below 35 to 40,000 lb/hr without experiencing problems with excessive smoke production. Electrostatic precipitators installed to meet federal emission standards operate effectively when the boilers are operating at more than 40,000 lb/hr, but are unable to handle the excessive smoke generated when operating below 40,000 lb/hr. The resultant smoke stack discharges exceed levels allowed by the present air pollution operating permit. When steam demand falls below the minimum operating point of one boiler, excess steam is vented to the atmosphere. This practice results in increased operating and maintenance costs to replace the mass of water (steam) lost from the system.

Purpose of the Study

The purpose of this study is to identify and evaluate the technical and economic feasibility of alternative methods of meeting the steam requirements of the Area "A" industrial complex.

The following items were specifically requested to be evaluated.

- Evaluate the use of two new gas-fired packaged boilers sized to meet the requirements
 of the industrial complex. The new boilers would be installed adjacent to the existing
 steam plant and would utilize the existing smokestacks and steam distribution system.
- Evaluate using the existing steam distribution system rather than locating multiple boilers at various sites.
- Existing steam driven chillers will be replaced with electric driven equipment. Evaluate this impact on the steam system requirements.
- Field survey and test two existing gas-fired packaged boilers located at the Volunteer Army Ammunition Plant in Chattanooga, Tennessee. The two boilers were last used about 1980 and are presently laid away. The boilers are approximately the same capacity and operating characteristics as the ones at HSAAP. Relocation of the existing boilers and ancillary equipment (feedwater pumps, deaerators, fans, etc.) would be required as well as repairs or modifications necessary to meet current operating conditions and standards. The packaged boilers would be installed adjacent to the existing steam plant and would utilize the existing smokestacks and steam distribution system.
- Include maintenance and operating costs as well as savings in evaluations. This should include lay away costs of existing equipment.
- Present natural gas service to Area "A" is billed at an uninterruptible rate and is not likely to change. Evaluate dual fuel (No. 2 fuel oil) capability of packaged boiler installations including present storage and costs of additional storage.

Evaluate impact of any proposed installations or permit.



 Evaluate turbine drives on equipment such as rielectric drives. (It was noted during investigation used in an attempt to maintain boiler demand above 4,000 lbs/hr).

Alternate methods of meeting Area "A" steam requirements which were identified and which were not evaluated as part of this study are as follows:

- Replace the existing spreader stoker dump grate equipment on one or more boilers to a
 more efficient continuous ash discharge stoker. This would retain the capability of
 burning coal but utilize a more efficient stoker. Operating and maintenance costs should
 be reduced.
- Replace the existing spreader stoker dump grate equipment on one or more boilers with gas fired burners. This should reduce operating and maintenance costs at the expense of losing the capability of burning coal.

The two alternatives identified above are presented as possible future studies. Retrofiting boilers of this vintage requires a detailed study of the boilers which is beyond the scope of the present study.

Study Approach

Technical and economic evaluation of alternative methods for efficiently providing steam to the anhydride production processes at Area A are based on comparisons to baseline information developed from documents representing various historical production and consumption data. Data to represent uniform annual production rates down to the projected 2 million lbs of explosive in 1996 (0.167 million lbs per month) and for the mobilization rate of 27 million lbs per month are extrapolated from the historical data.

The following assumptions have been made:

- 1) System piping losses (heat loss and steam leakage) are constant.
- 2) Oxygen content of coal fired boiler flue gas varies uniformly from 6 percent by weight at 100,000 lbs/hr steam output to 12 percent by weight at 40,000 lbs/hr steam output.
- 3) Natural gas burners operate at 7.5 percent excess air throughout a turndown ratio of 4:1; burners cycle off/on at boiler output below 25 percent of full load.
- 4) Electrical consumption of steam plant equipment for baseline conditions is 2.8 kWh/K# steam.
- 5) Fixed maintenance cost is \$37,500 per month for coal fired operation and \$18,750 per month for relocated natural gas fired boiler operation; variable maintenance cost for coal fired operation (including coal handling, ash disposal and miscellaneous consumables) is \$.50 per thousand pounds steam and \$.15 per thousand pounds of steam for natural gas fired boilers. Fixed maintenance cost for system operation with the new 30,000 #/hr boiler will be significantly reduced and is assumed to be between one third and one fifth of costs used for relocated boilers.
- Fixed plant overhead cost is \$70,000 per month; with Building 8A functionally viable; variable overhead cost is \$0.25 per thousand pounds of steam. With Building 8A "layed away" and steam supplied by the new 30,000 #/hr boiler, fixed plant overhead is assumed to be between \$35,000 and \$50,000 per year.
- 7) Unburned fuel losses are zero under all operating conditions.
- 8) Coal fired boiler minimum load of 40000 #/hr is maintained artificially by venting steam from the 100 psig steam header.
- 9) Mollier diagram back pressure turbine steam state lines with saturated throttle steam are parallel to design process lines in the superheat region as indicated in Figure 1 and Figure 2 on the following pages.

Figure 1 - Boiler Feed Pumps

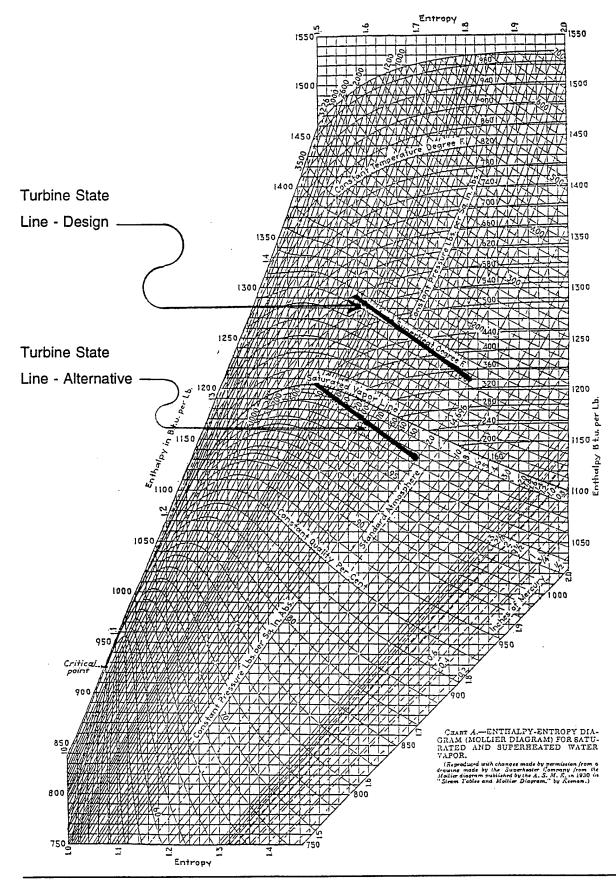
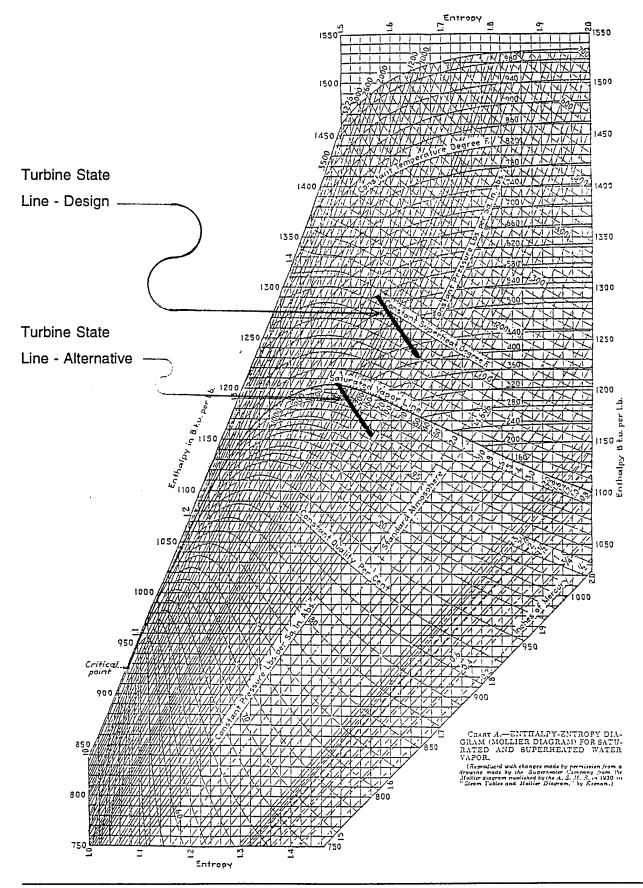


Figure 2 - River Water Pumps



10) Reduced production rates of equivalent RDX explosives will be accommodated by continuous process operation, rather than limited duration batch operations at a higher rate and with systems idle for appropriate durations.

Energy Consumption Calculations

Historical data provided by Holston Defense Corporation (HDC), including Area A Monthly Report Steam Production Data for calendar years 1989 through 1994 and partial 1995 information, and reports for fiscal years 1991, 1992, partial 1993, 1994 and partial 1995 for equivalent RDX explosives production, were used as input for computerized spreadsheet preparation. The data was then reduced to unit rating parameters pursuant to development of production curves of steam rate (lbs stm per lb equivalent RDX) versus uniform monthly production rate of explosives.

Curves for boiler efficiency versus boiler steam output were developed from abbreviated ASME combustion and boiler heat balance calculations, utilizing representative parameters from coal analysis reports for fuel delivered in February, March, May and October 1994, and January 1995, and for natural gas having heating value of 1,000 Btu/cf as indicated on United Cities Gas Company utility bill.

Conversion value used for all electrical energy calculations was 3,413 Btu/kWh.

Process steam flow rates at 400 psig, 575°F conditions were converted to equivalent flow rates for 350 psig saturated steam using steam enthalpy ratio as the conversion factor.

Completed calculation sheets and data provided by HDC are presented in Appendix 1.

Graphical representation of historical data and results of calculations are presented in Figure 3 through Figure 7 on the following pages.

Production rates below 167 thousand pounds per month have not been evaluated. This rate represents the projected production level of 2 million pounds in 1996, which is the production level included in meeting notes of the entry interview of June 2, 1995.

Figure 3 - Facility Production Rates Historical Data

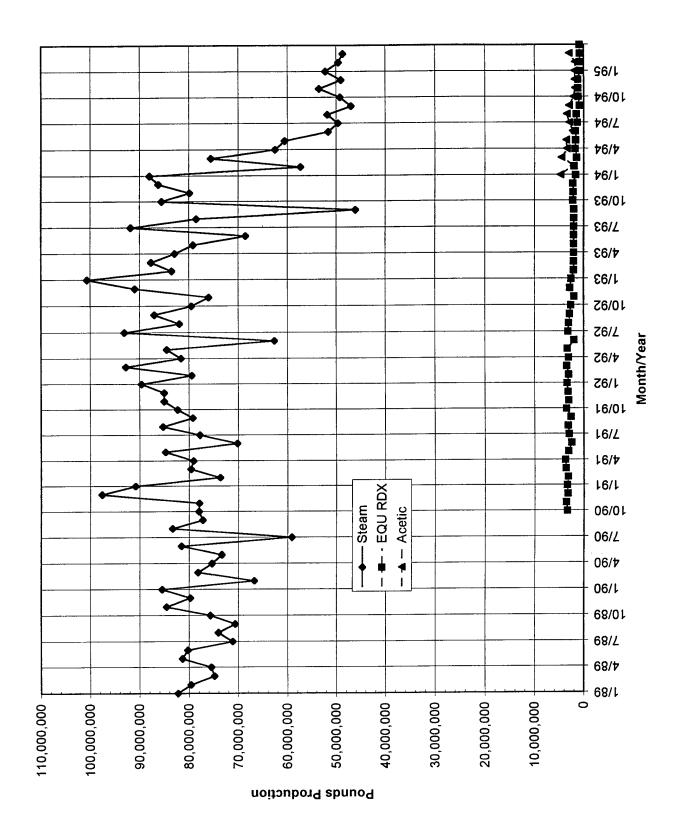


Figure 4 - Equivalent RDX Production Historical Data

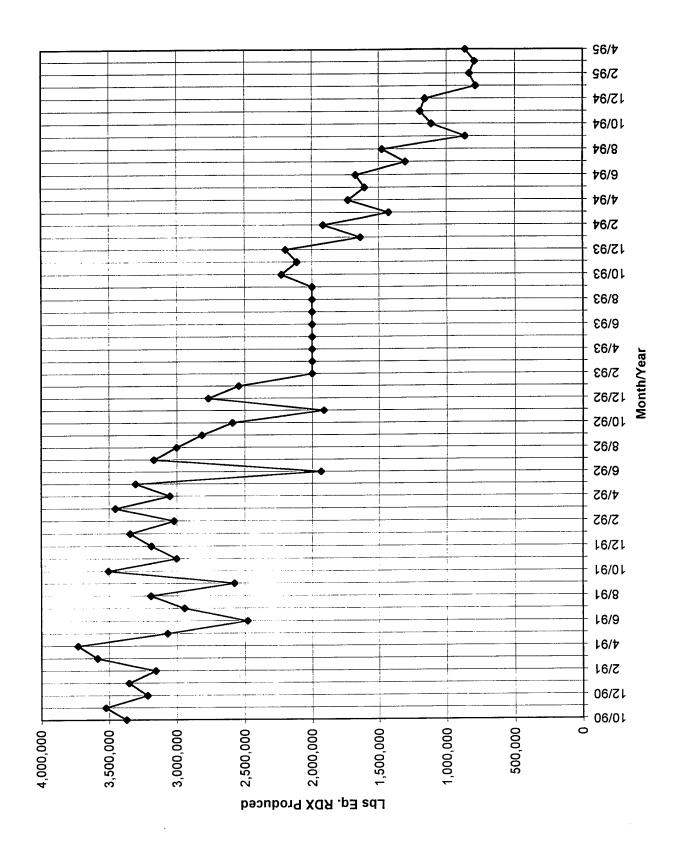


Figure 5 - Steam Production Historical Data

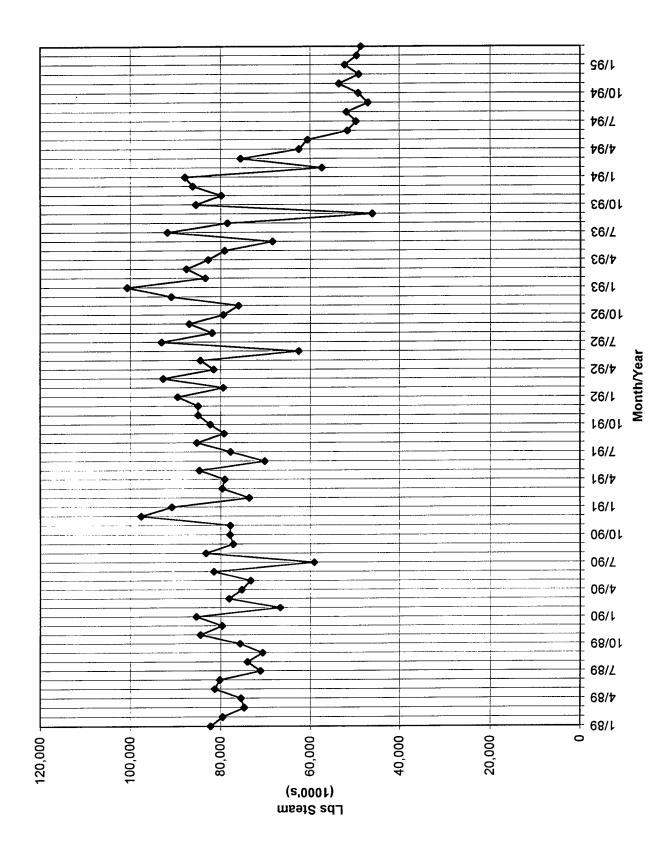


Figure 6 - Steam versus Eq. RDX Production

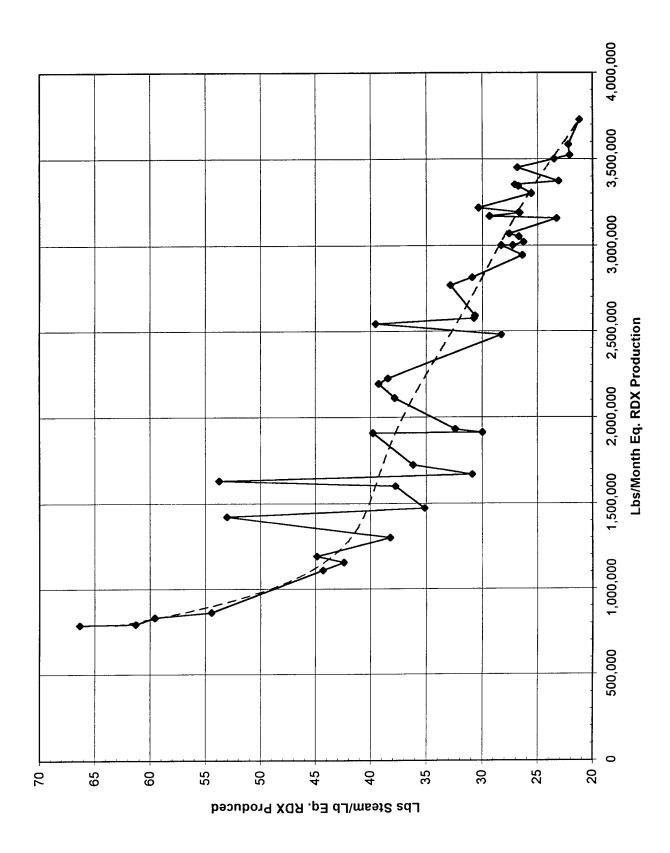
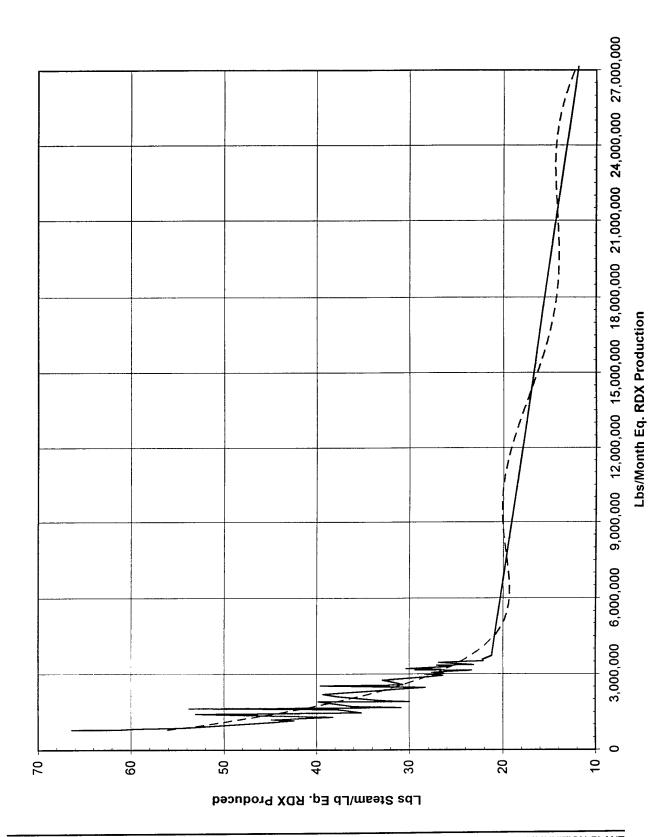


Figure 7 - Steam versus Eq. RDX Production with MOB Production Projection



Alternative Energy and Cost Savings

Baseline system energy and operating cost results (Case 1) were compared to seven alternative operating scenarios (Case 2 through Case 8). Delineated system operating mode for each case, and results of each analysis, are as follows:

Case 1 baseline scenario represents operation using coal fired, stoker operated steam boilers with boiler feedwater pumps, river water pumps and ID/FD fans driven by the existing non-condensing back pressure steam turbines.

For eight discrete equivalent RDX production rates between 0.15 million pounds per month, steam requirements and associated costs were calculated using the Microsoft Excel spreadsheet program. Keyboard input included unit cost of fuel, steam enthalpy, steam rate per unit of production (from Figures 6 and 7), and boiler efficiency (from modified ASME combustion and heat balance calculations). Formulae for calculated values in other spreadsheet columns are presented in Appendix 1.

Table 1 and Figure 8 on the following pages show baseline conditions of Case 1.

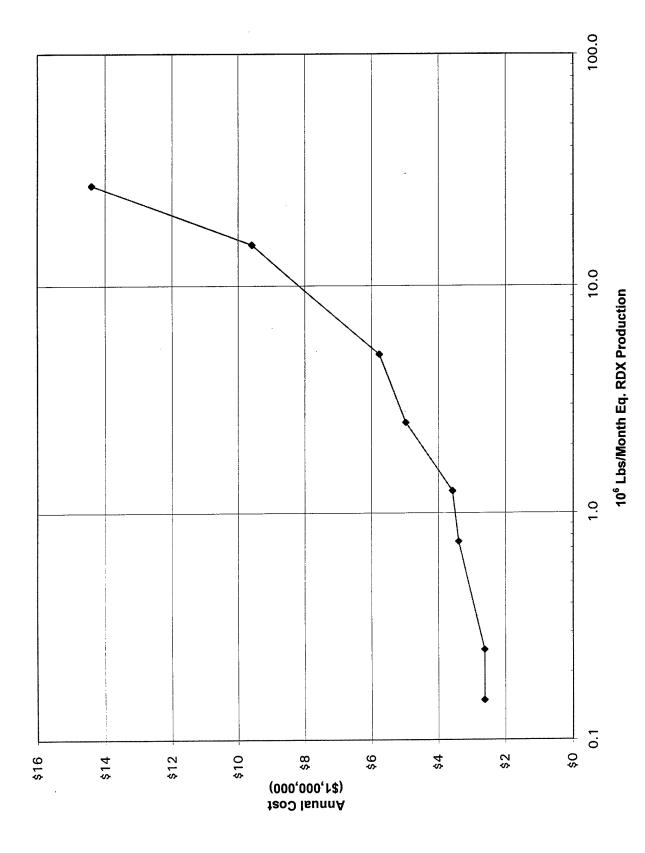
Corresponding tabular and graphical representation for comparative cases (ECO's), as well as applicable Life Cycle Cost Analysis Summary sheets, are presented following each case description.

Case 2 scenario represents operation of baseline coal fired steam production, with boiler feedwater pumps and river water pumps electric driven, and ID/FD fans turbine driven.

Appropriate input parameters were changed in the Excel spreadsheet, resulting in new annual cost values. These results are shown in Table 2 and Figure 9 herein. LCCID analysis summary for Case 2 follows on page 23.

Case 3 is similar to Case 2, with one of the existing boilers retrofitted with a natural gas burner installed in the existing abandoned tar burner opening to enable steam production rates below 40,000 #/hr without exceeding regulated emission rates. Results of changing the appropriate input parameters are shown in Table 3 and Figure 10 herein. LCCID analysis summary for Case 3 follows on page 28.

CASE NO. 1: EXSTG. SYST - RIV. WTR. & BLR. FD. PMPS. & ID/FD FANS TURB. DRVN.							
CASE	NO. 1.	EX31G. 31	51 - KIV. WIIK. 0	BEIC. I D. I IVII C	J. WIDH DITANG	TORD. DITTI	
MILL. #	₽/MO	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQUIV		·	BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
	0.15			110.00	38759.32	40000.00	75.00
	0.25		1290.20	85.00	39697.60	40000.00	75.00
	0.75		1290.20	65.00	45129.79	66780.82	80.70
	1.25		1290.20	42.00	45870.55	71917.81	79.50
	2.50		1290.20	33.00	68093.15	113013.70	77.20
	5.00	1.86	1290.20	20.50	75994.52	140410.96	79.20
	15.00	1.86	1290.20	13.00	151057.53	267123.29	82.10
	27.00	1.86	1290.20	11.50	280837.53	425342.47	82.90
MILL. #	#/MO.	FUEL MILL.	ANNUAL	ANNUAL	ANNUAL;	ANNUAL	TOTAL
EQUIV	'. RDX	BTU/MO	FUEL COST	ELECT. COST	MNTNC. COST	OVRHD. COST	ANNUAL COST
	0.15		\$1,034,274.28	\$34,339.20	\$625,200.00	\$927,600.00	\$2,621,413.48
	0.25	46,338	\$1,034,274.28	\$34,339.20	\$625,200.00	\$927,600.00	\$2,621,413.48
	0.75		\$1,604,778.96	\$57,330.00	\$742,500.00	\$986,250.00	\$3,390,858.96
	1.25			\$61,740.00	\$765,000.00	\$997,500.00	\$3,578,549.89
	2.50	127,191	\$2,838,904.51	\$97,020.00	\$945,000.00	\$1,087,500.00	\$4,968,424.51
	5.00	154,035	\$3,438,055.00	\$120,540.00	\$1,065,000.00	\$1,147,500.00	\$5,771,095.00
	15.00	282,691	\$6,309,654.67	\$229,320.00	\$1,620,000.00	\$1,425,000.00	\$9,583,974.67
	27.00	445,787	\$9,949,957.14	\$365,148.00	\$2,313,000.00	\$1,771,500.00	\$14,399,605.14

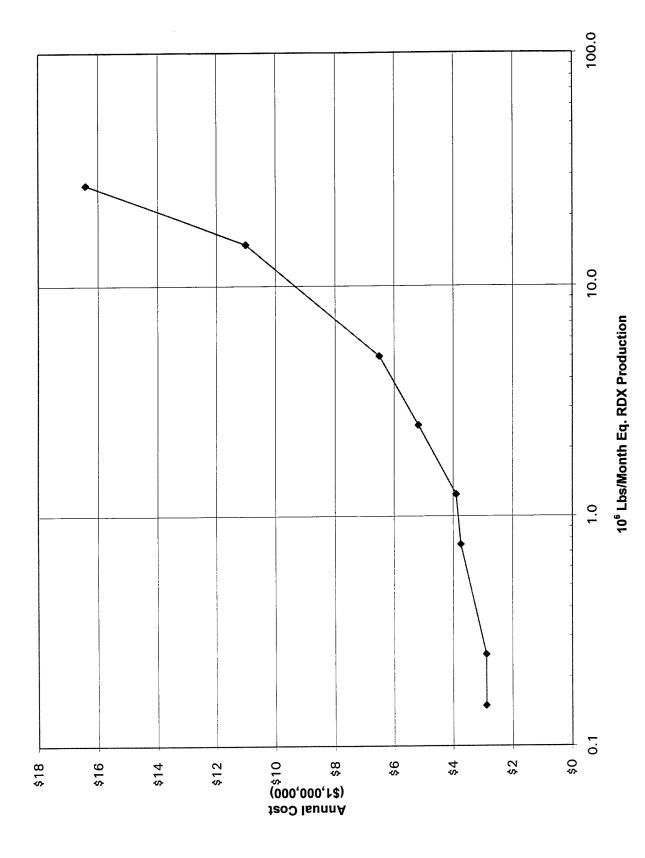


Life Cycle Analysis Summary

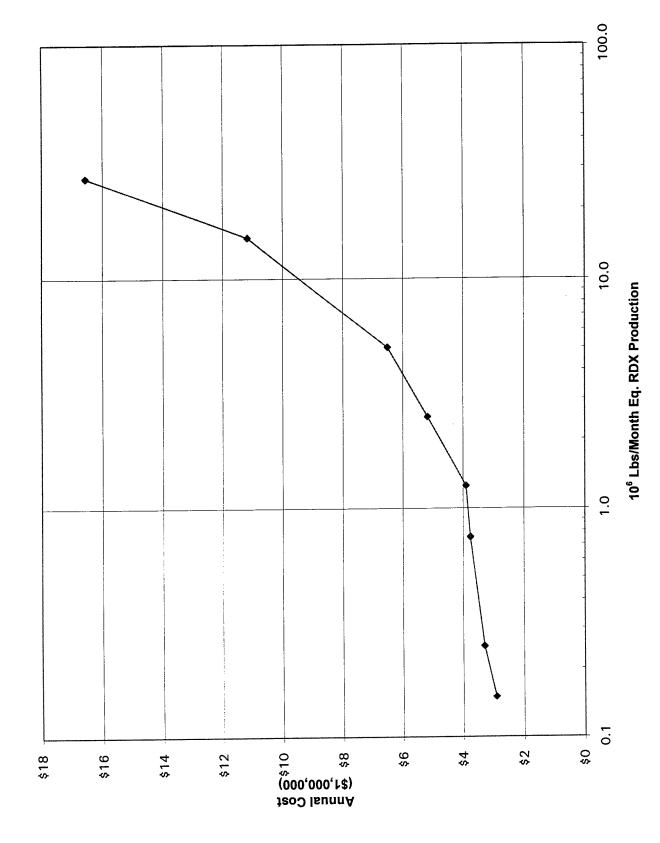
LIFE CYCLE COST ANALYSIS SUMMARY STUDY: 95046 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080 INSTALLATION & LOCATION: HOLSTON AAP REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 95046-00 LIMITED ENERGY STUDY FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE 2: ELECT. VS. TURB. PMPS. ANALYSIS DATE: 10-26-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE 1. INVESTMENT 0. A. CONSTRUCTION COST 0. B. SIOH C. DESIGN COST D. TOTAL COST (1A+1B+1C) \$ E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ F. PUBLIC UTILITY COMPANY REBATE G. TOTAL INVESTMENT (1D - 1E - 1F) ***** No investment costs; Other items should be checked. ***** 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 UNIT COST SAVINGS ANNUAL \$ DISCOUNT DISCOUNTED \$/MBTU(1) MBTU/YR(2) SAVINGS(3) FACTOR(4) SAVINGS(5) FUEL \$ -3248254. 12.43 A. ELECT \$ 10.25 -25495. \$ -261324. 0. 0. 13.56 B. DIST \$.00 0. 0. 15.09 0. 0. C. RESID \$.00 D. NAT G \$ 3.95 0. 15.86 0. 0. 0. 13.61 0. 0. E. COAL \$ 1.86 12.64 F. LPG \$.00 0. 0. 0. 11.85 M. DEMAND SAVINGS N. TOTAL -25495. \$ -261324. \$ -3248254. 3. NON ENERGY SAVINGS(+) / COST(-) 0. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 11.85 0. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS(+) / COSTS(-) DISCNT SAVINGS(+) YR DISCOUNTED FACTR SAVINGS(+)/ COST(-) OC ITEM (1) (3) COST(-)(4)(2) d. TOTAL \$ 0. 0. C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ -261324. .00 YEARS 5. SIMPLE PAYBACK PERIOD (1G/4) \$ -3248254. 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) 7. SAVINGS TO INVESTMENT RATIO (SIR)=(6 / 1G)=(IF < 1 PROJECT DOES NOT QUALIFY) 931.00 % 8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

CASE NO. 2:	EXSTG SV	ST PUMPS ELI	ECTRIC DRIVEN	I ID/FD FANS T	URB DRVN	
CAGE NO. 2.	LXOTG. OT	OT FORM O LLI	LOTRIO BRIVER	, IDN BITARE I	ORD. DIVIN.	
MILL. #/MO.	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQUIV. RDX		BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
0.15		1290.20	110.00	1629.66	40000.00	75.00
0.25	1.86	1290.20	85.00	2098.80	40000.00	75.00
0.75			65.00	4814.90	66780.82	77.50
1.25	1.86	1290.20	42.00	5185.27	71917.81	78.10
2.50			33.00	16296.58	113013.70	
5.00	1.86	1290.20	20.50	20247.26	140410.96	78.20
15.00	1.86	1290.20	13.00	57778.77	267123.29	81.00
27.00	1.86	1290.20	11.50	122668.77	425342.47	83.20
MILL. #/MO.	FUEL MILL.	ANNUAL	ANNUAL	ANNUAL;	ANNUAL	TOTAL
EQUIV. RDX	BTU/MO	FUEL COST	ELECT. COST	MNTNC. COST	OVRHD. COST	ANNUAL COST
0.15	46,338	\$1,034,274.28	\$295,783.15	\$625,200.00	\$927,600.00	\$2,882,857.43
0.25	46,338	\$1,034,274.28	\$295,783.15	\$625,200.00	\$927,600.00	\$2,882,857.43
0.75	74,867	\$1,671,040.80	\$340,270.35	\$742,500.00	\$986,250.00	\$3,740,061.15
1.25	80,007	\$1,785,757.18	\$348,803.70	\$765,000.00	\$997,500.00	\$3,897,060.88
2.50	118,019	\$2,634,175.82	\$507,784.20	\$945,000.00	\$1,087,500.00	\$5,174,460.02
5.00	156,004	\$3,482,019.90	\$804,623.40	\$1,065,000.00	\$1,147,500.00	\$6,499,143.30
15.00	286,530	\$6,395,341.33	\$1,560,573.00	\$1,620,000.00	\$1,425,000.00	\$11,000,914.33
27.00	444,179	\$9,914,079.89	\$2,418,811.92	\$2,313,000.00	\$1,771,500.00	\$16,417,391.81





CASE NO 3: 0	ONE CASE N	NO.2 BOILER RE	TROFIT W/ N.G	.BURNER		
0,102 110.0.						
MILL. #/MO.	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQUIV. RDX	BTU	BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
0.15	3.95	1290.20	110.00	1629.66	22602.74	77.00
0.25	3.95	1290.20	85.00	2098.80	29109.59	77.90
0.75	1.86	1290.20	65.00	4814.90	66780.82	76.80
1.25	1.86	1290.20	42.00	5185.27	71917.81	78.00
2.50	1.86	1290.20	33.00	16296.58	113013.70	83.10
5.00	1.86	1290.20	20.50	20247.26	140410.96	78.00
15.00	1.86	1290.20	13.00	57778.77	267123.29	79.00
27.00	1.86	1290.20	11.50	122668.77	425342.47	82.00
MILL. #/MO.	FUEL MILL.	ANNUAL	ANNUAL	ANNUAL;	ANNUAL	TOTAL
EQUIV. RDX	BTU/MO	FUEL COST	ELECT. COST	MNTNC. COST	OVRHD. COST	ANNUAL COST
0.15	25,504	\$1,208,903.14	\$266,883.54	\$549,000.00	\$889,500.00	\$2,914,286.68
0.25	32,467	\$1,538,933.18	\$277,692.45	\$577,500.00	\$903,750.00	\$3,297,875.63
0.75	75,550	\$1,686,271.64	\$340,270.35	\$742,500.00	\$986,250.00	\$3,755,291.99
1.25	80,110	\$1,788,046.62	\$348,803.70	\$765,000.00	\$997,500.00	\$3,899,350.32
2.50	118,161	\$2,637,345.70	\$507,784.20	\$945,000.00	\$1,087,500.00	\$5,177,629.90
5.00	156,404	\$3,490,948.15	\$804,623.40	\$1,065,000.00	\$1,147,500.00	\$6,508,071.55
15.00	293,784	\$6,557,248.71	\$1,560,573.00	\$1,620,000.00	\$1,425,000.00	\$11,162,821.71
27.00	450,679	\$10,059,163.99	\$2,418,811.92	\$2,313,000.00	\$1,771,500.00	\$16,562,475.91



Life Cycle Analysis Summary

STUDY: 95046 LIFE CYCLE COST ANALYSIS SUMMARY LCCID 1.080 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) REGION NOS. 4 CENSUS: 3 INSTALLATION & LOCATION: HOLSTON AAP PROJECT NO. & TITLE: 95046-00 LIMITED ENERGY STUDY FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE 3:N.G. BRNR. IN COAL BLR. ANALYSIS DATE: 10-26-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE 1. INVESTMENT 65000. A. CONSTRUCTION COST B. SIOH 3575. 3900. C. DESIGN COST S D. TOTAL COST (1A+1B+1C) \$ 72475. 0. E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ F. PUBLIC UTILITY COMPANY REBATE 72475. G. TOTAL INVESTMENT (1D - 1E - 1F) 2. ENERGY SAVINGS (+) / COST (-) DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993 DISCOUNTED ANNUAL \$ DISCOUNT UNIT COST SAVINGS SAVINGS(3) FACTOR(4) SAVINGS(5) \$/MBTU(1) MBTU/YR(2) FUEL \$ -2889093. \$ -232429. 12.43 A. ELECT \$ 10.25 -22676. 13.56 0. 0. B. DIST \$.00 0. .00 0. 15.09 0. C. RESID \$ 0. 15.86 \$-18863010. ***** \$-1189345. D. NAT G \$ 3.95 \$ 1034264. \$ 14076340. 13.61 E. COAL \$ 1.86 556056. 12.64 0. 0. F. LPG \$.00 0. 11.85 0. M. DEMAND SAVINGS 0. \$ -7675769. 232280. \$ -387510. N. TOTAL 3. NON ENERGY SAVINGS(+) / COST(-) 114300. A. ANNUAL RECURRING (+/-) (1) DISCOUNT FACTOR (TABLE A) 11.85 1354455. (2) DISCOUNTED SAVING/COST (3A X 3A1) B. NON RECURRING SAVINGS(+) / COSTS(-) DISCNT DISCOUNTED SAVINGS(+) YR FACTR SAVINGS(+)/ COST(-) OC ITEM (2) (3) COST(-)(4)(1) 0. 0. d. TOTAL C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 1354455. 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ -273210. -.27 YEARS SIMPLE PAYBACK PERIOD (1G/4) 6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C) \$ -6321314. (SIR)=(6 / 1G)=7. SAVINGS TO INVESTMENT RATIO (IF < 1 PROJECT DOES NOT QUALIFY) **** Project does not qualify for ECIP funding; 4,5,6 for information only.

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

N/A

Case 4 scenario represents operation with natural gas fired steam boilers, relocated from the Volunteer Army Ammunition Plant (VAAP), and with feedwater pumps and river water pumps turbine driven. VAAP boiler FD fans are electric driven. Results of changing the appropriate input parameters are shown in Table 4 and Figure 11 herein. LCCID Analysis Summary for Case 4 follows on page 32.

Case 5 scenario is similar to Case 4, with all pumps electric driven rather than turbine driven. Results of changing the appropriate input parameters are shown in Table 5 and Figure 12 herein. LCCID analysis summary for Case 5 follows on page 35.

Case 6 scenario represents system operation utilizing a new boiler producing 100 psig saturated steam, with the existing 400 psig steam production and distribution system "layed away" for future return to service as required. The new system includes new deaerating heater-feed pump set and packaged firetube 850 bhp boiler with dual fuel (natural gas and No. 2 oil) capability. An above ground 200,000 gallon oil storage tank is also included.

Case 7 represents systems identical to Case 6, but with fixed maintenance at the upper limit of assumed value (one third of costs for relocated VAAP units) and with fixed overhead at the upper limit of assumed value (\$50,000).

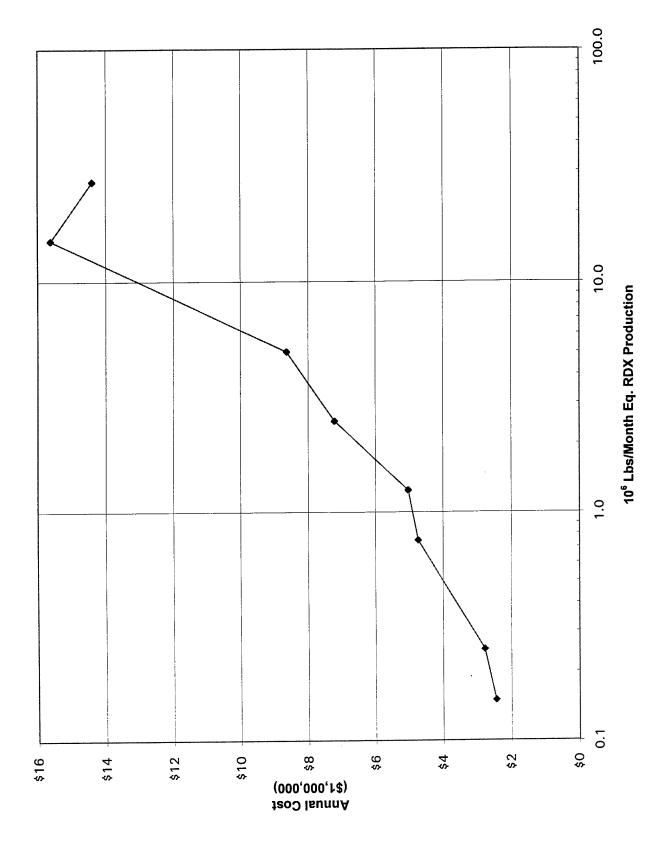
Case 8 is a further extension of the above, with fixed costs incrementally increased until the resultant SIR was below the ECIP qualifying value of 1.25.

Table 6 shows results of Both Case 6 and Case 7.

LCCID analysis summaries for Cases 6, 7 and 8 follow on pages 37, 38, and 39.

Total annual operating cost data shows that Case No. 4: VAAP natural gas boilers, with river water and boiler feedwater pumps turbine driven, and Case Nos 6 and 7: New 100 psig boiler offer annual cost savings over the baseline, and only then at explosive production rates below approximately 2.4 million pounds per year (±200,000 lbs/mo equivalent RDX).

CASE NO. 4: VAAP N. G. BLRS. W/ RIV. WTR. & BLR. FD. PMPS TURBINE DRIVEN							
CAO	L 110. 4.	VAAI 14. G.	DEIG. VVI ICIV. V	VIIV. & BEIV. I B.	THE CHARLE	L DITTUEN	
MILL	#/MO.	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQU	IV. RDX	BTU	BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
	0.15		1204.00	118.57	37256.62	37256.62	78.00
	0.25	3.95	1204.00	91.63	37762.39	37762.39	78.50
	0.75		1204.00	70.07	40690.37	71988.45	81.00
	1.25	3.95	1204.00	45.28	41089.63	77526.03	81.80
	2.50	3.95	1204.00	35.57	53067.40	121826.61	82.50
	5.00	3.95	1204.00	22.10	57326.16	151360.34	
	15.00	3.95	1204.00	14.01	133284.41	287953.81	82.00
	27.00	1.86	1290.20	11.50	122668.77	425342.47	82.00
MILL	#/MO.	FUEL MILL.	ANNUAL	ANNUAL	ANNUAL;	ANNUAL	TOTAL
EQU	IV. RDX	BTU/MO	FUEL COST	ELECT. COST	MNTNC. COST	OVRHD. COST	ANNUAL COST
	0.15	25,173	\$1,193,210.90	\$56,719.09	\$273,955.19	\$921,591.99	\$2,445,477.18
	0.25	32,215	\$1,526,978.38	\$56,866.41	\$274,619.78	\$922,699.63	\$2,781,164.21
	0.75	71,626	\$3,395,065.05	\$66,835.44	\$319,592.83	\$997,654.71	\$4,734,174.98
	1.25	76,381	\$3,620,466.21	\$68,448.37	\$326,869.20	\$1,009,782.00	\$5,025,565.77
	2.50	119,009	\$5,641,031.16	\$81,351.80	\$385,080.17	\$1,106,800.28	\$7,214,263.41
	5.00			\$89,954.09	\$423,887.48	\$1,171,479.14	\$8,634,908.37
	15.00	283,009	\$13,414,647.26	\$129,739.67	\$603,371.31	\$1,470,618.85	\$15,618,377.09
	27.00	450,679	\$10,059,163.99	\$2,418,811.92	\$2,313,000.00	\$1,771,500.00	\$16,562,475.91



LIFE CYCLE COST ANALYSIS SUMMARY STUDY: 95046
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080

INSTALLATION & LOCATION: HOLSTON AAP REGION NOS. 4 CENSUS: 3

PROJECT NO. & TITLE: 95046-00 LIMITED ENERGY STUDY

FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE 4:VAAP N.G.BLRS./ TURB. PMPS ANALYSIS DATE: 10-27-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE

- 1. INVESTMENT
- A. CONSTRUCTION COST \$ 350000.
- B. SIOH \$ 27500.
- C. DESIGN COST \$ 30000.
- D. TOTAL COST (1A+1B+1C) \$ 407500.
- E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.
- F. PUBLIC UTILITY COMPANY REBATE \$
- G. TOTAL INVESTMENT (1D 1E 1F) \$ 407500.
- 2. ENERGY SAVINGS (+) / COST (-)

DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993

	UNIT COST	SAVINGS	ANNUAL \$	DISCOUNT	DISCOUNTED
FUEL	\$/MBTU(1)	MBTU/YR(2)	SAVINGS(3)	FACTOR(4)	SAVINGS(5)
A. ELECT	\$ 10.25	-2182.	\$ -22366.	12.43	\$ -278003.
B. DIST	\$.00	0.	\$ 0.	13.56	\$ 0.
C. RESID	\$.00	0.	\$ 0.	15.09	\$ 0.
D. NAT G	\$ 3.95	*****	\$-1193200.	15.86	\$-18924160.
E. COAL	\$ 1.86	556056.	\$ 1034264.	13.61	\$ 14076340.
F. LPG	\$.00	0.	\$ 0.	12.64	\$ 0.
M. DEMAN	D SAVINGS		\$ 0.	11.85	\$ 0.
N TOTAL		251798	S -181302		\$ -5125825.

0.

- 3. NON ENERGY SAVINGS(+) / COST(-)
 - A. ANNUAL RECURRING (+/-) \$ 357255.
 - (1) DISCOUNT FACTOR (TABLE A) 11.85
 - (2) DISCOUNTED SAVING/COST (3A X 3A1) \$ 4233472.
 - B. NON RECURRING SAVINGS(+) / COSTS(-)

	ITEM	SAVINGS(+)		DISCNT FACTR	DISCOUNTED SAVINGS(+)/
	11EM	(1)	(2)	(3)	COST(-)(4)
1.	BLR. LAYUP	\$-225000.	0	1.00	-225000.
a	ΤΟΤΑΙ	\$-225000			-225000

- C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 4008472.
- 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 160953.
- 5. SIMPLE PAYBACK PERIOD (1G/4)

2.53 YEARS

6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)

\$ -1117353.

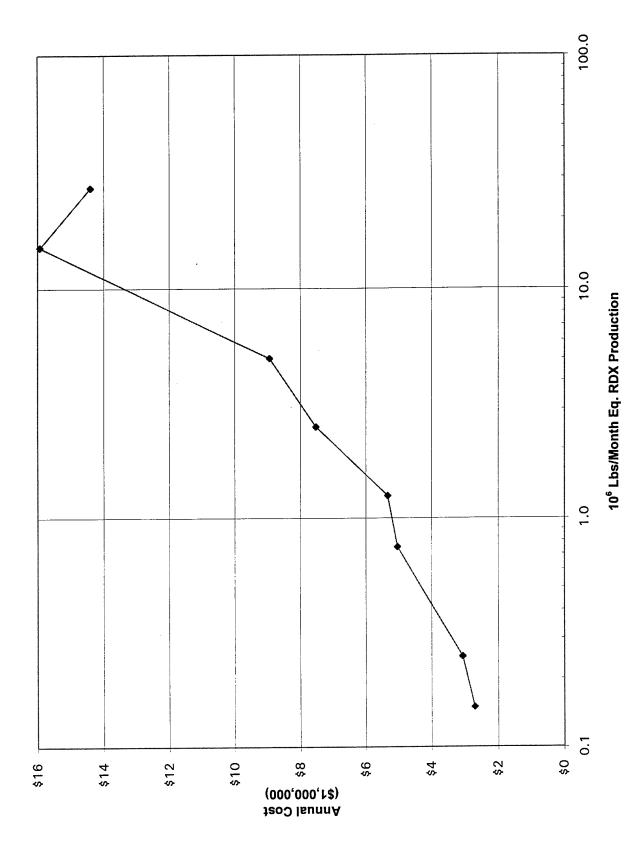
7. SAVINGS TO INVESTMENT RATIO (SIR)=(6 / 1G)= -2.

(IF < 1 PROJECT DOES NOT QUALIFY)

**** Project does not qualify for ECIP funding; 4,5,6 for information only.

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

CACE NO. E.	VAADNC I	DUDG W// DUMP	S EL ECTRIC DE	IV/ENI		
CASE NO. 5:	VAAP N.G.	BLRS. W/ PUMP	S ELECTRIC DR	IVEN		
MILL. #/MO.	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQUIV. RDX	BTU	BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
0.15		1204.00	118.57	0.00	24363.60	78.00
0.25	3.95	1204.00	91.63	0.00	31378.51	78.50
0.75	3.95	1204.00	70.07	0.00	71988.45	
1.25	3.95	1204.00	45.28	0.00	77526.03	
2.50	3.95	1204.00	35.57			82.50
5.00	3.95	1204.00	22.10	0.00	151360.34	
15.00	3.95	1204.00	14.01	0.00		
27.00	1.86	1290.20	11.50	122668.77	425342.47	82.00
-						
MILL. #/MO.	FUEL MILL.	ANNUAL	ANNUAL	ANNUAL;	ANNUAL	TOTAL
EQUIV. RDX	BTU/MO	FUEL COST	ELECT. COST	MNTNC. COST	OVRHD. COST	ANNUAL COST
0.15	25,173	\$1,193,210.90	\$362,568.43	\$257,013.78	\$893,356.29	\$2,706,149.40
0.25			\$364,611.66	\$266,231.36	\$908,718.93	\$3,066,540.33
0.75	71,626	\$3,395,065.05	\$376,440.12	\$319,592.83	\$997,654.71	\$5,035,391.23
1.25	76,381		\$378,053.05	\$326,869.20	\$1,009,782.00	\$5,335,170.45
2.50	119,009	\$5,641,031.16	\$390,956.48	\$385,080.17	\$1,106,800.28	\$7,523,868.09
5.00	146,616	\$6,949,587.66	\$399,558.77	\$423,887.48	\$1,171,479.14	\$8,944,513.05
15.00	283,009	\$13,414,647.26	\$439,344.35	\$603,371.31	\$1,470,618.85	\$15,927,981.77
27.00	450,679	\$10,059,163.99	\$2,418,811.92	\$2,313,000.00	\$1,771,500.00	\$16,562,475.91



LIFE CYCLE COST ANALYSIS SUMMARY

STUDY: 95046

LCCID 1.080 ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP)

REGION NOS. 4 CENSUS: 3 INSTALLATION & LOCATION: HOLSTON AAP

LIMITED ENERGY STUDY PROJECT NO. & TITLE: 95046-00

FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE 5: VAAP N. G. BLRS/ ELECT PMPS.

ANALYSIS DATE: 10-27-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE

- 1. INVESTMENT
- A. CONSTRUCTION COST 350000.
- \$ 27500. B. SIOH
- 30000. \$ C. DESIGN COST
- D. TOTAL COST (1A+1B+1C) \$ 407500.
- E. SALVAGE VALUE OF EXISTING EQUIPMENT \$
- F. PUBLIC UTILITY COMPANY REBATE
- 407500. G. TOTAL INVESTMENT (1D - 1E - 1F)
- 2. ENERGY SAVINGS (+) / COST (-)

DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993

	UNIT COST	SAVINGS	ANNUAL \$	DISCOUNT	DISCOUNTED
FUEL	\$/MBTU(1)	MBTU/YR(2)	SAVINGS(3)	FACTOR(4)	SAVINGS(5)
A. ELECT	\$ 10.25	-32007.	\$ -328072.	12.43	\$ -4077932.
B. DIST	\$.00	0.	\$ 0.	13.56	\$ 0.
C. RESID	\$.00	0.	\$ 0.	15.09	\$ 0.
D. NAT G	•	*****	\$-1193200.	15.86	\$-18924160.
E. COAL	\$ 1.86	556056.	\$ 1034264.	13.61	\$ 14076340.
F. LPG	\$.00	0.	\$ 0.	12.64	\$ 0.
M. DEMANI	SAVINGS		\$ 0.	11.85	\$ 0.
N. TOTAL		221973.	\$ -487008.		\$ -8925753.
			•		

- NON ENERGY SAVINGS(+) / COST(-)
 - A. ANNUAL RECURRING (+/-)

402431.

(1) DISCOUNT FACTOR (TABLE A)

- 11.85
- (2) DISCOUNTED SAVING/COST (3A X 3A1)

4768808.

B. NON RECURRING SAVINGS(+) / COSTS(-)

	2.02. 2.200		,		
		SAVINGS(+)	YR	DISCNT	DISCOUNTED
	ITEM	COST(-)	OC	FACTR	SAVINGS(+)/
		(1)	(2)	(3)	COST(-)(4)
1.	BLR. LAYUP	\$-225000.	0	1.00	-225000.
d.	TOTAL	\$-225000.			-225000.

- C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 4543808.
- 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ -99577.
- SIMPLE PAYBACK PERIOD (1G/4)

-4.09 YEARS

6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)

\$ -4381946.

7. SAVINGS TO INVESTMENT RATIO

(SIR)=(6 / 1G)=-10.75

(IF < 1 PROJECT DOES NOT QUALIFY)

**** Project does not qualify for ECIP funding; 4,5,6 for information only.

ADJUSTED INTERNAL RATE OF RETURN (AIRR):

CASE NO 6	NEW 30.0	00#/HR, 100PSIG	N.G.FIRED BO	DILER @ MIN. FI	XED MNTNC &	OVRHD
0710L 110. U.	11211 00,0		, , , , , , , , , , , , , , , , , , , ,			
MILL. #/MO.	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQUIV. RDX	BTU	BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
0.15	3.95	1187.20	120.41	0.00	24741.86	
0.25	3.95	1187.20	93.04	0.00	31864.52	84.50
MILL. #/MO.	FUEL MIL	ANNUAL	ANNUAL	ANNUAL;	ANNUAL	TOTAL .
EQUIV. RDX	BTU/MO	FUEL COST	ELECT. COST	MNTNC. COST	OVRHD. CST	ANNUAL COST
0.15	23,238	\$1,101,504.66	\$334,011.50	\$77,510.81	\$474,184.68	\$1,987,211.65
0.25	29,928	\$1,418,604.49	\$336,086.12	\$86,869.98	\$489,783.30	\$2,331,343.89
·-						
CASE NO.7:	NEW 30,00	⊔ 0#/HR, 100PSIG,	N.G.FIRED BO	ILER @ MAX. FI	XED MNTNC &	OVRHD
MILL. #/MO.	\$/MILL.	STEAM	# STEAM	STEAM TURB-	STEAM	BOILER
EQUIV. RDX	BTU	BTU/#	PER #RDX	INE #/HR	AVG.#/HR	EFFIC.
0.15	3.95	1187.20	120.41	0.00	24741.86	84.50
0.25	3.95	1187.20	93.04	0.00	31864.52	84.50
MILL. #/MO.	FUEL MIL	ANNUAL	ANNUAL	ANNUAL:	ANNUAL	TOTAL
EQUIV. RDX		FUEL COST		MNTNC. COST		ANNUAL COST
0.15			\$334,011.50		\$654,184.68	\$2,197,211.65
0.25			\$336,086.12	\$116,869.98	\$669,783.30	\$2,541,343.89

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: 95046
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080

INSTALLATION & LOCATION: HOLSTON AAP REGION NOS. 4 CENSUS: 3

PROJECT NO. & TITLE: 95046-00 LIMITED ENERGY STUDY

FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE 6: NEW 30K #/HR 100PSI BLR ANALYSIS DATE: 10-27-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE

- 1. INVESTMENT
- A. CONSTRUCTION COST \$ 362500.
- B. SIOH \$ 27500.
- C. DESIGN COST \$ 30000.
- D. TOTAL COST (1A+1B+1C) \$ 420000.
- E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0
- F. PUBLIC UTILITY COMPANY REBATE \$ 0.
- G. TOTAL INVESTMENT (1D 1E 1F) \$ 420000.
- 2. ENERGY SAVINGS (+) / COST (-)

DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993

UNIT COST	SAVINGS	ANNUAL \$	DISCOUNT	DISCOUNTED
FUEL \$/MBTU(1)	MBTU/YR(2)	SAVINGS(3)	FACTOR(4)	SAVINGS(5)
A. ELECT \$ 10.25	-29236.	\$ -299669.	12.43	\$ -3724886.
B. DIST \$.00	0.	\$ 0.	13.56	\$ 0.
C. RESID \$.00	0.	\$ 0.	15.09	\$ 0.
D. NAT G \$ 3.95	*****	\$-1101481.	15.86	\$-17469490.
E. COAL \$ 1.86	556056.	\$ 1034264.	13.61	\$ 14076340.
F. LPG \$.00	0.	\$ 0.	12.64	\$ 0.
M. DEMAND SAVINGS		\$ 0.	11.85	\$ 0.
N. TOTAL	247964.	\$ -366886.		s -7118043.

- 3. NON ENERGY SAVINGS(+) / COST(-)
 - A. ANNUAL RECURRING (+/-)

\$ 1001105. 11.85

- (1) DISCOUNT FACTOR (TABLE A)
- (2) DISCOUNTED SAVING/COST (3A X 3A1)

\$ 11863100.

B. NON RECURRING SAVINGS(+) / COSTS(-)

		SAVINGS(+)	YR	DISCNT	DISCOUNTED
	ITEM	COST(-)	OC	FACTR	SAVINGS(+)/
		(1)	(2)	(3)	COST(-)(4)
1.	PLNT LAYUP	\$ -2 50000.	0	1.00	-250000.
а	ΤΩΤΑΙ.	\$-250000			-250000

- C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 11613100.
- 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 617552.
- 5. SIMPLE PAYBACK PERIOD (1G/4)

.68 YEARS

6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)

\$ 4495052.

7. SAVINGS TO INVESTMENT RATIO (SIR

(SIR)=(6 / 1G)= 10.70

(IF < 1 PROJECT DOES NOT QUALIFY)

**** Project does not qualify for ECIP funding; 4,5,6 for information only.

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY

STUDY: 95046 LCCID 1.080

ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LC

INSTALLATION & LOCATION: HOLSTON AAP REGION NOS. 4 CENSUS: 3 PROJECT NO. & TITLE: 95046-00 LIMITED ENERGY STUDY

FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE NO. 7: NEW 30K #/HR 100PSI BLR ANALYSIS DATE: 10-27-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE

- 1. INVESTMENT
- A. CONSTRUCTION COST \$ 362500.
- B. SIOH \$ 27500.
- C. DESIGN COST \$ 30000.
- D. TOTAL COST (1A+1B+1C) \$ 420000.
- E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.
- F. PUBLIC UTILITY COMPANY REBATE \$ 0.
- G. TOTAL INVESTMENT (1D 1E 1F) \$ 420000.
- 2. ENERGY SAVINGS (+) / COST (-)

DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993

UNIT COS'	T SAVINGS	ANNUAL \$	DISCOUNT	DISCOUNTED
FUEL \$/MBTU(1) MBTU/YR(2)	SAVINGS(3)	FACTOR(4)	SAVINGS(5)
A. ELECT \$ 10.25	-29236.	\$ -299669.	12.43	\$ -3724886.
B. DIST \$.00	0.	\$ 0.	13.56	\$ 0.
C. RESID \$.00	0.	\$ 0.	15.09	\$ 0.
D. NAT G \$ 3.95	*****	\$-1101481.	15.86	\$-17469490.
E. COAL \$ 1.86	556056.	\$ 1034264.	13.61	\$ 14076340.
F. LPG \$.00	0.	\$ 0.	12.64	\$ 0.
M. DEMAND SAVINGS		\$ 0.	11.85	\$ 0.
N. TOTAL	247964.	\$ -366886.		\$ -7118043.

- NON ENERGY SAVINGS(+) / COST(-)
 - A. ANNUAL RECURRING (+/-)

(1) DISCOUNT FACTOR (TABLE A)

- 11.85
- (2) DISCOUNTED SAVING/COST (3A X 3A1)

\$ 9374606.

791106.

B. NON RECURRING SAVINGS(+) / COSTS(-)

		SAVINGS(+)	YR	DISCNT	DISCOUNTED
	ITEM	COST(-)	OC	FACTR	SAVINGS(+)/
		(1)	(2)	(3)	COST(-)(4)
1.	PLNT. LAYUP	\$-250000.	0	1.00	-250000.
а	ТОТАТ	\$-250000			-250000

- a. 101AL \$-230000.
- C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 9124606.
- 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 407553.
- 5. SIMPLE PAYBACK PERIOD (1G/4)

1.03 YEARS

6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)

\$ 2006563.

7. SAVINGS TO INVESTMENT RATIO

(SIR)=(6 / 1G)= 4.78

(IF < 1 PROJECT DOES NOT QUALIFY)

**** Project does not qualify for ECIP funding; 4,5,6 for information only.

8. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

LIFE CYCLE COST ANALYSIS SUMMARY STUDY: 95046
ENERGY CONSERVATION INVESTMENT PROGRAM (ECIP) LCCID 1.080

INSTALLATION & LOCATION: HOLSTON AAP REGION NOS. 4 CENSUS: 3

PROJECT NO. & TITLE: 95046-00 LIMITED ENERGY STUDY

FISCAL YEAR 1996 DISCRETE PORTION NAME: CASE 8:NEW 30K #/HR 100PSI BLR ANALYSIS DATE: 10-27-95 ECONOMIC LIFE 15 YEARS PREPARED BY: P. D. LITTLE

- 1. INVESTMENT
- A. CONSTRUCTION COST \$ 362500.
- B. SIOH \$ 27500.
- C. DESIGN COST \$ 30000.
- D. TOTAL COST (1A+1B+1C) \$ 420000.
- E. SALVAGE VALUE OF EXISTING EQUIPMENT \$ 0.
- F. PUBLIC UTILITY COMPANY REBATE \$
- G. TOTAL INVESTMENT (1D 1E 1F) \$ 420000.
- 2. ENERGY SAVINGS (+) / COST (-)

DATE OF NISTIR 85-3273-X USED FOR DISCOUNT FACTORS OCT 1993

	UNIT COST	SAVINGS	ANNUAL \$	DISCOUNT	DISCOUNTED
FUEL	\$/MBTU(1)	MBTU/YR(2)	SAVINGS(3)	FACTOR(4)	SAVINGS(5)
A. ELECT	\$ 10.25	-29236.	\$ -299669.	12.43	\$ -3724886.
B. DIST	\$.00	0.	\$ 0.	13.56	\$ 0.
C. RESID	\$.00	0.	\$ 0.	15.09	\$ 0.
D. NAT G	\$ 3.95	*****	\$-1101481.	15.86	\$-17469490.
E. COAL	\$ 1.86	556056.	\$ 1034264.	13.61	\$ 14076340.
F. LPG	\$.00	0.	\$ 0.	12.64	\$ 0.
M. DEMAN	D SAVINGS		\$ 0.	11.85	\$ 0.
N. TOTAL		247964.	\$ -366886.		\$ -7118043.

0.

- NON ENERGY SAVINGS(+) / COST(-)
 - A. ANNUAL RECURRING (+/-)
 - (1) DISCOUNT FACTOR (TABLE A) 11.85
 - (2) DISCOUNTED SAVING/COST (3A X 3A1)

\$ 7880251.

665000.

B. NON RECURRING SAVINGS(+) / COSTS(-)

		SAVINGS(+)	YR	DISCNT	DISCOUNTED
	ITEM	COST(-)	OC	FACTR	SAVINGS(+)/
		(1)	(2)	(3)	COST(-)(4)
1.	PLNT. LAYUP	\$-250000.	0	1.00	-250000.
d.	TOTAL	\$-250000.			-250000.

- C. TOTAL NON ENERGY DISCOUNTED SAVINGS(+)/COST(-)(3A2+3Bd4)\$ 7630251.
- 4. FIRST YEAR DOLLAR SAVINGS 2N3+3A+(3Bd1/(YRS ECONOMIC LIFE))\$ 281447.
- 5. SIMPLE PAYBACK PERIOD (1G/4)

1.49 YEARS

6. TOTAL NET DISCOUNTED SAVINGS (2N5+3C)

\$ 512208.

7. SAVINGS TO INVESTMENT RATIO (SIR)=(6 / 1G)=
(IF < 1 PROJECT DOES NOT QUALIFY)

1.22

**** Project does not qualify for ECIP funding; 4,5,6 for information only.

. ADJUSTED INTERNAL RATE OF RETURN (AIRR):

At equivalent RDX production of 1.8 million pounds per year, total annual cost savings are as follows:

Case 4 - \$176,000

Case 6 - \$634,200

Case 7 - \$424,200

Corresponding energy savings are:

Case 4 - 254 x 109 Btu/yr

Case 6 - 277 x 109 Btu/yr

Case 7 - 277 x 109 Btu/yr

In each of these cases, cost of natural gas burned is greater than the corresponding coal costs, but these increased costs are offset by reduced maintenance and overhead, producing the positive total cost savings.

For the new 30,000 lbs/hr steam boiler, submittal of an Operating Permit Application to the Tennessee Division of Air Pollution Control will be required. In addition, initial compliance tests for particulate emissions and nitrogen oxide emissions will be required. The nitrogen oxide initial compliance test requires monitoring stack gases for 30 successive steam generating unit operating days.

Energy Rate Data

Coal costs were developed from HDC cost center 2230 breakdown dated 11 May 1995 representing April 1995 data, and from steam unit cost calculations for 1994 out-of-pocket expenses prepared by J. Bouchillon and dated 03/29/95. Value used in the LCCID program is \$1.86 per million Btu.

Electrical unit costs were calculated from Kingsport Power Company bill for March 1995. No attempt was made to differentiate between energy cost and demand cost for the scenario analyses. Value used in the LCCID program is \$10.25 per million Btu (electrical).

Natural gas unit costs were calculated in a similar manner to electrical costs from United Cities Gas Company bill for April 1995. Value used in the LCCID program is \$3.95 per million Btu.

Copies of the cost breakdowns, utility bills, and J. Bouchillon calculations are included in Appendix 1.

Conclusion

Energy (Btu) savings and maintenance cost savings resulting from using natural gas to replace coal in Building 8-A at Holston Army Ammunition Plant are not great enough to offset increased energy costs and justify construction costs. Installation of a new 100 psig firetube boiler at a location closer to the major process steam usage point, permitting complete shutdown of Building 8A, is recommended.

Conversion of existing refrigeration equipment from steam driven to electric driven will have no impact on steam system operation. The turbines being removed function as "pressure reducers", each of which are in parallel with river water pump turbines and with a PRV station and desuper-heating station. The parallel equipment to remain has the capability to meet all expected future conditions.

Existing boiler feedwater/condensate return systems at Holston are suitable for operation in conjunction with relocated boilers from VAAP. In reality, there will be insignificant variations from pressures and flows experienced at present when system load is roughly 40,000 #/hr steam demand. Therefore, transporting the ancillary equipment from VAAP and refurbishing that equipment is not justified.

To carry this theme one more step, the cost of adding fuel oil storage as standby for relocated VAAP boilers has not been included since case studies indicate no economical advantage can be realized even without added storage costs. Also, the coal storage at Area "B" can be considered a standby fuel, although its use in "layed away" boilers would dictate an extended time period for transfer to that fuel.

Definitions/Abbreviations

AESE: Affiliated Engineers SE, Inc.

ASME: American Society of Mechanical Engineers

bhp: Boiler Horsepower

ECO: Energy Conservation Opportunity

<u>Energy Conservation Investment Program (ECIP)</u>: This is a federal government program which allocates funds for projects which increase energy efficiency.

HDC: Holston Defense Corporation

HSAAP: Holston Army Ammunition Plant

ID/FD Fan: Induced Draft and/or Forced Draft fans used for steam boilers.

Excess Air: A term used to describe the amount of air that is supplied to fossil fired boilers over and above the amount theoretically required for complete combustion.

lb/hr: pounds per hour

lb/mo: pounds per month

<u>Life Cycle Cost in Design (LCCID)</u>: Government software package used to evaluate projects for ECIP funding.

MMBtu: million British thermal units

psig: pounds per square inch gauge

RDX: Research Development Explosive

SIR: Savings to Investment Ratio

VAAP: Volunteer Army Ammunition Plant, Chattanooga, Tennessee

A BOILER CONDITION AND USEFUL LIFE STUDY

FOR

AFFILIATED ENGINEERS SE, INC

AT

VOLUNTEER ARMY AMMUNITION PLANT
CHATTANOOGA, TENNESSEE

Submitted By:

Hartford Steam Boiler
Inspection & Insurance Company
200 Ashford Center North
Suite 300
Atlanta, GA 30338
August 2, 1995
404 928 0788

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INTRODUCTION

During the time period of July 24 through 28, 1994, The Hartford Steam Boiler Inspection and Insurance Company (HSB) performed a Boiler Condition Study on two Babcock & Wilcox water tube boilers located in building 451 at the facilities of the Volunteer Army Ammunition Plant, Chattanooga Tennessee. The objective of this study was to determine the current condition of the two boilers for possible relocation.

The physical condition, description and evaluation is based upon information obtained through visual inspection, nondestructive examination and hydrostatic testing. Subsequent portions of this report contain a description of the boilers, an evaluation of their existing condition, and the inspection techniques utilized.

Also included is a description of the two deaerating tanks and the current condition of the vessels.

Preceding the survey text is a summary of our inspection findings and corresponding suggestions for correction of observed discrepancies.

This study was directed by J.A. Dognazzi, Regional Supervisor Engineering Services assigned to the Atlanta Regional Office of HSB. Should any portion of this report require clarification or elaboration, please feel free to contact Mr. Dognazzi at 404 928 0788.

SUMMARY

As the following text elaborates, the overall physical integrity of these Babcock & Wilcox boilers appears satisfactory (with the exception of several generating tubes) for continued service at a pressure not to exceed the maximum allowable working pressure as stamped on the Manufacturer's Name Plate. A boiler's physical integrity is for the most part dependent on the material's strength and/or remaining material thickness of the drums and tubes. This detailed physical condition evaluation failed to disclose any significant abnormalities in the strength of material, depletion of material thicknesses, or discontinuities in major weldments that could significantly have an adverse effect on the pressure containing properties of any of the boiler's pressure containing components.

Although the integrity of the pressure containing components is acceptable at this time, several observations were made that should receive corrective action or modification prior to putting these boilers into service. Those observations pertain to the boilers pressure containing components. Summary comments pertaining to those observations are contained in the section immediately following, titled Conclusions/Recommendations, with detailed explanations contained throughout remaining portions of this report.

CONCLUSIONS/RECOMMENDATIONS

Those conditions observed requiring attention prior to placing these boilers in service are as follows:

 The condition of the four safety valves (2 from each boiler) is questionable due to external condition, broken locking seals, leakage through the seat and disk during hydrostatic test, unable to lift valve seat with lifting lever.

Recommendation: The valves should be sent to a reliable safety valve repair facility in possession of a valid VR Certificate of Authorization for repair, adjustment and sealing.

2. The tubes in the L & M rows of the west boiler, at the rear of the furnace (approximately the last 18 tubes in each row - total 36) have small blisters. The blisters are very small and almost discernable. The exact cause of the blistering is not known at this time.

Recommendation: Prior to putting the west boiler into operation, these tubes should be replaced.

Additionally, the remaining tubes in these rows are behind the waterwall tubes, it is virtually impossible to determine if any of these tube are also blistered.

Recommendation:

Perform a metallurgical analysis on a blistered tube to identify the cause of the blistering. Procedures can be provided for the removal of the tube, shipping and laboratory services upon request.

3. The casing should be removed from both boilers and both economizers to ensure no corrosion has effected the inner components and to properly inspect the insulation.

Recommendation: The casing on both boilers and economizers should be cleaned of all corrosion/rust and preserved with an approved weather resistant paint designed for high temperature surfaces.

4. The east boiler's economizer has indications of previous leakage as noted in the base of the chimney.

Recommendation: The economizer should be hydrostatically tested to a pressure not to exceed the maximum allowable working pressure as stamped on the vessel.

5. Waterwall tubes of the west boiler - Flame impingement of both walls in the furnace.

Recommendation:
The burner flame pattern should be investigated to determine the cause of the impingement. Consideration should be given to performing a burner alignment and a flame pattern analysis to determine cause.

Failure to correct this problem could cause tube failure due to mild prolonged overheating.

6. Scale deposits within the tubes and drums.

Recommendation:

The boilers should be cleaned of the scale deposits using any method that will not remove any thickness from the tubes or drums. A recommended method would be high pressure water washing of the tubes and drums.

BOILER DESCRIPTION

These Babcock and Wilcox boilers (2) are bent tube, watertube boilers, manufactured originally for Atlas Chemical Industries, Inc at the Volunteer Army Ammunition Plant (VAAP), Chattanooga, Tennessee. Construction was in accordance with the ASME Code, Section 1, Power Boilers, 1968 Edition with addenda to 12/70. This fact is documented on the Manufacturer's Data Report, a copy of which is contained in Appendix B.

These boilers consist of one steam drum, one mud drum and one bank of generating tubes. Appendix D contains a representative layout of all the tubes in the boilers from the steam drum.

The west boiler is considered a left hand boiler (as the furnace is on the left) and the east boiler is a right hand.

The ASME Code stamping is located on the steam drum's head and normally would be included in this report, as the possibility that asbestos insulation may be installed, the insulation was not disturbed to view the stamping on the drums, therefore, the Manufacturer's Name Plate data is presented as being representative of the ASME construction of the boilers:

West Boiler

Manf: Babcock & Wilcox Co.
Contract No: FM-2126
Capacity,lb/hr: 150,000
Design Pressure: 375 psi
Steam Temp, F: 442 F
Blr H.S. Sq.Ft: 8167 Sq.Ft.
Year Built: 1972
Nat'l Bd: 23635

East Boiler

Manf: Babcock & Wilcox Co.
Contract No: FM-2126
Capacity,lb/hr: 150,000
Design Pressure: 375 psi
Steam Temp, F: 442 F
Blr H.S. Sq.Ft.: 8167 Sq.Ft.
Year Built: 1972
Nat'l Bd: 23636

The ASME "S" stamp is also indicated on both name plate.

The following pertinent information reflects the construction details, documented on the Manufacturer's Data Report, for the major components of these boilers upon which their overall physical integrity is predominately dependent; namely the steam drum, mud drum and tubes.

Steam Drum

48" Nominal diameter: 32' 1.5625" Overall length: Design thickness: 1.53125" (1 17/32") tubesheet: .90625" (29/32") shell plate: SA-515-70 Material: 2-fusion welded/90% efficiency Longitudinal joint: 2-fusion welded/90% efficiency Circumferential Joints: Tube hole efficiencies: 35.68% Longitudinal: 31.63% Circumferential: 39.24% Diagonal: Dished, 1.1875" (1 3/16"), SA-515-70 Heads:

Mud Drum

24" Nominal Diameter: 30' 6.1250" Overall Length: .8750" (29/32") Design thickness: SA-515-70 Material: Longitudinal Joint: 90% 4-fusion welded/90% efficiency Circumferential Joint: Tube hole efficiencies: 42.73% Longitudinal: 19.98% Circumferential: Dished, .75" (.750"), SA-515-70 Heads:

Tubes

Generating:

2" x .095", SA-178-A
2" x .134", SA-178-A
2" x .095", SA-178-A
2.75" x .165" SA-178-A
2" x .165", SA-178-A

We understand all pressure containing components are original and that no weld repairs have been made to any pressure retaining component in either boiler, or any tube/s had been replaced or plugged. As reported, operating pressures and temperatures were limited to a operation of 290 psi with no high pressure or high temperature; excessive high water or low water excursions being reported. Additionally, as reported, there had not been any periods of over firing of the boilers.

We further understand these boilers were operated primarily on natural gas constituting 90 % usage with an occasional period on #2 oil.

INSPECTION DETAILS

The inspection of these B & W boilers consisted of a thorough internal and external visual inspection supplemented by ultrasonic thickness measurements of various waterwall tubes. Additional inspection techniques included dry powder magnetic particle examination of the weld joints in all drums and Remote Field Eddy Current (RFEC) examination of twenty five percent of the generating tubes of each boiler.

All the tubes examined are identified within the boxes on the Boiler Tube Layout sheets. These areas were selected due to being the most likely for tube problems to develop either from over heating or external general corrosion from low temperatures. The center section was examined to get a general indication of the tubes. There were no tube thickness loss which would be cause for concern at this time.

While basic comments relative to all inspection techniques will be contained within this section of the report, specific details pertaining to the ultrasonic thickness testing and the RFEC examination of the generating tubes are presented in Appendix C.

During the process of conducting our survey, the following observations were noted reflecting the existing condition of these boilers. Each boilers components will be addressed separately.

The installed internals for both steam drums consist of a row of baffle plates which extend the full length of the drum and cover the last couple of row of tubes. The baffles plates are properly installed, not bowed or otherwise damaged. The piping within the drum consists of a surface blow line, feed line and dry pipe. The piping is properly installed. There is no separators installed in these steam drums. Additionally, there are no internal components installed in the mud drums.

Numerous ultrasonic thickness measurements were taken on the shell, tubesheet and heads of the steam and mud drums from each boiler to identify any possibility of thinning due to corrosion. All the thickness measurements taken were above the nominal thicknesses indicated on the Manufacturer's Data Report.

There were three containers of a desiccant material located on each end of all 4 drums. The containers were removed and were noted to have been last changed anywhere from 1987 to 1990. The desiccant material appeared to be slightly saturated with moisture in that the pellets were a pink to white color as opposed to being blue.

The safety valves on both boilers were painted, including the spring. The safety valves were very difficult to open with the lifting levers. Rust buildup was noted on the spindle where it passes through the tension adjusting nut.

The safety valve name plates revealed the following:

North valve - Manufactured by: Consolidated

Type: 1811 NA-20

Size: 4" x 4"

Set pressure: 355 psi

Capacity: 74,525 lbs/hr

South valve - Manufactured By: Consolidated

Type: 1811 PA-20

Size: 4" x 4" Set pressure: 360 psi

Capacity: 111,039 lbs/hr

All 4 safety valves have broken locking seals, this condition renders the safety valves unreliable for future operation.

West Boiler Steam Drum

The visual inspection of the internal components of the steam drum failed to identify any conditions that would be considered serious. Some small scale deposits were noted throughout the top portion of the tubes and around the tube ends. The deposits were flaking off the tube metal and accumulating in the mud drum. As the RFEC probe was inserted into the tubes, additional deposits were scrapped of and settling in the steam drum. The amount of deposits indicate the tubes are in need of a good cleaning, most preferable is the high pressure water jet method.

The surface of the shell and all components within the drum was noted to have a light coating of surface rust. There was no significant corrosion noted any where within the drum.

The tube ends were not eroded or corroded nor were any split tube ends noted. Minor pitting was noted through out the drum and on some of the tube ends. The pitting is not considered serious.

To perform the RFEC examination of the tubes, they were identified from the front of the boiler (burner end) by numbering from 1 through 97 and lettered circumferentially from top to bottom, A to M. Therefore, the A-1 tube is located in the top right corner of the steam drum when facing the flue gas outlet of the boiler with the burner on the right.

The tubes within the dotted lines on the Boiler Tube Layout sheets were noted to have small blisters on many of the tubes. The blisters were first noted during the RFEC examination of those tubes with an indication of a change in permeability of the tube metal. Further investigation within the furnace revealed the blistering.

West Boiler Mud Drum

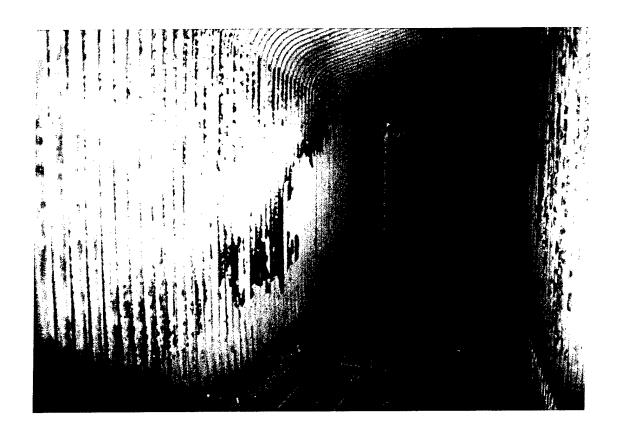
The internal visual inspection noted a significant quantity of loose deposits laying in the drum. The deposits appear to be from the tubes which has flaked off over the years. The quantity of deposits also appear to contain a sand like material, there was no indication how the sand like material got into the boiler.

The waterside surfaces have a slight scale like deposit adhered to the shell and heads, this is not considered significant and a water blast cleaning would most likely remove the deposits. Where the deposits had flaked off, a slight amount of surface corrosion was noted. This is not considered serious.

West Boiler Fireside

The inspection of the firesides was limited to the furnace area. The refractory within the furnace appears to be in satisfactory condition. There were no "soft spots", loose walls, severely broken brick, extremely spalled castable, or significant holes in the refractory noted.

The waterwall and generating tubes were noted to have a coating of fireside deposits which could be removed by brushing. The tube surfaces have a limited amount of general surface corrosion. The waterwall tubes on both sides were noted to have a "carbon pattern" impingement from the burner flame. The pattern was more predominate on the left wall. See photograph next page.



The tubes appeared to be straight with no sagging, warping or other physical distortions noted except the tubes in the beginning of the second pass (as indicated in the dotted red border on the Boiler Tube Layout sheet - identified as L & M rows). Many of these tubes have small blisters which are almost invisible to the naked eye. The cause of the blisters could not readily be determined but a primary source of this type of condition is related to overheating, either mild prolonged overheating or, the boiler experienced a momentary water circulation problem during high firing conditions.

See photograph next page.



The tubes in the L & M row, and possibly other rows, located behind the water wall tubes could also have been effected by the same cause. As these tubes can not be closely examined, it is not know if these tubes have been effected.

Ultrasonic thickness measurements were taken on the waterwall tubes within the furnace area. The measurements taken were at or above the thicknesses identified on the Manufacturer's Data Report. The actual thickness measurements are illustrated in Appendix E.

Additional pictures are located in Appendix F.

West Boiler External Surface

The external condition of the west boiler is satisfactory with some general corrosion noted on the casing, primarily on the top but also on the sides at the top and bottom of both sides. The one concern is that moisture has gotten under the casing and some corrosion may have developed on the inner surfaces.

See photograph next page.



The casing of the economizer of this boiler has several areas where corrosion has come through the metal. The corrosion may have been the result of moisture getting behind the casing. There was no inspection activity of the economizer's pressure retaining components.

The base of the chimney, beneath the economizer tubes was entered with no indication of any leakage being noted.

West Boiler General Notes

1. The surface corrosion within the steam and mud drums is believed to be the result of the desiccant material not being rejuvenated periodically.

West Boiler Hydrostatic Test

The boiler was hydrostatically tested in accordance with the requirements of the National Board Inspection Code (NBIC) and ASME Code, Section 1, Power Boilers, applicable paragraphs. The purpose of the hydrostatic test was to determine the tightness of the rolled and welded joints. The test pressure of 480 psi was attained with no leakage of any tube or welded joint.

During the hydrostatic test, there were numerous valves and one safety valve leaking through that could not be isolated. The leaking safety valve was gagged to prevent the valve from lifting under pressure.

East Boiler Steam Drum

The visual inspection of the internal components of the steam drum failed to identify any conditions that would be considered serious. The conditions noted are basically the same as the west drum in that some minor scale deposits were noted throughout the top portion of the tubes and around the tube ends. The deposits are flaking off the tube metal and accumulating in the mud drum. During the RFEC examination, additional deposits was scrapped off and settled in the mud drum. The amount of deposits indicate the tubes are in need of a good cleaning, most preferable is the high pressure water jet method.

The surface of the shell and all components displayed a light coating of surface rust. There was no significant corrosion noted within the drum.

The condition of the tube ends are essentially the same as the tubes in the west boiler.

The tubes were numbered and lettered in the same manner as the west boiler with the exception the A-1 tube is in the upper left corner when facing the flue gas outlet and the burner is on the left.

East Boiler Mud Drum

The internal visual inspection noted a significant quantity of loose deposits laying in the drum. The deposits appear to be from the tubes which has flaked off over the years. The quantity of deposits also appear to contain a sand like material, there was no indication how the sand like material got into the boiler.

The waterside surfaces have a slight scale like deposit adhered to the shell and heads, this is not considered serious and most likely could be removed with high pressure water cleaning.

East Boiler Firesides

The inspection of the firesides was limited to the furnace area. The refractory within the furnace appears to be in satisfactory condition. There were no "soft spots", loose walls, severely broken fire brick, extremly spalled castable, or holes in the refractory.

The waterwall and generating tubes were noted to have a coating of fireside deposits which could be removed by wiping. The tube surfaces have a slight amount of surface rust which is not a concern at this time. There were no warping, sagging or other physical distortions of the tubes.

East Boiler External Surfaces

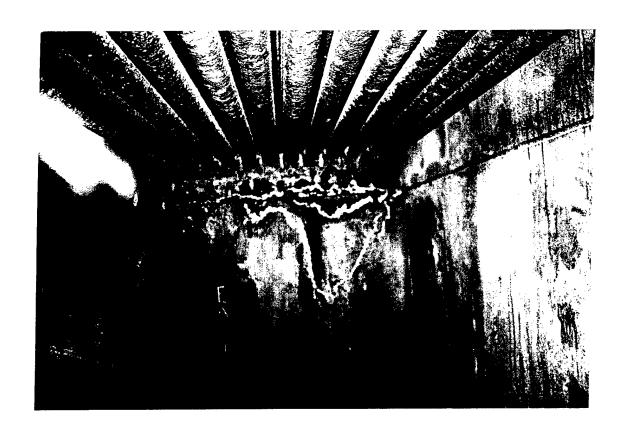
The external condition of the east boiler is satisfactory with some general corrosion noted on the sides and top of the boiler. The concern is moisture may have gotten under the casing and corrosion may have developed on the inner surfaces.

The casing of the economizer has several areas where corrosion has come through the metal. The corrosion may most likely is moisture getting under the casing. There was no inspection activity of the economizer pressure retaining components.



The base of the chimney was entered to investigate the cause of the water stains noted on the rear wall. There was no noted failed tube or welded joint. The possibility of a leaking tube in the tube bank should be considered and corrective action taken.

Photograph view of the lower row of economizer tubes and inner casing. Note white water mark and pattern of corrosion (heavy on the rear wall, light on the side walls). Possibly these indications are the result of leakage within the economizer tube bank.



East Boiler Hydrostatic Test

A hydrostatic test was applied to this boiler in accordance with the requirements of the National Board Inspection Code and ASME Code, Section 1, Power Boilers, applicable paragraphs. The test pressure could only be raised to 280 psi due to numerous valves leaking through that could not be blanked off. Under this pressure, there were no tubes or welded joints leaking.

APPENDIX A

CALCULATIONS

The tubes in the boilers examined with RFEC were 2" \times .095" wall thickness, SA-178-A material with a tensile value of 11,500 psi at 700 degree F. The original MAWP of the tubes was 530 psi.

The following indicates the actual wall thickness for each 10 % of wall loss.

The following equation is given in paragraph P-22 (a) and is used to determine the maximum allowable working pressure (MAWP) of tubes.

$$P = S \times \frac{2t - .01D - 2e}{D - (t - .005D - e)}$$

Where:

P = Maximum Allowable Working Pressure, psi

D = Outside diameter, inches

S = Stress value, psi

t = Minimum required thickness, inches

e = Thickness factor for expanded tubes

For the 2" x .095 tubes, a 10 % wall loss equates to a calculated thickness of .0855". To determine the MAWP of a tube with a 10 % wall loss, the following calculation is performed:

$$P = 11500 \times \frac{2 \times .0855 - .01 \times 2 - 2 \times 0.4}{2 - (.0855 - .005 \times 2 - 0.4)} = 415 \text{ psi}$$

Tubes with a 20 % wall loss = 302 psi

The calculated MAWP of tubes with a maximum of 10 % wall loss does not take into consideration any pitting, overheating or other physical conditions which could further reduce the MAWP.

The tubes from 10 to 20 % wall loss are indicated in RED on the Boiler Tube Layout sheets. The tubes with a 10 % or less wall loss are indicated in white.

APPENDIX B MANUFACTURER'S DATA REPORTS

FORM P-3 MANUFACTURERS' DATA REPORT FOR WATER-TUBE BOILERS, SUPERHEATERS, WATERWALLS, AND ECONOMIZERS

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DILER MADE BY	e Babcock & Wilcox	Company			···
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The	Hartford S. B. I.	& I. Co. of	Hartford, Co	onnecticut	
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FORM P-3 MANUFACTURERS' DATA REPORT FOR WATER-TUBE BOILERS, SUPERHEATERS, WATERWALLS. AND ECONOMIZERS

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201-2126	As Required by th	e Provisions of the	ASME Code Rules	
	The Babcock & W		Barberton, Ohio	
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I the undersigned, hold	ling a valid commission issued	by the National Board of	Boiler and Pressure Vessel Inspectors and/or the S	tate or
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and state that, to the b	est of my knowledge and belief,	the manufacturer has consti	ucted this boiler in accordance with the applicable sect	
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By signing this certifica	te neither the Inspector nor his	mployer makes any warranty	, expressed or implied, concerning the boiler described	in this
manufacturer's data repo	rt.Furthermore, neither the Inspec	ctor nor his employer shall b	e liable in any manner for any personal injury or propert	y dam-
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						_									+	 	 	+	· · · · · · · · · · · · · · · · · · ·
				<u> </u>								!_				8(b) Supe	theater T	ubes	
80	a) Supe	heate	Hea	ders						1		-1			T	T		T	
<u> </u>				 						+		-			 		<u> </u>		
_						-+				+		+			+	1			
-				 						\dashv					1				
				T: 1.1	Cond		ਹ.~	لـــــــــــــــــــــــــــــــــــــ	Pire							9(b) Tube	e for Orl	er Da	rts
9(a) Other	Parts	(1)_	F.W.	Cont	(2)) <u>re</u>	eu .	Pipe	(3)						א(ס) ז מסע			
	17 ()50 ¹¹	OD.	QA 7	06 I	1	135"	Min		Т		$\neg \tau$			T				
2		5" 0.			L06 I				Flg'd.	Ends									
3			<i></i>	1 21123		- '	- ,,,				No	Conr	ection	1s '	To Ite	m 10 Ex	cept A	s Li	sted
		- (1)		1	12"	Flan	ge P	ad				(2) Safety	Valv	e 2	4" Flan, size, and t	ge Pad	S	
10	Opening			(Ne	., size	, and ty	pe of r	nozzle	s or outlets)										
		(2)	Rlow	off 1	-1 1,	/2" F	lang	ge Co	onnection s or outlets)	1		(4) Feed_	<u>] -</u>	<u>-4" Fl</u>	ange Co	nnecti	on S	team
		(3)	∪#\	(N	o., s i z e	, and ty	pe of r	nozzle	es or outlets)					(No	., size, typ	e, anu locai	_		nead
	1			ximum A		Code P	ar, and	/or	Shop hydro too	Heating							12 Field hydro, test		
V.	able Working Pressure					AWP i	s Base	which Shop hydro Based		1_	Surface		<u>'</u>		·		۲		
а	Boiles			375		PG27	.2.2		563		7095		Heating to be		ace ped on		-		
Ь	Water	wall						(,	Assembled	1	1072		drum				-		
c	Econo	mizer							Boiler)		7883				surface sed for		 		
d	Super	neater	\top							1					sea for g minimum	1	⊢		

e Other parts

APPENDIX C

REMOTE FIELD EDDY

CURRENT FIELD DATA





Engineering Services

FIELD DATA REPORT

V	A	ΑP		
٧.	ລ	U.	•	

			4-3 F-			r				AAP,		о TIN	7/25/05
													Date 7/25/95
Fred	quency $\frac{1}{2}$	05 MHz	Cur	rent <u>30</u>	0 ma	No.	of Cha	nnels _	3	Sens	4.8		Ref. Std. Ser. #
Unit	No. Wes	t Boil	er	_ Tube S	Size	211			Gauge		95	١	Material <u>SA-178-A</u>
	Dav. #	Tibe #	Diversed	Blocked				Wall L	oss %				Location/Remarks
	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-509	51-60%	61-70%	70% +	
1	A	11	ļ	ļ		X	ļ	<u> </u>	ļ	 			Membrane-thicker tube
2	<u> </u>	2	<u> </u>	<u> </u>	X	<u> </u>	ļ	 	<u></u>	<u> </u>	-	ļ	
3		3			X	ļ	-		-	-	<u> </u>	-	
4		4			X		-	-	 		 		
5		- 5			X			ļ	-		 		
6		6	<u> </u>		X		 	-	 	+	 		
7		7		<u> </u>	X		ļ	 	<u> </u>	-	-	 	
8	ļ	8			X	<u> </u>	<u> </u>		-			 	
9		9			X		 	-			 	<u> </u>	
10		10			X		-	-	-	 	 		
11		11			X		 	 	 	 	 	-	
12		12			X			-		 			
13		13			X		ļ	-	 		-		
14		14			X				-		 		
15		15			X		-	-	 		1	 	
16 17		16 17			X				 		 		
18		18			X		 	<u> </u>	 	-			
19		60			X					-	<u> </u>		
20		61			X			 					
21		62			X								
22		63	-		X								
23		64			X			_	<u> </u>	<u> </u>			
24		65			X			 	 				
25	В	1				Х							Membrane
26	-	2			х	-							
26 27 28		3			Х								
28		4			Х								
29		5			х					1			
30		6			Х								

TOTALS

Probe S/N __0015

Technician Brian Galvan

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Engineering Services

200 Ashford Center North Suite 300 Atlanta, Georgia 30338 (404) 396-4820

FIELD DATA REPORT

Cust	omer A	ffilia	ted En	gineer	s, S.	Ε.		F	vz Plant <u>Cł</u>	natta	nooga	, TN		Date _7	/25/9	5	
				rent <u>30</u>													
				_ Tube S													
		I		Blocked	Ι		·	Wall L	oss %				I				
	Row #	Tube #	Plugged	Blocked Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	ļ	Loca	tion/Rer	narks	
1		7			X					ļ							
2		8			X												
3		9			х				ļ								
4		10			Х							ļ					
5		- 11			Х							<u></u>					
6		12			X												
7		13			X												
8		14			Х				<u> </u>								
9		15			Х												
10		16			Х												
11		17			Х												
12		18			Х												
13		60			Х												
14		61			Х												
15		62			Х												
16	-	63			Х												
17		64			Х		-										
18		65			Х												
19	С	1			-	Х							Membr	ane			
20		2			Х		-										
21		3			X												
22		4			X												
23		5			X												
24		6			Х												
25		7			X												
26		8			X												
27		9			X												
28		10			X												
29		11			X												
30		12			X												
1201											1						

TOTALS

Probe S/N ___0015

Technician Brian Galvan

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Engineering Services

200 Ashford Center North Suite 300 Atlanta, Georgia 30338 (404) 396-4820

						FI	ELD	DAI	A K	EPO AAP,	Kı							
Cus	tomer A	ffilia	ted En	gineer	s, S	Ε.		F	lant Cl	hatta	nooga	a, TN	<u> </u>	Date	7/25	/95		
Fred	quency <u>1</u>	05 MHz	Cur	rent <u>30</u>	0 ma	_ No. 0	of Char	nnels _	3 8	Sens	4.8				_ Ref.	Std. Se	r. #	
		est Bo																
	T		<u></u>					Mall	V									
_	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	İ	Lo	cation/	Remark	s 	
1		13	ļ		Х			<u> </u>		ļ	ļ	ļ	ļ					
2	ļ	14			X			<u> </u>	ļ		ļ	ļ						
3		15			X		ļ	ļ		<u> </u>	ļ	ļ	ļ					
4	<u> </u>	16			X	<u> </u>		ļ	<u> </u>	<u> </u>	<u> </u>	<u> </u>	ļ. <u>.</u>					
5		- 17			X		ļ		ļ	ļ	ļ	ļ						
6		18			X			ļ	<u> </u>									
7		60			Х		<u> </u>	<u></u>	ļ				ļ					
8	<u> </u>	61			X			<u> </u>	<u> </u>	ļ		<u> </u>						
9		62		ļ 	Х				ļ									
10		63			X				<u> </u>				ļ					
11		64			X	.		<u> </u>					<u> </u>	 .				
12		65			Х													
13	D	1				Х	<u> </u>						Memb	rane				
14		2			Х				<u> </u>									
15		3			Х				<u> </u>	<u> </u>	<u> </u>							
16		4			Х													
16 17 18 19 20		5			Х							<u> </u>						
18		6			Х													
19		7			Х													
20		8			Х													
21	·	9			Х													
22		10			Х													
22 23		11			Х													
24		12			Х													
25		13			Х													
26		14			X				İ									
27		15			X													
28		16			X													
29		17			Y													

TOTALS

Probe S/N ___0015

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Technician Brian Galvan

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FIELD DATA REPORT

		<i>cc:</i> 1:-			•	_				VAAP,			7/05/05
													<u>N</u> Date 7/25/95
Fred	quency $\frac{1}{}$	05 MH2	Cur	rent <u>30</u>	0 ma	_ No.	of Chai	nnels _	3_ ;	Sens	4.8		Ref. Std. Ser. #
Unit	NoW	est Bo	iler	Tube S	Size	2"			Gauge		95	١	Material <u>SA-178-A</u>
	Row #	Tube #	Plugged	Blocked			· · · · · · · · · · · · · · · · · · ·	Wall L	oss %		T	T	Location/Remarks
1		60	Plugged	Obstructed	1·10% X	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	
2	 	61			X			 	 	\dagger			
3	 	62			X						<u> </u>		
4		63			X				<u> </u>		<u> </u>	†	
5		64			X								
6		65			X				1				
7	Е	1				х							Membrane
8		2			Х								
9		3			Х								
10		4			Х								
11		5			Х								
12		6			Х								
13		7			<u> </u>								
14		8			X								
15		9			Х						ļ		
16		10			Х								
17		11			Х				ļ				
18		12			Х							ļ	
19		13			_ X				ļ				
20		14			X			ļ 					
21		15			X			ļ					
22		16			_X								
23		17			Х				ļ				
24		18			Х								
25		60			Х								
26		61			_ X								
27		62			X					L			
28		63			Х								
29		64			_X								
30		65			Х								

TOTALS

Probe S/N __0015

Technician Brian Galvan

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Engineering Services

										/AAP,								
Cus	tomer A	ffilia	ted En	gineer	s, S	Е.		P	lant(Chatt	anoog	ga, T	N	Date_	7/2	<u>5/95</u>		
Fred	uency 1	05 MHz	Cur	rent <u>30</u>	0 ma	_ No. 0	of Char	nels_	3 §	Sens	4.8				Ref. S	Std. Ser	:. #	
Unit	No. <u>W</u>	est Bo	iler	_ Tube S	Size	2"			Gauge	.0	95	١	Material .	SA-1	78-A			
	D #	T.b. #	Diversed	Blocked	I			Wall L	oss %					۱۰۰۰	ation /	Remarks		
	Row #	Tube #	Plugged	Obstructed	1-10%	T	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	ļ		ation	Terraina	·	
1	F	11	<u> </u>	ļ		X	<u> </u>	 	 		 		Memb:	rane				
2		2			X	ļ	ļ		<u> </u>			ļ	<u> </u>					
3		3			X	ļ	ļ				<u> </u>		ļ					
4	<u> </u>	4			X	<u> </u>	ļ				ļ			-				
5		- 5			X				<u> </u>									
6		6			X					<u> </u>		ļ						
7		7			X													
8		8			Х													
9		9			X											-		
10		10		<u> </u>	X													
11		11			Х	ļ .						<u> </u>						
12		12			X													
13		13			Х													
14		14			Х						<u> </u>							
15	ø	15			Х													
16		16			Х													
17		17			Х													
18		18			Х													
19		60			Х			,										
20	-	61			Х													
21		62			Х													
22		63			X													
23		64			X													
24		65			X													
25		80			X		-											
$\overline{}$					X													
26		81																
27		82 83			X													
28 I	1	- X 1	1	· • • • • • • • • • • • • • • • • • • •	X							· •						

TOTALS

Probe S/N <u>0015</u>

84

85

X

Technician <u>Brian Galvan</u>

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FIELD DATA REPORT

Cus	_{tomer} A	ffilia	ted En	gineer	s, S.	Ε.		F		Chatt	anoog	ga, T	'n	Date 7/25	/95	
														Ref.		
														SA-178-		
Unit	NO	COC DO		lube s	oize								vialei iai _	<u> </u>		
	Row #	Tube #	Plugged	Blocked Obstructed	1.10%	111.200	121.20%	Wall L	OSS %	Is1-80%	61.70%	70% +	-	Location	Remarks	
1		86		Costructed	X	111-20-6	21-30-6	31-40-0	41-30-	31-00-a	31 70 0	1001	<u> </u>		• • • • • • • • • • • • • • • • • • • •	
2	<u> </u>	87			X	1	1		†	<u> </u>						
3	-	88	 	<u> </u>	X	 							†			
4		89	†		X			 		 						
5		90		 	X	1			 	1						
6		91			X			1	1	1						
7		92			X			1					· · · · · · · · · · · · · · · · · · ·			
8		93			X	-										
9		94			X		ļ		1							
10		95			X	İ	-		<u> </u>							
		96			Х											
11 12		97			Х	İ			<u> </u>					·····		
13	G	1				X							Membr	ane		
14		2			Х											
15		3			X											
16		4			X											
17		5			X											
18		6	-		X											
19		7			X											
20		8			Х			<u> </u>								
21		9			X											
22		10			X											
23		11			X											
24		12			X											
25		13			Х											
26		14			X									-		, , ,
27		15			X											
28		16			Х											
29		17			Х				Ì							
80		18			Х											
	TALC		<u>-</u>			···	· · · · ·									

TOTALS

Probe S/N ___0015

Brian Galvan Technician _

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Engineering Services

Customer Affiliated Engineers, S.E. Plant Chattanooga, TN Date 7/25/95 Frequency 105 MHz Current 300 ma No. of Channels 3 Sens. 4.8 Ref. Std. Ser. #									DAI	V	AAP.			
Frequency 105 MHz	Cus	tomer A	ffilia	ted En	gineer	s, S.	E.		PI	ant _C	hatt	anoog	a, T	N Date7/25/95
Now # Tube # Plugged Commerced 1.10% 1.20% 2.1% Malerial SA-178-A	Fred	uency <u>1</u>	05 MHz	Cur	rent _30	0 ma	_ No. c	of Char	nnels _3	3 8	Sens	4.8		Ref. Std. Ser. #
No. No.		-												•
No. No.		<u> </u>	1	<u> </u>	Blocked	1	-		Wall Lo	ss %			-	Landing (Daniel
Color	<u> </u>	How #	 -	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61 · 70%	70% +	Location/ Hemarks
3	$\overline{}$		60			X								
4 63 X X A B B B A A B			1	ļ			ļ	ļ						
5 64 X X Ceneral wall loss-midway 7 80 X Ceneral wall loss-midway 8 81 X Possible material change 0 83 X Possible material change 11 84 X Possible material change 13 86 X Possible material change 14 87 X Possible material change 15 88 X Possible material change 17 90 X Possible material change 18 91 X Possible material change 20 93 X Possible material change 21 94 X Possible material change 22 95 X Possible material change 24 97 X Possible material change 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	3			<u> </u>										
6 6 65	4		 					<u> </u>						
7 80 X General wall loss-midway 8 81 X Possible material change 0 83 X Possible material change 11 84 X Possible material change 12 85 X Possible material change 14 87 X Possible material change 15 88 X Possible material change 16 89 X Possible material change 18 91 X Possible material change 19 92 X Possible material change 20 93 X Possible material change 21 94 X Possible material change 22 95 X Possible material change 24 97 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	5		 			X								
8 81 X X Possible material change 10 83 X X Possible material change 11 84 X X Possible material change 12 85 X Possible material change 14 87 X Possible material change 15 88 X Possible material change 16 89 X Possible material change 18 91 X Possible material change 20 93 X Possible material change 21 94 X Possible material change 22 95 X Membrane 24 97 X Possible material change 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	6		65			X		ļ						
9	7		80	ļ	!		X	ļ						General wall loss-midway
No	8		81			X								
11 84 X X Possible material change 12 85 X Possible material change 13 86 X Possible material change 14 87 X Possible material change 15 88 X Possible material change 17 90 X Possible material change 18 91 X Possible material change 20 93 X Possible material change 21 94 X Possible material change 22 95 X Possible material change 24 97 X Possible material change 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	9		82				Х							Possible material change
12 85 X N Possible material change 13 86 X N Possible material change 14 87 X N N N 15 88 X N N N 16 89 X N N Possible material change 17 90 X N N Possible material change 18 91 X N N Possible material change 20 93 X N Possible material change 21 94 X N Possible material change 22 95 X N Membrane 24 97 X N Membrane 25 H 60 X N Possible material change 26 61 X N Possible material change 28 63 X N N Possible material change	10		83			X								
13 86 X Possible material change 14 87 X X X 15 88 X X X X 16 89 X X Possible material change 17 90 X Possible material change 18 91 X Y Possible material change 20 93 X Possible material change 21 94 X Possible material change 22 95 X Possible material change 24 97 X Possible material change 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	11		84			X								
14 87 X Image: square sq	12		85			X								
15 88 X X Possible material change 16 89 X Possible material change 17 90 X Possible material change 18 91 X Possible material change 20 93 X Possible material change 21 94 X Possible material change 22 95 X Membrane 23 96 X Membrane 24 97 X Possible material change 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	13		86				X							Possible material change
16 89 X N Possible material change 17 90 X N Possible material change 18 91 X N N 19 92 X N N 20 93 X N Possible material change 21 94 X N Possible material change 22 95 X N Membrane 24 97 X Membrane 25 H 60 X N Possible material change 26 61 X N Possible material change 28 63 X N N N 29 64 X N N N	14		87			X								
17 90 X X Possible material change 18 91 X X X 19 92 X X X 20 93 X X Possible material change 21 94 X Possible material change 22 95 X Membrane 24 97 X Membrane 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	15		88			X								
18 91 X S	16		89			X								
19 92 X X	17		90				Х					•		Possible material change
20 93 X Possible material change 21 94 X Possible material change 22 95 X Membrane 23 96 X Membrane 24 97 X Membrane 25 H 60 X Possible material change 26 61 X Possible material change 28 63 X Possible material change	18		91			X								
21 94 X Possible material change 22 95 X S S 23 96 X S Membrane 24 97 X Membrane 25 H 60 X S 26 61 X S Possible material change 28 63 X S S 29 64 X S S	19		92			X								
22 95 X Image: square sq	20		93			Х								
23 96 X Membrane 24 97 X Membrane 25 H 60 X Membrane 26 61 X Possible material change 27 62 X Possible material change 28 63 X N 29 64 X N	21	·	94				Х							Possible material change
23 96 X Membrane 24 97 X Membrane 25 H 60 X Membrane 26 61 X Possible material change 27 62 X Possible material change 28 63 X N 29 64 X N						Х								
24 97 X Membrane 25 H 60 X S 26 61 X S Possible material change 27 62 X Possible material change 28 63 X S 29 64 X S	$\neg \neg$		96			Х								
25 H 60 X	一						Х							Membrane
26 61 X Possible material change 27 62 X Possible material change 28 63 X X 29 64 X X	$\neg \neg$	Н				х								
27 62 X Possible material change 28 63 X Section 1 29 64 X Section 2	- 1													
28 63 X 29 64 X	- 1						Х							Possible material change
29 64 X						X								
	- 1			i										
														

TOTALS

*Tubes 82, 86, 90, 94 may be of a greater thickness to allow for attachments (soot blower).

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						FI	ELD	DA	IA K	EPU VAAP,			
Cus	tomer <u>A</u>	ffilia	ted En	gineer	s, S	.E.		f	Plant	Chatt	anoo	ga, I	<u>N</u> Date 7/25/95
Frec	uency 1	05 MHz	Cui	rrent 30	0 ma	_ No.	of Cha	nneis _	3 :	Sens	4.8		Ref. Std. Ser. #
Unit	No <u>W</u>	est Bo	iler	Tube S	Size	2"			Gauge	0	95		Material <u>SA-178-A</u>
	ı		T	Blocked	T			Wall I	oss %				T
	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61 -70%	70% +	Location/Remarks
1		80				X		ļ			<u> </u>		Possible material change
2		81			X		ļ	ļ					
3		82		<u> </u>	X	<u> </u>	<u> </u>	<u> </u>					
4		83			Х	<u> </u>	ļ		<u> </u>		ļ		
5		84		<u> </u>	ļ	Х	ļ			ļ	ļ		Possible material change
6		85			Х		ļ						
7		86			Х	<u> </u>	<u> </u>	ļ	<u> </u>	ļ <u>.</u>			
8		87			X			<u> </u>	ļ		ļ <u> </u>		
9		88				Х	<u> </u>			ļ			Possible material change
10		89			X		ļ	<u> </u>	ļ				
11		90			X	ļ	<u> </u>	<u> </u>		ļ			
12		91			Х	<u> </u>		ļ					·
13		92				X		<u> </u>	<u> </u>	<u> </u>			Possible material change
14		93			X								
15		94			X		ļ		<u> </u>				
16		95			X				<u> </u>				
17		96				X		ļ	<u> </u>			_	Possible material change
18		97				Х	<u></u>		<u> </u>	<u></u>			
19	I	60			X								
20		61			X								
21		62			X								
22		63			X		<u> </u>						
23		64			X								
24		65			X								
25		80			X								
26		81			X_								
27		82			X								
28		83			Х								
29		84			X								
30		85			Х					<u> </u>			
TO	ΓALS			80, 8 hments					be o	fag	reate	er th	ickness to allow

Probe S/N ___0015

Technician Brian Galvan

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Engineering Services

						Fi	ELD	DAT	AR	EPO VAAP	RT							
Cus	tomer A	ffilia	ted En	gineer	s, S	Е.		F	Plant _	Chatt	anoog	ga, T	N	Date.	7/25	/95		<u></u>
Frec	uency <u>1</u>	05 MHz	Cur	rent 30	0 ma	_ No.	of Char	nnels _	3	Sens	4.8				Ref. S	Std. Ser	. #	
			iler															
Γ	D#	T.5- #	Diversed	Blocked	Γ			Wall L	oss %					10	cation /	Remarks		
	Row #	Tube #	Pluggea	Obstructed		11-20%	21-30%	31-40%	41-509	51-60%	61-70%	70% +			Jalionii	Terriarks		
1		86			X		<u> </u>	ļ	<u> </u>	 	-	ļ						
2		87	ļ		X	ļ	<u> </u>	ļ	<u> </u>	ļ	ļ							
3		88	ļ	ļ	X	ļ				<u> </u>								
4		89			X		<u> </u>	<u> </u>	ļ									
5		90			Х						<u> </u>							
6		91			Х					<u> </u>								
7		92			Х			ļ	ļ									
8		93			Х													
9		94			Х						<u> </u>							
10		95			Х													
11		96			Х													
12		97				Х							Memb	cane				
13	J	60			X													
14		61			Х													
15		62			Х													
16		63			X													
17		64			Х					1								
18		65	-		Х													
19		80			X					1								
20		81			X													
21		82			X												,	
22		83			X									•				
23		84			X					1								
24		85			X					 								
		86			X										· - · · · · · · · · · · · · · · · · · ·			
25		87			X		-			 								
26										 								
27		88			X					 								
28		89			X					 								

TOTALS

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Probe S/N ___0015

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200 Ashford Center North Suite 300 Atlanta, Georgia 30338 (404) 396-4820

Engineering Services

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FIELD DATA REPORT

		<i>ffili</i> a	tad Em	~	- c	E				AAP,		T	NT.	_	7/25/05
															7/25/95
Freq	uency $\frac{1}{2}$	05 MHz	Cur	rent <u>30</u>	0 ma	_ No.	of Chai	nnels _	<u>3</u> s	Sens	4.8				Ref. Std. Ser. #
Unit	No. <u>W</u>	est Bo	iler	_ Tube S	Size	2"			Gauge	.09	5	١	/laterial	SA-1	78-A
Γ	Row #	Tube #	Plugged	Blocked				Wail L	oss %					1.00	cation/Remarks
-	now #		Flugged	Obstructed	1	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +			
1		92	<u> </u>	-	X	 	ļ		-			ļ			
2		93	 	-	X	 	ļ	<u> </u>	ļ						
3		94			X	ļ	ļ	ļ 1	-						
4		95	ļ		X		<u> </u>		-						
5		96	ļ	ļ	X	<u> </u>	 					ļ			
6	:	97	ļ			X	<u> </u>	-	 				Memb:	rane	
7	K	60			X		<u> </u>	ļ				ļ			
8		61			X		ļ		ļ						
9		62			X	ļ	ļ		ļ						
10		63			X				ļ						
11		64			X			ļ							
12		65			Х				<u> </u>						
13		80				X	<u> </u>		<u> </u>				Gen.	wall	loss-low-mid
14		81				X			<u> </u>				Gen.	wall	loss-mid-upper
15		82			X										
16		83			X										
17		84			Х										
18		85			X										
19		86	,		X								· · · · · · · · · · · · · · · · · · ·		
20		87			X										
21		88			Х										
22		89			Х										
23		90			Х										
24		91			Х										
25		92				Х							Gen.	wall	loss-upper
26		93			Х										
27		94		i	X										
28		95			Х										
29		96			X										
30		97				х							Membr	ane	
	-AI C				1		1		·	<u>.</u>	 1 .				

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							ELD			VAAP,				
Cus	tomer <u>A</u>	ffilia	ted En	gineer	s, S	.E.		F	Plant	Chatt	anoo	ga, T	N Date 7/25/95	···
Fred	quency <u>1</u>	05 MHz	Cur	rent <u>30</u>	0 ma	_ No.	of Char	nnels _	3	Sens	4.8		Ref. Std. S	ier. #
Unit	No. <u>W</u>	est Bo	iler	_ Tube S	Size	2"			Gauge	09	5	I	Material <u>SA-178-A</u>	
	Row #	Tubo #	Plugged	Blocked		_		Wall L	oss %				Location/Remai	rke
-	 	 	riugged	Obstructed	I	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location / Hernal	
1	L	60			X	-	 	<u> </u>	 	 	<u> </u>	├		
2		61		ļ	X	-	 		ļ		 	 		
3		62			X		ļ	ļ			<u> </u>			
4		63	-		X		 	-				 		1
5		64			X		 	ļ	-	 	<u> </u>	-		
6	<u> </u>	65			X		<u> </u>		 	ļ	 	 		
8		80			X		<u> </u>	 				 	· · · · · · · · · · · · · · · · · · ·	
9		81 82			X	\		<u> </u>	 		 	<u> </u>	Gen. wall loss-lo	
10		83			v	X		-	 	-			Gen. wall loss-ic	JW-III LU
11		84			X X		 							
12		85		-	X									
13		86			X				 				· · · · · · · · · · · · · · · · · · ·	
14		87			X				 					
15		88			X				<u> </u>					
16		89			X									
17		90			X									
18		91				Х							Gen. wall loss-lo	w-mid
19		92		-	Х									
20		93			Х									
21	•	94			Х									
22		95			Х									
23		96			Х									
24		97				Х							Membrane	
25														
26														
27														
28														
29														
30							I							
TO.	TALS	*Bli	sters 1	were no	oted	on L	-82 u	ipon	subse	equen	t vis	sual	inspection.	

Technician <u>Brian Galvan</u> **79**





Engineering Services

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FIELD DATA REPORT

VAAP,

Cus	tomer <u>A</u>	ffilia	ted En	gineer	s, S	.E.		F	Plant C	hatta	noog	a, TN	Date 7/24/95
Frec	quency <u>1</u>	05 MHz	Cur	rent <u>A</u>	.C	_ No. o	of Chai	nnels _	3_ 8	Sens	4.8		Ref. Std. Ser. #
													Material <u>SA-178-A</u>
_	Τ	1		r				VA I - II I	0/				T
	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location/Remarks
1	A	1				Х		<u> </u>				ļ	Membrane
2		2			Х								
3		3			Х								
4		4			Х								
5		5			X								
6		6			X								
7		7			Х								
8		8			X								
9		9			Х			<u> </u>					
10		10			Х								
11		11			X								
12		12			X								
13		13			X				<u> </u>				
14		14			X				<u> </u>				
14 15		15			X								
16		16			X			<u> </u>					
17		17			X								
18		18			Х								
19		60			X								
20		61			Х								
21		62			Х								
22		63			Х								
23		64			Х								
24		65			Х								
25	В	1				Х							Membrane
26		2			Х								
27		3			Х								
28		4			Х								
29		5			Х								
30		6			X								

TOTALS

Probe S/N <u>1537128</u>

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FIELD DATA REPORT

								ם או	, v	AAP,			
Cus	tomer	Affilia	ated Er	ngineer	s, S	.E.		P	lant C	hatta	noog	a, TN	N Date _7/24/95
Fred	quency_	105 MH	Z Cui	rent A	rC	_ No. (of Char	nnels _	3 8	Sens	4.8		Ref. Std. Ser. #
Unit	No	East		_ Tube S	Size	2"			Gauge	.09	<u> </u>	^	Material <u>SA-178-A</u>
	Row #	Tubo #	D'	Blocked				Wall L	oss %				Location/Remarks
	How #	lube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location/ Remarks
1		7			X		ļ	<u> </u>			ļ		
2	ļ	8		ļ	X	ļ	<u> </u>	ļ		ļ			
3		9	<u> </u>		X	ļ	<u> </u>	<u> </u>					
4		10			Х								
5		- 11			Х								
6		12			Х								
7		13			х								
8		14			Х								
9		15			Х								
10		16			Х								
11		17			X								
12		18			X								
13		60			X								
14		61			X								
15		62			X		-						
16		63			X								
17		64			X								
18		65			X								
19	С	1			Λ	Х							Membrane
20		2			X								Helibrane
21	-	3			X								
22		4			X								
		 											
23		5			X								
24		6			<u>X</u>								
25		7			X								
26		8			X								
27		9			X								
28		10				X							Possible pitting midway
~ I		1 11 1			37	1						1	

TOTALS

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FIELD DATA REPORT

VAAP.

Cus	tomer A	ffilia	ted En	gineer	s, S	.Е.		F	Plant C	hatta	nooga	a, TN	Date _7/24/95
Fred	quency <u>1</u>	05 MHz	Cur	rent <u>A</u>	C	No.	of Char	nnels _	3	Sens	4.8	8	Ref. Std. Ser. #
Unit	NoE	ast		_ Tube S	Size	2"	····		Gauge		95		Material <u>SA-178-A</u>
Г	Row #	Tube #	Plugged	Blocked	<u> </u>		,	Wall L	.oss %				Location/Remarks
-	11000 #	 	riugged	Obstructed		11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location/Remarks
2		13			X			<u> </u>					
3		14			X	-			 	 	 		
4		15 16			X X		-	 	 	 			
5		17			X					 			
6		18			X		1						
7		60			X	<u> </u>							
8		61			Х								
9		62			Х								
10		63			Х								
11		64			Х								
12		65			Х								
13	D	1				Х							Membrane
14		2			Х								
15		3			Х					ļ			
16		4			Х								
17		5			Х					<u> </u>			
18		6			Х					<u> </u>			
19		7			x				ļ				
20		8			<u> </u>								
21		9			X								
22		10			Х								
23		11			Х				ļ	ļ			
24		12			Х				<u> </u>				
25		13			X				ļ				
26		14			X_								
27		15			Х							-	
28		16			X								
29		17			X							-	
30		18			X								

TOTALS

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Engineering Services

FIELD DATA REPORT

VAAP,	AAP,
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Cus	tomer A	ffilia	ted En	gineer	s, S.	E.		P	lant <u>Cl</u>	natta	nooga	, TN	Date _7/24/95
Fred	uency <u>1</u>	05 MHz	Cur	rent <u>A</u>	С	No. o	of Char	nels _	3 8	Sens	4.8		Ref. Std. Ser. #
													Material <u>SA-178-A</u>
	т	,	1	Blocked	T			Wall L					<u> </u>
	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61 - 70%	70% +	Location / Remarks
1		60			Х				ļ	ļ			
2		61		ļ	Х	ļ <u></u>	ļ <u>.</u>	ļ					
3		62_			X						ļ		
4		63_			X					ļ			
5		64		<u> </u>	X	ļ							
6		65			X				ļ				
7	E	1				X					<u> </u>		Membrane
8		2		<u> </u>	X								
9		3	 		X							ļ	
10		4	<u> </u>		X							<u>. </u>	
11		5			X		-						
12		6 7			X						ļ		
13		8			X	L							
15		9			X								
16		10			X								
17		11			X								
18		12			X								
19		13			Х								
20		14			Х								
21	·	15			Х								
22		16			Х								
23		17			Х								
24		18			Х								
25		60			Х								
26		61			Х								
27		62			X								
28		63			Х								
29		64			X								
30		65			X								

TOTALS

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FIELD DATA REPORT

Cur	A	ffilia	ited Er	gineer	s. S				V.	AAP,	anoog	a, Tì	N Date 7/24/95
													Ref. Std. Ser. #
													Material <u>SA-178-A</u>
	T_	T	T	Blocked	T			Wall L	oss %				Leasting (Remarks
	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location/Remarks
1	F	1				X			ļ	<u> </u>	ļ	ļ <u> </u>	Membrane
2		2			X			ļ	<u> </u>	ļ	ļ		
3		3			X	<u></u>		<u> </u>					
4		4			X				ļ	<u> </u>	<u> </u>		
5		- 5			X		<u> </u>						
6		6			х	<u> </u>	<u>.</u>		<u> </u>	<u> </u>			
7		7			X						<u></u>		
8		8			Х								
9		9			Х								
10		10			Х								
11		11			Х								
12		12			Х								
13		13			X								
14		14				Х	_						Lower
15		15			Х								
16		16			X					-			
17		17			X			l					
18		18			X				<u> </u>	<u> </u>			
19		60		, .	X								
20		61			Х								
		62			X					-			
21		63			X								
22									ļ				1 W - N-100
22 23 24 25		64			X								,
24		65			X								
		80			X		-						
26		81			X								
27		82	· · · · · · · · · · · · · · · · · · ·		X								
28		83			X								
29		84			Х								

TOTALS

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FIELD DATA REPORT

Cus	tomer A	ffilia	ted En	gineer	s, S	.E.		F	Plant C	hatta	nooga	a, TN	Date 7/24/95
Fred	uency <u>1</u>	05 MHz	Cur	rent <u>A</u>	С	No. o	of Char	nels _	3 :	Sens	4.8	8	Ref. Std. Ser. #
													Material <u>SA-178-A</u>
	Row #	Tube #	Plugged	Blocked Obstructed				Wall L	oss %	1	las 200	Izon .	Location/Remarks
-	1100 "		liuggou	Obstructed		11-20%	21-30%	31 - 40%	41-50%	51-60%	61-70%	70% +	
1		86 87			X		 	<u> </u>					
3		88	-		X			-					
4	<u> </u>	89			X				 				
5		90			X								
6		91			X								
7		92			X								
8		93			X				<u> </u>				
9		94			X			<u></u>					
10		95			X								
11		96			X								
12		97				Х							Membrane
13	G	1				Х							Membrane
14		2			Х								
15		3			X								
16		4			Х								
17		5			X								
18		6	_		X				<u> </u>				
19		7			X								
20		8			X								
21		9			X				<u> </u>				
22		10			X								
23		11			X								
24		12			Х								
25		13			X								
26		14			X								
27		15			Х								
28		16			X								
29		17			<u> x</u>								
30		18			X								

TOTALS

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Engineering Services

200 Ashford Center North Suite 300 Atlanta, Georgia 30338 (404) 396-4820

						FI	ELD	DAT	A RI	EPO	RT				
Cus	tomer A	ffilia	ted En	gineer	s, S	.E.		P			noog	a, TN	Date	7/24/95	··
Fred	quency <u>1</u>	05 MHz	Cur	rent A	.C	_ No. (of Char	nnels _	3 8	Sens	4.8			_ Ref. Std. Se	r. #
													MaterialSA		
Г	Row #	Tube #	Plugged	Blocked	1.10%	11.20%	21-30%	Wall L	oss %	51-60%	61-70%	70% +	L	ocation/Remark	s
1		60		Conracted	X	1,, 25 0		9, 100							
2		61			Х										
3		62			Х										
4		63			Х										
5		64			Х										
6		65			Х									a	
7		80			Х										
8	Ĺ	81			Х										
9	<u> </u>	82				X			_				Possible	material	change
10		83			Х				ļ						
11		84			Х										
12		85			Х										
13		86				Х							Possible	material	change
14		87			X										<u> </u>
		ı	ı	ı		I .		i l				1			

15		88		Х		<u> </u>			
16		_89		X					
17		90			Х				Possible material change
18		91		X					
19		92		Х					
20		93		Χ					
21		94			X				Possible material change
22		95		Х					
23		96		Х					
24		97			Х				Membrane
25	Н	60		Х					
26		61		X					
27		62		Х					
28		63		Х					-
29		64		Х		•			

TOTALS

*Tubes 82, 86, 90, 94 may be of a greater material thickness to allow for attachments (soot blower).

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Engineering Services

FIELD DATA REPORT

			. 1 5	•		_				AAP,		- (11)	7/2//05
													Date 7/24/95
Fred	quency $\underline{1}$	05 MH2	Cur	rrent <u>A</u>	'C	_ No.	of Cha	nnels _	<u> 3 </u>	Sens	4.8		Ref. Std. Ser. #
Unit	NoE	ast		_ Tube S	Size	2"			Gauge	.09	5	١	Material <u>SA-178-A</u>
	1	T	т	I District	Τ			Mall I	oss %				T
	Row #	Tube #	Plugged	Blocked Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location/Remarks
1		80				х		<u> </u>					Possible material change-
2						<u> </u>							attachment
3		81			X								
4		82			X					Ĺ			
5		83			Х								
6		84				Х							Possible material change-
7													attachment
8		85			Х								
9		86			Х								
10		87			Х								
11		88				Х							Possible material change-
12													attachment
13		89			Х								
14		90			Х								
15		91		- "	Х								
16		92				Х							Possible material change
17		93			X								•
18		94			Х								
19		95			Х								
20		96			Х								
20 21	·	97			·	Х							Membrane or change in
22													thickness
22 23	I	60			X								
24		61			Х								
25		62			Х						_		
26		63			Х								
27	1	64			Х								
28		65			X								
29		80			X	-							
30		81			Х								
	TALS	*Tub	es 80,	84, 8	8, 9	2 may	be	of a	great	ter m	ater	ial t	hickness to allow

for attachment (soot blower).

Probe S/N __1537128

Technician Brian Galvan

Page <u>8</u> of <u>11</u>





Engineering Services

FIELD DATA REPORT

VAAP.

Cus	tomer <u>A</u>	ffilia	ted En	gineer	s, S	.E.		f	Plant _	Chatt		ga, I	N	Date 7/24/95	
Free	quency <u>1</u>	05 MHz	Cur	rent A	.C	_ No. (of Chai	nnels _	3	Sens	4.8	8		Ref. Std. Ser. #	! <u></u>
Unit	NoE	ast		_ Tube S	Size	2"			Gauge	.09	5	ا	Material ,	SA-178-A	
_	1		т	1	·								T		
L_	Row #	Tube #	Plugged	Blocked Obstructed	1-10%	11-20%	21-30%	31 - 40%	_OSS %	51-60%	61-70%	70% +	1	Location/Remarks	
1		82			Х										
2		83			X										
3		84			Х										
4		85			Х					ļ					
5		86			X						<u> </u>				
6		87			X		<u> </u>								
7		88			X		<u> </u>		<u> </u>	ļ			<u> </u>		
8		89			X				<u> </u>						
9		90			X										
10		91			X				ļ						
11		92			X				<u> </u>						
12		93			X										
13		94			X				<u> </u>						
14		95			X				<u> </u>						
15		96			X				<u> </u>						
16		97				X							Memb	rane	
17	J	60			X										
18		61			Х				<u> </u>						
19		62			X										
20		63			X				ļ						
21		64			Х										
22		65			X										
23		80			X										
24 25		81			Х										
		82			Х										
26		83			<u> </u>								··n		
27		84			Х										
28		85			х										
29		86			х										
30		87			Х]	·		

TOTALS

Probe S/N <u>1537128</u>

Technician <u>Brian Galvan</u>

Page 9 of 11





Engineering Services

200 Ashford Center North Suite 300 Atlanta, Georgia 30338 (404) 396-4820

FIELD DATA REPORT

Cust	omer A	ffilia	ted En	gineer	s, S.	Ε.		P	lant <u>Ch</u>	atta	nooga	a, TN	Date <u>7/24/95</u>
													Ref. Std. Ser. #
													Material <u>SA-178-A</u>
		-	<u></u>	Blocked	I			Wall L	oss %				Location/Remarks
	Row #		Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Eccation/ Hemarks
1_		94			X	 	ļ		<u> </u>		ļ		
2		95			X	ļ							
3		96			X	<u> </u>			ļ	<u> </u>			
4		97				X			ļ				Membrane
5	L	60			X	ļ	<u> </u>		<u> </u>	ļ			
6		61			X		<u> </u>						
7		62			X		<u> </u>		ļ			ļ	
8		63			Х	ļ			ļ				
9		64			Х		ļ	ļ					
0		65			X				<u> </u>				
1_		80			_ X_								
2		81			Х	<u> </u>							
3	-	82			Х		<u> </u>		<u> </u>			ļ	
4		83			Х				<u> </u>				
5		84			X			١					
6		85			Х								
7		86			Х								
8		87			Х								
9		88			Х								
0		89			Х								
21		90			Х					[
22		91			Х								
3		92			Х								
24		93	1			Х							General wall loss
25		94			Х								
26		95			Х								
27		96		<u> </u>	Х								
28		97	1			Х							Membrane
29													
30		-	.,										
	TALS		·	L	·		-				<u>•</u>	•	

Probe S/N <u>1537128</u>

Technician Brian Galvan

Page <u>11</u> of <u>11</u>





Engineering Services

200 Ashford Center North Suite 300 Atlanta, Georgia 30338 (404) 396-4820

FIELD DATA REPORT

V	Α	Α	P	
٠			-	,

Customer Affiliated Engineers, S.E. Plan													
Frequency 105 MHz Current AC No. of Channels 3						<u>3</u> s	ens	4.8	3	Ref. Std. Ser. #			
Unit	NoE	ast		_ Tube S	Size	2"		(Gauge .	.09	5	N	Material <u>SA-178-A</u>
	٦	+ - "	DI	Blocked				Wall Lo	oss %				Location/Remarks
	Row #	Tube #	Plugged	Obstructed	1-10%	11-20%	21-30%	31-40%	41-50%	51-60%	61-70%	70% +	Location/Hemaiks
1	ļ	88			X			ļ			ļ		
2		89			X			ļ	ļ				
3		90	,		Х			ļ					
4		91			X			ļ	<u> </u>		ļ		
5		92			Х					ļ			·
6		93			X	<u> </u>	ļ						
7		94			Х		ļ	<u> </u>					
8		95			Х			ļ					
9		96			Х				ļ				
10		97				X							Membrane
11	К	60			Х								
12		61			Х			<u> </u>			<u> </u>		
13		62			X				<u> </u>				
14		63			Х								
15		64			Х								
16		65			Х								
17		80			Х								
18		81			Х								
19		82			Х	Ī							
20		83			Х								
21		84			Х								
22		85			Х								
23		86			Х								
24		87			Х								
25		88			Х								
26		89			X								
27		90			X								
28		91			X								
29		92			X								
30		93	>		X						ĺ		

TOTALS

Probe S/N <u>1537128</u>

Technician Brian Galvan

Page <u>10</u> of <u>11</u>

APPENDIX D BOILER TUBE LAYOUT

Not To Scale

EAST BOIL

National



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←——— C

EAST BOILER TUBE LAYOUT

National Board # 23636



Harttord Steam Boiler Inspection and Insurance Company Atlanta, Georgia

← Gas Flow

Burner

៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰៰ Flue Ges Outlet

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90

621 ● ●0 ○● 00 ○● 00 ○● 00 ○● 00 00 00 00 00 00 00 00 00 0

- Tubes with Blisters

Not To Scale

WEST



tar Janaan

62 30 ੶

3bsters

WEST BOILER TUBE LAYOUT
National Board # 23635



Flue Gos Outlet

15 37 45

Ges Flow

Burner

TUOYA.

5



APPENDIX E

TUBE THICKNESS

Right (long) Water Wall

Tube #	Loc. 1	Loc. 2	Loc. 3	Loc. 4
1	.172	.176	.177	.176
6	.174	.171	.170	.170
11	.171	.170	.171	.172
16	.170	.169	.170	.171
21	.168	.167	.167	.167
26	.169	.170	.170	.170
31	.169	.168	.170	.169
36	.171	.172	.171	.173
41	.170	.168	.169	.166 Original
46 .	.171	.171	.168	.172 thickness
51	.172	.173	.168	.171 .165" these
56	.173	.174	.174	.172 tubes.
61	.172	.172	.170	.170
66	.168	.170	.168	.169
71	.169	.168	.168	.170
76	.167	.169	.168	.168
81	.169	.171	.172	.171
86	.170	.171	.172	.173
91	.171	.172	. 171	. 171
Rear Wate	r Wall			
Tube #	Loc. 1	Loc. 2	Loc. 3	Loc. 4
2	.143	.139*	.142	.142
4	.136	.137	.135	.135
6	.136	.136	.137	.138
8	.140	.140	. 141	.141 Original
10	.135	.136	.135	.136 thickness
12	.138	.141	.141	.140 .134" these
14	.141	.142	.142	.142 tubes
16	.143	.145	.144	.145
18	. 144	.142	.140	.142
20	.137	.138	.138	.137

Left (long) Water Wall

Tube #	Loc. 1	Loc. 2	Loc. 3	Loc. 4
5	.172	.174	.173	.174
10	.170	.171	.171	. 171
15	.172	.173	.170	.172
20	.168	.169	.169	.169
25	.169	.170	.172	.172 Original
30	.169	.171	.171	.172 thickness
35	.170	.171	.172	.172 .165" these
40	.172	.170	.171	.173 tubes.
45	.168	.168	.169	.170
50	.170	.170	.172	.171
55	.168	.169	.168	.170
60	.169	.170	.171	.170
65	.168	.169	.170	.170
70	.169	.171	.172	.170
75	.169	.170	.171	.171
80	.169	.171	.171	.170
85	.170	.172	.172	.171
90	.169	.169	.170	.170

East Boiler Tube Thickness

Left (short) Water Wall

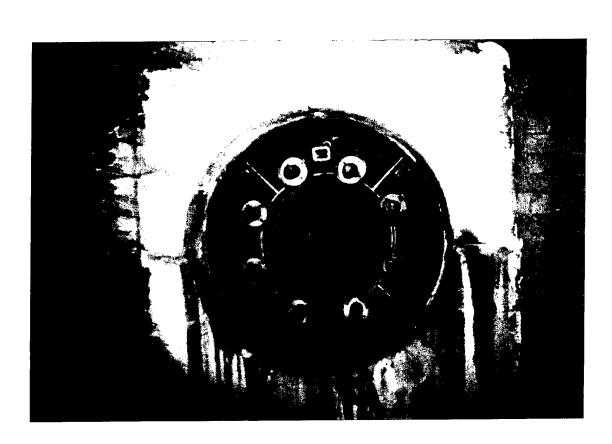
T	ube #	Loc. 1	Loc.	2	Loc.	3	Loc.	4
	1	.136	.134		.139		.135	
	6	.139	.140		.139		.140	
	11	.135	.136		.133		.134	
	16	.138	.137		.139		.140	
	21	.136	.134		.137		.137	Original
	26	.134	.134		.137		.134	thickness
	31	. 141	.141		.140		.141	.134 these
	36	.138	.140		.141		.142	tubes.
	41	.139	.140		.141		.141	
	46	.138	.138		.141		.141	
	51	.140	.139		.139		.139	
	56	.139	.139		.140		.141	
	61	.142	.143		.142		.142	
	66	.137	.140		.138		.139	
	71	.137	.137		.136		.136	
	76	. 105	.103		. 104		.103	Original
	81	. 100	.103		. 101		.101	_
	1		.102		.106		.107	i
	86	. 105					.107	1
	91	. 107	.106		.107		. 10/	canes.

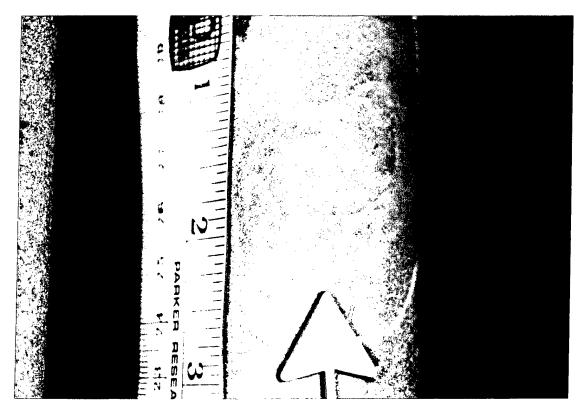
APPENDIX F BOILER PICTURES

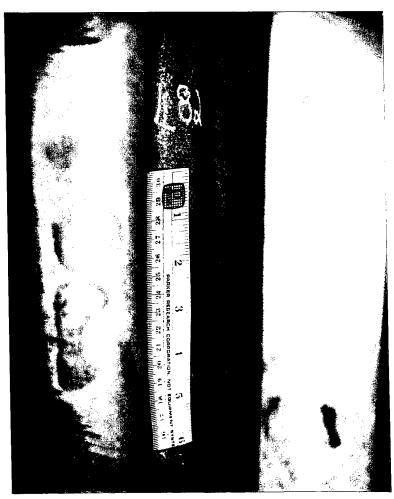
Boiler Photograph Log

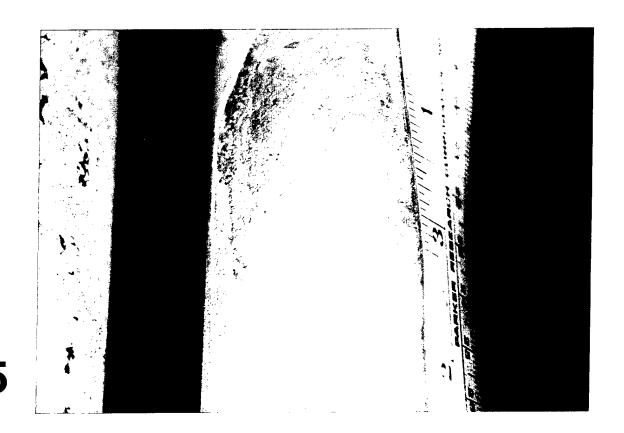
Photograph #	Description
1	Casing of east economizer. Notice corrosion is in a straight line pattern at 2 levels.
2	West boiler burner. Staining appears to be from water. Condition of refractory is good.
3	Blister on west boiler tube. Notice length of blister.
4	Another tube in west boiler, this tube is in the 2nd row in.
5	Another tube blister, same boiler.
6	West boiler water wall (left side). Notice degree of carbon buildup. Most likely from improper burner alignment.
7	West boiler water wall (right side). Notice fireside deposits and minimum amount of carbon buildup.
8	West boiler economizer. Notice straight line corrosion at 2 levels.



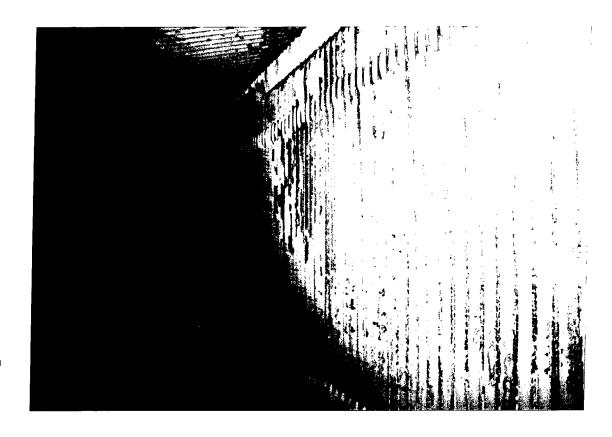


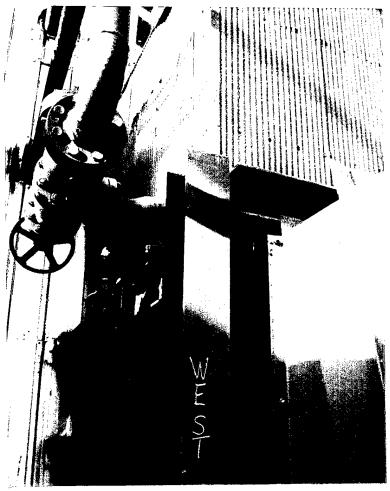












APPENDIX G DEAERATING TANK INSPECTION

Deaerating Feed Tanks

The two deaerating feed tanks were visually inspected both internally and externally. The name plate data is as follows:

	East DA Tank		West DA Tank
Mfg by: MAWP:	Dun-Rite Tank C		Dun-Rite Tank Corp 30 psi @ 500F
Mfg Ser #:	5560-2	S	5560-1
Nat'l Bd #:	1721	Div 1	1720
Year built:	1972	W	1972
Shell t:	1/4" (.250")		1/4" (.250")
Head t:	1/4" (.250")		1/4" (.250")
Head Radius:	66"		66"

Safety valves (both deaerators)

a. Name plate data:

Manufacturer - Lonergan

Size - 3" x 3"

Capacity - 3,785 lbs/hr

b. Condition - Top seal broken

- Valve stuck closed

East Deaerating Feed Tank

Storage Section, internal:

- Internal pitting, most predominately adjacent to weld seams but scattered throughout vessel.
- 2) Significant coating of deposits at water line, lower portion of vessel the deposits are moderate.
- 3) Gasket surface of manway ring slightly corroded, most notable at inner edge.
- 4) One desiccant container installed.
- 5) Moderate surface corrosion from water line down

Deaerating Section, internal:

- 1) Spray valves (5), appear satisfactory, loose rust flakes noted inside spray valves when opened.
- No corrosion of tray storage area or trays

External.

- The following components were noted to be cracked, most likely from freezing conditions:
 - a. Lower float chamber of water level control
 - b. Lower piping of level control
 - c. Secondary lower pipe level control
 - d. Sight glass lower pipe connection

West Deaerating Feed Tank

Storage Section, internal:

- 1) Internal pitting, most predominantly adjacent to weld seams but scattered throughout vessel.
- 2) Gasket surface of manway ring inner edge corroded.
- 3) Thick coating of deposits adhered to shell from water line down.
- 4) Large amount of loose sediment and rust flakes laying in vessel.
- 5) 1 desiccant container in vessel.
- 6) Moderate to heavy amount of surface rust, mostly from water line down.

Deaerating Section, internal:

- 1) 1 of 5 spray valve is stuck closed.
- 2) Rust flakes inside other 4 spray valves when opened.
- 3) no corrosion of tray storage area or trays.

External:

The following components were noted to be cracked, most likely from freezing conditions:
a. Overflow float chamber

Recommendations for East and West Deaerators:

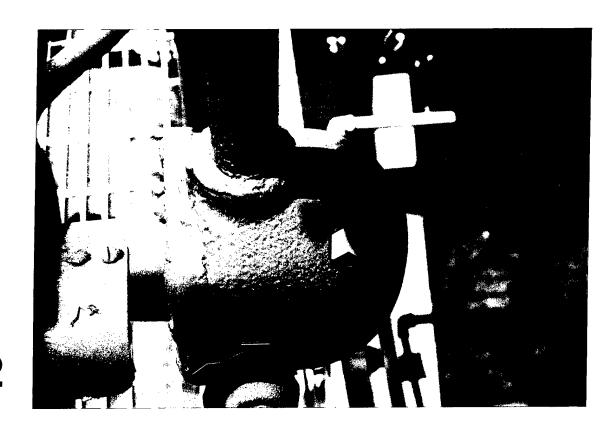
- Remove all internal deposits, recommended method high pressure water.
- 2) Perform wet fluorescent magnetic particle examination of all internal weld joints to identify any cracking that may have developed during the years of operation.
- 3) The depth of pitting in the storage section is a concern the pitting should be measure and compared to the original thickness to identify the current MAWP.
- 4) The storage section shell and heads should be measured for thickness to determine the extent of thinning from corrosion to determine the current MAWP.
- 5) Repair of replace both safety valves
- NOTE: These vessels should not be placed into operation until the current conditions as indicated in the Recommendations Section are performed.

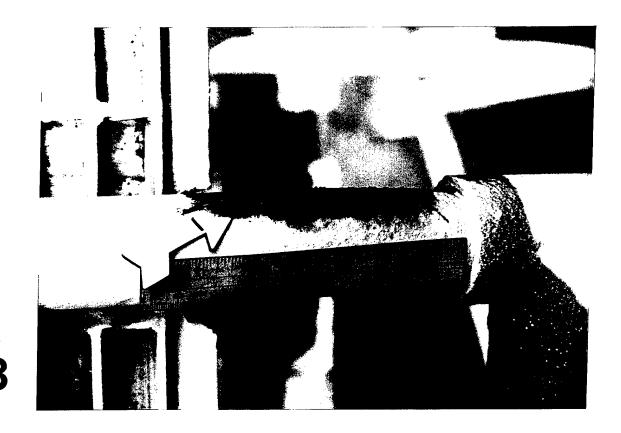
APPENDIX H DEAERATING TANK PICTURES

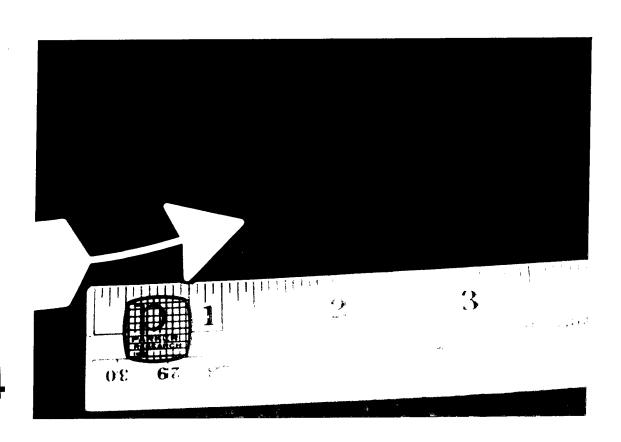
Deaerating Feed Tank Photograph Log

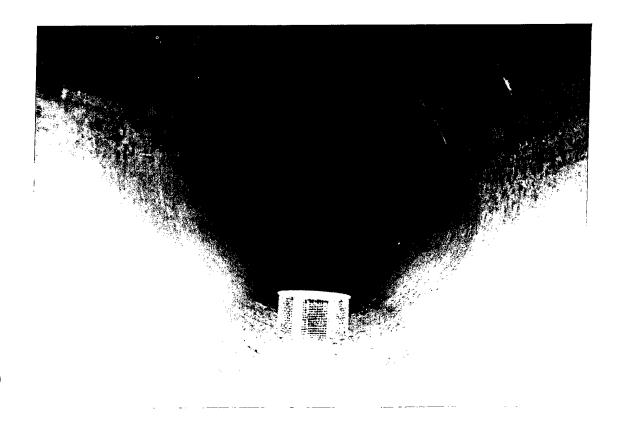
Photograph #	<u>Description</u>
1	West DA tank. Crack in overflow float chamber
2	East DA tank. Crack in float chamber of liquid level control.
3	East DA tank. Crack and rust on piping
4	Typical of both DA tanks. Notice the pitting adjacent to the weld joint. The depth of the pitting is of concern due to the thickness of the shell $(1/4")$.
5	Typical of both DA tanks. Notice the extent of corrosion on the bottom half of the vessel. Additionally, notice the heavier concentration of corrosion and sediment at the water line.











NSTALLATION AND L	Y 19 <u>96</u> MILITARY (Q 4, PRO	JECT T	ITLE		10U.1995
HOLSTON A Kingspor	RMY AMMUNITH	EC EC	:1P	NEW	800 b	he Boile
ROGRAM ELEMENT	6. CATEGORY CODE	7. PROJECT NU	MBER	8. PROJE	CT COST (S	0001
	9. C	OST ESTIMATES				
	ITEM		υ/м	QUANTITY	UNIT	COST (\$000)
STOH	W. C					362.5
DESIGN						30.0
TOTAL						420.0

10. DESCRIPTION OF PROPOSED CONSTRUCTION

INSTALL ONE 800 bhp (27,000 LB/HR) NATURAL GAS
FIRED 100 PSIG OPERATING PRESSURE STEAM
BOILER AND PACKAGED DEAERATING HEATER/FEEDPUMP
SET IN BUILDING 7 - ACETIC ANHYDRIDE MANUFACT
TURING. PROPOSED INSTALLATION TO BE AT
GROUND FLOOR LEVEL IN GENERAL PROXIMITY
TO EXISTING HEAT RECOVERY BOILER.

DD FORM 1391

PREVIOUS EDITIONS MAY BE USED INTERNALLY
UNTIL EXHAUSTED

PAGE NO.

FOR OFFICIAL USE ONLY

installation: HOLSTON ARMY AN	
project: INSTALL NATURAL GAS	FIRED BOILER
project number temporary:	
permanent:	category code
point of contact:	
name <u>Scott Shelton</u>	date
title STOHS-EN	phone 423-247-9/// x 347/
	autovon
dfae name	date
title	phone
	autovon
engineer district TONY BATTAGLIA	date
title CF5AM -EN	
4	autovon
other (A-E) name	
title	phone
	autovon
reviewed by: installation facility engineer	
name	date
title	phone
	autovon
approved by:	
macom engineer name	date
title	
	autovon

project development brochure, PDB-1

DA FORM 5020-R, Feb 82

facility

HOLSTON ARMY AMMUNITION PLANT

project coordinator for using service

SCOTT SHELTON SIOHS-EN

MAAP - ARMY

functional requirements summary, PDB-1

OBJECTIVE

THE OBJECTIVE OF THIS PROJECT IS

TO IMPROVE THE OPERATING CAPABILITY

OF THE EXISTING STEAM PRODUCTION

SYSTEM AT LOW PRODUCTION RATES WHILE

STILL MAINTAIN ING FACILITIES CAPABLE

OF BEING RETURNED TO SERVICE WITHIN A

SHORT TIME FRAME PURSUANT TO SUPPLYING

ANY INCREASED PRODUCTION DEMANDS.

BUILDINGS SERVED

BLDG / ADMINISTRATION

BLOG. IA GAURD HOUSE

BLDG. 2 ACID CONCENTRATION BLDG.

BLDG.4 ELECTRICAL INSTR. SHOP

BLDG. 5 REFRIGERATION PLANT

B CDG. 6 ACOTIC ANHYDRIDO ROFINING

BLDG. 7 ACETIC ANHYDRIDE MANUFACTURING

BLDG. 9 WATER PLANT

BLDG. 11 PUMP House

BLDG.14 CHANGE HOUSE

BLDG. 15 STOREHOUSE

BIDG. 16 FIREHOUSE

BLDG. 18 RED CROSS

functional requirements summary, PDB-1

BUILDINGS SERVED (CONT.)

BLDG. 20 ACETIC ANHYDRIDE FURNACES

BLDG. 27A OFFICE

BLDG. 27B OFFICE

BLDG. 31 CHANGEHOUSE

TANK HEATING AND PIPELINE TRACING

SOLUTION

PROVIDE 800 bhp NATURAL GAS FIRED

FIRETUBE STEAM BOILER TO DELIVER

SATURATED STEAM AT 100 PSIG TO THE

EXISTING STEAM DISTRIBUTION PIPING

SYSTEM, NEW BOILER TO BE INSTALLED

IN SPACE AVAILABLE IN EXISTING

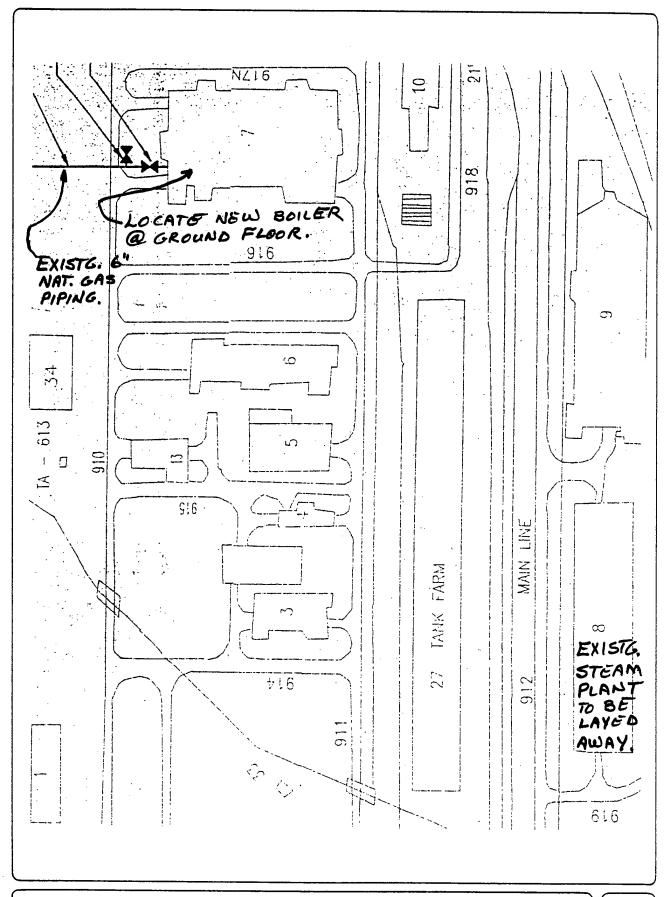
BUILDING T. EXISTING COAL FIRED STEAM

BOILERS AND BOILER AUXILIARIES WILL

BE "LAYED AWAY" FOR FUTURE REACTIVATION.

functional requirements summary, PDB-1

DA FORM 5020-2-R, Feb 82



facilities requirements sketch, PDB- $\frac{1}{2}$

DA FORM 5022-R, Feb 82

TM 5-800-3

A-21

A. SPECIAL CONSIDERATIONS

	ITEM	Requir Not Re	To Be Detern	Comm	Docum Attach
A-1	Cost estimates for each primary and supporting facility	R	D		
A-2	Telecommunications system coordination with USACC and authorization for exceptions	NR			
A-3	Coordination with state and local governmental requirements (blind vendors, medical facilities, construction and operating permits, clearinghouse ecoordination, etc.)	NR			
A-4	Assignment of airspace	NR			
A-5	Economic analysis of alternatives	R	D		
A-6	Approval for new starts	NR			
A-7	International balance of payments (IBOP) coordination with U.S. European command and NATO—overseas cost estimates and comparables (include rate of exchange used in estimates)	NR			
A-8	Impact on historic places—on site survey by authorized archeologist and coordination with state historic preservation officer and advisory council on historic preservation	NR			
A-9	Exceptions to established criteria	NR			
A-10	Coordination with various staff agencies (Provost Marshall-physical security, etc.)	NR			
A-11	Identification of related or support projects (so projects can be coordinated)	NR			
A-12	Required completion date	R	A		

REQUIRED OR NOT REQUIRED — Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

TO BE DETERMINED — Information needed but not currently available. Enter code for information source.

COMMENT ATTACHED — Significant information summarized or explained and attached.

DOCUMENT ATTACHED — Significant information is in an existing document which is attached.

*BY WHOM (Check and insert appropriate letter)

- A OFAE
- B Using Service
- C Construction Service
- D Designer
- E Other (Check Comments Attached and explain)

documentation checklist

DA FORM 5023-A-R, Feb 82

B. SITE DEVELOPMENT

E	B. SITE DEVELOPMENT		* ined	ant ed	ent
	ITEM	Required or Not Required	To Be * Determined	Comment Attached	Document Attached
8-1	Consultation with the District Office to determine and evaluate flood plain hazards	NR			
B-2	Preparation, submission, and/or approval of new General Site Plan	MR			
(B)	Annotated General Site Plan	NR		-,	
(c)	Sketch Site Plan	NR			
(0)	Facilities Requirements Sketch	NR			
8-3	Preparation of				
(A)	Site Survey	NR			
(B)	Subsoil information	NR	-	-	
8-4	Approval by Department of Defense Explosive Safety Board (DDESB) for Safety Site Plan	NR	1		
	Other Site Development Considerations (List and number items)				

REQUIRED OR NOT REQUIRED - Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

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COMMENT ATTACHED - Significant information summarized or explained

DOCUMENT ATTACHED - Significant information is in an existing document which is attached.

*BY WHOM (Check and insert appropriate letter)

- A DFAE
- B Using Service
- C Construction Service
- D Designer
- E Other (Check Comments Attached and explain)

documentation checklist

DA FORM 5023-B-R, Feb 82

C. ARCHITECTURAL & STRUCTURAL

	ITEM	Requir Not Re	To Be Detern	
C-1	Reconciliation with troop housing programs and requirements	NR		ĺ
C-2	Evaluation of existing facilities (including degree of utilization)	R	Δ	ĺ
C-3	Approval for removal and relocation of existing useable facilities	NR		ĺ
C-4	Evaluation of off-post community facilities	NR		ĺ
C-5	Storage and maintenance facilities (including nuclear weapons)	NR		ĺ
C-6	Coordination hospitals, medical and dental facilities with Surgeon General	NR		ĺ
C-7	Coordination of aviation facilities with FAA	NR		ĺ
C-8	Coordination air traffic control and navigational aids with USACC	NR		ĺ
C-9	Tabulation of types and numbers of aircraft	NR		ĺ
C-10	Evaluation of laboratory, research and development, and technical maintenance facilities	NR		١
C-11	Coordination chapels with Chief of Chaplains	NR		ĺ
C-12	Review food service facilities by USATSA	NR		١
C-13	Automated data processing system or equipment approvals—cost analysis when ADP and/or communication centers not co-located with related facilities	NR		
C-14	Coordination postal facilities with U.S. Postal Service Regional Director	NR		1
C-15	Laundry and dry cleaning facilities coordination with ASD(I&L)	NR		١
C-16	Tenant facilities coordination with installation where sited		B	l
C-17	Facilities for or exposed to explosions, toxic chemicals, or ammunition—review by DDESB (See also Item B-4)		NB	
C-18	Analysis of deficiencies	NR		i
C-19	Consideration of alternatives	R	A/B	l
C-20	Determination whether occupants will Include physically handicapped or disabled persons	NR		
C-21	As-build drawings for alterations or additions	NR R NR	AIB	
C-22	Availability of Standard Design or site adaptable designs	NR		l
	Other Architectural & Structural (List and number items)			

REQUIRED OR NOT REQUIRED — Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

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documentation checklist

DA FORM 5023-C-R, Feb 82

Comment

D. MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS

	ITEM	Require Not Rec	To Be Determ	Comme	Docume
D-1	Fuel considerations and cost comparison analysis		D		
D-2	Energy requirements appraisal (ERA)	R			
D-3	Conformance with DOD Energy Reduction requirements	R	0		
D-4		R	0		
1	Evaluation of existing and/or proposed utility systems Other Mechanical and Utility Systems (List and number items)	RRR	D		
			1]	
l				l	1

REQUIRED OR NOT REQUIRED — Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

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documentation checklist

DA FORM 5023-D-R, Feb 82

E. ENVIRONMENTAL CONSIDERATIONS

	ITEM	Require Not Rec	To Be Determ	Comme Attache	Docume
E-1	Environmental impact assessment	NR			
E-2	EIA conclusions require Environmental Impact Statement	NR			
E-3	Determination of health, environmental or related hazards. Assistance to determine existence of any health, environmental or related hazard may be requested from Aberdeen Proving Ground, MD 21010, the Office of the Surgeon General, Attn: DASG-HCH (Army Environmental Hygiene Agency)	NR			
E-4	Air/water pollution permit, coordination with agencies and compliance with standards at Federal, state and local level	R	В		
E-5	Corrective measures associated with Environmental Impact Statements or assessment—list separately and evaluate.	NR			

REQUIRED OR NOT REQUIRED — Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

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documentation checklist

DA FORM 5023-E-R, Feb 82

A. SPECIAL CONSIDERATIONS

	ITEM	Required Not Req	To Be Determi	Commer Attached	Docume Attached
A-1	Factors of risk, restriction or unusual circumstance expected to increase costs beyond applicable area averages	NR			
A-2	Construction phasing requirements	NR			
A-3	Functional support equipment (mechanical, electrical, structural, and security) to be built in	NR			
A-4	Equipment in place and justification	NR		l	
A-5	Other equipment and furniture (O&MA, OPA) and costs	NR		 	
A-6	Special studies and tests (hazards analyses, compatibility testing, new technology testing, etc.)	NR			
A-7	Type of construction (permanent, temporary, semi-permanent)	NR NR NR R	A		
A-8	Government furnished equipment (quantities, procurement time, availability and special handling and storage requirements). Funds used for procurement.	NR			
	Other special considerations (list and number items)				

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technical data checklist

DA FORM 5024-A-R, Feb 82

B. SITE DEVELOPMENT

		Requ	a E	men	imer ched
	site access and preferred construction routes Airfield clearance, explosive storage, working hours, safety, etc Facilities and/or functions or adjoining areas (structures, materials, impact) Real estate actions (acquisition, disposal, lease, right-of-way) Demolition/relocation required (data) Special considerations due to explosives/radioactivity/ chemical contamination/asbestos emissions/toxic gases Restrictions on disposal of demolished/relocated material including hazardous waste	Required Not Requ	To Be Determine	Comment Attached	Documen Attached
ł .		NR	\		
	· · · · · · · · · · · · · · · · · · ·	NR]	
		NR			
B-2 Real estate acti	ons (acquisition, disposal, lease, right-of-way)	NR			
B-3 Demolition/rel	ocation required (data)				
(A) Special cons	siderations due to explosives/radioactivity/ ntamination/asbestos emissions/toxic gases	R	B		
(8) Restrictions including ha	on disposal of demolished/relocated material azardous waste	R	В		
		NR			
B-5 Landscape cons	siderations	10			
(A) Protection of	of existing vegetation	NR	ļ	<u> </u>	
(B) Stockpile t	topsoil	NR			
Other Site Dev	relopment (List and number items)				

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technical data checklist

C. ARCHITECTURAL & STRUCTURAL

=		2 8	Be erm	ache	ache
	ITEM	Require Not Re	To Be Determ	Comme	Docum
C-1	Vibration-producing equipment requiring isolation	NR			
C-2	Seismic zone and other design load criteria (typhoon, hurricane, earthquake loads, high or low loss potential)	NR			
C-3	Protective shelter evaluation and resistant design criteria (conventional/nuclear blast and radiation, chemical/biological)	NR			
C-4	Unusual foundation requirements (pier, pile, caisson, deep foundations, mat, special treatment, permafrost areas, soil bearing)	NR			
C-5	Designation and strength of units to be accommodated	NR			l
C-6	Requirements and data for special design projects	NR	<u></u>		
C-7	Unusual floor and roof loads (safes, equipment)	NR	1		l
C-8	Security features (arms rooms, vaults, interior secure areas)	NR	.		

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technical data checklist

DA FORM 5024-C-R, Feb 82

D. MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS

	ITEM	Requir Not Re	To Be Detern	Comm	Docum Attach
D-1	Special mechanical requirements or considerations (elevator, crane, hoist, etc.)	NR			
D-2	Special peak usage periods and peak leveling techniques	NR			
D-3	Maintenance considerations (accessibility of equipment, compatibility with existing equipment)	R	D		
D-4	Plumbing—availability, general system type and characteristics (proposed and/or existing, incl. compressed air and gas)	NR	1		
D-5	Heating—availability, general system type and characteristics (proposed and/or existing)	NR			
D-6	Ventilating, air condition/refrigeration—availability, general system type and characteristics (proposed and/or existing)	R	D		
D-7	Electrical—availability, general system type and characteristics incl. airfield lighting, communication, etc. (proposed and/or existing)	R	D		
D-8	Water supply/waste treatment—availability, general system type and characteristics (proposed and/or existing)	RRNR	D		
D-9	Energy requirements/fuel conversion (sources, availability, loads, types of fuel, etc.)	R	a		
D-10	Solar energy evaluation	NR			

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technical data checklist

DA FORM 5024-D-R, Feb 82

E. ENVIRONMENTAL CONSIDERATIONS ITEM E-1 | Waste water treatment, air quality, and solid waste disposal criteria Other Environmental Considerations (List and number items)

REQUIRED OR NOT REQUIRED — Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

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technical data checklist

DA FORM 5024-E-R, Feb 82

Required or Not Required F. FIRE PROTECTION To Be * Determined Document Attached Comment Attached **ITEM** NR F-1 Special fire protection systems or features (detection and suppression equipment, hazards, etc.) Other Fire Protection Considerations (List and number items)

REQUIRED OR NOT REQUIRED — Not relevant or no information to communicate. Enter "R" if item is relevant and is required for this project. Enter "NR" if item is irrelevant and is not required for this project.

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 - 8 Using Service
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technical data checklist

DA FORM 5024-F-R, Feb 82

installation: HOLSTON ARMY 1	AMMUNITION PLANT
project: INSTALL NATURAL GAS !	FIRED BOILER
project number temporary:	program year <u>FY 96</u>
permanent:	
point of contact:	
name <u>Scott</u> SHELTON	
title SIOHS-EN	_ phone <u>423-247-9/// x 347 /</u>
	autovon
dfae name	date
title	
	autovon
engineer district TONY BATTAGLIA	
titleCESAM -EN	•
title CBSAMI-ER	
other (A-E)	autovon
name	date
title	phone
	autovon
to and have	
reviewed by: installation facility engineer	
	date
title	phone
	autovon
approved by:	
approved by: macom engineer	data
name	
title	
	autovon

project development brochure, PDB-2

DA FORM 5021-R, Feb 82

facility

HOLSTON
ARMY AMMUNITION
PLANT

project coordinator for using service

SCOTT SHELTON SIOHS-EN

MAAP- ARMY

detailed functional requirements, PDB-2

DA FORM 5021-1-R, Feb 82

TM 5-800-3

OBJECTIVE

THE OBJECTIVE OF THIS PROJECT IS

TO IMPROVE THE OPERATING CAPABILITY

OF THE EXISTING STEAM PRODUCTION

SYSTEM AT LOW PRODUCTION RATES WHILE

STILL MAINTAINING FACILITIES CAPABLE

OF BEING RETURNED TO SERVICE WITHIN

A SHORT TIME FRAME PURSUANT TO

SUPPLYING ANY INCREASED PRODUCTION DEMAND.

SOLUTION

PROVIDE 800 bhp NATURAL GAS
FIRED STEAM BOILER TO DELIVER
SATURATED STEAM AT 100 PSIG TO THE
EXISTING STEAM DISTRIBUTION PIPING
SYSTEM. NEW BOILER TO BE INSTALLED
IN SPACE AVAILABLE IN EXISTING
BUILDING 7. EXISTING COAL FIRED STEAM
BOILERS AND BOILER AUXILIARIES WILL
BE "LAYED AWAY" FOR FUTURE REACTIVATION.

detailed functional requirements, PDB-2

DA FORM 5021-2-R, Feb 82

background information

PRODUCTION OF RESEARCH DEVELOPMENT EXPLOSIVE (RDX), FOLLOWING THE MINIMAL CURRENT PRODUCT DEMAND, IS AT A LOVEL LOW FROUGH TO DICTATE WASTEFUL OPERATING PRACTICES TO AVOID VIOLATIONS OF AIR POLLUTION REGULATIONS AT THE EXISTING COAL FIRED STEAM BOILERS. IT HAS BEEN NECESSARY TO RELEASE STEAM TO ATMOS-PERE WHILE OPERATING ONE OF THE EXISTING SEVEN BOILERS AT ITS LOWEST SAFE OPERATING COMBUSTION RATE. THIS PROJECT WILL ELIMINATE THE NEED FOR EMPLOYING THIS WASTEFUL PRACTICE, AND WILL PROVIDE A PROPERLY SIZED BOILER, THUS PERMITTING OPERATION AT LOADS CONDUCING TO MAXIMIZING EFFICIENCIES.

detailed functional requirements, PDB-2

THREE OTHER METHODS FOR RESOLVING
THE STEAM PLANT OPERATING DILEMMA WERE
CONSIDERED, BUT EACH OF THEM WAS FOUND
TO BE EITHER ECONOMICALLY OR OPERATIONALLY UNSOUND.

THE PROBABLE \$362500 CONSTRUCTION

COST AND THE ONE-TIME \$250,000 COST TO

LAYUP EXISTING BLDG. 8 STEAM PLANT

WILL SAVE 277,200 MILLION BTU'S ADDUCTY

AT CURRENT RDX PRODUCTION RATE, AND

WILL REDUCE MAINTENANCE AND OVERHEAD

COSTS SIGNIFICANTLY. AN OPTIMISTIC

EVALUATION OF MAINTENANCE AND OVERHEAD

SAUINGS WILL RESULT IN SAUINGS TO

INVESTMENT RATIO OF 10.70. A MORE

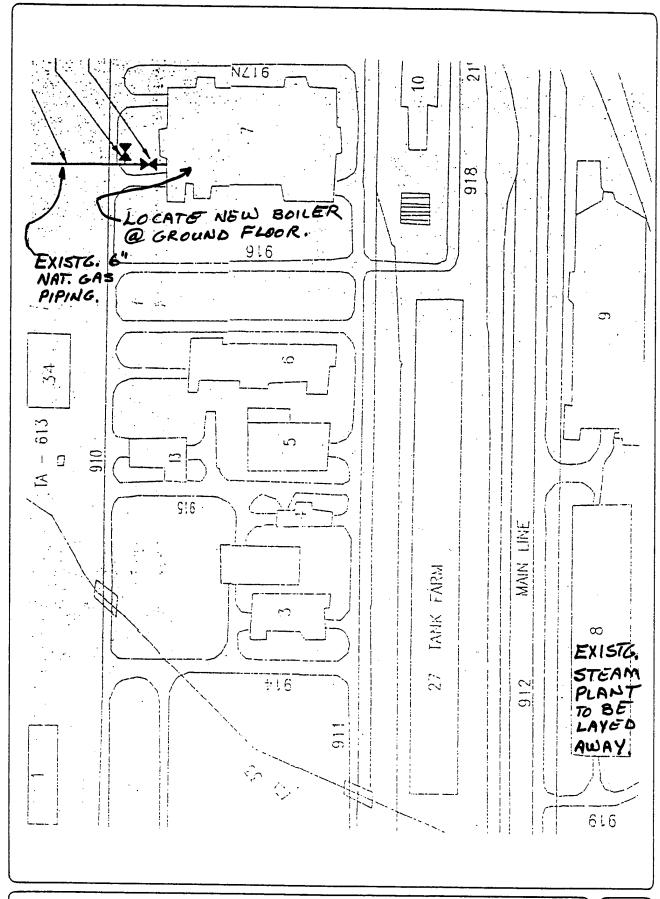
CONSERVATIVE VALUE STILL PRODUCES

AN SIR OF 4.78, WHILE A PESSIMISTIC

APPROACH STILL WILL PRODUCE ECIP

QUALIFYING RESULTS.

detailed functional requirements, PDB-2



facilities requirements sketch, PDB- ½

DA FORM 5022-R, Feb 82

TM 5-800-3

A. SPECIAL CONSIDERATIONS

	ITEM	Requ Not F	Tò Be Deter	Comr	Docu
A-1	Cost estimates for each primary and supporting facility	R	D		
A-2	Telecommunications system coordination with USACC and authorization for exceptions	NR			
A-3	Coordination with state and local governmental requirements (blind vendors, medical facilities, construction and operating permits, clearinghouse ecoordination, etc.)	NR			
A-4	Assignment of airspace	NR			
A-5	Economic analysis of alternatives	R	D		
A-6	Approval for new starts	NR			.
A-7	International balance of payments (IBOP) coordination with U.S. European command and NATO—overseas cost estimates and comparables (include rate of exchange used in estimates)	NR			
A-8	Impact on historic places—on site survey by authorized archeologist and coordination with state historic preservation officer and advisory council on historic preservation	NR			
A-9	Exceptions to established criteria	NR			
A-10	Coordination with various staff agencies (Provost Marshall-physical security, etc.)	NR			
A-11	Identification of related or support projects (so projects can be coordinated)	NR			
A-12	Required completion date	R	A		.

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A - OFAE

B - Using Service

C - Construction Service

D - Designer

E — Other (Check Comments Attached and

documentation checklist

C-

B. SITE DEVELOPMENT

			, ninec	ent ed	ed
	ITEM	Required o	To Be , Determined	Comment Attached	Document Attached
B-1	Consultation with the District Office to determine and evaluate flood plain hazards	NR			
B - 2	Preparation, submission, and/or approval of new	71.0			
(A)	General Site Plan	MR	L		
(B)	Annotated General Site Plan	NR			
(c) L	Sketch Site Plan	NR			
(0)	Facilities Requirements Sketch	NR	_		
8-3	Preparation of				
(A)	Site Survey	NR	}		
(8)	Subsoil information	NR			-
B-4	Approval by Department of Defense Explosive Safety Board (DDESB) for Safety Site Plan	NR			

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documentation checklist

DA FORM 5023-B-R, Feb 82

C. ARCHITECTURAL & STRUCTURAL

	ITEM
C-1	Reconciliation with troop housing programs and requirements
C-2	Evaluation of existing facilities (including degree of utilization)
C-3	Approval for removal and relocation of existing useable facilities
C-4	Evaluation of off-post community facilities
C-5	Storage and maintenance facilities (including nuclear weapons)
C-6	Coordination hospitals, medical and dental facilities with Surgeon General
C-7	Coordination of aviation facilities with FAA
C-8	Coordination air traffic control and navigational aids with USACC
C-9	Tabulation of types and numbers of aircraft
C-10	Evaluation of laboratory, research and development, and technical maintenance facilities
C-11	Coordination chapels with Chief of Chaplains
C-12	Review food service facilities by USATSA
C-13	Automated data processing system or equipment approvals—cost analysis when ADP and/or communication centers not co-located with related facilities
C-14	Coordination postal facilities with U.S. Postal Service Regional Director
C-15	Laundry and dry cleaning facilities coordination with ASD(I&L)
C-16	Tenant facilities coordination with installation where sited
C-17	Facilities for or exposed to explosions, toxic chemicals, or ammunition—review by DDESB (See also Item 8-4)
C-18	Analysis of deficiencies
C·19	Consideration of alternatives
C-20	Determination whether occupants will Include physically handicapped or disabled persons
C-21	As-build drawings for alterations or additions
C-22	Availability of Standard Design or site adaptable designs
	Other Architectural & Structural (List and number items)

NAN SERVEN SERVEN S REquired or SERVEN SERVE	To Be * Determined	Comment Attached	Document Attached
NR			
R	D		
NR			
	B		
	B A/B A/B		
NR			
R	A/B		
NR			
NR R NR NR	AIB		
NR	ļ		

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documentation checklist

D. MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS

D-1 Fuel considerations and cost comparison analysis D-2 Energy requirements appraisal (ERA) D-3 Conformance with DOD Energy Reduction requirements D-4 Evaluation of existing and/or proposed utility systems Other Mechanical and Utility Systems (List and number items)	Waliec Not Required Determined	Commen Attached Documer	Attached
	el considerations and cost comparison analysis		7
	ergy requirements appraisal (ERA)		_
	nformance with DOD Energy Reduction requirements		
Other Mechanical and Utility Systems (List and number items)	eluation of existing and/or proposed utility systems		

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documentation checklist

DA FORM 5023-D-R, Feb 82

E. ENVIRONMENTAL CONSIDERATIONS

	ITEM	Require Not Rec	To Be Determi	Comme	Docume
		NR	<u> </u>	0 4	_
E-1	Environmental impact assessment EIA conclusions require Environmental Impact Statement	NR			
E-2 E-3	Determination of health, environmental or related hazards. Assistance to determine existence of any health, environmental or related hazard may be requested from Aberdeen Proving Ground, MD 21010, the Office of the Surgeon General, Attn: DASG-HCH (Army Environmental Hygiene Agency)	NR			
E-4	Air/water pollution permit, coordination with agencies and compliance with standards at Federal, state and local level	R	В		
E-5	Corrective measures associated with Environmental Impact Statements or assessment—list separately and evaluate.	NR			
	Other environmental considerations (list and number items)				

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documentation checklist

DA FORM 5023-E-R, Feb 82

(E) (C) (C) (C) (C) (C) (C) (C) (C) (C) (C	Site access and preferred construction routes Site restrictions (airfield clearance, explosive storage, etc.) Existing facilities/functions on adjoining areas (structures, materials, impact) Disposal areas (trash, excavated material, constraints) Borrow and spoil areas Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding)	RAZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZ	B/C To Be Determined	Comment	Document Attached
(A) (E) (C) (E) (F) (C) (I) (J)	Site access and preferred construction routes Site restrictions (airfield clearance, explosive storage, etc.) Existing facilities/functions on adjoining areas (structures, materials, impact) Disposal areas (trash, excavated material, constraints) Borrow and spoil areas Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR NR			
(E) (C) (C) (C) (C) (C) (C) (C) (C) (C) (C	Site restrictions (airfield clearance, explosive storage, etc.) Existing facilities/functions on adjoining areas (structures, materials, impact) Disposal areas (trash, excavated material, constraints) Borrow and spoil areas Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR NR		· — —	
	Site restrictions (airfield clearance, explosive storage, etc.) Existing facilities/functions on adjoining areas (structures, materials, impact) Disposal areas (trash, excavated material, constraints) Borrow and spoil areas Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR NR	B/c B/C		
(F) (1) (1) (1) (1) (1) (1) (1) (1) (1) (1	Existing facilities/functions on adjoining areas (structures, materials, impact) Disposal areas (trash, excavated material, constraints) Borrow and spoil areas Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR	B/C		
(E (F (C) (I) (J)	D) Disposal areas (trash, excavated material, constraints) Borrow and spoil areas F) Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR	B/c	· — —	
(F (C) (I) (J)	Borrow and spoil areas Grades or contours existing Existing trees, turf, ground cover, landscape development, erosion control Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR			
	Existing trees, turf, ground cover, landscape development, erosion control H) Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR NR NR			Į.
	H) Bridges and fences (applicable design criteria) Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location	NR			
	Railroads (routing, sidings, docks, yards, grounding) Fire station and security police location			. – –	
	Fire station and security police location		:	- — —	
11-	_			· — —	
(+	Site utilities—capacity and quantity available to project (sanitary and storm	NR		· 	
11 —	sewers, drainage ditches, water and gas service, communication lines, hydrants and sprinklers, etc.)	NR			
(L	L) New facilities clearly identified	NR	1		
(6	Necessary support facilities required for complete functional project (ware-house, igloo, fuel storage, waste treatment, etc.)	R	BIC		
C-4 B-2	Subsoil conditions (actual or expected—groundwater, permafrost, etc.)	NR			
B-2 B-3	Real estate actions (acquisition, disposal, lease, right-of-way)	NR			
B-3 B-4	4 Demolition/relocation required to clear site (date)	NR			
B-4 B-5	5 Pavement types and requirements	-			
	A) Design loading and use frequency by type of paving	NR			ĺ
(E	B) Street size and layout (traffic control)	NR			
	C) Parking lots (signage, etc.)	NR	11		
(t	D) Sidewalks and curbs (handicapped, etc.)	NR	11	'	
(E	E) Gutters, culverts and other drainage factors	NR			
(F	F) Runways, aprons and taxiways	NR			
	G) Tie-down anchors or grounds	NR	.		
——— I——	H) Special surface conditions réquired	NR			
D-9, B-6	6 Energy conservation siting and features (wind solar, etc.). See also DDC Item D-13 (D) & (E)	NR			

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*BY WHOM (Check and insert appropriate letter)

- A DFAE
- B Using Service
- C Construction Service
- D Designer
- E Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-B-1-R, Feb 82

See Tech. Data Checklist	B. SITE DEVELOPMENT (Continued)	Required or Not Required	To Be • Determined	Comment Attached	Document Attached
Item	ITEM	No Re	To	Con	Doc
B-5 B-7 (A)	Landscape treatment Preservation of existing features	NR			
(B)	Proposed planting (low maintenance species, locations away from power lines, etc.)	NR			
B-5 B-8	Storm drainage (See also Item E-4)				
(A)	Total run-off area affecting project	NR			
(B)	Design intensity for floods	NR			
(c)	Design of storm drainage system to include pick-up system and outfall lines	NR			
B-9	Consideration of Coastal Zone Management Act (PL 92-583, 1972; Amendment PL 94-370, 1976)	NR			

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D - Designer

E — Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-B-2-R, Feb 82

See Fech. Data Checklist		C. ARCHITECTURAL & STRUCTURAL	Required or Not Required	To Be * Determined	Comment Attached	Document Attached
Item		ITEM	Requ	To B Dete	Comi	Docu
	C-1	Material availability limitations (include fill and paving)	NR			
	C-2	Architectural style (existing, planned or desired, use of pre-engineered buildings considered)	NR			
C-7	C-3	Floors (type, finish, special loading, subgrade moisture control, low maintenance types particularly in spill areas)	NR			
C-3	C-4	Walls	NR			
	(A)	Exterior (materials, sealing of joints, general maintenance)	NR			
	(B)	Interior walls and partitions (material, finish, fire resistance, subgrade moisture control)	NR			
	C-5	Ceilings (height, finish, acoustics)	NR			
	C-6	Windows (type, size, special treatment)	NR			
	C-7	Doors (type, size, power operation, panic hardware, durability)	NR			
	C-8	Hardware (finish, location, special metal restrictions, durability)	NR			
	C-9	Special finishes (protective coatings, non-sparking, conductive, acid-resistant)	NR			
C-8	C-10	Security features (windows, doors, hardware, construction of walls, floors & ceilings, arms rooms, vaults, etc.)	NR			
	C-11	Sound attenuation requirements (expected and required levels, location)	NR			
	C-12	Stairs, elevators and chutes (location, size, type of usage)	NR			<u> </u>
	C-13	Loading docks and canopies	NR			
C-1	C-14	Vibration-producing equipment requiring isolation	NR			
C-4	C-15	Unusual foundation requirements (pier, pile, caisson, deep foundations, mat, special treatment, creep control)	NR			
	C-16	Span or unusual clearance requirements (span or height)	NR			
	C-17	Special bay sizes (reflect access dimensions)	NR			
	C-18	Overhead support requirements (hoists, cranes)	NR	<u> </u>		
C-7	C-19	Roof loads and requirements (live/dead loads, materials, access, low maintenance features like exterior drains, etc.)	NR			ļ
	C-20	Structural specialities (slabs, sumps, trenches, pits)	NR			
C-2	C-21	Seismic zone design criteria Area wind loads (summer/winter prevailing wind, hurricane, typhoon)	NR	ļ		
-C-2	C-22 C-23		NR	ļ		
	(A)	Protective shelter evaluation and resistant design criteria Explosive/nuclear blast (protective, resistive, suppressive, venting and contain-				
	\^'	ment structures)	NR			
	(B)	Radiation protection (type of radiation, intensity, source)	NR			
	(C)	Chemical/biological protection	NR			

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E - Other (Check Comments Attached and explain)

design data checklist

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DA FORM 5025-C-1-R, Feb 82

E-11

See Tech. Data Checklist		C. ARCHITECTURAL & STRUCTURAL (Continued)	Required or Not Required	To Be *	Comment Attached	Document Attached
item		ITEM	R _e	To	Con	Doc
C·5	C-24	Designation and strength of units to be accommodated	NR			
C-6	C-25	Requirements for special design projects	NR			
	C-26	Safety features (occupant load, maximum travel distance to exits, hazard to be controlled or eliminated)	NR NR			
	C-27	Special design features for handicapped. Other Architectural and Structural (list and number items)	NR			

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design data checklist

DA FORM 5025-C-2-R, Feb 82

See Tech. Data Checklist	D. MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS	Required or Not Required	To Be * Determined	Comment Attached	Document Attached
Item	ITEM	Req.	To B Dete	Com	Docu
D-1	D-1 Special mechanical requirements or considerations	R	D		
D-2	D-2 Special peak usage periods and peak leveling techniques	NR			
D-3	D-3 Maintenance considerations (equipment room size, layout, location, general accessibility of equipment, compatibility with existing equipment.)	R	D		
D-9	D-4 Energy monitoring control system (EMCS) and permanent utilities metering	NR			
D-4	D-5 Plumbing system (proposed and/or existing)	NR			
D-4	D-5 Plumbing system (proposed and/or existing) (A) General piping and storage system (1) Materials (galvanized, copper, etc.) (2) Insulation (3) Natural or LP gas (4) Venting (5) Distilled water (6) Compressed air (7) Hospital & surgical gases (8) Other (chemical, fuel) (B) Facility water supply (C) Garbage disposal (D) Sanitary drainage system (E) Grease interception (F) Chemical waste drainage & disposal (incl. explosive process waste) (G) Radioactive waste (H) Drinking fountains (I) Water treatment (J) Emergency fixtures (showers, eyewash fountains) D-6 Heating system (A) Existing generation plant (1) Location and distance from new facility (2) Equipment (type, age, fuel, etc.) (3) Current loads (average, peak, reserves for this and other projects, load leveling system) (4) Type of plant (5) Manning & support requirements	NR	B B B B B		
	(6) Pollution controls (7) Type of product		B B		

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D - Designer

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design data checklist

DA FORM 5025-D-1-R, Feb 82

See Tech. Data Checklist	D. N	MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS (Continued)	Required or Not Required	To Be • Determined	Comment Attached	Document Attached
Item		ITEM	Rec	To	Corr Atta	Doc Atta
D-5	D-6	Heating system (continued)	NR			
1	(B)	Requirements for proposed facility	1			
	(i)	Type of system	1			
	(2)	Heat load requirements (special temperature demands)	11			
	(3)	Controls, metering & EMCS requirements	1			
	(4)	Distribution system (valves, steam pressure, fluid temperature)	1		.	
	(5)	Corrosion control	 	1		
1	(6)	Insulation	ļ .	1		
	(7)	Additional equipment specifications	V	ļ		
D-6	D-7	Ventilating/air conditioning/refrigeration system				
	(A)	Existing facilities	NR			
	(1)	Location	 			
	(2)	Type of plant (refrigeration, chilled water, etc.)	ļ.,ļ.,	1		
	(3)	Current loads (average, peak, reserves for this and other projects, load leveling system)				
	(4)	Type of product (CFM, temperature, GPM, etc.)		1		
	(5)	Distribution system	1.1			
	(6)	Special filtration requirements	1.1	1		
	(7)	Special humidity, ventilation, or temperature requirements	1.1	1		
	(8)	Security restrictions for open ducting		1		
	(9)	Freezers or coolers	Α	1	1	
	(B)	Requirements for proposed facility	R	P		
	(1)	Type of system		P		
İ	(2)	Temperature, humidity and vent conditions special to this design	NR	1		
	(3)	Control, cycling, metering and EMCS requirements	NP			
	(4)	Distribution (length of extension, location, fluid temperature)	NR NR			
	(5)	Corrosion control	NR]	1
	(6)	Insulation		D]	
	(7)	Special fire and security considerations for this project	NR			.
1	(8)	Occupancy hours and days per week	NR			
D-5,	D-8	Heat and chilled water distribution system	NR		_	
D-6	(A)	Heat system	-	.		
	(1)	Type of service		.	.	
	(2)	Existing system components	.	.		.
	(3)	Valving and sectionalizing requirements	\ .	.		.
	(4)	Allowable shut-down of service for main connections	 .	.		.
	(5)	Sizing for future facilities	 '7	-L	.	.

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C - Construction Service

D -- Designer

E — Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-D-2-R, Feb 82

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D - Designer

E — Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-D-3-R, Feb 82

See Tech. Data Checklist		D. N	MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS (Continued)		Required or Not Required		To Be Determined	Comment	ned	Document Attached
Item			ITEM		Req		To B Dete	Com	Attac	Docu Attac
D-7	l	D-9	Electrical system (continued)			T				
		(U)	Other special power requirements (traffic control, antenna, etc.)		NR				_ _	
		(V)	Applicability of task lighting considerations	1	NR	-			_ -	
		(w)	Power management and metering requirements	•	NR	-				
		D-10	Electrical Distribution		NR				_ -	
	Н	(A)	Actual & estimated loads (peak & average (KW demand))			-				
		(B)	Utility compnay distribution system (substations, transmission lines, rate schedule, etc.)				·			
		(C)	Government owned distribution system (switching station, transmission lines, feeders, etc.)			-				
		(D)	Estimated impact of proposed equipment installation on power factor, load balance and costs for corrective action proposed							
	ll	(E)	Overhead/underground (voltage, conductor size, grounding, etc.)		_L_					
		(F)	Estimated power demand factor and diversity factor						_ _	
		(G)	Power quality requirements (voltage and frequency regulation)	L		_			_	
		(H)	Power to intrusion, detection alarm systems around perimeter	L	V	_ _			_	
		D-11	Airfield lighting requirements		NR	_ _		l	_ _	
		(A)	Area & location to be served	Į. ļ	-4-	- -		l	_ _	
		(B)	Source of power (normal & emergency)	١.	- -	- -			_ -	
	П	(C)	Vault requirements	┨.	-	- -		<u> </u>	_ -	
		(<u>a</u>)	Primary feeders		-	- -		l — .	_ -	
		(E)	Control cabling		-	- -		l — -	- -	
		(F)	Runway lighting (centerline, edge, distance markers, intensity control)		-	- -			- -	
		(G)	Threshold, approach, & strobe beacon lighting		-	- -		l — -	- -	
		(H)	Visual approach slope indicators (VASI)	١.	-	- -			- -	
		(1)	Obstructions lighting/barrier markers	┨.	-	- -	- -		- -	
		(K)	Taxiway edge lighting Helipad/heliport lighting (perimeter, landing direction, hoverlane, etc.)	- 	- 4 -	- -			- -	
D-8		D-12		·	NR	-		— ·	-	
D-0		(A)	Water supply system Source (commercial, well, storage, etc.)	1 :		-		 	-	
		(B)	Average rate of supply (FPD at PSI) Current & Future	┨ :	 - -	- -		 	- -	
		(C)	Treatment requirements	┨ :	 -	- -		-	- -	
	1	(0)	Existing system components (type, size, capacity, age, material, location,	1	- - -	- -		-	- -	
			valving, pressure, etc.)		<u> </u>	- -		-	-	- — -

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D — Designer

E — Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-D-4-R, Feb 82

See Tech. Data Checklist	D. N	MECHANICAL, ELECTRICAL, & UTILITY SYSTEMS (Continued)	Required or Not Required	To Be • Determined	Comment Attached	Document Attached
Item		ITEM	R S	De J	Cor	Att
D-8	D-12	Water supply system (continued)	NR			
	(E)	Chemical analysis of water	1 1			
	(F)	Emergency storage requirements	17-			
	(G)	Peak hours of supply (hours & estimated quantity)	T 7			
	(H)	Known minimal requirements of supported function or Government equipment (quantity & quality)				
	(1)	Chemical feeder & piping systems	- -			
	(n)	Corrosion control (existing & planned)				
	(K)	Metering or usage restrictions	-			
	; <u></u>	Location of tie points (available capacity, interruption schedule)	1-1-			
D-8	D-13	Waste water treatment system	NR			
	(A)	Existing system & components (size, capacity, characteristics)	11			
	(1)	Treatment plant	17			ΓI
	(2)	Collector sewers	17			
	(3)	Sewer mains (materials, depth)				
1 1	(4)	Complete treatment — industrial process				
	(5)	Chemical, fuel or oil spill collection facilities	1 .		l	
	(6)	Existing flows (min., avg., peak)	1			
	(7)	Hydraulic capacity	1.			
	(B)	Known/estimated industrial or functional discharges (quantity & quality)	L			
	(C)	Contributory population & per capita contribution	<u> </u>	.	 ,	
	(D)	Proposed system & components	-	.	<u>. </u>	
	(1)	Treatment plant	. 			l l
	(2)	Callection sewers				
	(3)	Lift station	 		ļ <i>.</i>	l l
	(4)	Complete treatment (additions or modifications)	.		.	
	(5)	Chemical, fuel or oil spill collection facilities		.		l
	(6)	Waste water from portable water treatment plant	│	.	.	
	(7)	Projected flows—average or peak	.			
	(8)	By-pass restrictions		.]		
1	(9)	Location of tie points (available capacity, interruption schedule)	-	-		
	(E)	Compliance requirements (federal, state, local)	-	-		
	(F)	National Pollution Discharge Elimination System (NPDES) permit	{ -	-		
	(G)	Corrosion control (existing or planned)	¥.			

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- A DFAE
- 8 Using Service
- C Construction Service
- D Designer
- E Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-D-5-R, Feb 82

D-14 E (A) (1) (2) (3) (4) (5)	nergy Sources Gas systems (LP, natural, special)	Required or Not Require	To Be Determined	Comment Attached
(A) (1) (2) (3) (4)	Gas systems (LP, natural, special)			
(1) (2) (3) (4)				
(2)		R	P	
(3)	Loads and areas served	NR		
(4)	Source of gas & type of service	NR.		
	Supply pressure average	NR		
151	Heating valve & type of gas (BTU per cubic foot)	NR		
1 (2/ 1	Valving & sectionalizing criteria	R	D	
(6)	Pressure regulation — reduction stations	NR		
(7)	Existing lines, pumping stations, pressurization, base system	NR		
(8)	Control & metering	NR		
(B)	POL systems	1,		
(1)	Fuel (primary or standby source, grade and analysis)	R	D	
(2)	Storage (tank size, location, type, number of storage days)	R	D	
(3)	Areas served	NR	· . •• · · ·	
(4)	Fuel requirements (known, estimated, quantity & type)	110		
	.,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	NR		
. (5)	Distribution system characteristics (piping, types of fuel, pumps, capacities) Ventilation system (Vapor Emission Control)	12.2		.
(6)		NP		
(7)	Safety specifications	NR		
(8)	Filter separators	NR		
(C) -	Coal systems	NR		
(1)	Storage (location & capacity)			
(2)	Source of supply (primary & emergency)	, !		
(3)	Type, energy value, analysis (i.e. sulfur, ash, etc.)	!		l
(D)	Solar energy systems	NR	··	ļ —
(1)	Building heating, air conditioning, domestic hot water			 .
(2)	Heating process water	1.4		1
(3)	Collector type & location	1.1	1	
(4)	Liquid, chemical or rock storage	1.1	J:	.
(5)	Freeze protection	₩	.	l
(E)	Energy conservation data (U values, orientation, passive solar considerations, etc.)	NR		1

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A - DFAE

8 - Using Service

C - Construction Service

D - Designer

E - Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-D-6-R, Feb 82

See Tech. Data Checklist	E	E. ENVIRONMENTAL CONSIDERATIONS	Required or Not Required	To Be • Determined	ment :hed	Document Attached
Item		ITEM	Requ Not	To B Dete	Comment Attached	Docu Attac
E-1	E-1	Water quality	NR			
	(A)	Waste water treatment management program (PL 92-500 & PL 95-217)				
	(B)	Water quality criteria & standards (federal, state and local)				
	(c)	Treatment requirements coordinated with EPA				
	(a)	Facilities to be installed to meet regulatory agency criteria	4			
E-1	E-2	Air quality	L			
	(A)	Applicable air quality criteria (federal, state and local; PL 95-95 and Clean Air Act Amendment of 1977)	R	D		
	(B)	Action taken to comply with requirements	R	B		
	(c)	Type & amount of pollutants generated	R R NR	B		
	(0)	Results of proposed abatement measures	NR		l:	
	(E)	Existing control equipment & monitoring procedures	R	B		
E-1	E-3	Solid waste disposal	MR			
	(A)	Applicable solid waste criteria (federal, state and local)				
	(B)	Waste volume generated (type & characteristics)	$\perp I_{-}I_{-}$		l	
1	(C)	Method of disposal (land fill and availability of land, leachate, etc.)	L_L_	<u> </u>		
]	(D)	Disposition of recyclable materials for reuse or as combustion fuel	_ L _	<u></u>		
	(E)	Impact on installation recycling programs	1		l	<u> </u>
	E-4	Effects of terrain changes (such as excavations, roadways, drainage structures, etc.)	NR			
	(A)	Measures to control erosion	NR			<u></u>
E-1	E-5	Treatment of hazardous material	NR	<u> </u>	l	
	(A)	Handling and disposal of plychlorinated biphenyls (PCB) in electrical transformers	1			
	(B)	Handling and disposal of asbestos materials				
•	(C)	Handling and disposal of fiberglass products	- -		l	
Ī	(0)	Storage of fuels and solvents				
	(E)	Coordination with installation spill control plans	4			
		Other Environmental Considerations (list and number items)				

TO BE DETERMINED — Information needed but not currently available. Enter code for information source.

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design data checklist

DA FORM 5025-E-R, Feb 82

See Tech. Data Checklist		F. FIRE PROTECTION	Required or Not Required	To Be • Determined	Comment Attached	Document Attached
Item		ITEM	R _e	To Det	Con	Doc
F-1	F-1	General design guidance	NR			
	(A)	Occupancy type (see NFPA 101, Chap 4)				
	(B)	Water supply characteristics (existing or planned extensions) (capacity, pump activation, storage tanks and pumps, etc.)	AB			
	(C)	Mobile fire apparatus (response distance/time)	III			
	(a)	Fire detection and alarm systems (existing or planned, type, location, etc.)				
	(E)	Automatic suppression systems (water sprinkler, CO ₂ , foam etc.—existing or planned				
	(F)	Hazard of contents (low, ordinary, high-see NFPA 101; type—explosives, flam-mable/toxic chemicals, radioactive materials)	1			
F-1	F-2	Special fire suppression system requirements	NR			
	(A)	Means of egress	1777			
	(8)	Fire area limitations				
	(C)	Fire walls, partitions, draft curtains	177			
	(Q)	Detection system (type, detectors, supervision, transmitters, annunciators, backup provisions)				
	(E)	Suppression system (damage by water to costly equipment, shut down of operations)	1			
		Other Fire Protection (list and number items)				

TO BE DETERMINED — Information needed but not currently available. Enter code for information source.

COMMENT ATTACHED — Significant information summarized or explained and attached.

DOCUMENT ATTACHED — Significant information is in an existing document which is attached.

*BY WHOM (Check and insert appropriate letter)

- A DFAE
- B Using Service
- C Construction Service
- D Designer
- E Other (Check Comments Attached and explain)

design data checklist

DA FORM 5025-F-R, Feb 82

Appendix 1 - Calculations/Formulas

MICROSOFT EXCEL PREPARATION

- Cells of the spreadsheet used for development of baseline and ECO Energy and Annual Cost Data versus equivalent RDX production rate contain either text, constant values, or formulae. Contents of each cell prior to calculation are presented on the following pages.
- 2. Cells A1 through A156, not reproduced here, contain input text and numerical data, all of which is self explanatory.
- Where cells shown here contain text and discrete numerical values, the text or numbers are input data.
- 4. Explanations for formulae shown in the remaining cells are as follows:

Steam Turbine #/hr: Calculate value from monthly RDX production rate,

pounds steam per pound RDX, turbine design steam

rate per horsepower, and conversion factors.

Steam Average #/hr: Conditional tests to select the greater of product

driven steam demand, turbine steam demand, or

40,000 lbs/hr, using appropriate conversion factors.

Fuel Million Btu/Mo: Conditional test to limit coal fired boilers to minimum

40,000 lbs/hr, otherwise calculate value from steam enthalpy difference, monthly RDX production, pounds steam required per pound RDX, and boiler efficiency.

Annual Fuel Cost: Calculate value from unit fuel cost and calculated

fuel million Btu/mo.

Annual Electrical Cost: Calculate value from assumed electric kWh per

thousand pounds of steam, unit cost per kWh and calculated average steam flow rate, plus electric motor energy for pumps and fans when applicable.

Annual Maintenance Cost: Calculated value from assumed fixed value, assumed

variable rate, and calculated steam production rate.

Annual Overhead Cost: Calculated value from assumed fixed value, assumed

variable rate, and calculated steam production rate.

Total Annual Cost: Summation of individually calculated annual costs.

	В
1	
2	
	\$/MILL.
	BTU
	1.86
	1.86
	1.86
	1.86
	1.86
	1.86
	1.86
	1.86
13	
14	
	FUEL MILL.
	BTU/MO
	=IF(F5=40000,(C5-100)*40000*730*100/(G5*1000000),(C5-100)*A5*D5*100/G5)
18	=IF(F6=40000,(C6-100)*40000*730*100/(G6*1000000),(C6-100)*A6*D6*100/G6)
19	=IF(F7=40000,(C7-100)*40000*730*100/(G7*1000000),(C7-100)*A7*D7*100/G7)
20	=(C8-100)*A8*D8*100/G8
	=(C9-100)*A9*D9*100/G9
	=(C10-100)*A10*D10*100/G10
	=(C11-100)*A11*D11*100/G11
24	=(C12-100)*A12*D12*100/G12
25	
26	
27	
	\$/MILL.
	BTU
	1.86
	1.86
	1.86
	1.86
—	1.86
	1.86
	1.86
	1.86
38	
39	
	FUEL MILL.
	BTU/MO
	=IF(F30=40000,(C30-100)*40000*730*100/(G30*1000000),(C30-100)*A30*D30*100/G30)
43	=IF(F31=40000,(C31-100)*40000*730*100/(G31*1000000),(C31-100)*A31*D31*100/G31)
44	=IF(F32=40000,(C32-100)*40000*730*100/(G32*1000000),(C32-100)*A32*D32*100/G32)
	=(C33-100)*A33*D33*100/G33
	=(C34-100)*A34*D34*100/G34
	=(C35-100)*A35*D35*100/G35
48	=(C36-100)*A36*D36*100/G36
	=(C37-100)*A37*D37*100/G37

	В
50	
51	
52	
53	
	\$/MILL.
55	BTU
	3.95
	3.95
	1.86
-	1.86
	1.86
	1.86
	1.86
	1.86
64	
65	
	FUEL MILL.
	BTU/MO
	=(C56-100)*A56*D56*100/G56
	=(C57-100)*A57*D57*100/G57
	=(C58-100)*A58*D58*100/G58
71	=(C59-100)*A59*D59*100/G59
	=(C60-100)*A60*D60*100/G60
73	=(C61-100)*A61*D61*100/G61
74	=(C62-100)*A62*D62*100/G62
75	=(C63-100)*A63*D63*100/G63
76	
77	
78	
	\$/MILL.
	ВТИ
	3.95
	3.95
	3.95
	3.95
	3.95
86	3.95
	3.95
88	1.86
89	
90	
	FUEL MILL.
92	BTU/MO
93	=(C81-100)*A81*D81*100/G81
	=(C82-100)*A82*D82*100/G82
	=(C83-100)*A83*D83*100/G83
96	=(C84-100)*A84*D84*100/G84
	=(C85-100)*A85*D85*100/G85
98	=(C86-100)*A86*D86*100/G86

	В
99	=(C87-100)*A87*D87*100/G87
100	=(C88-100)*A88*D88*100/G88
101	
102	
103	
	\$/MILL.
	BTU
	3.95
	3.95
	3.95
	3.95
110	3.95
	3.95
	3.95
	1.86
114	
115	
	FUEL MILL.
	BTU/MO
118	=(C106-100)*A106*D106*100/G106
119	=(C107-100)*A107*D107*100/G107
120	=(C108-100)*A108*D108*100/G108
121	=(C109-100)*A109*D109*100/G109
122	=(C110-100)*A110*D110*100/G110
123	=(C111-100)*A111*D111*100/G111 =(C112-100)*A112*D112*100/G112
124	=(C113-100)*A113*D113*100/G113
126	
127	
128	
129	
130	
	\$/MILL.
132	вти
	3.95
	3.95
135	
136	
137	FUEL MIL.
138	BTU/MO
139	=(C133-100)*A133*D133*100/G133
140	=(C134-100)*A134*D134*100/G134
141	
142	
143	
144	
145	
146	

	В
147	\$/MILL.
148	BTU
	3.95
150	3.95
151	
152	
153	FUEL MIL.
154	BTU/MO
	=(C149-100)*A149*D149*100/G149
156	=(C150-100)*A150*D150*100/G150

	С
1	
2	
3	STEAM
4	BTU/#
5	1290.2
6	1290.2
7	1290.2
8	1290.2
9	1290.2
10	1290.2
11	1290.2
12	1290.2
	1290.2
13	
	A & (S M 1 A 1
15	ANNUAL
16	FUEL COST
17	=B5*B17*12
18	=B6*B18*12
19	=B7*B19*12
	=B8*B20*12
21	=B9*B21*12
22	=B10*B22*12
23	=B11*B23*12
24	=B12*B24*12
25	
26	
07	
27	
28	STEAM
	STEAM BTU/#
28	
28 29	BTU/#
28 29 30 31 32	BTU/# 1290.2
28 29 30 31 32 33	BTU/# 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34	BTU/# 1290.2 1290.2 1290.2
28 29 30 31 32 33	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36 37	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36 37 38	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36 37 38	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36 37 38 39 40	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36 37 38 39 40 41	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2
28 29 30 31 32 33 34 35 36 37 38 39 40 41 42	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1E90.2 1290.2
28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 ANNUAL FUEL COST =B30*B42*12 =B31*B43*12
28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 ANNUAL FUEL COST =B30*B42*12 =B31*B43*12 =B32*B44*12
28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 ANNUAL FUEL COST =B30*B42*12 =B31*B43*12 =B32*B44*12 =B33*B45*12
28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 ANNUAL FUEL COST =B30*B42*12 =B31*B43*12 =B32*B44*12 =B33*B45*12 =B34*B46*12
28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47	BTU/# 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 1290.2 ANNUAL FUEL COST =B30*B42*12 =B31*B43*12 =B32*B44*12 =B33*B45*12 =B34*B46*12 =B35*B47*12

	С
50	
51	
52	
53	
	0.75
	STEAM
55	BTU/#
56	1290.2
57	1290.2
58	1290.2
59	1290.2
60	1290.2
61	1290.2
62	1290.2
63	1290.2
64	
65	
66	ANNUAL
67	FUEL COST
68	=B56*B68*12
69	=B57*B69*12
70	=B58*B70*12
71	=B59*B71*12
72	=B60*B72*12
73	=B61*B73*12
74	=B62*B74*12
75	=B63*B75*12
76	
77	
78	
79	STEAM
80	BTU/#
81	1204
82	1204
83	1204
84	1204
85	1204
86	1204
87	1204
88	1290.2
89	
90	
91	ANNUAL
92	FUEL COST
93	=B81*B93*12
	=B82*B94*12
	=B83*B95*12
96	=B84*B96*12
97	=B85*B97*12
98	=B86*B98*12
	1 200 200 .2

	С
99	=B87*B99*12
100	=B88*B100*12
101	
102	
103	
	STEAM
	BTU/#
	1204
	1204
	1204
	1204
	1204
111	1204
112	1204
113	1290.2
114	1290.2
115	
	ANINILIAI
	ANNUAL
	FUEL COST
	=B106*B118*12
	=B107*B119*12
	=B108*B120*12
	=B109*B121*12
	=B110*B122*12 =B111*B123*12
	=B112*B124*12
	=B112 B124 12 =B113*B125*12
126	-B113 B123 12
127	
128	
129	
130	
_	STEAM
_	BTU/#
133	1187.2
134	1187.2
135	
136	
137	ANNUAL
138	FUEL COST
	=B133*B139*12
	=B134*B140*12
141	
142	
143	
144	
145	
146	
<u>. ,,,</u>	

	С
147	STEAM
148	BTU/#
149	1187.2
150	1187.2
151	
152	
	ANNUAL
154	FUEL COST
	=B149*B155*12
156	=B150*B156*12

	D
1/	
2	
	# STEAM
	PER #RDX
	110
	85
	65
	42
	33
	20.5
	13
	11.5
13	
14	
	ANNUAL
	ELECT. COST
	=2.8*0.035*F5*8760/1000
	=2.8*0.035*F6*8760/1000
	=2.8*0.035*F7*8760/1000
	=2.8*0.035*F8*8760/1000
	=2.8*0.035*F9*8760/1000
	=2.8*0.035*F10*8760/1000
	=2.8*0.035*F11*8760/1000
24_	=2.8*0.035*F12*8760/1000
2	
26	
27	
28	# STEAM
	PER #RDX
30	110
31	85
32	65
33	42
34	
	20.5
36	
37	11.5
38	
39	
	ANNUAL
	ELECT. COST
	=2.8*0.035*F30*8760/1000+(F30/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
43	=2.8*0.035*F31*8760/1000+(F31/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
	=2.8*0.035*F32*8760/1000+(F32/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
	=2.8*0.035*F33*8760/1000+(F33/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
	=2.8*0.035*F34*8760/1000+(F34/100000)*700*0.035*0.748*8760+0.035*1000*0.748*8760
	=2.8*0.035*F35*8760/1000+(F35/100000)*700*0.035*0.748*8760+0.035*2000*0.748*8760
484	8*0.035*F36*8760/1000+(F36/100000)*1050*0.035*0.748*8760+0.035*3000*0.748*8760
49	.8*0.035*F37*8760/1000+(F37/100000)*1400*0.035*0.748*8760+0.035*3000*0.748*8760

	D
50	
51	
52	
53	
	# STEAM
	PER #RDX
	110
57	
58	
59	
60	
	20.5
62	13
63	11.5
64	
65	
	ANNUAL
	ELECT. COST
68	=2.8*0.035*F56*8760/1000+(F56/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
69	=2.8*0.035*F57*8760/1000+(F57/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
70	=2.8*0.035*F58*8760/1000+(F58/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
71	=2.8*0.035*F59*8760/1000+(F59/100000)*350*0.035*0.748*8760+0.035*1000*0.748*8760
72	=2.8*0.035*F60*8760/1000+(F60/100000)*700*0.035*0.748*8760+0.035*1000*0.748*8760
_	=2.8*0.035*F61*8760/1000+(F61/100000)*700*0.035*0.748*8760+0.035*2000*0.748*8760 8*0.035*F62*8760/1000+(F62/100000)*1050*0.035*0.748*8760+0.035*3000*0.748*8760
74	
75	-2.8°0.035 F63 8760/1000+(F63/100000) 1400 0.033 0.748 8700+0.033 3000 0.740 0700
76	
77	
78	
	# STEAM
	PER #RDX
81	=(1290.2-100)/(1204-100)*D5-(F5*20.6*350/100000)/(A81*1000000) =(1290.2-100)/(1204-100)*D6-(F6*20.6*350/100000)/(A82*1000000)
82	=(1290.2-100)/(1204-100) D6-(F6 20.6 350/100000)/(A62 1000000) =(1290.2-100)/(1204-100)*D7-(F7*20.6*350/100000)/(A83*1000000)
	=(1290.2-100)/(1204-100)*D8-(F8*20.6*350/100000)/(A84*1000000)
	=(1290.2-100)/(1204-100)*D9-(F9*20.6*350/100000)/(A85*1000000)
	=(1290.2-100)/(1204-100)*D10-(F10*20.6*350/100000)/(A86*1000000)
	=(1290.2-100)/(1204-100)*D11-(F11*20.6*350/100000)/(A87*1000000)
	11.5
89	
90	
91	ANNUAL
92	ELECT. COST
	=0.95*0.035*F81*8760/1000+0.035*200*0.748*8760
	=0.95*0.035*F82*8760/1000+0.035*200*0.748*8760
	=0.95*0.035*F83*8760/1000+0.035*200*0.748*8760
96	=0.95*0.035*F84*8760/1000+0.035*200*0.748*8760
97	
98	95*0.035*F86*8760/1000+0.035*200*0.748*8760

D
9 0.95*0.035*F87*8760/1000+0.035*200*0.748*8760
100-2.8*0.035*F88*8760/1000+(F88/100000)*1400*0.035*0.748*8760+0.035*3000*0.748*8760
101
102
103
104 # STEAM
105 PER #RDX
106 =(1290.2-100)/(1204-100)*D30-(F30*20.6*350/100000)/(A106*1000000)
107 =(1290.2-100)/(1204-100)*D31-(F31*20.6*350/100000)/(A107*1000000)
108 = (1290.2-100)/(1204-100)*D32-(F32*20.6*350/100000)/(A108*1000000)
109 = (1290.2-100)/(1204-100)*D33-(F33*20.6*350/100000)/(A109*1000000)
110 =(1290.2-100)/(1204-100)*D34-(F34*20.6*350/100000)/(A110*1000000)
111 =(1290.2-100)/(1204-100)*D35-(F35*20.6*350/100000)/(A111*1000000)
112 =(1290.2-100)/(1204-100)*D36-(F36*20.6*350/100000)/(A112*1000000)
113 11.5
114
115
116 ANNUAL
117 ELECT. COST
118 = 0.95*0.035*F106*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760
119 =0.95*0.035*F107*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760
120 = 0.95*0.035*F108*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760
121 =0.95*0.035*F109*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760 122 =0.95*0.035*F110*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760
1 0.95*0.035*F111*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760 1 0.95*0.035*F111*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760
124 ≤ 0.95*0.035*F112*8760/1000+0.035*200*0.748*8760+0.035*1350*0.748*8760
125 = 2.8*0.035*F113*8760/1000+(F113/100000)*1400*0.035*0.748*8760+0.035*3000*0.748*8760
126
127
128
129
130
131 # STEAM
132 PER #RDX
133 =(1290.2-100)/(1187.2-100)*D56-(F56*20.6*350/100000)/(A133*1000000)
134 =(1290.2-100)/(1187.2-100)*D57-(F57*20.6*350/100000)/(A134*1000000)
135
136
137 ANNUAL
138 ELECT. COST
139 =0.95*0.035*F133*8760/1000+0.035*75*0.748*8760+0.035*1350*0.748*8760
140 =0.95*0.035*F134*8760/1000+0.035*75*0.748*8760+0.035*1350*0.748*8760
141
142
143
144
145
14

	D
147	# STEAM
148	PER #RDX
149	=(1290.2-100)/(1187.2-100)*D56-(F56*20.6*350/100000)/(A149*1000000)
150	=(1290.2-100)/(1187.2-100)*D57-(F57*20.6*350/100000)/(A150*1000000)
154	
15	
153	ANNUAL
154	ELECT. COST
	=0.95*0.035*F149*8760/1000+0.035*75*0.748*8760+0.035*1350*0.748*8760
156	=0.95*0.035*F150*8760/1000+0.035*75*0.748*8760+0.035*1350*0.748*8760

l	E
15	
-24	
3	STEAM TURB-
	INE #/HR
	=(A5*D5*1000000/100000)*20.6*700/730+35.5*1000
6	=(A6*D6*1000000/100000)*20.6*700/730+35.5*1000
7	=(A7*D7*1000000/100000)*20.6*700/730+35.5*1000
	=(A8*D8*1000000/100000)*20.6*700/730+35.5*1000
	=(A9*D9*1000000/100000)*20.6*1400/730+35.5*1000
10	=(A10*D10*1000000/100000)*20.6*1400/730+35.5*1000
11	=(A11*D11*1000000/100000)*20.6*2100/730+35.5*1000
12	=(A12*D12*1000000/100000)*20.6*2800/730+35.5*1000
13	
14	
15	ANNUAL;
16	MNTNC. COST
17	=37500*12+(0.5*F5*8760/1000)
18	=37500*12+(0.5*F6*8760/1000)
19	=37500*12+(0.5*F7*8760/1000)
	=37500*12+(0.5*F8*8760/1000)
	=37500*12+(0.5*F9*8760/1000)
	=37500*12+(0.5*F10*8760/1000)
23	=37500*12+(0.5*F11*8760/1000)
1 2/1	=37500*12+(0.5*F12*8760/1000)
24	3,000 12 (3,001,123,001,001)
2	
2 26	
26 27	
26 26 27 28	STEAM TURB-
26 27 28 29	STEAM TURB- INE #/HR
26- 27 28 29 30	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730
26 27 28 29 30 31	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730
26 27 28 29 30 31 32	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730
26 27 28 29 30 31 32 33	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730
26- 27 28 29 30 31 32 33 34	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730
2 26 27 28 29 30 31 32 33 34 35	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730
26 27 28 29 30 31 32 33 34 35 36	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730
26 27 28 29 30 31 32 33 34 35 36 37	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730
26 27 28 29 30 31 32 33 34 35 36 37	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730
2 26 27 28 29 30 31 32 33 34 35 36 37 38 39	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1400/730
2 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40	STEAM TURB- INE #/HR =(A30*D30*100000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1400/730 ANNUAL;
26 27 28 29 30 31 32 33 34 35 36 37 38 39 40	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1400/730 ANNUAL; MNTNC. COST
2 26- 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1400/730 ANNUAL; MNTNC. COST =12*37500+(0.5*F30*8760/1000)
2 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A35*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1400/730
2 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A32*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A34*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/10000)*20.6*1050/730 =(A37*D37*1000000/10000)*20.6*1400/730 ANNUAL; MNTNC. COST =12*37500+(0.5*F30*8760/1000) =12*37500+(0.5*F31*8760/1000) =12*37500+(0.5*F32*8760/1000)
2 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45	STEAM TURB- INE #/HR =(A30*D30*100000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A36*D36*100000/100000)*20.6*700/730 =(A36*D36*100000/100000)*20.6*1050/730 =(A37*D37*100000/100000)*20.6*1400/730 ANNUAL; MNTNC. COST =12*37500+(0.5*F30*8760/1000) =12*37500+(0.5*F31*8760/1000) =12*37500+(0.5*F32*8760/1000) =12*37500+(0.5*F33*8760/1000) =12*37500+(0.5*F33*8760/1000)
26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A32*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A34*D35*1000000/100000)*20.6*700/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/10000)*20.6*1050/730 =(A37*D37*1000000/10000)*20.6*1400/730 ANNUAL; MNTNC. COST =12*37500+(0.5*F30*8760/1000) =12*37500+(0.5*F31*8760/1000) =12*37500+(0.5*F32*8760/1000)
2 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47	STEAM TURB- INE #/HR =(A30*D30*1000000/100000)*20.6*350/730 =(A31*D31*1000000/100000)*20.6*350/730 =(A32*D32*1000000/100000)*20.6*350/730 =(A33*D33*1000000/100000)*20.6*350/730 =(A34*D34*1000000/100000)*20.6*700/730 =(A36*D35*1000000/100000)*20.6*700/730 =(A36*D35*1000000/100000)*20.6*1050/730 =(A36*D36*1000000/100000)*20.6*1050/730 =(A36*D37*1000000/100000)*20.6*1050/730 =(A37*D37*1000000/100000)*20.6*1400/730 ANNUAL; MNTNC. COST =12*37500+(0.5*F30*8760/1000) =12*37500+(0.5*F31*8760/1000) =12*37500+(0.5*F33*8760/1000) =12*37500+(0.5*F33*8760/1000) =12*37500+(0.5*F33*8760/1000) =12*37500+(0.5*F33*8760/1000)

55 51. 52	
52 53	
53	
54 STEAM TURB-	
55 INE #/HR	
56 =(A56*D56*1000000/100000)*20.6*350/730	
57 =(A57*D57*1000000/100000)*20.6*350/730	
58 =(A58*D58*1000000/100000)*20.6*350/730	
59 =(A59*D59*1000000/100000)*20.6*350/730	
60 =(A60*D60*1000000/100000)*20.6*700/730	
61 =(A61*D61*1000000/100000)*20.6*700/730	
62 =(A62*D62*1000000/100000)*20.6*1050/730	
63 =(A63*D63*1000000/100000)*20.6*1400/730	
64	
65	
66 ANNUAL;	
67 MNTNC. COST	
68 =12*37500+(0.5*F56*8760/1000)	
69 =12*37500+(0.5*F57*8760/1000)	
70 =12*37500+(0.5*F58*8760/1000)	
71 =12*37500+(0.5*F59*8760/1000)	
72 =12*37500+(0.5*F60*8760/1000)	
73_=12*37500+(0.5*F61*8760/1000)	
7 2*37500+(0.5*F62*8760/1000)	
75 -12*37500+(0.5*F63*8760/1000)	
76	
77	
78	
79 STEAM TURB-	
80 INE #/HR	
81 =(A81*D81*1000000/100000)*20.6*350/730+35.5*1000	
82 =(A82*D82*1000000/100000)*20.6*350/730+35.5*1000	
83 =(A83*D83*1000000/100000)*20.6*350/730+35.5*1000	
84 =(A84*D84*1000000/100000)*20.6*350/730+35.5*1000	
85 =(A85*D85*1000000/100000)*20.6*700/730+35.5*1000	
86 =(A86*D86*1000000/100000)*20.6*700/730+35.5*1000	
87 =(A87*D87*1000000/100000)*20.6*1050/730+35.5*2000	
88 =(A88*D88*1000000/100000)*20.6*1400/730	
89	
90	
91 ANNUAL;	
92 MNTNC. COST	
93 =18750*12+(0.15*F81*8760/1000)	
94 =18750*12+(0.15*F82*8760/1000)	
95 =18750*12+(0.15*F83*8760/1000)	
96 =18750*12+(0.15*F84*8760/1000)	
97 148750*12+(0.15*F85*8760/1000)	
9 8750*12+(0.15*F86*8760/1000)	

E
99 8750*12+(0.15*F87*8760/1000)
100 -12*37500+(0.5*F88*8760/1000)
101
102
103
CO4 STEAM TURB-
105 INE #/HR
106 0
107 0
108 0
109 0
110 0
111 0
112 0 113 =(A113*D113*1000000/100000)*20.6*1400/730
114
116 ANNUAL;
117 MNTNC. COST
118 =18750*12+(0.15*F106*8760/1000)
119 =18750*12+(0.15*F107*8760/1000)
120 =18750*12+(0.15*F108*8760/1000)
121 =18750*12+(0.15*F109*8760/1000)
122 18750*12+(0.15*F110*8760/1000)
12 8750*12+(0.15*F111*8760/1000)
124 =18750*12+(0.15*F112*8760/1000)
125 =12*37500+(0.5*F113*8760/1000)
126
127 128
129
130
131 STEAM TURB- 132 INE #/HR
133 0 134 0
135
136
137 ANNUAL;
138 MNTNC. COST
139 =3750*12+(0.15*F133*8760/1000)
140 =3750*12+(0.15*F134*8760/1000)
141
142
143
144
145
14

	E
147	STEAM TURB-
148	INE #/HR
149	0
150	0
151 15	
	ANNUAL;
154	MNTNC. COST
155	=6250*12+(0.15*F149*8760/1000)
156	=6250*12+(0.15*F150*8760/1000)

	TEAM
	VG.#/HR
	IF(E5<40000,IF(A5*D5*1000000/730<40000,40000,A5*D5*1000000/730),IF(E5>A5*D5*1000000/730,E5,A5*D5*1000000/
6 =	IF(E6<40000,IF(A6*D6*1000000/730<40000,40000,A6*D6*1000000/730),IF(E6>A6*D6*1000000/730,E6,A6*D6*1000000/
7 =	IF(E7<40000,IF(A7*D7*1000000/730<40000,40000,A7*D7*1000000/730),IF(E7>A7*D7*1000000/730,E7,A7*D7*1000000/
8 =	IF(E8<40000,IF(A8*D8*1000000/730<40000,40000,A8*D8*1000000/730),IF(E8>A8*D8*1000000/730,E8,A8*D8*1000000/
9 =	IF(E9<40000,IF(A9*D9*1000000/730<40000,40000,A9*D9*1000000/730),IF(E9>A9*D9*1000000/730,E9,A9*D9*1000000/
10 =	IF(E10<40000,IF(A10*D10*1000000/730<40000,40000,A10*D10*1000000/730),IF(E10>A10*D10*1000000/730,E10,A10*
11 =	IF(E11<40000,IF(A11*D11*1000000/730<40000,40000,A11*D11*1000000/730),IF(E11>A11*D11*1000000/730,E11,A11*
12 =	IF(E12<40000,IF(A12*D12*1000000/730<40000,40000,A12*D12*1000000/730),IF(E12>A12*D12*1000000/730,E12,A12*
13	
14	
	NNUAL
	DVRHD. COST
	70000*12+(0.25*F5*8760/1000)
	70000 12+(0.25 1 5 6760/1000) 70000*12+(0.25*F6*8760/1000)
	70000 12*(0.25*F7*8760/1000)
	70000 12 (0.25 1 7 0700/1000)
	70000 12 (0.25 F 0 0700/1000)
	70000*12+(0.25*F10*8760/1000)
	70000*12+(0.25*F11*8760/1000)
	70000*12+(0.25*F12*8760/1000)
24	
20	
27	
	STEAM
	VG.#/HR
	IF(E30<40000,IF(A30*D30*1000000/730<40000,40000,A30*D30*1000000/730),IF(E30>A30*D30*1000000/730,E30,A30*
31 =	IF(E31<40000,IF(A31*D31*1000000/730<40000,40000,A31*D31*1000000/730),IF(E31>A31*D31*1000000/730,E31,A31*
32 =	IF(E32<40000,IF(A32*D32*1000000/730<40000,40000,A32*D32*1000000/730),IF(E32>A32*D32*1000000/730,E32,A32*
	IF(E33<40000,IF(A33*D33*1000000/730<40000,40000,A33*D33*1000000/730),IF(E33>A33*D33*1000000/730,E33,A33*
34 =	IF(E34<40000,IF(A34*D34*1000000/730<40000,40000,A34*D34*1000000/730),IF(E34>A34*D34*1000000/730,E34,A34*
35 =	IF(E35<40000,IF(A35*D35*1000000/730<40000,40000,A35*D35*1000000/730),IF(E35>A35*D35*1000000/730,E35,A35*
36 =	IF(E36<40000,IF(A36*D36*1000000/730<40000,40000,A36*D36*1000000/730),IF(E36>A36*D36*1000000/730,E36,A36*
37 =	IF(E37<40000,IF(A37*D37*1000000/730<40000,40000,A37*D37*1000000/730),IF(E37>A37*D37*1000000/730,E37,A37*
38	
39	
40 A	NNUAL
	OVRHD. COST
	70000*12+(0.25*F30*8760/1000)
	70000*12+(0.25*F31*8760/1000)
	70000*12+(0.25*F32*8760/1000)
	70000*12+(0.25*F33*8760/1000)
	70000*12+(0.25*F34*8760/1000)
	70000*12+(0.25*F35*8760/1000)
	70000*12+(0.25*F36*8760/1000)
4	0000*12+(0.25*F37*8760/1000)

	F
5	
52	
53	
54	STEAM
55	AVG.#/HR
56	=D56*A56*1000000/730
	=D57*A57*1000000/730
	=D58*A58*1000000/730
	=D59*A59*1000000/730
60	=D60*A60*1000000/730
	=D61*A61*1000000/730
62	=D62*A62*1000000/730
63	=D63*A63*1000000/730
64	
65	
66	ANNUAL
	OVRHD. COST
	=70000*12+(0.25*F56*8760/1000)
	=70000*12+(0.25*F57*8760/1000)
	=70000*12+(0.25*F58*8760/1000)
	=70000*12+(0.25*F59*8760/1000)
	=70000*12+(0.25*F60*8760/1000)
73	=70000*12+(0.25*F61*8760/1000)
7.	(0000*12+(0.25*F62*8760/1000)
75	/0000*12+(0.25*F63*8760/1000)
76	
77	
78	
	STEAM
	AVG.#/HR
	=IF((A81*D81*1000000/100000)*20.6*350/730+35.5*1000>A81*D81*1000000/730,(A81*D81*1000000/100000)*20.6*350/73
82	=IF((A82*D82*1000000/100000)*20.6*350/730+35.5*1000>A82*D82*1000000/730,(A82*D82*1000000/100000)*20.6*350/73
	=IF((A83*D83*1000000/100000)*20.6*350/730+35.5*1000>A83*D83*1000000/730,(A83*D83*1000000/100000)*20.6*350/73
84	=IF((A84*D84*1000000/100000)*20.6*350/730+35.5*1000>A84*D84*1000000/730,(A84*D84*1000000/100000)*20.6*350/73
85	=IF((A85*D85*1000000/100000)*20.6*350/730+35.5*1000>A85*D85*1000000/730,(A85*D85*1000000/100000)*20.6*350/73
86	=IF((A86*D86*1000000/100000)*20.6*350/730+35.5*1000>A86*D86*1000000/730,(A86*D86*1000000/100000)*20.6*350/73
87	=IF((A87*D87*1000000/100000)*20.6*350/730+35.5*1000>A87*D87*1000000/730,(A87*D87*1000000/100000)*20.6*350/73
	=D88*A88*1000000/730
89	
90	
91	ANNUAL
	OVRHD. COST
	=70000*12+(0.25*F81*8760/1000)
	=70000*12+(0.25*F82*8760/1000)
	=70000*12+(0.25*F83*8760/1000)
	=70000*12+(0.25*F84*8760/1000)
	- 70000*12+(0.25*F85*8760/1000)
	0000*12+(0.25*F86*8760/1000)

	F
0	
_	70000*12+(0.25*F87*8760/1000)
16.	70000*12+(0.25*F88*8760/1000)
101	
102	
103	
104	STEAM
105	AVG.#/HR
106	=A106*D106*1000000/730
	=A107*D107*1000000/730
108	=A108*D108*1000000/730
	=A109*D109*1000000/730
	=A110*D110*1000000/730
111	=A111*D111*1000000/730
112	=A112*D112*1000000/730
113	=D113*A113*1000000/730
114	
115	
116	ANNUAL
	OVRHD. COST
118	=70000*12+(0.25*F106*8760/1000)
	=70000*12+(0.25*F107*8760/1000)
	=70000*12+(0.25*F108*8760/1000)
	=70000*12+(0.25*F109*8760/1000)
	=70000*12+(0.25*F110*8760/1000)
1	70000*12+(0.25*F111*8760/1000)
124	=70000*12+(0.25*F112*8760/1000)
	=70000*12+(0.25*F113*8760/1000)
126	
127	
128	
129	
130	
	STEAM
	AVG.#/HR
	=A133*D133*1000000/730
134	=A134*D134*1000000/730
135	
136	
	ANNUAL
	OVRHD. CST
	=35000*12+(0.25*F133*8760/1000)
	=35000 12+(0.25 F133 6760/1000) =35000*12+(0.25*F134*8760/1000)
	-00000 12-\0.20 1 104 0700/1000/
141	
142	
143 144	
145	
1	

	. F	
147 STEAM		
148 AVG.#/HR		
149 =A149*D149*1000000/730		
150 =A150*D150*1000000/730		
151		
15		
153 ANNUAL		
154 OVRHD. CST		
155 =50000*12+(0.25*F149*8760/1000)		
156 =50000*12+(0.25*F150*8760/1000)		

l	G
1	
2	
3	BOILER
4	EFFIC.
5	75
6	75
7	80.7
8	79.5
9	77.2
10	79.2
11	82.1
12	82.9
13	
14	
15	TOTAL
16	ANNUAL COST
17	=C17+D17+E17+F17
18	=C18+D18+E18+F18
19	=C19+D19+E19+F19
20	=C20+D20+E20+F20
21	=C21+D21+E21+F21
22	=C22+D22+E22+F22
23	=C23+D23+E23+F23
24	=C24+D24+E24+F24
25	
26	
27	
28	BOILER
29	EEEIO.
	EFFIC.
30	75
30 31	
31 32	75 75 77.5
31 32 33	75 75 77.5 78.1
31 32 33 34	75 75 77.5 78.1 83.2
31 32 33 34 35	75 75 77.5 78.1 83.2 78.2
31 32 33 34 35 36	75 75 77.5 78.1 83.2 78.2 81
31 32 33 34 35 36 37	75 75 77.5 78.1 83.2 78.2
31 32 33 34 35 36 37 38	75 75 77.5 78.1 83.2 78.2 81
31 32 33 34 35 36 37 38 39	75 75 77.5 78.1 83.2 78.2 81
31 32 33 34 35 36 37 38 39 40	75 75 77.5 78.1 83.2 78.2 81 83.2
31 32 33 34 35 36 37 38 39	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST
31 32 33 34 35 36 37 38 39 40 41 42	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42
31 32 33 34 35 36 37 38 39 40 41 42 43	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42 =C43+D43+E43+F43
31 32 33 34 35 36 37 38 39 40 41 42 43 44	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42 =C43+D43+E43+F43 =C44+D44+E44+F44
31 32 33 34 35 36 37 38 39 40 41 42 43 44 45	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42 =C43+D43+E43+F43 =C44+D44+E44+F44 =C45+D45+E45+F45
31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42 =C43+D43+E43+F43 =C44+D44+E44+F44 =C45+D45+E45+F45 =C46+D46+E46+F46
31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42 =C43+D43+E43+F43 =C44+D44+E44+F44 =C45+D45+E45+F45 =C46+D46+E46+F46 =C47+D47+E47+F47
31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46	75 75 77.5 78.1 83.2 78.2 81 83.2 TOTAL ANNUAL COST =C42+D42+E42+F42 =C43+D43+E43+F43 =C44+D44+E44+F44 =C45+D45+E45+F45 =C46+D46+E46+F46

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	G
50	
51	
52	
53	
54	BOILER
55	EFFIC.
56	77
57	77.9
58	76.8
59	78
60	83.1
61	78
62	
63	82
64	
65	
66	TOTAL
67	ANNUAL COST
68	=C68+D68+E68+F68
69	=C69+D69+E69+F69
70	=C70+D70+E70+F70
71	=C71+D71+E71+F71
72	=C72+D72+E72+F72
73	=C73+D73+E73+F73
74	=C74+D74+E74+F74
75	=C75+D75+E75+F75
76	
77	
78	
79	BOILER
80	EFFIC.
81	78
82	78.5
83	
84	81.8
	82.5
85 86	83.2
87	82 82
88	UZ
89	
90	
91	TOTAL
92	ANNUAL COST
93	=C93+D93+E93+F93
94	=C94+D94+E94+F94
95	=C95+D95+E94+F95
96	=C96+D96+E96+F96
97	=C97+D97+E97+F97
98	=C98+D98+E98+F98

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99 =C99+D99+E99+F99 100 =C100+D100+E100+F100 101 102 103	
100 =C100+D100+E100+F100 101 102	
101 102	
102	
[103]	
104 BOILER	
105 EFFIC.	
106 78	
107 78.5	
108 81	
109 81.8	
110 82.5	
111 83.2	
112 82	
113 82	
114	
115	
116 TOTAL	
117 ANNUAL COST	
118 =C118+D118+E118+F118	
119 =C119+D119+E119+F119	
120 =C120+D120+E119+F120	
121 =C121+D121+E121+F121	
122 = C122+D122+E122+F122	
123 = C123+D123+E123+F123	
124 = C124+D124+E124+F124 125 = C125+D125+E125+F125	
126	
127	
128	
129	
130	
131 BOILER	
132 EFFIC.	
133 84.5	
134 84.5	
135	
136	
137 TOTAL	
138 ANNUAL COST	
139 =C139+D139+E139+F139	
140 =C140+D140+E140+F140	
141	
142	
143	
144	
145	
146	

	G
147	BOILER
148	EFFIC.
149	84.5
150	84.5
151	
152	
153	TOTAL
154	ANNUAL COST
155	=C155+D155+E155+F155
156	=C156+D156+E156+F156



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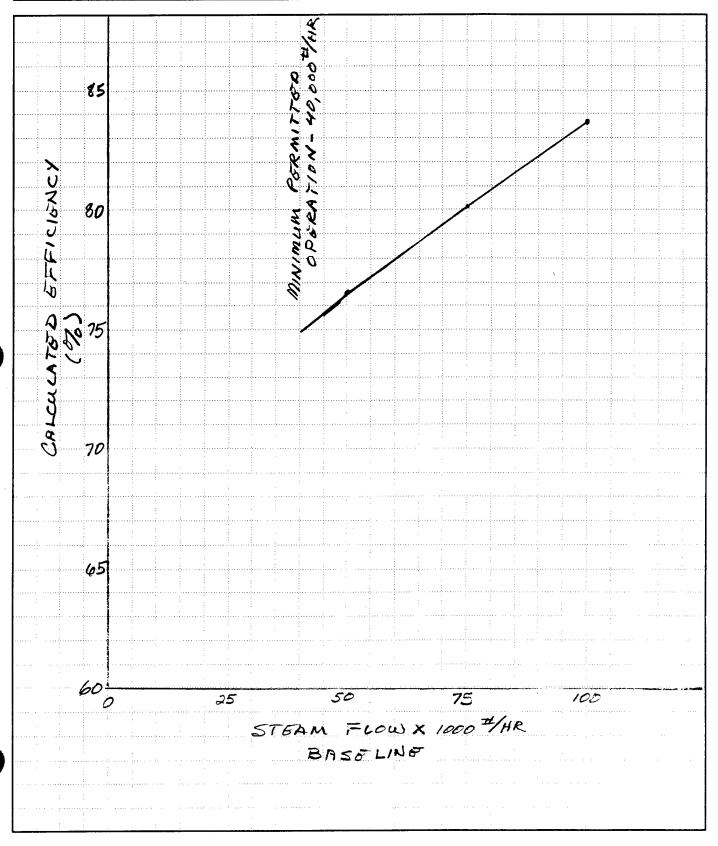
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Sheet No:

Calculations For:

BASELINE CONDITIONS-CASE / \$2 BLR. EFF.



Z - r		N CALCULATIONS 100,0 ES PER 10,000 BTU FUEL INPUT	00 #/HR	٤ ,	Z - r
E			& CASI	5142	Ε
1	TOLLIN CONTENTS OF STREET ON STREET OF STREET			DATE	a
2	ANALYSIS AS FIRED	BY TEST OR SPECIFICATION	8-7	6-75	
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR AIR TEMPERATURE TO HEATER	%		Ь
4	c 74.7 Moisture 2.9			80	٠
5	H ₂ 5, 3 VOLATILE 34.7	AIR TEMPERATURE FROM HEATER	F	375	
6	S 0.7 FIXED CARBON 56.	FLUE GAS TEMPERATURE LEAVING UNIT		0.0132	-
7	0: 8.5 ASH 6, 3	HO PER LO DRI AIR		بيورو الالووي	9
8	N ₂ 1,6	LINIBURDIED ELIEL LOCC	虹	0	5
9	H ₂ O 2.9	UNBURNED FUEL LOSS	~ Z		1:1
10	ASH <u>6.3</u>	UNACCOUNTED LOSS			╁╬┪
	ANU DED IN AS EIDED ALLONG BLA	UNACCOUNTED LOSS RADIATION LOSS (ABA1), FIG. 20, CHAPTER	<i>-</i> /0	1,0,/2	1:-
12	BTU PER LB, AS FIRED, 14000 B/#				
13	QUANTITIES PER	10,000 BTU FUEL INPUT	· · · · · · · · · · · · · · · · · · ·		13
14	4 FUEL BURNED, 10,000 ÷ LINE 12.				14
15	TOTAL AIR REQUIRED, LINE 6 ÷ 100 × VALUE FROM FIG. DOR TABLE 5 OR 6 = 1.7× 7.575 LB //				15
16	19 177				16
17	1 191/2 7/2				17
18	I I I I I I I I I I I I I I I I I I I				18
19	9 H_2O IN FLUE GAS, TOTAL, LINE 16 + LINE 18				19
20	H ₂ O IN FLUE GAS, TOTAL, IN PER CENT, (LINE 19 ÷ LIN	E 17) × 100		3.8	20
21	DRY GAS, TOTAL, LINE 17—LINE 19		LB	13.23	21
22	LOSSES PER 10,000 BTU FUEL INPUT				
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		STU	0	23
24		••••••	вти	250	24
25	RADIATION, 10,000 × LINE j ÷ 100		BTU	. 75	25
26	LATENT HEAT, H ₂ O IN FUEL, 1040 X LINE 18		BTU	374	26
27		@ LINE & AND LINE 20 = 13.76 X 67	ВТО	922	27
1	TOTAL LOSSES, LINES (23 + 24 + 25 + 26 + 27)	•••		1621	28
29	TOTAL LOSSES IN PER CENT, LINE (28 ÷ 10,000) × 100		%	16.21	29
30	5 0276			83.79	30
31	QUANTITIES PER 10,000 BTU FUEL INPUT				
32	HEAT INPUT FROM FUEL		BTU	10000	32
33	HEAT INPUT FROM AIR, LINES (15 + 16) X BTU FROM F		вти		33
34	PTII (ARCO			34	
35			BTU	374_	35
36	1 _			9625	36
37			вти	163	37
38	DEAT AVAILABLE LINE 24 LINE 27		вти	9463	38
39			688		39
40			2500		40

^{*} NOTE: IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM 1/2 TO 1/2 OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

L			000 #/H	FR	1
М	BASED ON QUANTITI	· - · · · · · · · · · · · · · · · ·	LOAD	م است م	N E
E			ASE C	756 14	
1	FUEL- COAL	CONDITIONS		DATE	٥
2	ANALYSIS AS FIRED	BY TEST OR SPECIFICATION	1 8-6	13-75	 -
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR AIR TEMPERATURE TO HEATER	%	238	Ь
4	c 74.7 MOISTURE 2.9			80	<u>.</u>
5	H ₂ 5. 3 VOLATILE 34.7		s	··· 80 ····	1
6	S 0.7 FIXED CARBON 56.	FLUE GAS TEMPERATURE LEAVING UNIT		0,0132	,
7	02 8.5 ASH 6.3	H ₂ O PER LB DRY AIR			g
8	N ₂ /.6	UNBURNED FUEL LOSS	%	م ا	h
9	H ₂ O 2, 9	UNACCOUNTED LOSS	% %	2.5	i
10	ASH <u>6,3</u>	RADIATION LOSS (ABA1), FIG. 20, CHAPTER	7 %	1.00	j
)	BTU PER LB, AS FIRED, 14000			.1	k
13	QUANTITIES PER	10,000 BTU FUEL INPUT			13
14	FUEL BURNED, 10,000 ÷ LINE 12.		LE	0.74	14
	TOTAL AIR REQUIRED, LINE b + 100 X VALUE FROM (FIG.	G. 4 OR TABLE 5 OR 6 = 2.38×7.5	57 5 L	18.03	1:
- 1	H ₂ O IN AIR, LINE 15 × LINE f =			0.24	10
7	1				
18	B H ₂ O IN FUEL, (LINE $5 \div 100$) × LINE 14 × 8.94 + (LINE $9 \div 100$) × LINE 14; OR FROM TABLE 5 LB 0.36			18	
19	H ₂ O IN FLUE GAS, TOTAL, LINE 16 + LINE 18		LI	0.60	19
20	H_2O IN FLUE GAS, TOTAL, IN PER CENT, (LINE 19 \div LIN	NE 17) × 100			
21	DRY GAS, TOTAL, LINE 17—LINE 19		LI	18.38	12
22	LOSSES PER 10,0	000 BTU FUEL INPUT			2:
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		87U	0	2
				250	2.
25	RADIATION, 10,000 X LINE j ÷ 100		BTU	حور	2:
	LATENT HEAT, H2O IN FUEL, 1040 X LINE 18		BTU	374	2
27	SENSIBLE HEAT, FLUE GAS, LINE 17 X BTU FROM FIG. 2	2 @ LINE & AND LINE 20 = 18.98X 67	BTU	1272	2
	TOTAL LOSSES, LINES (23 + 24 + 25 + 26 + 27)		BTU	1996	
29	TOTAL LOSSES IN PER CENT, LINE (28 ÷ 10,000) × 100	0	%	19.96	2
30	EFFICIENCY, BY DIFFERENCE, 100—LINE 29		%	80.04	A^3
31		ER 10,000 BTU FUEL INPUT			3
32	HEAT INPUT FROM FUEL		вти	10000	. 3
33	HEAT INPUT FROM AIR, LINES (15 + 16) X BTU FROM	FIG. 3 @ LINE & TEMP	BTU		_ 3
34	HEAT INPUT, TOTAL, LINES (32 + 33)		BTU	10000	. 3
35	l		BTU	_ 374_	- 3
36	HEAT AVAILABLE, MAXIMUM		BTU	.9626	- 13
37			BTU	_ 175	
38	1		BTU	9451	3
39	1	E 17 BTU	500		3
40	ADIABATIC TEMPERATURE, FROM FIG. 2 FOR LINES 20	8, 39 F	1900		4

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM 1/2 TO 1/2 OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

L	COMBUSTIO	N CALCULATIONS 50 000		L I	
и.	BASED ON QUANTITE	ES PER 10,000 BTU FUEL INPUT LOAL		И	
Ε		BASO CAS	50/42	E	
1	FUEL-	CONDITIONS	DATE	٥	
2	ANALYSIS AS FIRED		-23-9S		
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR 96	285	ь	
4	C MOISTURE	AIR TEMPERATURE TO HEATER F	80	د	
5	H ₂ VOLATILE	AIR TEMPERATURE FROM HEATER F		d	
6	S FIXED CARBON	FLUE GAS TEMPERATURE LEAVING UNIT F	375		
7	O ₂ ASH	H2O PER LB DRY AIR LB	0,0132	f	
8	N ₂		1	g	
9	H ₂ O	UNBURNED FUEL LOSS 9	0	h	
10	ASH	UNACCOUNTED LOSS %	3.0	i	
11		RADIATION LOSS (ABA1), FIG. 20, CHAPTER 7 %		j	
12	BTU PER LB, AS FIRED,			k	
13	QUANTITIES PER	10,000 BTU FUEL INPUT	· • • • • • • • • • • • • • • • • • • •	13	
14	FUEL BURNED, 10,000 ÷ LINE 12	L	0,714	14	
15	FUEL BURNED, 10,000 \div UNE 12. TOTAL AIR REQUIRED, LINE b \div 100 \times VALUE FROM FIG.	5. 4 OR TABLE 5 OR 6 = 2,85x 7.575 LI	21.59	15	
1		Ų		16	
	wet Gas. Total, lines $(14 + 15 + 16)$				
	H ₂ O IN FUEL, (LINE 5 ÷ 100) \times LINE 14 \times 8.94 + (LINE 9 ÷ 100) \times LINE 14; OR FROM TABLE 5 LB 0.36 1			18	
19	H ₂ O IN FLUE GAS, TOTAL, LINE 16 + LINE 18			19	
20				20	
21				21	
22	LOSSES PER 10,000 BTU FUEL INPUT				
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100	вти	Ø	23	
24		вти	300	24	
25		вти	150	25	
26	·	вти	374	26	
27	SENSIBLE HEAT, FLUE GAS, LINE 17 X BTU FROM FIG. 2	@ LINE & AND LINE 20 = 22,58X 67 BTU	<u> 1513</u>	27	
28	TOTAL LOSSES, LINES (23 + 24 + 25 + 26 + 27)	BTU	2337	28	
29	TOTAL LOSSES IN PER CENT, LINE (28 ÷ 10,000) X 100	% }	<i>23.</i> 37	29	
30	EFFICIENCY, BY DIFFERENCE, 100-LINE 29	%	76.63	30	
31		R 10,000 BTU FUEL INPUT TEMPERATURE, ADIABATIC		31	
-		9711	10000	32	
32				33	
33			10000	34	
34			374	35	
35	*********		9625	36	
36			225	37	
37	the second second second second	RTII	9400	⊣ · · · · · ∤	
38		17 RTU 4//0		39	
39				40	
40	ADIABATIC TEMPERATURE, FROM FIG. 2 FOR LINES 20	11030		3	

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM ½ TO ½ OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.



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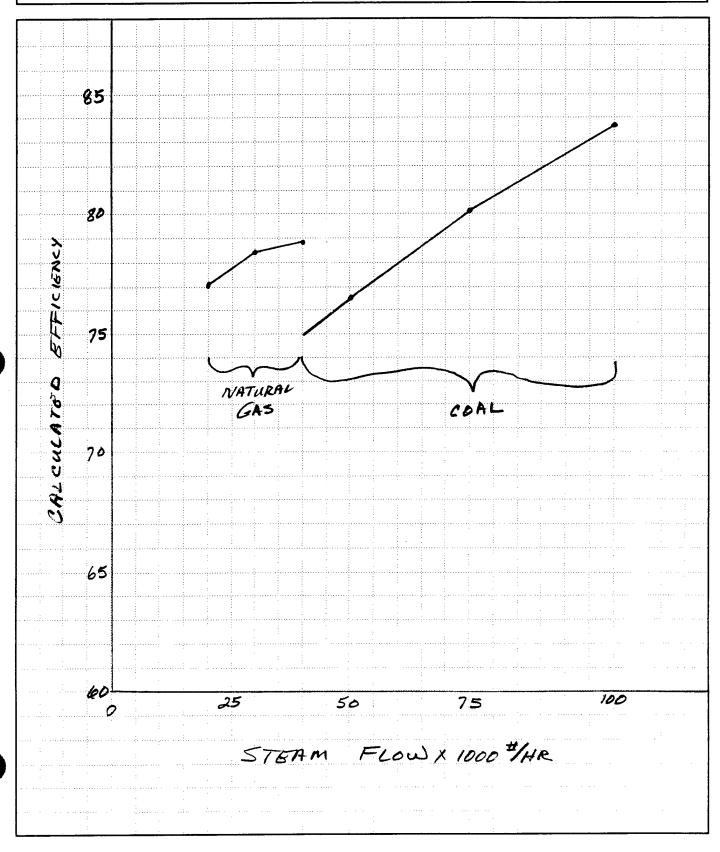
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Sheet No:

Calculations For:

RETROFIT EXISTG. BOILER W/ N.G. BURNOR-CASE 3



			CASE		
L T Z E		N CALCULATIONS S PER 10,000 BTU FUEL INPUT	40,000#/ LOAD RETROFIT É		コースm
1	FUEL— NATURAL GAS CONDITIONS DATE ANALYSIS AS FIRED BY TEST OR SPECIFICATION 9-1-9.				٥
2	ANALYSIS AS FIRED				
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR	%	107.5	ь
4	c 69, 3 MOISTURE	AIR TEMPERATURE TO HEATER	_	80	5
5	H ₂ 22.7 VOLATILE	AIR TEMPERATURE FROM HEATE			.d.
6	S - FIXED CARBON	FLUE GAS TEMPERATURE LEAVIN	NG UNIT	375	•
7	O ₂ — ASH	H2O PER LB DRY AIR	LB	40134	
8	N ₂ 8./				
9	H ₂ O —	UNBURNED FUEL LOSS	% 		
10	ASH —	UNACCOUNTED LOSS	%	3, ک	ļl
11		UNACCOUNTED LOSS RADIATION LOSS (ABA1), FIG. 20,	, CHAPTER 7 %	2.0	اللا
12	BTU PER LB, AS FIRED, 21825				k
13	QUANTITIES PER 10,000 BTU FUEL INPUT				
14	FUEL BURNED, 10,000 ÷ UNE 12.		LE	0.458	14
15	18 7			7.633	15
16	IRIO 1			0.101	16
17	INIT IN THE RESERVE OF THE PARTY OF THE PART			8.192	17
18	8 H ₂ O IN FUEL, (LINE 5 \div 100) \times LINE 14 \times 8.94 $+$ (LINE 9 \div 100) \times LINE 14; OR FROM TABLE 5			18	
19	1			19	
20	H ₂ O IN FLUE GAS, TOTAL, IN PER CENT, (LINE 19 ÷ LINE 17) × 100			20	
	DRY GAS, TOTAL, LINE 17—LINE 19		LI	7.162	21
22					
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		BTU	0	23
24			n T1 1 1	300	24
25				200	25
26	LATENT HEAT, HZO IN FUEL, 1040 X LINE 18	••••••	BTU		26
27	SENSIBLE HEAT, FLUE GAS, LINE 17 X BTU FROM FIG. 2	@ LINE & AND LINE 20 = 8.19	2×78 BTU	440	27
1	TOTAL LOSSES, LINES $(23 + 24 + 25 + 26 + 27)$	U.I.I.	BTU	2106	28
29	TOTAL LOSSES IN PER CENT, LINE $(28 \div 10,000) \times 100$)	%	21.06	29
30	EFFICIENCY, BY DIFFERENCE, 100—LINE 29		%	78,94	30
31	QUANTITIES PE	R 10,000 BTU FUEL INPUT TEMPERATURE, ADIABATIC			31
32			вти	10000	32
33	HEAT INPUT FROM AIR, LINES (15 + 16) X BTU FROM	FIG. 3 @ LINE & TEMP	BTU		33
34				10000	34
35			6711	966	35
- 1				9034	36
36				250	37
37			8111	8784	38
38			RTUI 1677		39
39			F 3400		40
			12/		

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM 1/2 TO 1/2 OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

PA	4	2
レハ	$\boldsymbol{\mathcal{L}}$	

		LA.	500 =	<u> </u>	 ,
L	COMBUSTIO	N CALCULATIONS 30,000	#/HR >		1
7	BASED ON QUANTITE	EC DED 10.000 BTH EHEN INDHIT			И
E		RETROFIT	OXI	316.	E
1	FUEL- NATURAL GAS	CONDITIONS		DATE	٥
2	ANALYSIS AS FIRED	BY TEST OR SPECIFICATION	9	-1-95	
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR	%	07.5	ь
4	C 69.3 MOISTURE	AIR TEMPERATURE TO HEATER	F	80	٢
5	H2 22.7 VOLATILE	AIR TEMPERATURE FROM HEATER	F		d
6	S FIXED CARBON	FLUE GAS TEMPERATURE LEAVING UNIT	F	80	.e
7	O ₂ ASH	H2O PER LB DRY AIR	LB.	0.032	f
8	N2 8.1		1		.g
9	H ₂ O — '	UNBURNED FUEL LOSS	%	. O	h
10	ASH —	UNACCOUNTED LOSS	%	.3, O	ļ.i
111		UNACCOUNTED LOSS RADIATION LOSS (ABA1), FIG. 20, CHAPTER 7	%	2.5	j
12	BTU PER LB, AS FIRED, 21825				k
13	QUANTITIES PER	10,000 BTU FUEL INPUT			13
14	FUEL BURNED, 10,000 ÷ LINE 12		LB 6	2458	14
15	IB 7 6			7 633	15
	6 H ₂ O IN AIR, LINE 15 \times LINE f =			0.101	16
17	7! WET GAS TOTAL LINES (14 \pm 15 \pm 16)			, , , , , , , , , , , , , , , , , , , 	1 1
18	8 H ₂ O IN FUEL, (LINE 5 ÷ 100) × LINE 14 × 8.94 + (LINE 9 ÷ 100) × LINE 14; OR FROM TABLE 5			18	
110	91 H ₂ O IN FLUE GAS, TOTAL, LINE 16 + LINE 18			19	
20	0 H ₂ O IN FLUE GAS, TOTAL, IN PER CENT, (LINE 19 ÷ LINE 17) × 100			20	
21	DRY GAS, TOTAL, LINE 17—LINE 19			21	
22	LOSSES PER 10,0	DOO BTU FUEL INPUT			22
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		BTU	0	23
24				300	24
25	RADIATION, 10,000 × LINE j ÷ 100			250	25
			вти	966	26
	SENSIBLE HEAT, FLUE GAS, LINE 17 X BTU FROM FIG. 2	@ LINE e AND LINE 20 =	вти	640	27
	TOTAL LOSSES, LINES (23 + 24 + 25 + 26 + 27)	••••	BTU 2	156	28
29)		1,56	29
30	EFFICIENCY, BY DIFFERENCE, 100—LINE 29		% ;	18.44	30
31	QUANTITIES PER 10,000 BTU FUEL INPUT COMBUSTION TEMPERATURE, ADIABATIC				31
32			вти /	000 .	32
33	the same and the s	FIG. 3 @ LINE d TEMP	вти	-	33
34	1		BTU /	500	34
35	The state of the state of		вти	966_	35
36	†		8TU 9	1934_	36
37	i .		BTU	275	37
38			BTU	759	38
39		E 17 BTU 106			39
40	ADIABATIC TEMPERATURE, FROM FIG. 2 FOR LINES 20	& 39 F 340	0		40

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM 1/2 TO 1/2 OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

CASO 3	,
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			UNSO		
7 - 7		CALCULATIONS ER 10,000 BTU FUEL INPUT	aoodo#/ Load Retrofit		- Z =
E			KBINCOFII (5X/3/6.	E
1	FUEL- NATURAL GAS	CONDITION BY TEST OR SPECI		DATE	a
2	ANALYSIS AS FIRED ULTIMATE, % BY WT PROXIMATE, % BY WT TO			71 // 0	ь
3		DTAL AIR	97 F	30	
4				0	d
5		R TEMPERATURE FROM HEATER UE GAS TEMPERATURE LEAVIN			
6					
7		O PER LB DRY AIR		COOL	1 1
8	N2 8. /		ć	6 0	9
9		NBURNED FUEL LOSS			
10	71011	NACCOUNTED LOSS		6 S.O	
11		ADIATION LOSS (ABA1), FIG. 20,	CHAPTER 7	3.8	
12					k
13	QUANTITIES PER 10,0	000 BTU FUEL INPUT			13
	FUEL BURNED, 10 000 : LINE 12			80458	14
	FUEL BURNED, 10,000 \div LINE 12. TOTAL AIR REQUIRED, LINE $b \div 100 \times VALUE$ FROM FIG. 4	OR TABLE 5 OR 4 -		8 7 911	1.5
16	H ₂ O IN AIR, LINE 15 X LINE f =			0.102	17
17	WET GAS, TOTAL, LINES (14 + 15 + 16)			0,3/0	
18	$_{12}$ O IN FUEL, (LINE 5 \div 100) $ imes$ LINE 14 $ imes$ 8.94 $+$ (LINE 9	÷ 100) × LINE 14; OR FROM	IABLE 3	0 6,707	
19	H ₂ O IN FLUE GAS, TOTAL, LINE 16 + LINE 18			1,02	20
20	${ m H_2O}$ in flue gas, total, in per cent, (line 19 \div line 17	′) × 100		※/み. 3 :	20
21	DRY GAS, TOTAL, LINE 17—LINE 19			B 7.340	<u> </u>
22	LOSSES PER 10,000	BTU FUEL INPUT			22
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		810	0	23
24				300	24
25					25
	LATENT HEAT U.O. IN EUEL 1040 VINE 10		BTU		26
1		INF . AND LINE 20 = \$. 37	2×78 BTU		27
27			BTU		28
1				22.99	29
29	TOTAL LOSSES IN PER CENT, LINE (28 ÷ 10,000) × 100			••••	30
30	EFFICIENCY, BY DIFFERENCE, 100—LINE 29			77.01	+
31		D,000 BTU FUEL INPUT PERATURE, ADIABATIC			31
32	HEAT INPUT FROM FUEL		вти	10000	32
33	HEAT INPUT FROM AIR, LINES (15 \pm 16) $ imes$ BTU FROM FIG.	3 @ LINE d TEMP	BTU	L ~ -	33
34				10000	34
35	LESS LATENT HEAT LOSS, H2O IN FUEL, LINE 26			_ 966_	35
36					36
37	1		p.T.I	1	37
38			8716	- ' -	38
1					39
39		······································	f 3590		40
40	ADMODIL TEMPERATURE, FROM FIG. 2 FOR BIRES 20 & 37		3070		77

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM ½ TO ½ OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.



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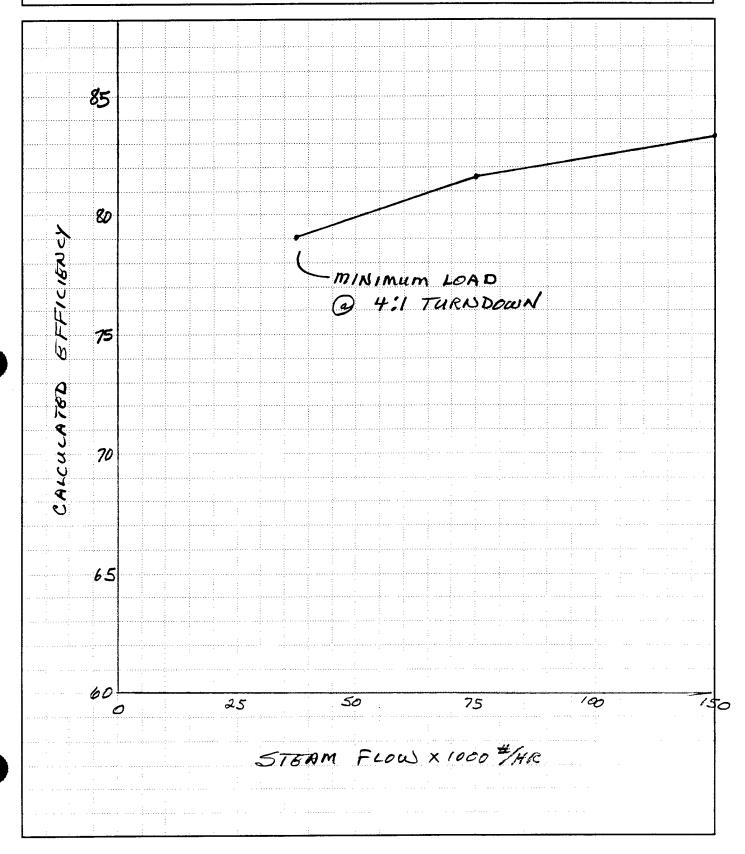
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Calculations For:

BOILERS FROM VAAP - CASE 4\$5



95046-00 Case 4\$5

			730 1 0					
ı	COMPLICTION	N CALCULATIONS 150		L				
	COMBOSTION CALCULATIONS							
И	BASED ON QUANTITIES FER 10,000 BID FOR INFO 4320 5 SATURATOD!							
E	VAAP BOILORS							
\Box	FUEL-NATURAL GAS	CONDITIONS	DATE					
	ANALYSIS AS FIRED	BY TEST OR SPECIFICATION	9-5-95					
1 1	ULTIMATE, % BY WT PROXIMATE, % BY WT			<u>. </u>				
3		***************************************	F 00					
4	c 69, 3 MOISTURE	AIR TEMPERATURE TO HEATER	_ 1 _ 1	ď				
5	H ₂ 22,7 VOLATILE	AIR TEMPERATURE FROM HEATER	F 7					
6	S - FIXED CARBON	FLUE GAS TEMPERATURE LEAVING UNIT		·				
7	O ₂ — ASH	H2O PER LB DRY AIR	18 0,002					
8	N ₂ 8, 1			.g				
9	H ₂ O	UNBURNED FUEL LOSS	% Ø	h				
10	ASH -	UNACCOUNTED LOSS	% 1.5	Li.				
111		RADIATION LOSS (ABA1), FIG. 20, CHAPTER	7 % 0.65	j				
12	BTU PER LB, AS FIRED, 21825		***************************************	k				
	2.000			П				
13	QUANTITIES PER	10,000 BTU FUEL INPUT		13				
			18 0.458	14				
14	FUEL BURNED, 10,000 \div LINE 12. TOTAL AIR REQUIRED, LINE 5 \div 100 $ imes$ VALUE FROM FIG	1076471	10 2/22	1.5				
1	TOTAL AIR REQUIRED, LINE $b\div 100 imes VALUE FROM FIG$	6. A OR TABLE 5 OR 6 = 1,075x 7-1	19 7.6 33					
16	H ₂ O IN AIR, LINE 15 × LINE f = LB 0.101							
17	/ WET GAS, TOTAL, LINES (14 + 15 + 16)							
18	B H ₂ O IN FUEL, (LINE 5 \div 100) \times LINE 14 \times 8.94 $+$ (LINE 9 \div 100) \times LINE 14; OR FROM TABLE 5							
19	9 H_2O IN FLUE GAS, TOTAL, LINE 16 + LINE 18 1.03 O .							
20	0 H ₂ O IN FLUE GAS, TOTAL, IN PER CENT, (LINE 19 \div LINE 17) \times 100 % 12.58							
21								
122	LOSSES BED 10.0	OO BTU FUEL INPUT		22				
22				\vdash				
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		BTU 💪	23				
24	UNACCOUNTED, 10,000 X LINE ; ÷ 100		BTU 150	24				
25	RADIATION, 10,000 × LINE J ÷ 100			25				
26	A COMPANY OF A STATE O			26				
27		@ LINE & AND LINE 20 = 8.192 X (00	BTU 492	27				
	TOTAL LOSSES, LINES (23 + 24 + 25 + 26 + 27)		BTU 1673	28				
				29				
29	1			30				
30			~ 03.4/	+				
31		R 10,000 BTU FUEL INPUT TEMPERATURE, ADIABATIC		31				
32			BTU 10000	32				
33		FIG. 3 @ LINE d TEMP	•••••••••••••••••••••••••••••••••••••••	33				
	1		10000	34				
34				35				
1 ~ -	15 LESS LATENT HEAT LOSS, H ₂ O IN FUEL, LINE 26							
35	36 HEAT AVAILABLE, MAXIMUM BTU 9034							
36	1		2711	37				
- 1	1		BTU_108_	37				
3 <i>6</i> 37 38	LESS LINES (24 + 25) × 0.5* HEAT AVAILABLE, LINE 36—LINE 37		BTU 108 _ BTU 8926	38				
3 <i>6</i> 37 38	LESS LINES (24 + 25) × 0.5*	17 BTU	BTU_108_	⊣ · · · · · 1				

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, UNE 36, BY FROM ½ TO ½ OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

			C 4 = =	- 11 d	_		
			CASO		3		
L	COMBUSTION CALCULATIONS 75000 T/ LOAD: 340 F						
7	BASED ON QUANTITIE	ES PER 10,000 BTU FUEL INPUT	433°F SA	TURNIOT	N		
E			VAAP BO	KERS	E		
1	FUEL- NATURAL GAS	CONDITIONS	_	DATE	٥		
2	ANALYSIS AS FIRED	BY TEST OR SPECIFICATE		5.95			
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR	%	107.5	ь		
4	c 69,3 MOISTURE	AIR TEMPERATURE TO HEATER		80	٩		
5	H2 22,7 VOLATILE	AIR TEMPERATURE FROM HEATER	F		d		
6	S C FIXED CARBON	FLUE GAS TEMPERATURE LEAVING UN		300	•		
7	O ₂ — ASH	H ₂ O PER LB DRY AIR	LB	0.0132			
8	N ₂ 8, 1		on i	Λ			
9	H ₂ O ~ '	UNBURNED FUEL LOSS	%	<i>,</i> .	h		
10	ASH	UNACCOUNTED LOSS	%	5			
11		RADIATION LOSS (ABA1), FIG. 20, CHAP	nex 7 %	1,2	1		
12	BTU PER LB, AS FIRED, 21825				*		
13	QUANTITIES PER	10,000 BTU FUEL INPUT			13		
14	FUEL BURNED, 10,000 ÷ UNE 12.		LB	0.458	14		
15	FUEL BURNED, 10,000 \div LINE 12. TOTAL AIR REQUIRED, LINE $b \div 100 \times VALUE$ FROM FIG.	3. 4 OR TABLE 5 OR 6 = 4.075 77.	/ 18	7.633	15		
					16		
17	WET GAS, TOTAL LINES $(14 + 15 + 16)$						
18	$_{12}$ O IN FUEL, (LINE 5 \div 100) $ imes$ LINE 14 $ imes$ 8.94 $+$ (LINE	E 9 ÷ 100) X LINE 14; OR FROM TABL	E 5 LB	0.929	18		
119	H ₂ O IN FLUE GAS, TOTAL, LINE 16 + LINE 18			V.030.	19		
20	${ m H_2O}$ in flue gas, total, in per cent, (line 19 \div lin	IE 17) × 100	%	1.2.58.	20		
21	1		LB	7.162	21		
22	LOSSES PER 10,0	000 BTU FUEL INPUT			22		
23	UNBURNED FUEL, 10,000 × LINE h ÷ 100		вти	. 0	23		
24		••••••	BTU	. 15 a	24		
25	DADIATION 10.000 × 11NE 1 ± 100		BTU	120	25		
1	LATENT HEAT, H2O IN FUEL, 1040 X LINE 18		вти	766	26		
27			BTU	492	27		
28			вти	1728	28		
29			97. 1	17.28	29		
30			%	82,72	30		
31	QUANTITIES PE	R 10,000 BTU FUEL INPUT TEMPERATURE, ADIABATIC			31		
-	COMBUSTION		вти	10000	32		
32		FIG. 3 @ LINE d TEMP	•••••••••••••••••••••••••••••••••••••••		33		
33	i e			10000	34		
34	HEAT INPUT, TOTAL, LINES (32 + 33) LESS LATENT HEAT LOSS, H ₂ O IN FUEL, LINE 26	••••••		966	35		
				9034	36		
- 1	HEAT AVAILABLE, MAXIMUM LESS LINES (24 + 25) × 0.5*		07111	 135	37		
37			BTU	399	38		
	HEAT AVAILABLE PER LB OF FLUE GAS, LINE 38 + LINE		TU 1086		39		

^{*} NOTE: IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM 1/2 TO 1/2 OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

HEAT AVAILABLE PER LB OF FLUE GAS, LINE 38 ÷ LINE 17 BTU 1086

ADIABATIC TEMPERATURE, FROM FIG. 2 FOR LINES 20 & 39

95046-00 CASE 4\$5

		U/1 3	9 14	<u> </u>			
-	COMBUSTIO	N CALCULATIONS 37500	H/HR	L			
N	BASED ON QUANTITIES PER 10,000 BTU FUEL INPUT 435 SATURATED						
E	VAAP BOILERS E						
1	FUEL- NATURAL GAS	CONDITIONS	9-5-95				
2	ANALYSIS AS FIRED			H			
3	ULTIMATE, % BY WT PROXIMATE, % BY WT	TOTAL AIR	% 110.0	Ь			
4	c 67.3 MOISTURE	AIR TEMPERATURE TO HEATER		١٠			
5	H ₂ 22,7 VOLATILE	AIR TEMPERATURE FROM HEATER	: —	d			
6	S FIXED CARBON	FLUE GAS TEMPERATURE LEAVING UNIT	300	•			
7	O ₂ — ASH	H2O PER LB DRY AIR	B 0.0132	[]			
8	N: 8.1			9			
-	- ·	UNBURNED FUEL LOSS	% O	h			
9	H ₂ O '	UNACCOUNTED LOSS	% /5	1:1			
10	ASH	UNACCOUNTED LOSS RADIATION LOSS (ABA1), FIG. 20, CHAPTER 7	7. 2 2	1:1			
111	* . *	RADIATION LOSS (ABAT), FIG. 20, CHAPTER 7	/el5.2	1:-1			
12	BTU PER LB, AS FIRED, 21825		w	╀┤			
13	QUANTITIES PER	10,000 BTU FUEL INPUT		13			
1,7	ELIEL BUIDNED 10 000 - UNE 12		18 0.458	14			
14		- 1 OP TARIF 5 OR 6 = 1.1X 7.1	LB 7.810	15			
15	TOTAL AIR REQUIRED, LINE B = 100 X VALUE FROM THE	S. A. Ok. TABLE D. Ok. C	18 0.103	16			
16	H ₂ O IN AIR, LINE 15 X LINE f =		18 9 37/	17			
17	WET GAS, TOTAL, LINES (14 + 15 + 16)	OR FROM TABLE C	10,279	1 8			
18	$_{12}$ O IN FUEL, (LINE 5 \div 100) $ imes$ LINE 14 $ imes$ 8.94 $+$ (LINE	9 ÷ 100) X LINE 14; OR FROM TABLE 3	19 1 037	10			
19	H2O IN FLUE GAS, TOTAL, LINE 16 + LINE 18		10 770 330	11			
20		E 17) × 100	ب د میراند.				
21			LB 7.339	21			
22	LOSSES PER 10,0	OO BTU FUEL INPUT		22			
1	LINIBURNIED EUEL 10 000 × LINE L ÷ 100	870		23			
23		BTI	150				
24	UNACCOUNTED, 10,000 × LINE i ÷ 100	BT8	1	t.:::1			
25	l e e e e e e e e e e e e e e e e e e e		1 37				
26	LATENT HEAT, H ₂ O IN FUEL, 1040 X LINE 18 SENSIBLE HEAT, FLUE GAS, LINE 17 X BTU FROM FIG. 2	0 mm	/ E.G J _553	27			
27	1	6 T i	12099	28			
28	TOTAL LOSSES, LINES (23 + 24 + 25 + 26 + 27)		· · · · · · _ · <u>_ · · · · · · </u>	29			
29	TOTAL LOSSES IN PER CENT, LINE (28 ÷ 10,000) × 100	76	20.99				
30	EFFICIENCY, BY DIFFERENCE, 100-LINE 29		779.M	30			
31		R 10,000 BTU FUEL INPUT TEMPERATURE, ADIABATIC		31			
-			1000	32			
32	HEAT INPUT FROM FUEL			33			
33	1		18000	34			
34				35			
3.5		·····································	10021	36			
36			· · · · · · · · · · · · · · · · · · ·	• • • • • • • • • • • • • • • • • • • •			
37	LESS LINES (24 + 25) × 0.5*	BT		37			
38	HEAT AVAILABLE, LINE 36-LINE 37	BT	··· down	38			
39		17 BTU 1653		39			
40		k 39 F 3350		40			
	<u>, I.,,</u>						

^{*} NOTE IT IS CUSTOMARY TO REDUCE THE MAXIMUM HEAT AVAILABLE, LINE 36, BY FROM 1/2 TO 1/2 OF THE UNACCOUNTED PLUS RADIATION LOSSES, ON THE ASSUMPTION THAT A PORTION OF THESE LOSSES OCCURS IN THE COMBUSTION ZONE.

COMBUSTION

FORMULAB

CALCULATIONS

Heat Losses in Steam Generating Units

(Based on ASME Test Form for Abbreviated Efficiency Test)

Dry refuse per 1b of as-fired fuel, 1b/1b

100 - % combustible in refuse sample % ash in as-fired fuel

Carbon burned per 1b of as-fired fuel, 1b/1b

% carbon by weight in fuel sample _ (dry refuse per 1b fuel × Btu per 1b of refuse) 14,500

Note: If flue dust and ash pit refuse differ materially in combustible content they should be estimated separately.

Dry gas per Ib of as-fired fuel burned, 15/16

 $11 \text{ CO}_2 + 8 \text{ O}_2 + 7 \text{ (N}_2 + \text{ CO)} \times \text{(1b carbon burned per 1b as-fired fuel} + 3/8 \text{ S)}$

CO₂, O₂ and CO are the per cents by volume of carbon dioxide, oxygen and carbon monoxide, respectively in the flue gas, N₂ is the per cent of volume of nitrogen, by difference, in the flue gas. S is the pound of sulfur per lb of asfired fuel from the fuel analysis, or % sulfur in fuel where:

2

1. Heat loss due to dry gas

ا ق Ib dry gas per Ib as-fired fuel burned X .24 (ig where: .24 = specific heat of gas
 ig = temperature of gas leaving unit, it = temperature of air entering unit, it = temperature of air entering unit, it

2. Heat loss due to moisture in fuel

 $rac{ extsf{H}_2 extsf{O}}{100} imes$ (enthalpy of vapor at 1 PSIA and tg - enthalpy of liquid at ta) where: H₂O = % moisture in fuel 3. Heat loss due to hydrogen in fuel

= $\frac{9 \text{ Hz}}{100}$ × (enthalpy of vapor at 1 PSIA and tg — enthalpy of liquid at ta) where: H₂ = % hydrogen in fuel
tg = temperature of gas leaving unit, F
ta = temperature of air entering unit, f

4. Heat loss due to CO in flue gas

where: CO and CO2 are per cent by volume of carbon monoxide and carbon dioxin flue gas = CO1 × CO × 10,160 × 1b carbon burned per 1b as-fired fuel 10,160 = Btu generated burning 1 lb of CO to CO ပ္ပ

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COMBUSTION CALCULATIONS FORMULAS

Heat loss due to unburned combustible

ABMA STANDARD RADIATION LOSS CHART

Calculations for each of the above five losses will give the Btu per lb for each loss. To determine the per cent loss in efficiency, which is the per cent of heating value of as-fired fuel: = dry refuse (ash pit + fly-ash) per 1b as-fired fuel \times 8tu per 1b in refuse (weighted average)

Btu in loss
$$\frac{\text{Btu in loss}}{\text{Btu per Ib as-fired fuel}} \times 100 = \% \text{ loss}$$

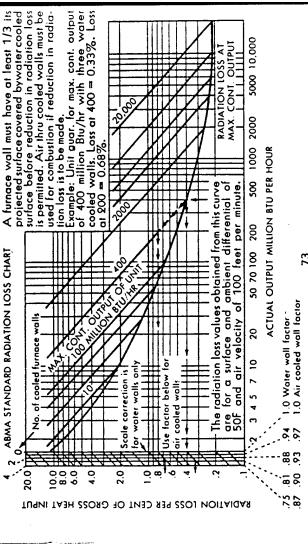
Heat loss due to radiation

The per cent loss in efficiency due to radiation may be obtained from the ABMA Standard Radiation Loss Chart on page 73.

Unaccounted for losses

These losses include relatively minor losses such as sensible heat in ash or slag, radiation to ash pit, moisture in air, heat pickup in cooling water, etc., generally not measured because the effort is not justifiable. A previously agreed upon amount can be assigned for these losses, if they are not measured.

Unit efficiency as determined by heat loss measurement then becomes the total of the above percentage efficiency losses subtracted from $100\,\%$.



Chapter 4. Principles of Combustion REFERENCE

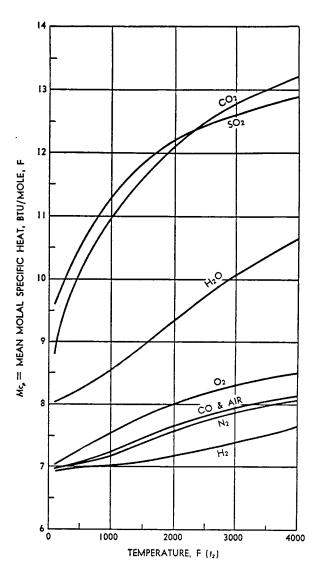


Fig. 1. Mean molal specific heat of gases between final temperature $\binom{t_2}{2}$ and 80 F at std atmospheric pressure

TABLE 5

Theoretical Air, Fuel, and Resulting Moisture Per 10,000 Btu As Fired

	Theoretical Air,*	Fuel,	Moisture,
Fuel	lb/10kB	lb/10kB	lb/10kB
Fuel oil	7.46	0.544	0.51
Natural gas	7.10	0.496	0.93
Coal (prox ar	nal.) See Fig. 4	_	
Coal (ult anal	l.) See Table 6		

*Dry air. To obtain wt of wet air required, moisture in air at standard conditions (0.0132 lb per lb dry air @ 60% relative humidity and 80 F dry bulb) must be added.

TABLE 6

Formula for Calculating Theoretical Air*
In lb per 10,000 Btu of Fuel as Fired

Ultimate Analysis of Fuel on As-Fired Basis,

Per Cent by Weight

C = Carbon

H₂ = Hydrogen

 $O_2 = Oxvgen$

S = Sulfur

Btu/lb = Heat value of fuel

$$\begin{array}{c} \text{Theoretical Air.} \dagger \text{ lb} = 144 \times \frac{8\text{C} + 24 \left\{ \text{ H}_2 - \frac{\text{O}_2}{8} \right\} + 3\text{S}}{\text{Btu/lb}} \\ \end{array}$$

^oThis formula should be used only when the exact ultimate analysis and the correct heating value are given for the fuel.

†Dry air. To obtain wt of wet air required, moisture in air at standard conditions (0.0132 lb per lb dry air @ 60% relative humidity and 80 F dry bulb) must be added.

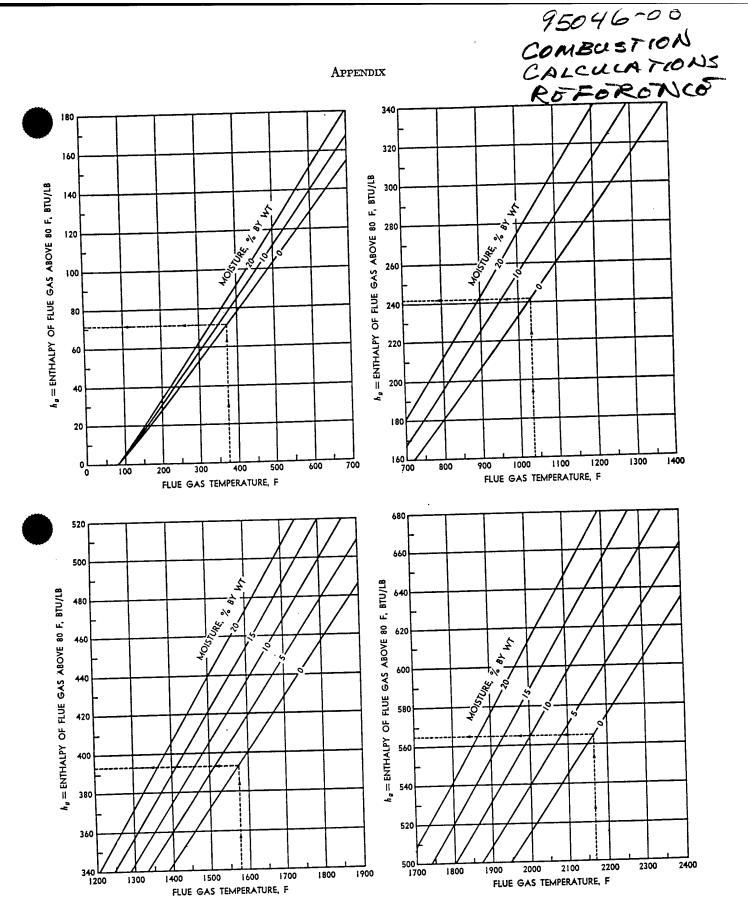


Fig. 2. Enthalpy of flue gas above 80 F at 30 in. Hg, Btu per lb

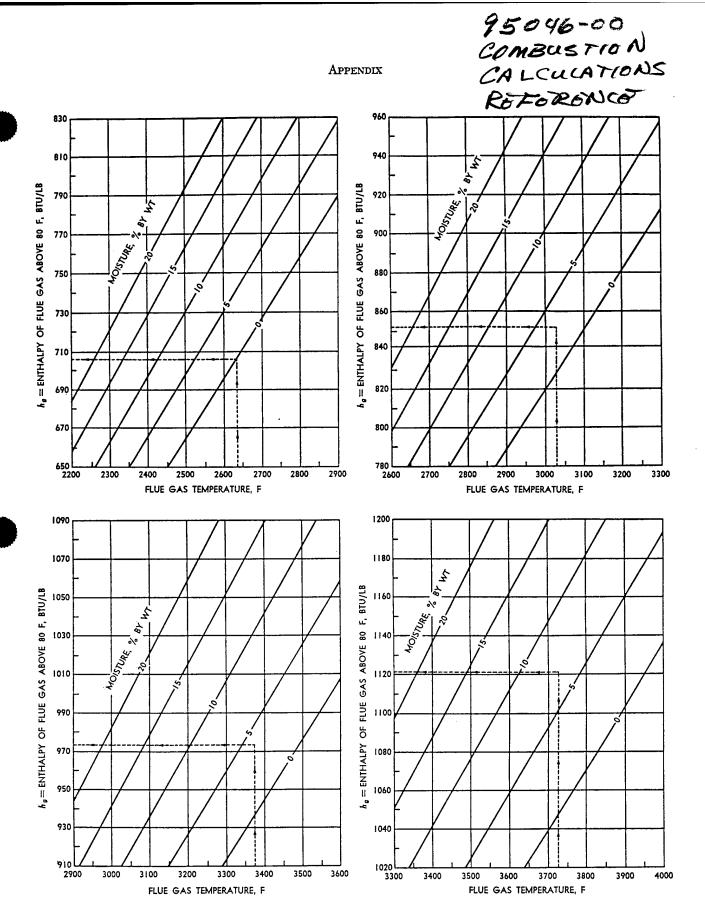


Fig. 2. (Cont'd) Enthalpy of flue gas above 80 F at 30 in. Hg, Btu per lb 4-A3

95046-00 COMBUSTIONS CALCULATIONS REFERENCE

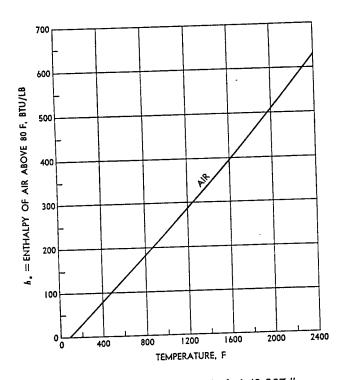


Fig. 3. Enthalpy (above 80 F) of air (0.987 lb dry air plus 0.013 lb water vapor per lb mixture) at 30 in. Hg, Btu per lb

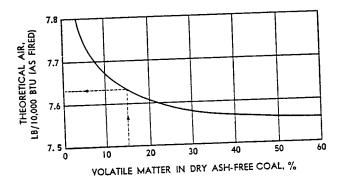


Fig. 4. Theoretical air in lb per 10,000 Btu heat value of coal with a range of volatile



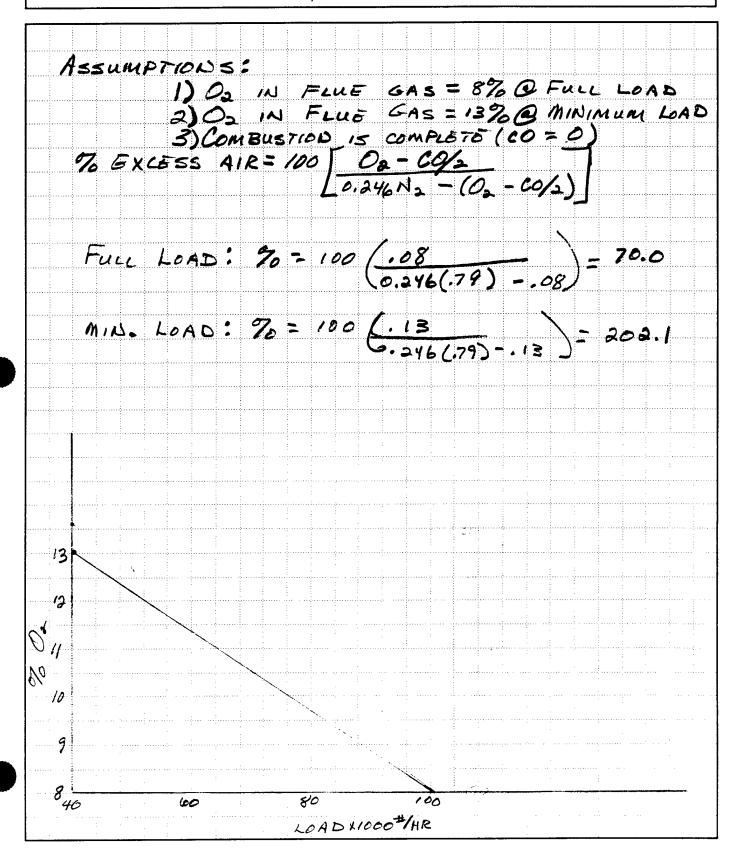
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EXCESS AIR FTOTAL AIR - STOKER OPER, COALBUR



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Calculations For:

BLOG. 2-A AUX BURNOR ROTROFIT @ HT. ROCOU. BOILORS

CRACKING FURNACE BURNOR DATA: 1750 MBH RATED CAP. 360 SCFM COMBUSTION AIR N.G. #/HR = 1750000 B/H - 80.2 H 81825 B/# AIR \$/4 = 360 FT/m (60 /4)(0.075 \$/FT)= 1620 \$/4 THEOR. AIR = 1750000 (7,10 108+0.093 #108) = 1260 #/HR Excess AIR = 16200 128.6 70 FLUE GAS FLOW = 1620 + 80 = 1700 TH @ 6=EF FIND N.G. AND PPI. AIR ROD. TO GIVE FLUE GAS TOMP. OF 1250 F @ 110% GX, AIRS DBTU FOR FURNACE GAS= 1700/H (325 4-180 4) (8 FOR) = 3944,000 BTUH

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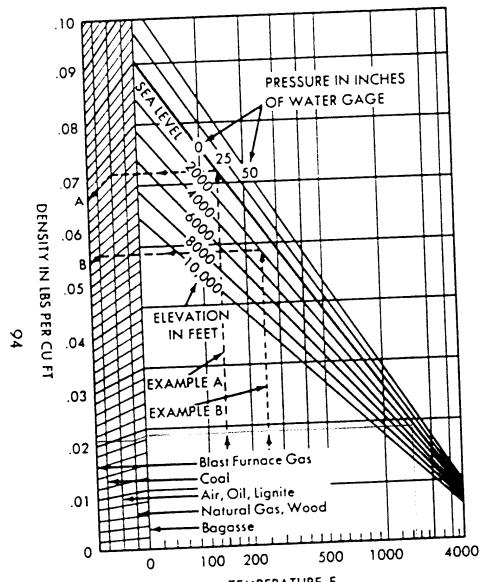
Calculations For:

BLOG 7-A AUX BRNR RETROFIT @ HT. ROC. BOILERS

BOILER GAS SIDE FLOW = (1700 #HR)(16)=27200#H APPROX. FLUE GAS SP. VOL.@ 625°F= 30 FT/# GAS CFM = 27200 (30) _ 13600 FIRE TUBE MAX. VEZ. = 13600 FT/MIN (700TUBES)(0.0171FT/TUB) - 1/36 F/MIN AIR AVAILABLE IN FURNACE BXIT GAS FOR AUX. BURNOR : AIR = (1620-1260)(16) = 5760 #/HR. BURNER RATING @ 110% & XCES AIR: RATING = (5760) 104 (7.10+0.093)(103) = 7280 MBH TRY 7000 MBH BURNOR: 7000000B/H = 321 #/H Q = WC> OT 7000000 = 27500 (0.32)(7-625) T= 1420°F GAS ENTERING BOILER

BLDG 7-A AUX BRAR RETROFIT





TEMPERATURE, F

<u> </u>		Density
Example A	Air at std atmospheric pressure (sea level) and 140 f	.0662 16/cu ft
В	Flue gas from coal combustion — £4000 tr elevation and 250 F	.0543 lb/cu ft

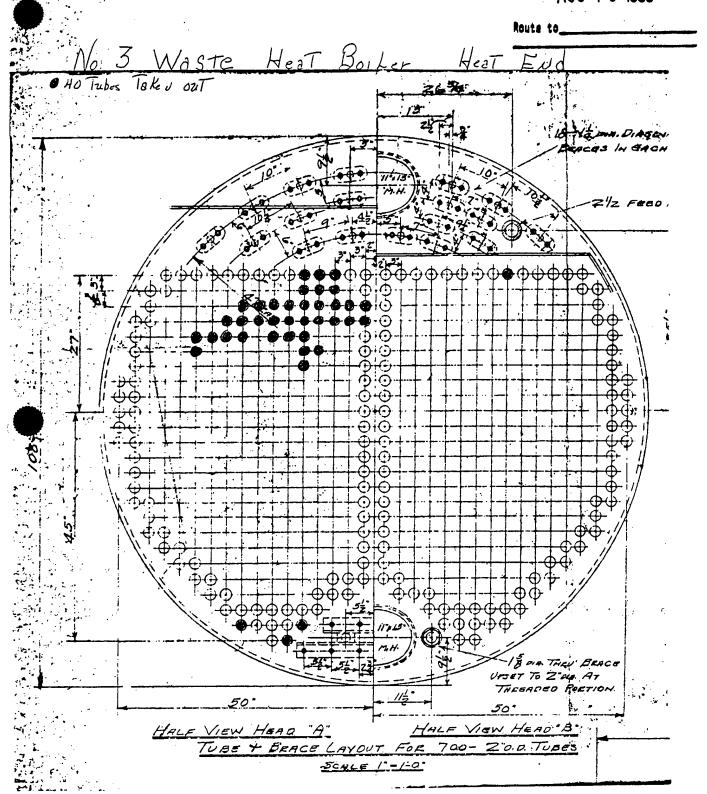
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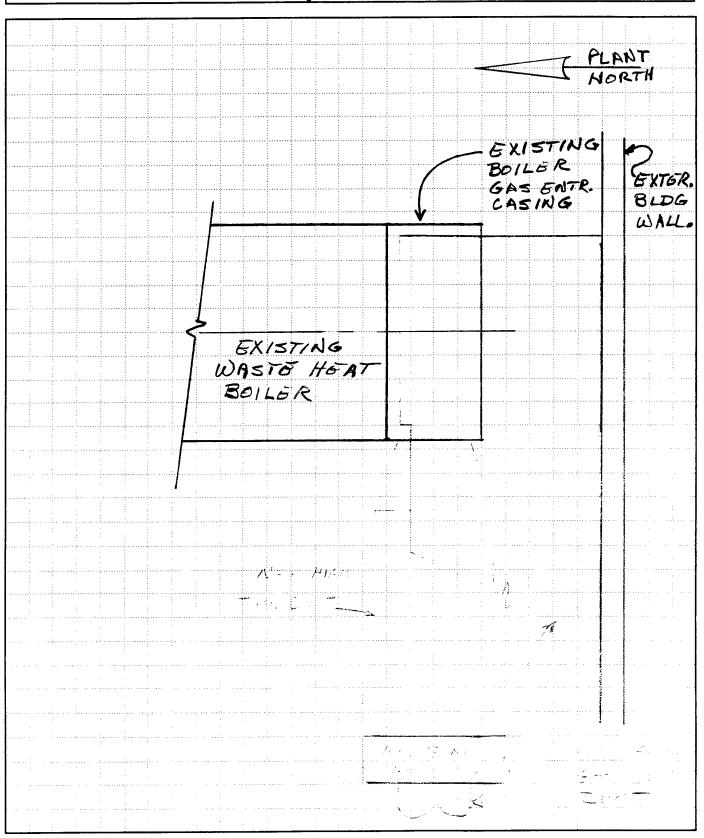
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Calculations For:

BLDG. NO. 7-AWASTE HEAT BOILER RETROPT



3300 SW Archer Road Gainesville, Florida 32608 (904) 376-5500 FAX (904) 375-3479

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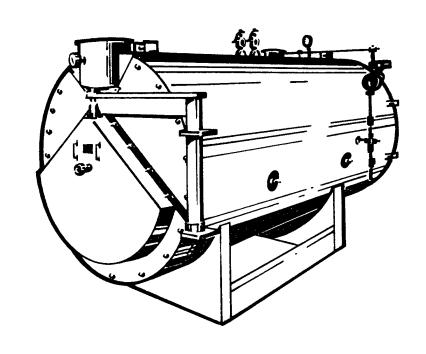
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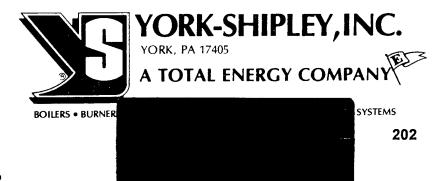
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SELECTION AND SIZING OF HEAT RECOVERY BOILERS







SELECTION OF HEAT RECOVERY BOILERS

BOILER HORSEPOWER AT VARIOUS WORKING PRESSURES FOR VARIOUS INLET GAS TEMPERATURES

The following table will provide the boiler horsepower for various working pressures and various inlet gas temperatures; however, should you want more exact data or if your operating conditions are not included in the table, use the procedure on the following pages.

In the following table, the horsepower is given for one thousand (1000) pounds of waste gas.

Determine pounds of waste gas (see steps 2, 3, & 4 on following page); then multiply the number of thousand pounds by the horsepower for the working pressure and inlet gas temperature.

Example: 15,000 Lbs./Hr.

Working Pressure 150 PSI Inlet Gas Temp. 1600°F.

 $15 \times 8.4 = 126$ Boiler HP

Boiler Horsepower for 1000 Lbs. Per Hr.

OF. Inlet Gas Temperature

W.P. RANGE P.S.I.	2000	<u>1900</u>	1800	1700	<u>1600</u>	1500	1400
0- 15	12.4	11.6	10.9	10.1	9.3	8.5	7.8
16- 50	12.0	11.3	10.5	9.7	8.9	8.2	7.4
51-100	11.8	10.9	10.2	9.4	8.6	7.9	7.1
101-125	11.6	10.8	10.1	9.3	8.5	7.8	7.0
126-150	11.5	10.7	10.0	9.2	8.4	7.6	6.9
151-200	11.3	10.6	9.8	9.0	8.2	7.5	6.7
201-250	11.2	10.4	9.7	8.9	8.1	7.3	6.6

Boiler Horsepower for 1000 Lbs. Per Hr.

OF. Inlet Gas Temperature

W.P. RANGE P.S.I.	1300	1200	1100	1000	<u>900</u>	800
0- 15 16- 50	7.0 6.6	6.2 5.8	5.4 5.1	4.7 4.3	3.9	3.1
51-100	6.3	5.5	4.8	4.0	3.5 3.2	2.7 2.4
101 – 125 126–150	6.2 6.1	5.4 5.3	4.7 4.5	3.9 3.8	3.1 3.0	2.3
151-200 201-250	5.9 5.8	5.1 5.0	4.4 4.2	3.6 3.4	2.8 2.7	2.0 1.9

The following procedure can be used to determine the amount of heat (BTU per Hr.) that can be recovered with a heat recovery boiler.

Step 1 - Determine the waste gas temperature.

Step 2 - Determine the amount of waste gas in Pounds per Hour.

Step 3 - If the amount of waste gas is measured in CFM - convert CFM to pounds using Table below:

Temp. °F.	Density in Pounds/Cu.Ft.
60°F. (Std)	0.0763
900°F.	0.0292
1000°F.	0.0272
1200°F.	0.0239
1400°F.	0.0214
1600°F.	0.0193
2000°F.	0.0176
2500°F.	0.0161
3000°F.	0.0134

Step 4 - The following can be used to estimate the waste gas available from various processes:

Nat. gas produces 1.0 Lb. waste gas per Cu.Ft. Oil produces 135 Lbs. waste gas per Gal. Wood (dry) produces 10 Lbs. waste gas per Lb. Wood (50% moist) produces 6 Lbs. waste gas per Lb.

Step 5 - The following equation can be used to determine the available heat from the waste gas:

Use 350°F. for Low Press. Boiler Stack Temp. 500°F. for High Press. (150#) Boiler Stack Temp. 550°F. for High Press. (Over 150#) Boiler Stack Temp.

Example: 15,000 Lbs. Gas/Hr. at 1600°F. 150 PSI Steam Required

BTUH = 15,000 X .26 (1600 - 500) BTUH = 4,290,000 (128 HP)

SELECTION OF BOILER SIZE

The following table will provide the boiler heating surface per boiler horsepower for various pressures and various inlet gas temperatures.

Using the horsepower from the chart on Page 1 or as calculated in accordance with the equation on Page 2, multiply the horsepower by the square feet of heating surface from the chart for the working pressure and inlet gas temperature.

Select a heat recovery boiler from the brochure with the proper heating surface. If the calculated heating surface falls between two sizes, use the larger size.

Example:

126 HP from table Page 1 Working Pressure 150 PSI Inlet Gas Temp. 1600°F.

126 HP \times 7.0 Sq.Ft./HP = 882 Sq.Ft. Heating Surface Use Model HRH-1000

HEATING SURFACE PER BOILER HORSEPOWER, SQ. FT.

			<u>Ga</u>	s Temper	ature ^O F	· •	
Press. Range P.S.I.	2000	1900	1800	<u>1700</u>	1600	<u>1500</u>	1400
0- 15 16- 50 51-100 101-125 126-150 151-200 201-250	4.7 4.8 4.9 5.0 5.1 5.2 5.3	5.0 5.2 5.4 5.4 5.5 5.6	5.3 5.6 5.7 5.8 5.9 6.0	6.0 6.1 6.2 6.3 6.4 6.5	6.3 6.5 6.8 6.9 7.0 7.1 7.2	6.9 7.1 7.3 7.4 7.6 7.8 7.9	7.1 7.3 7.5 7.6 7.9 8.1 8.3

HEATING SURFACE PER BOILER HORSEPOWER, SQ. FT.

			<u>Ga</u>	s Temper	ature ^O F	<u>.</u>
Press. Range	1300	1200	1100	1000	<u>900</u>	800
0- 15	7.2	7.4	8.3	9.5	10.5	11.5
16- 50	7.5	7.7	8.7	9.9	10.9	11.9
51-100	7.8	8.0	9.2	10.2	11.3	12.4
101-125	8.0	8.3	9.4	10.4	11.8	12.9
126-150	8.1	8.4	9.5	10.6	12.2	13.5
151-200	8.3	8.6	9.8	10.9	12.4	13.8
201-250	8.5	8.8	10.0	11.2	12.9	14.3

CALCULATING PRESSURE DROP THROUGH BOILER

- Step 1. Determine the standard CFM of waste gas.
- Step 2. Correct the standard CFM by using the temp. correction factor from table below:

Temp. Corr. Factor	Temp. $o_{\mathbf{F}_{\bullet}}$	Temp. Corr. Factor	
.88	1500°F	.98	
	1600	1.00	
	1700	1.02	
.91	1800	1.04	
.92	1900	1.06	
. 94	2000	1.08	
.96			
	.88 .89 .90 .91 .92	Factor of. .88 1500°F .89 1600 .90 1700 .91 1800 .92 1900 .94 2000	

Step 3. Determine the Pressure Drop Correction Factor by dividing the corrected CFM by the base CFM from below and square the result.

Press. Drop Corr. Factor =
$$\begin{bmatrix} \frac{\text{Corrected CFM}}{\text{Base CFM}} \end{bmatrix}^2$$

Step 4. Determine the actual pressure by multiplying the base pressure drop from following table by the correction factor calculated in Step 3.

	Base	Base		Base	Base
<u>Model</u>	CFM	Press. Drop	<u>Model</u>	CFM	Press. Drop
HR-125	220	.10" W.C.	HR-1000	1760	2.50" W.C.
HR- 150	2 6 5	.20''	HR-1125	1980	3.00"
HR-200	350	.40"	HR-1250	2200	1.50''
HR-250	440	. 65'' .	HR-1500	2640	2.20"
HR-300	525	.85''	HR-1750	3 08 0	3.00"
HR-350	615	1.20"	HR-2000	3520	3.00"
HR-400	700	1.50"	HR-2500	4400	3.00"
HR-500	880	.85"	HR-3000	5280	4.50"
HR-625	1100	1.40"	HR-3500	6160	4.20''
HR-750	1320	2.00"	HR- 4250´	8,800	4.00"
HR-875	1540	1.75"		′	

Example:

15,000 Lbs./Hr. at 1600° F. Using HR-1000 Boiler

$$\frac{15,000 \text{ Lbs.}}{60 \text{ X .0193 Lbs/Cu.Ft.}} = 12,953 \text{ ACFM}$$

Press. Drop Corr. Factor =
$$\left[\frac{12,953}{7,200}\right]^2$$

P.D.C.F. = 3.2

Actual Press. Drop = Base press. Drop X P.D.C.F.

Actual Press. Drop = 2.50" X 3.2

Actual Press. Drop = 8.0" W.C.

HEAT RECOVERY BOILERS

Standard Equipment:

A.S.M.E. Three Pass Boiler

3 Pc. Rear Cover (3 Pass Design)

2 Pc. Front Cover

Two Inches Insulation

Metal Jacket

Rear Head Refractory with Davit

Trim Consisting of:

Safety Valves

Press. Gauge

Limit Control

Water Column with L.W.C.O. and Pump Control, Gauge Glass

and Try Cocks

Lifting Lugs

Front Furnace Protective Refractory

Control Wiring to Terminals in Junction Box

Optional Equipment:

Particulate Drops - Front and/or Rear

Soot Blowers

Inducer Brackets

Blowdown Valves

Steam Stop Valve

Steam Non-Return Valve

F.W. Stop/Check Valves

Abrasion resistant Refractory Rear Cover

Aux. L.W.C.O.

Vertical Vent (125 thru 750)

Front Cover Hinges (125 thru 750)



AFFILIATED ENGINEERS SE, INC.

3300 SW Archer Road Gainesville, Florida 32608 (904) 376-5500 FAX (904) 375-3479

Made By: PDL

Checked By:

10-26-95 Date:

Date:

Job No:

95046-00

Sheet No:

of

Calculations For:

CASE 6 \$ 7 No.2 FUEL OIL STORAGE

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Appendix 2 - Cost Estimates/ Energy Cost Development

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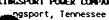
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KINGSPORT POWER



TARIFF I. P. (Industrial Power)

AVAILABILITY OF SERVICE

Available to industrial and large commercial customers. Customers shall contract for a definite amount of electrical capacity in KW which shall be sufficient to meet normal maximum requirements but in no case shall the capacity contracted for be less than 3,000 KW. Contract capacities will be specified in multiples of 100 KW.

MONTHLY RATE

Tariff _Code	Service Voltage	Demand Charge <u>per KW</u>	Energy Charge per KWH	Service Charge		
322	Primary	\$ 8.70	2.302 cents	\$ 240.00		
323	Subtransmission	\$ 7.79	2.269 cents	\$ 730.00		
324	Transmission	\$ 7.60 HOC	2.241 cents	\$1,930.00	4-	HOC

Reactive Demand Charge for each Kilovar of Lagging Reactive Demand

in excess of 50 percent of the KW of monthly metered demand \$ 0.75 per KVAR

MINIMUM CHARGE

This tariff is subject to a minimum monthly charge equal to the sum of the service charge, the product of the demand charge and the monthly billing demand and the fuel clause adjustment.

FUEL CLAUSE

When the unit cost of fuel in the charges for power purchased from Appalachian Power Company under Federal rgy Regulatory Commission rate schedule No. 23 is above or below a base unit price of 15.8563 mills per KWH, justed for losses, the bill for service shall be increased or decreased respectively at a rate per KWH equal to the amount that such cost of fuel is above or below the unit base cost of 15.8563 mills per KWH, adjusted for losses, applied to the KWH measured in the period for which the bill is rendered. The adjustment shall be based on the most recent calendar month for which fuel cost data is available.

PROMPT PAYMENT DISCOUNT

A discount of 1.5 percent will be allowed if account is paid in full within 15 days of date of bill.

DETERMINATION OF DEMAND

The billing demand in KW shall be taken each month as the single highest 30-minute integrated peak in KW as registered during the month by a demand meter or indicator, or, at the Company's option, as the highest registration of a thermal type demand meter or indicator, but the monthly billing demand so established shall in no event be less than 60% of the greater of (a) the customer's contract capacity or (b) the customer's highest previously established monthly billing demand during the past 11 months nor less than 3,000 KW.

The reactive demand in KVARS shall be taken each month as the single highest 30-minute integrated peak in KVARS as registered during the month by a demand meter or indicator, or, at the Company's option, as the highest registration of a thermal type demand meter or indicator.

METERED VOLTAGE

The rates set forth in this tariff are based upon the delivery and measurement of energy at the same voltage, thus measurement will be made at or compensated to the delivery voltage. At the sole discretion of the Company, such compensation may be achieved through the use of loss compensating equipment, the use of formulas to calculate losses or the application of multipliers to the metered quantities. In such cases, the metered KWH and KW values will be adjusted for billing purposes. If the Company elects to adjust KWH and KW based on multipliers, the adjustments shall be in accordance with the following:

- 1. Measurements taken at the low-side of a customer-owned transformer will be multiplied by 1.01.
- Measurements taken at the high-side of a Company-owned transformer will be multiplied by 0.98.

Issued: October 30, 1992

By: Michael J. Holzaepfel, President

Kingsport, Tennessee

Effective: November 3, 1992 Pursuant to an Order in Docket Number 92-04425

CUSTOMER NO.

The Philo

60444-3

METER NO. | S9225055

AMOUNT

SERVICE ADDRESS:

501 S WILCOX DR

32 N EASTMAN RD E 2A GSPORT, TN 37664 615 245-4189

HOLSTON DEFENSE C/O HOLSTON DEFENSE 4509 W. STONE DR KINGSPORT, TN 37660

DATE BILLED 5/04/95

DESCRIPTION

RATE CODE 240 - 7

					RATE SCH	EDULE AVAILABL	E UPON REQUEST	IN LOCAL OFFICE.
BILLIN	G PERIOD	METER	READING "	PRESSURE	MULTIPLIER	CCF	BTU	THERMS
FROM :	'- '- 'TO	PREVIOUS	PRESENT	FACTOR	MULTIPLIER	USED	FACTOR	USED
		1					!	
3/31/95	4/30/95	115916	121258	1.0000	l	53420	1.0000	53420

MESSAGES DON'T HAVE YOUR GAS TURNED OFF INSTALL A GAS WATER HEATER AND HAVE ALL THE HOT WATER YOU NEED AT LESS COST. NO SERVICE CALL IN THE FALL TO RESTORE SERVICE. YOUR GAS HEAT WILL BE READY WHEN YOU NEED IT. CALL TODAY ABOUT OUR WATER HTR PGM.

STOMER DEPOSIT INFORMATION

30

ER DEPOSIT DATE OF DEPOSIT DATE OF REFUND

LAST YEAR

CURRENT MONTH CHARGES GAS CHARGES 12,300.04 DEMAND CHARGE 9,409.24 DEMAND PGA 633.63CF PAYMENT RECEIVED - THANK YOU 4/17/95 30862.79

				7
	OMPARATI	VE USAGE	INFORMATION	<i>i</i>
BILLING	DAYS	USAGE	DAILY AVG. USAGE	DEGREE DAYS
CURRENT	3.0	53420	1780.67	. 273

127190

THIS AMOUNT DUE NOW

\$21,075.65

PAST DUE AFTER THIS DATE | 5/19/95

PAY THIS AMOUNT

\$22,129.43

LUE DATE DOES NOT EXTEND PAYMENT OF ANY PHEVIOUS BALANCE DUE THE TAIN THIS SECTION FOR YOUR SECOND BY THE TOEAN AMOUNT OUR FARIORS TO RECEIVE STATEMENT DOES NOT BELLEVE CUSTOMER OF RESPONDED OF TOEAN AMOUNT OUR.

DETACH AND RETURN THIS SECTION WITH SOME PARMENT.
PLEASE GO NOT STAPLE FOLD OR MUTILATE

CUSTOMER NO.

66444-1

MAKE CHECKS PAYABLE TO UNITED CITIES GAS CO.

JOHNSON CITY, TN 37605

CYCLE NO.

HOLSTON DEFENSE C/O HOLSTON DEFENSE 4509 W. STONE DR KINGSPORT, TN 37660

THIS AMOUNT DUE NOW

PAY THIS

\$21,075.65 \$22,129.43

PAST DUE AFTER THIS DATE 5/19/95

P O BOX 2970

AMOUNT

59100664441000221294300021075650002107565

4239.67

PETTOLEUM TESTING FACILITY - EAST N. J CUMBERLAND, PA 17070-500

Coal Analysis Report

02/28/94

allation:

CDR HOLSTON DEFENSE CORP 4509 WEST STONE DRIVE

KINGSPORT TN 37660-9982

Delivery Date:

10-FEB-94

Date Received:

24-FEB-94

Mine Name:

RED RIVER

Can Number:

County, State:

۷A

Sample Number:

1737 93114B

Contractor:

ONYX INTER

Activity Code:

AR11

Contract Number: DLA600-93-D-0674

Lab Number:

4056

Item Number:

Coal Sampler's Number:

92-6

Tons Reprst'd:

918.80

2.03

Size & Kind:

1 3/4" X 3/8"

Car, Truck or Barge Number:

NW12210, 168252, 133447, 11601, 75904, 168265, 145446, 94956, 12230, 167330,

NS312326

TESTS

RESULTS

[As Recd] [Moisture Free]

Air Dry Loss: Total Moisture:

2.9

Volatile Matter:

34.7

35.7

MATH MARKET

Fixed Carbon: Ar':

56.1 6.3 57.8 6.5

0.73

0.75

Htg Val-Btu/lb:

13900

14320

Ash Fusion Temp (Deg F)

Initial:

Softening:

Hemi:

Fluid:

Free Swelling Index:

Hardgrove Grind Ind:

Remarks:

Approved By:

Chief, Product Assurance Division

USAPC FL 707-E

r 92

(730)

S ARMY PETROLEUM CENTER PETROLEUM TESTING FACILITY - EAST NEW CUMBERLAND, PA 17070-5005

Coal Analysis Report

.04/14/94

Installation:

CDR HOLSTON DEFENSE CORP 4509 WEST STONE DRIVE

Delivery Date: 21-MAR-94 Date Received: 05-APR-94

KINGSPORT TN 37660-9982

1ine Name:

RED RIVER

Can Number:

0016

County, State:

VA

Sample Number:

93132B

Contractor:

ONYX INTER

Activity Code:

Coal Sampler's Number: 92-3

AR11

Contract Number: DLA600-93-D-0674

Lab Number:

4074

| tem Number:

îons Reprst'd: 3ize & Kind:

1 3/4" X 3/8"

lar. Truck or Barge Number:

IW5981, 143864, 131074, 3737, 92219, 6168, 7780, 118683, 12742, 145302, NS336022

S0U76864

ESTS

RESULTS

	[As Recd]	[Moisture Free]
\ir Dry Loss: 1	39	
otal Moisture:	2.3	
Volatile Matter:	33.7	34.5
i Carbon:	58.7	60.1
leh .	5.3	5.4
Sulfur:	0.70	0.72
Itg Val-Btu/1b:	14270	14610

sh Fusion Temp (Deg F)

Initial: Softening: Hemi: Fluid:

ree Swelling Index:

lardgrove Grind Ind:

emarks:

Approved By:

(730)

FL 707-E 1 Apr 92

Product Assurance Division

US ARMY PETROLEUM CENTER PETROLEUM TESTING FACILITY - EAST NEW CUMBERLAND, PA 17070-5005

Coal Analysis Report

06/17/94

nstallation: CDR HOLSTON DEFENSE CORP

4509 WEST STONE DRIVE KINGSPORT TN 37660-9982 Delivery Date: 25-MAY-94

Date Received: 10-JUN-94

ine Name:

RED RIVER

Can Number:

0470

ounty, State:

VΑ

Sample Number:

9416B

ontractor:

ONYX INTER

Activity Code:

AR11

ontract Number: DLA600-94-D-0670

Lab Number:

4095

tem Number:

Coal Sampler's Number:

92-2

ons Reprst'd:

922.85

ize & Kind: 1 3/4" X 3/8"

ar, Truck or Barge Number:

1W3142, 10408, 3004, 11945, 93533, 5219, 94167, 117629, S0U352051, 77068, 78855

ESTS

RESULTS

		[As Recd]	[Moisture Free]
\ir Dry Loss:	2.15		
rotal Moisture:		3.8	
/olatile Matter:		33.9	35.2
iy ' Carbon:		57.7	60.0
/a)		4.6	4.8
Sulfur:		0.78	0.81
ltα Val−Btu/lb:		14040	14600

\sh Fusion Temp (Deg F)

Initial: Softening:

Hemi: Fluid:

Free Swelling Index:

Hardgrove Grind Ind:

Remarks:

Approved By:

Date: 6/20/94

f, Product Assurance Division

FL. 707-E 92 **1** C

(730)

3 ARMY PETROLEUM CENTER PETROLEUM TESTING FACILITY - EAST NEW CUMBERLAND, PA 17070-5005

Coal Analysis Report

10/25/94

netarlation:

CDR HOLSTON DEFENSE CORP 4509 WEST STONE DRIVE

KINGSPORT TN 37660-9982

Delivery Date:

03-0CT-94

Date Received: 13-0CT-94

ne Name:

RED RIVER

Can Number:

0852

ounty, State:

V۸

Sample Number:

94047A

ontractor:

ONYX INTER

Activity Code:

14500

AR11

ntract Number: DLA600-94-D-0670

Lab Number:

em Number:

984.9

ona Reprat'd: ze & Kind:

1 3/4" X 3/8"

Coal Sampler's Number: 92-2

ar. Truck or Barge Number:

/68562, 119358, 68502, 146192, 94349, <mark>168269, 10252, 144945, 75163, NS327477,</mark>

36307, SOU351223

ESTS

RESULTS

		[As Recd]	[Moisture Free]
r Dry Loss:	2.13		
tal Moisture:		3.4	
latile Matter:		35.2	36.4
xCarbon:		55.7	57.7
carbon:		5.7	5.9
ılfur:		0.88	0.91
			•

14010

sh Fusion Temp (Deg F)

Initial:

Softening:

Hemi:

ig Val-Btu/lb:

Fluid:

ee Swelling Index:

ardgrove Grind Ind:

emarks:

Approved By:

(730)

707-E . Apr 92

ef. Product Assurance Division

3 ARMY PETROLEUM CENTER PETROLEUM TESTING FACILITY - EA NEW CUMBERLAND, PA 17070-5005

Coal Analysis Report

01/24/9

stallation: CDR HOLSTON DEFENSE CORP

4509 WEST STONE DRIVE KINGSPORT TN 37660-9982 Delivery Date: DB-JAN-BE

Date Received: 18-JAN-95

Mine Name: RED RIVER

Can Number:

0028

County, State: VA

Sample Number:

94067A

Contractor *** *** ONYX INTER

Activity Code:

AR11 5024

Item Number:

Contract Number: DLA600-94-D-0659

Lab Number: Coal Sampler's Number: 92-14

Tons Reprst'd:

935.55

0.82

Size & Kind:

1 3/4" X 3/8"

Car, Truck or Barge Number:

NW143778, 117599, 11517, 142405, 146022, 145718, 92688, 9647, 7019, 143234,

S0U351343

TESTS

RESULTS

.....

[As Recd] [Moisture Free]

Air Dry Loss: Total Moisture: Volatile Matter: Fixed Carbon:

36.8 54.6

1.8

37.5 55.6

ah:

6.8

6.9

lfur:

0.85

0.87

Htg Val-Btu/lb:

13990

14240

Ash Fusion Temp (Deg F)

Initial: Softening: Hemi:

Fluid:

Free Swelling Index:

Hardgrove Grind Ind:

Remarks:

Approved By:

USAPC FL 707-E

Apr 92

ef, Product Assurance Division

(730)



AFFILIATED ENGINEERS SE, INC. 3300 SW Archer Road/P.O. Box 1086 Gainesville, FL 32608 (904) 376-5500 (904) 378-3081 - Fax

Made By: PDL	Date: //-/-95	Job No: 95046-00				
Checked By:	Date:	Sheet No: of				

Calculations For:

VALUES FOR USE IN SPREADSHEETS

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.DATE 11 MAY 95 15:17:35 RID 1200 11 MAY 9	S M7971			
* CPP Vs ACT - APR 1995	AUG MTH	APR MTH.	PCT	ANNUA.
* CUST.EXP.		ACT CST.		

2230 STEAM - AREA A 2230 046 000 DISODIUM PHOSPHATE (573)	74	34	452	910
2230 046 000 DISODIUM PHOSPHATE (5/3)	70 100	116	7.3	714
2230 118 000 ROCK SALT (5629)		61254		
2230 137 000 BITUMINOUS COAL		01-04	20%	
2230 141 000 SODIUM SULFITE (5613)	7	4		14300
2230 143 000 SULFURIC ACID (560)	1195			
2230 306 051 LBR-DEPARTMENTAL CPERATIONS-OPER	60235	40/01	ەرن م	794616
2230 400 000 DEPT SUPPLIES & MISC EXPENSES	521	221		6250
2230 402 000 CLITHING	Ü		0% 	
2230 414 998 PRODUCTION FUNDED EQUIPMENT DIL		261	1243%	250
2230 714 721 SUB-CON CINDER/FLYACH RECOVERY	317			3800
2230 764 994 ROUTINE MAINT - SUBCONTRACT	0	164		
2230 764 997 ROUTINE MAINT - HDC LER @ CPP EST	26322	22074	78%	339867
2230 764 998 ROUTINE MAINT - MATERIALS	3454	7004	203%	41453
0030 766 994 MAJOR MAINT - SUBCONTRACT	11992		0%	
2230 766 997 MAJOR MAINT - HDC LBR @ CPP EST	6502	431	7%	78028
2230 766 998 MAJOR MAINT - MATERIALS	5827		0%	69929
2230 767 997 LBR-S&M CINDER/FLYASH RECOVER?	0	-436	0%	-
2230 781 997 LBR-S&M MATERIAL HANDLING	63			75c
2230 791 997 LBR-S&M FLYASH HANDLING	95		0%	1137
TOTAL STEAM - AREA A	249,271	156,016	63%	2,991,254
THE OTHER THEFT			=====	

.... END REPORT

```
Area A Monthly Usage Report
    Sum of individual boilers output (Steam Produced') = 695, 702,000 lbs
     Bldg net stoam output = Sum - Internal consumption (DA, trustum, etc.)
- 695.7 m lbs x . 836 = 581, 607, or 160
                              35,693 × 2000 × 14,100 16 =
                                                               1,007 mm Btu
     Bhi contact of roal=
     Cost of FW for makey water = (Steam rate Cond. return + blowdown) FW unit
                                           60% + 7% = SRx 1.53
                     = 695,702,000 ×1.53 × . 148 / 1000 gal = 3,700/yr
     Costy electricity (motors, precipitators electrons)

164,000 KWH × . 035 ± ×12m=

KWH cist fr"B"
      costor flyant desperal ( 5, 163 cy.) × 37.00 =
      cost of Water treatment Chemicals; Rot
                   Ruch Salt 101, 04 pt x . 02 1/16 = $2,020
                   Caustic 515, 718 16 × .0438 16 = 22,588
                 Sulfure Aad 132,584 x .035 16 = 4640
 Out-of-Packet Steam Cost =
               (545 x 35693) + 68.880 + 29.250 + 3700 + 5,000 + 23,950 = 1.74 million
                                                                                  581,607 Klbs
                                    581,607,000
                             1000 lbs | Not counting Maintenance tosts of Actual cost for plant
BUTUF Pocket =
                     3.00
Steam cust
                                                                           39, 795 (Mayor)
                                                                          728,795
                                                                     JBouchillon
                            = 5.92 $\frac{1}{\kilos
                                                          225
```

COST

FOR

STEAM

1994 OUT-OF-PUCKET

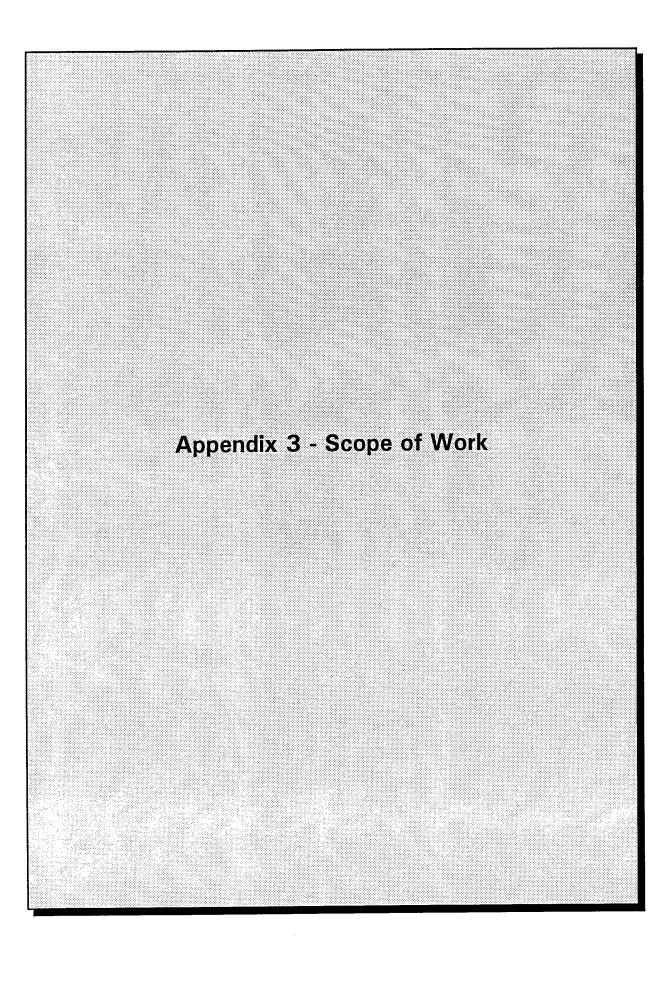
Month	Steam Produced (K Lbs.)	Evapo- ration Rate (%)	A-8 Coal (Tons)	A-8 Cinders Shipped (Cu.Yds.)		Flyash Shipped Off-Site)(Cu.Yds.)	Disodium Phosphate (Lbs.)	Sodium Sulfite (Lbs.)	Rock Salt (Lbs.)	Sulfuric Acid (Lbs.)	Gas Producers (K Cu. Ft.)	A-10 Ga Produce Coal (Tons)
Jan. 92	89,572.0	10.1	4,369.3	776.0	726.0	+	108.0	83.0	1,040.0	9,118.0	96,890.0	1,147
Feb. 92	•	9.9	3,919.2	737.0	660.0	33.0	101.0	60.0	11,440.0	6,913.0	103,263.0	1,079
Mar. 92		9.8	4,644.0	904.0	759.0			63.0	9,360.0	11,682.0	136,934.0	1,313
Apr. 92		9.4	4,229.0	790.0	793.0			96.0	3,120.0	9,365.0	110,228.0	1,189
May 92	-	9.0	4,591.1	986.5	726.0			72.0	3,000.0	11,663.0	104,003.0	1,038
Jun. 92	-	10.1	3,050.4	584.5	660.0			65.0	27,760.0	9,227.0	65,752.0	759
Jul. 92		9.6	4,257.0	951.0	693.0			67.0	2,080.0	9,075.0	120,189.0	1,166
Aug. 92		9.6	4,191.1	612.0	693.0		111.0	64.0	1,440.0	9,953.0	96,179.0	1,035
Sep. 92	•	9.7	4,431.1	738.0	942.0		140.0	51.0	11,960.0	9,600.0	83,983.0	907
Oct. 92	•	9.6	4,051.2	707.0	726.0		147.0	84.0	8,320.0	8,153.0	93,234.0	1,001
Nov. 92	•	9.1	4,131.4	847.0	647.0		125.0	51.0	1,040.0	7,716.0	55,267.0	695
Dec. 92	90,986.0	9.4	4,762.6	896.0	726.0	330.0	159.0	50.0	11,440.0	11,526.0	88,910.0	996
TOTALS	988,917.0	9.8	50,627.4	9,529.0			1,575.0	806.0	92,000.0	113,991.0	1,154,832.0	12,331
AVERAGE	82,409.8	9.6	4,218.9	794.1	729.3	192.0	131.3	67.2	7,666.7	9,499.3	96,236.0	1,027
Jan. 93	100,650.0	9.2	5,376.2	950.0	198.0	743.0	169.0	48.0	7,280.0	5,231.0	103,278.0	1,041
Feb. 93	83,448.0	9.5	4,328.2	810.0	363.0	624.0	159.0	41.0	7,280.0	4,629.0	62,995.0	685
Mar. 93	87,670.0	9.2	4,720.6	806.0	363.0	684.0	117.0	35.0	7,280.0	9,323.0	75,983.0	901
Apr. 93		9.3	4,392.6	701.0	462.0	495.0	120.0	39.0	4,160.0	7,022.0	62,280.0	659
May 93	79,146.0	9.4	4,180.9	671.0	462.0	462.0	105.0	33.0	9,360.0	11,692.0	57,611.0	657
Jun. 93		9.6	3,508.5	548.0	594.0	363.0	117.0	33.0	18,300.0	6,971.0	58,734.0	667
Jul. 93		10.1	4,492.3	1,053.0	495.0		122.0	30.0	8,320.0	18,223.0	87,087.0	878
Aug. 93		9.4	4,121.9	927.0	726.0		119.0	50.0	2,080.0	8,802.0	74,643.0	861
Sep. 93		9.3	4,029.5	987.0	462.0		118.0	27.0	2,080.0	10,587.0	62,690.0	710
Oct. 93		9.5	4,430.7	968.0	462.0		114.0	40.0	6,240.0	9,996.0	58,347.0	736
Nov. 93		9.5	4,158.0	800.5	396.0		143.0	36.0	16,640.0	16,347.0	61,650.0	766
Dec. 93	86,196.0	10.9	3,914.5	929.0	330.0	528.0	171.0	44.0	7,500.0	9,364.0	37,161.0	517
	1,000,304.0	9.7	51,653.9	10,150.5			1,574.0	456.0	96,520.0	118,187.0	802,459.0	9,083
AVERAGE	83,358.7	9.6	4,304.5	845.9	442.8	478.9	131.2	38.0	8,043.3	9,848.9	66,871.6	756
Jan. 94	87,958.0	9.0	4,860.2	785.0	231.0	775.0	140.0	48.0	2,520.0	23,110.0	6,525.0	292.
Feb. 94	57,326.0	9.4	3,027.1	698.0	400.0	231.0	109.0	29.0	14,000.0		10,588.0	108
Mar. 94	75,534.0	9.8	3,836.5	733.0	495.0	198.0	102.0	30.0	11,440.0	8,342.0		
Apr. 94	62,478.0	9.8	3,179.0	618.0	429.0	231.0	119.0	32.0	10,640.0	3,301.0		
May 94	60,546.0	9.8	3,102.3	522.0	348.0	242.0	105.0	80.0	4,960.0	10,960.0		
Jun. 94	51,624.0	10.0	2,578.8	457.0		512.0	96.0	38.0	4,220.0	11,314.0		
Jul. 94		10.4	2,397.1	481.0		482.0	92.0		7,220.0	20,889.0		
Aug. 94		9.9	2,615.9	427.0		479.0			10,400.0			
Sep. 94		9.3	2,534.2	474.0		462.0			21,080.0	21,028.0		
Oct. 94		9.8	2,512.2	591.0		561.0		44.0	2,040.0	1,159.0		
Nov. 94		10.1	2,649.9	534.0		528.0		59.0	5,200.0	8,068.0		
Dec. 94	49,050.0	10.2	2,400.3	410.0	66.0	462.0	72.0	60.0	7,320.0	24,413.0		
TOTALS	695,702.0	9.7	35,693.5	6,730.0	1,969.0	5,163.0	1,191.0	488.0	101,040.0	132,584.0	17,113.0	401.
AVERAGE		9.8		560.8				44.4	8,420.0	13,258.4	8,556.5	



PAGE 2

		Filtered											
		Water	River Water		Aluminum	Hydrated	Caustic	Waste Water	r1			City	
		Produced	Produced	Chlorine	Sulfate	Lime	Soda	Pumped	Fuel	0	Drinking	Sewage	El€
	Month	(K Gals.)		(Lbs.)	(Lbs.)	(Lbs.)	(Lbs.)		0il	Propane		Treated	cit
						(103.)	(LDS.)	(K Gals.)	(Gals.)	(Gals.)	(K Gals.)	(K Gals.)	(K
	Jan. 92	47,258.0	· · · · · · · · · · · · · · · · · · ·		5,600.0		56,566.0	14,450.0 *			930.5	930.5	
	Feb. 92	53,507.0	•	95.0	6,100.0		59,347.0	15,780.0 *		150.0	409.1	409.1	
	Mar. 92	47,418.0	• • • • • •	126.0	7,050.0		51,082.0	15,640.0 *		100.0	334.1	334.1	1
	Apr. 92	46,571.0			6,400.0		41,462.0	16,120.0 *			602.9	602.9	1
	May 92	44,382.0	•	106.0	6,600.0		57,289.0	16,196.0 *		134.3	187.0	187.0	
	Jun. 92	41,631.0	•	92.0	5,700.0		35,651.0	15,920.0 *		155.0	230.8	230.8	1
	Jul. 92	57,653.0	•	141.0	6,550.0	1,400.0	36,536.0	16,430.0 #		50.0	239.7	239.7	I
	Aug. 92	53,129.0	•	111.0	6,450.0	400.0	52,636.0	17,614.0 *		50.0	177.2	177.2	1
	Sep. 92	43,154.0	581,703.0	87.0	5,650.0		51,749.0	18,204.0 *		75.0	196.9	196.9	1
	Oct. 92	46,122.0	•	105.0	6,550.0		53,017.0	16,900.0 *		95.0	331.7	331.7	1
	Nov. 92	46,995.0	•	86.0	6,150.0	50.0		19,400.0 *	197.0	70.0	394.7	394.7	1
	Dec. 92	50,379.0	573,690.0	106.0	6,400.0	450.0		18,760.0 *	182.0	68.0	325.9	325.9	1
		•					•	,	101.0	00.0	323.7	323.7	
	TOTALS	578,199.0			75,200.0	2,300.0	556,021.0	201,414.0 *	379.0	877.3	4,360.5	4,360.5	11
_	AVERAGE	48,183.3	576,689.0	106.2	6,266.7	575.0	46,335.1	16,784.5 *	189.5	97.5	363.4	363.4	11
	an. 93	49,308.0	594,855.0	102.0	(050 0	1 000 0							
•	Feb. 93	43,342.0	523,392.0	102.0	6,950.0	1,000.0	•	17,337.0 *	138.0	65.0	321.8	321.8	
	Mar. 93	51,108.0	570,264.0	93.0	5,900.0	300.0	97,796.0	19,145.0 *	224.0	30.0	345.4	345.4	
	Apr. 93	48,552.0		109.0	7,600.0	350.0	60,260.0	25,763.0	104.0	155.0	375.4	375.4	1.
	May 93	47,880.0	585,066.0	105.0	6,600.0	350.0	39,796.0	23,073.0	26.0		450.0	450.0	
	Jun. 93	45,653.0	620,970.0	115.0	6,450.0	350.0	53,782.0	23,234.0	18.0		361.2	361.2	1.
	Jul. 93		598,032.0	111.0	5,250.0	250.0	83,718.0	23,604.0		175.2	265.4	265.4	
		47,284.0	693,060.0	117.0	5,600.0	650.0	98,570.0	24,452.0			267.5	265.4	1,
	Aug. 93	47,633.0	624,960.0	123.0	5,850.0	500.0	35,549.0	22,843.0			345.9	345.9	
	Sep. 93	43,568.0	604,800.0	139.0	5,550.0	500.0	37,112.0	19,102.0		25.0	345.6	345.6	1,
	Oct. 93	48,610.0	639,867.0		5,250.0	500.0	47,598.0	21,264.0			370.6	370.6	1,
	Nov. 93	46,145.0	627,030.0		5,750.0	450.0	26,742.0	19,323.0		10.0	397.7	397.7	-,
	Dec. 93	48,924.0	644,697.0		7,050.0		38,848.0	21,849.0		59.9	499.7	499.7	
	TOTALS	568,007.0	7,326,993.0	1,014.0	73,800.0	5.200.0	731,233.0	260,989.0	510.0	520 1	1 24/ 2		
	AVERAGE	47,333.9	610,582.8	112.7	6,150.0	472.7		21,749.1		520.1 74.3	4,346.2	4,344.1	11,
					,		***************************************	22,777.1	102.0	74.3	362.2	362.0	
	Jan. 94	50,300.0	639,306.0	.0	10,550.0		73,960.0	22,488.0	.0	25.0	644.9	644.9	
	Feb. 94	39,696.0	564,480.0	.0	6,050.0	150.0	55,270.0	19,804.0	.0	125.0	823.6	823.6	ı
	Mar. 94	43,723.0	624,960.0	.0	7,400.0		81,616.0	21,674.0	.0		548.6	548.6	1,(
	Apr. 94	40,687.0	599,130.0	.0	7,300.0		35,080.0	19,283.0	.0		581.9	581.9	٠,٠
	May 94	41,304.0	613,248.0	.0	4,300.0		35,297.0	20,726.0	.0	5.0	567.2	567.2	8
	Jun. 94	37,263.0	603,624.0	.0	5,350.0		46,352.0	17,886.0	.0		627.7	627.7	Ç
	Jul. 94	39,624.0	624,960.0	.0	7,300.0		33,083.0	16,685.0	.0		496.4	496.4	c
	Aug. 94	42,257.0	527,520.0	.0	5,200.0	450.0	56,917.0	15,087.0	.0		483.5	483.5	ç
4	ep. 94	34,361.0	604,758.0	.0	6,300.0		33,083.0	13,130.0	.0		533.7	533.7	1,0
1	t. 94	36,547.0	625,800.0	.0	5,600.0		33,565.0	12,525.0	.0		551.6	551.6	٤, د
	Nov. 94	35,920.0	584,640.0	.0	5,250.0		20,661.0	9,833.0			674.5	674.5	Ģ
	Dec. 94	37,857.0	624,960.0	.0	5,600.0		10,834.0	10,679.0			674.7	674.7	ç
	TOTALS	479,539.0	7,237,386.0	Λ	76 200 0	(00.0	(11, 710)	100 000 :					
	AVERAGE	39,961.6	603,115.5	.0 .0	76,200.0 6,350.0	600.0 300.0	515,718.d 42,976.5	199,800.0	.0			7,208.3	11,4
		,	,	. •	3,000.0	500.0	227	16,650.0	.0	51.7	600.7	600.7	•

	А	Rěa	A Evapo-	MO	NTH	₹ R	EFORT					
		Steam Produced	ration	A-8 Ccal	Produce Coal	kefrig- eration	Air Gompressor	Fuel	0	e Electricity		
	Month	(K Lbs.)	(2)	(Tons)	(Tons)	(Tons)) (K KW Hrs.)		
		-	۰									. 8
-		2 79568.9				9293.	9293.8			§ 826.9	مت	92 AN 77457 K/MO
و.		74798.8 75468.8	19.4 19.6									
	May 89	81345.5	9.9	4812.1	911.2	12963.1	12863.8	4.4	25.	9 795.4		
1989	Jun. 89 Jul. 89	89244.9 7113 9. 9	1 8.3 8.3									
	Aug. 89 Sea. 89	74852.8 78658.8	19.3		1936.9 1983.5	11587.4						
	Oct. 89	75686.9	18.6	3482.7	1234.6	11548.8	11548.9	5.6	75.	991.1	•	\$
5		84564. 5 79732. 5	! 1 ≸.2 .9.1		1838.7 986.7	11556.1					ſ	
अभेग विकास	TOTALS	929481.	~ 1 8. 28	45198.2	13494.5	133572.8	133572.6	1.1	471.	2 11658.#		
	Jan. 98 Feb. 98	85476. 8 6678 9. 9	15.1	4139.9	1152.2	3314.9	9992.	9.1 1.5	60.0	917.8	-	
	Mar. 95	78148.5		- 3646.7	857.9 1297.2	2866.8 3921.8	19329.9	9.1	65.4	967.8		
1/7/4	Apr. 9# May 9#	75362. 9 73356. 9	15.4	3562.1 3341.9	1986.8	3875.4 4288.9		1.f 1.f	29. J 25. J			
	Jun. 98 Jul. 98	81552.0 59107.0	19.3	3855.9 2751.3	1199.5 993.A	4698.5 4442.4		i.i i.i	45. 5			a sanda e entre
: f	Aug. 98	83342. Ø	19.7	3826.7	1976.9	4953.4	11795.6	6.8	1.5	626.5		
*	Sep. 98 Oct. 98	77218.8 77972.8	9.7 19.8	3883.9 3537.9	1154.9	4036.8 3697.6	11228.8 11779.8	9.9 18489.8	8. 9	83 3. 3 852. 6		
•	Nov. 99 Jec. 98	7789 9.\$ 97596. \$	18.2 11.5	3745.9 4185.J	989.6 1138.8	2597.8 2929.4	11315.5	8.8 3.8	59.9 19.9	784. <i>3</i> 641.2		
											•	
	TOTALS Jan. 91	933799.9 98882.8	18.78 13.16	43653.6 4466.8	13157.8	2544.2		9.9	437.3	19359.3		
	Feb. 91 Mar. 91	73648. 3 79624. 5	19.21 19.48	3688.2 3797.6	942.7 1286.9	228 9. 1 2779.2		1.1 202	148.8	648. <i>8</i> 651. <i>8</i>		
1001	Apr. 91 May 91	79948.9 84754.9	19.17	3885.5	1989.8	3\$29.6 2985.3		9.9 9.3	0.3 0.8	949. 2 762. 8		•
•	Jun. 91	78156.9	18.49 19.23	4848.8 3429.3	1996.3 89 3. 9	2278.9	11833.9	5.5	129.5	1946.8		
	Jul. 91 Aug. 91	77782. 8 85282. 8	18.84 18.37	3871.9 (4834.5	844.3	2261.2 3159.0		1.1 1.1	9.9 139.5	131 8.9 12 82.8		: *
2	Sep. 91 Oct. 91	79226.8 82338.9	18.18	3842.5	1091.2	2923.6 2686.9	11575.8 11121.9	8.9 9.8	9.2 15.5	1839.8 1849.8		
	Nov. 91	02338.8	19.15	3893.5	916.4	2000.7	11121.2	•••				
	Dec. 91						•					у.
Jan	TOTALS 8	9.572.0		38869.8 4,369.3	1#238.2_ 1,147.0		+0.622.0	1.1		9273. <u>3</u> 841.0		
	. 92 7' . 92 9:	9,422.0 2.748.0		3,919.2 4.644.0	1,079.7	2,636.3 3,591.0	95890.0 11,094.0		150.0 100.0			an and a second and a second and a second and a second and a second and a second and a second and a second and
Apr	. 92 8	1,590.0	9.4	4,229.0	1,313.9 1,189.1	2,755.4	11,212.0			889.0		A Participant
7992 May		1,530.0 2,588.0		4,591.1 3,050.4	1,038.8 759.8	2,978.6 2,141.8			134.3 155.0			
Jul. Aug.		3.096.0 1.898.0	9.6	4,257.0 4,191.1	1,166.9	3,506.5 3,140.0	11,031.0		50.0 50.0	1,062.0 1,017.0		
Sep.	92 87	,044.0	9.7	4,431.1	1,035.5 907.4	3,004.3	10,253.0		75.0 95.0	800.0		
75 34 - NOV.	92 76	,438.0 ,005.0		4,051.2 4,131.4	1,001.5 695.7	2,657.5 2,020.0	9,826.0 10,619.0	197.0		1,163.0 1,164.0		
Dec.	92 90	,986.0	9.4	4,762.6	996.5	2,429.4	11,843.0	182.0	68.0	854.0		•
		,917.0 ,650.0		0.627.4. 5,376.2	12,331.7	33,667_4 2,819.1	_128.851.0. 10,331.0	138.0	877.3 65.0	11.819.0 946.0		
Feb.	93 83	,448.0	9.5	4,328.2	1.041.3 685.9	1,895.7	9,980.0	224.0	30.0	956.0		
Mar. Apr.	93 82	,670.0 .862.0	9.3	4,720.6 4,392.6	901.8 659.5	2,046.2 1,670.1	11,517.0 10.458.0	104.0 26.0	155.0	1,087.0 957.0		
1993 Hay	93 79 93 68	,146.0 ,480.0	9.4	4.180.9 3,508.5	657.1 667.0	1,918.0 2,538.8	10,940.0 11,473.0	18.0	175.2	1,010.0 984.0		
Jul. Aug.	93 91	.788.0	10.1	1,492.3	878.5	3,275.1	11,903.0			1,098.0		
Sep.	76	,528.0 ,122.0	9.3	1,029.5	861.7 710.5	2,795.8	11,636.0 12,215.0		25.0	985.0 1,075.0		
Oct.	93 79	,538.0 ,876.0	9.5 9.5	1,430.7 1,158.0	736.1 766.8	2,248.9. 1,750.6	13,108.0 12,583.0	•	10.0	1,002.0 809.0		
T Dec.	93 86	.196.0		3,914.5	517.3	2,255.0	12,895.0		59.9	928.0		
	S 1,000		9.7 51				139,039.0	510.0	520.1	11,837.0		1/2
Jan. Feb.	94 57	,958.0 ,326.0	9.4 3	,860.2 3,027.1	292.7 108.3	1,801.2 431.3	12,863.0 11,306.0	.0	25.0	965.0 934.0		672 not 2 mass 17/10
Mar. Apr.		,534.0 ,478.0		3,836.5 3,179.0		1,960.2	12,588.0	.0	125.0	1,084.0		
Hay	94 60.	.546.0	9.8	.102.3		1,958.2 2.039.8	10,637.0 10,772.0	.0 .0	5.0	950.0 847.0		
Jun. Jul.				2,578.8 2,397.1		1.609.8	9,959.0	.0		906.0 950.0	-	
Aug. Sep	94 51. 94 46 ,	.806.0 974 .	9.9 2	2.615.9 2.5 54.2		1.971.1 1.641.5	9,834.0 9,226.0	.0 .0		960.0 1,012.0	. 2 4 5	7 - X
Tota			9.7 2	4	400.9	5.677.7			155.0	8,608.0		
				•								228





DEPARTMENT OF THE ARMY MOBILE DISTRICT, CORPS OF ENGINEERS P.O. BOX 2288-0001 Mobile, Alabama 36628-0001

22 June 1995

REPLY TO ATTENTION OF: Architect-Engineer Contracts Section

Affiliated Engineers SE, Inc.

Affiliated Engineers SE, Inc. 3300 SW Archer Road

JUN 2 6 1995

Gainesville, Florida 32608

Dear Mr. Miller:

Reference is made to Contract Number DACA01-94-D-0007, Delivery Order Number 003, for a Limited Energy Study for the Area A Package Boiler at Holston Army Ammunition Plant, TN.

We propose to modify referenced delivery order to provide for additional inspection effort in accordance with the enclosed Scope of Work..

Your are requested to prepare your fee proposal for accomplishing the additional work resulting from this change in sufficient detail to permit analysis thereof and submit it by 28 June 1995. Your proposal should be addressed as follows:

> District Engineer U.S. Army Engineer District, Mobile Attention: CESAM-EN-M/Mr. Dan Mizelle Post Office Box 2288 Mobile, Alabama 36628-0001

You are cautioned that no work or services for which an additional cost or fee will be charged should be furnished without the prior written authorization of the Contracting Officer.

If you have any questions concerning the work requirements, please contact Mr. Bill McClelland at telephone 334/441-6444.

Sincerely

O. B. Anderson

Authorized Representative of the Contracting Officer

Enclosure

CESAM-EN-DM 20 Jun 95

FY95 LIMITED ENERGY STUDY, AREA A PACKAGE BOILER HOLSTON ARMY AMMUNITION PLANT, TENNESSEE

MINIMUM REQUIREMENTS FOR INSPECTION OF EXISTING BOILERS AT VOLUNTEER ARMY AMMUNITION PLANT, TENNESSEE

- 1. Open all manway covers of both boilers and all handhole plates. Remove all internals to expose tube ends in steam drum. Open access to furnace area including base of chimney.
- 2. Perform in-depth visual internal and external inspection of the boilers to identify any condition that may affect the integrity of the pressure retaining components.
- 3. Remote Field Eddy Current (RFEC) testing of 25 percent of the boiler tubes to determine the amount of thinning that may have occurred during the life of the boiler. Each boiler has approximately one thousand 2-inch tubes. The inspector will determine which tubes to test.
- 4. Ultrasonic thickness measurements of shell and heads to identify any loss of thickness due to corrosion.
- 5. Ultrasonic thickness testing of the 2.75-inch membrane-attached tubes to identify any thinning that may have occurred.
- 6. Perform calculations to determine allowable operating pressure based on the obtained thicknesses, and compare with original design pressure of 375 psi at 442°F.
- 7. Provide labor and materials to replace gaskets for all manholes, handholes, and items removed for inspection prior to hydrostatic testing. Provide necessary blind flanges and gaskets on steam outlet to perform hydrostatic test.
- 8. Perform a hydrostatic test of each boiler to identify any abnormal condition not previously identified by other testing. Conduct the hydrostatic test at a pressure to be determined, based on the calculations for the shell, heads, and tubes, but not to exceed 150 percent of the original design pressure.
- 9. After hydrostatic testing is complete, drain boiler and dry internal parts in preparation for returning boiler to a lay-up condition.
- 10. Provide labor and material to replace desiccant in preparation for returning boilers to a lay-up condition. Closing of boilers will be the responsibility of the inspecting agency.

CESAM-EN-DM 20 Jun 95

11. Provide three spiral-bound copies of a detailed report on the conditions noted, results of all testing and inspections, including a color-coded tube layout diagram indicating the current thickness of all tubes examined with RFEC, calculations to verify the current maximum allowable working pressure of the tubes, shells and heads, recommendations to restore the boilers to a safe and reliable condition, a projected remaining useful life, and photographs, if required. Report to be delivered to AE not later than two weeks after testing is completed.

TASKS TO BE PERFORMED BY VOLUNTEER AAP PERSONNEL

- 1. Provide electrical power and water to building. Provide piping to boilers for hydrostatic test and means to drain boiler water after test.
- 2. Provide one copy of all prints and manufacturer's documents for the boilers to the inspecting group five working days prior to the scheduled inspection/testing, to be returned with the delivery of the final testing and inspection report to the AE.
- 3. Inspect boilers after all testing and inspections are complete to verify internals are dry prior to closure.

SCOPE OF WORK

FOR A

LIMITED ENERGY STUDY

AREA A PACKAGE BOILER

HOLSTON ARMY AMMUNITION PLANT, TN

Performed as part of the ENERGY ENGINEERING ANALYSIS PROGRAM (EEAP)

SCOPE OF WORK FOR A LIMITED ENERGY STUDY

AREA A PACKAGE BOILER HOLSTON ARMY AMMUNITION PLANT, TN

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- 7. WORK TO BE ACCOMPLISHED
 - 7.1 Review Previous Studies
 - 7.2 Perform a Limited Site Survey
 - 7.3 Evaluate Selected ECOs
 - 7.4 Combine ECOs into Recommended Projects7.5 Submittals, Presentations and Reviews

ANNEXES

- A DETAILED SCOPE OF WORK
- B EXECUTIVE SUMMARY GUIDELINE
- C REQUIRED DD FORM 1391 DATA

1. BRIEF DESCRIPTION OF WORK: The Architect-Engineer (AE) shall:

- 1.1 Review the previously completed Energy Engineering Analysis Program (EEAP) study which applies to the specific building, system, or energy conservation opportunity (ECO) covered by this study.
- 1.2 Perform a limited site survey of specific buildings or areas to collect all data required to evaluate the specific ECOs included in this study.
- 1.3 Evaluate specific ECOs to determine their energy savings potential and economic feasibility.
- 1.4 Provide project documentation for recommended ECOs as detailed herein.
- 1.5 Prepare a comprehensive report to document all work performed, the results and all recommendations.

2. GENERAL

- 2.1 This study is limited to the evaluation of the specific buildings, systems, or ECOs listed in Annex A, DETAILED SCOPE OF WORK.
- 2.2 The information and analysis outlined herein are considered to be minimum requirements for adequate performance of this study.
- 2.3 For the buildings, systems or ECOs listed in Annex A, all methods of energy conservation which are reasonable and practical shall be considered, including improvements of operational methods and procedures as well as the physical facilities. All energy conservation opportunities which produce energy or dollar savings shall be documented in this report. Any energy conservation opportunity considered infeasible shall also be documented in the report with reasons for elimination.
- 2.4 The study shall consider the use of all energy sources applicable to each building, system, or ECO.
- 2.5 The "Energy Conservation Investment Program (ECIP) Guidance", described in letter from DAIM-FDF-U, dated 10 Jan 1994 establishes criteria for ECIP projects and shall be used for performing the economic analyses of all ECOs and projects. The program, Life Cycle Cost In Design (LCCID), has been developed for performing life cycle cost calculations in accordance with ECIP guidelines and is referenced in the ECIP Guidance. If any program other than LCCID is proposed for life cycle cost analysis, it must use the mode of calculation specified in the ECIP Guidance. The output must be in the format of the ECIP LCCA summary sheet, and it must be submitted for approval to the Contracting Officer.

- 2.6 The following definitions apply to terms used in this scope of work:
- 2.6.1 "Contracting Officer", "Contracting Officer's Representative", or Government's Representative" refer to the contracting office of the Mobile District, U. S. Army Corps of Engineers.
- 2.6.2 "Installation Commander", or "Installation Representative" refer to the military commander of Holston Army Ammunition Plant.
- 2.6.3 "Plant Manager", Operating Contractor", or "Operating Contractor's Representative" refer to the Holston Defense Corporation, which operates Holston Army Ammunition Plant under contract to the U.S. Army.
- 2.7 Energy conservation opportunities determined to be technically and economically feasible shall be developed into projects acceptable to installation personnel. This may involve combining similar ECOs into larger packages which will qualify for ECIP or O&M funding, and determining in coordination with installation personnel the appropriate packaging and implementation approach for all feasible ECOs.
- 2.7.1 Projects which qualify for ECIP funding shall be identified, separately listed, and prioritized by the Savings to Investment Ratio (SIR).
- 2.7.2 All feasible non-ECIP projects shall be ranked in order of highest to lowest SIR.
- 2.8 Metric Reporting Requirements: In this study, the analyses of the ECOs may be performed using English or Metric units as long as they are consistent throughout the report. The final results of energy savings for individual recommended projects and for the overall study will be reported in units of MegaBTU per year and in MegaWattHours per year. Paragraph 7.5.2 details requirements for the contents of the final submittal.

3. PROJECT MANAGEMENT

and a project Managers. The AE shall designate a project manager to serve as a point of contact and liaison for work required under this contract. Upon award of this contract, the individual shall be immediately designated in writing. The AE's designated project manager shall be approved by the Contracting Officer prior to commencement of work. This designated individual shall be responsible for coordination of work required under this contract. The Contracting Officer will designate a project manager to serve as the Government's point of contact and liaison for all work required under this contract. This individual will be the Government's representative.

3.2 Installation Assistance.

- a. The Installation Commander will designate an individual to coordinate between the AE and the Holston Defense Corporation. This individual will be the Installation Representative, and all correspondence with Holston Army Ammunition Plant will be addressed to his attention.
- b. The Plant Manager will designate an individual to assist the AE in obtaining information and establishing contacts necessary to accomplish the work required under this contract. This individual will be the Operating Contractor's Representative.
- 3.3 <u>Public Disclosures</u>. The AE shall make no public announcements or disclosures relative to information contained or developed in this contract, except as authorized by the Contracting Officer.
- 3.4 Meetings. Meetings will be scheduled whenever requested by the AE or the Contracting Officer for the resolution of questions or problems encountered in the performance of the work. The AE's project manager and the Government's representative shall be required to attend and participate in all meetings pertinent to the work required under this contract as directed by the Contracting Officer. These meetings, if necessary, are in addition to the presentation and review conferences.
- 3.5 <u>Site Visits, Inspections, and Investigations</u>. The **AE** shall visit and inspect/investigate the site of the project as necessary and required during the preparation and accomplishment of the work.

3.6 Records

- 3.6.1 The AE shall provide a record of all significant conferences, meetings, discussions, verbal directions, telephone conversations, etc., with Government representative(s) relative to this contract in which the AE and/or designated representative(s) thereof participated. These records shall be dated and shall identify the contract number, delivery order number, participating personnel, subject discussed and conclusions reached. The AE shall forward to the Contracting Officer within ten calendar days, a reproducible copy of the records.
- 3.6.2 The AE shall provide a record of requests for and/or receipt of Government-furnished material, data, documents, information, etc., which if not furnished in a timely manner, would significantly impair the normal progression of the work under this contract. The records shall be dated and shall identify the contract number and modification number, if applicable. The AE shall forward to the Contracting Officer within ten calendar days, a reproducible copy of the record of request or receipt of material.

- 3.7 <u>Interviews</u>. The AE and the Government's representative shall conduct entry and exit interviews with the Plant Manager before starting work at the installation and after completion of the field work. The Government's representative shall schedule the interviews at least one week in advance.
- 3.7.1 Entry. The entry interview shall describe the intended procedures for the survey and shall be conducted prior to commencing work at the facility. As a minimum, the interview shall cover the following points:
 - a. Schedules.
 - b. Names of energy analysts who will be conducting the site survey.
 - c. Proposed working hours.
 - d. Support requirements from Holston Defense Corporation (HDC).
- 3.7.2 Exit. The exit interview shall briefly describe the items surveyed and probable areas of energy conservation. The interview shall also solicit input and advice from the Plant Manager.
- 4. <u>SERVICES</u> <u>AND MATERIALS</u>. All services, materials (except those specifically enumerated to be furnished by the Government), labor, supervision and travel necessary to perform the work and render the data required under this contract are included in the lump sum price of the contract.
- 5. PROJECT DOCUMENTATION. All energy conservation opportunities which the AE has considered shall be included in one of the following categories and presented in the report as such:
- 5.1 ECIP Projects. To qualify as an ECIP project, an ECO, or several ECOs which have been combined, must have a construction cost estimate greater than \$300,000, a Savings to Investment Ratio (SIR) greater than 1.25 and a simple payback period of less than ten years. The overall project and each discrete part of the project shall have an SIR greater than 1.25. All projects meeting the above criteria shall be arranged as specified in paragraph 2.7.1 and shall be provided with programming documentation. Programming documentation shall consist of a DD Form 1391 and life cycle cost analysis (LCCA) summary sheet(s) (with necessary backup data to verify the numbers presented). A life cycle cost analysis summary sheet shall be developed for each ECO and for the overall project when more than one ECO are combined. The energy savings for projects consisting of multiple ECOs must take into account the synergistic effects of the individual ECOs.

- 5.2 Non-ECIP Projects. Projects which do not meet ECIP criteria with regard to cost estimate or payback period, but which have an SIR greater than 1.25 shall be documented. Projects or ECOs in this category shall be arranged as specified in paragraph 2.7.2 and shall be provided with the following documentation: the life cycle cost analysis (LCCA) summary sheet completely filled out, a description of the work to be accomplished, backup data for the LCCA, ie, energy savings calculations and cost estimate(s), and the simple payback period. The energy savings for projects consisting of multiple ECOs must take into account the synergistic effects of the individual ECOs. In addition these projects shall have the necessary documentation prepared, as required by the Government's representative, for one of the following categories:
- a. Federal Energy Management Program (FEMP) Projects. A FEMP (or O&M Energy) project is one that results in needed maintenance or repair to an existing facility, or replaces a failed or failing existing facility, and also results in energy savings. The criteria are similar to the criteria for ECIP projects, ie, SIR ≥ 1.25 , and simple payback period of less than ten years. Projects with a construction cost estimate up to \$1,000,000 shall be documented as outlined in par 5.2 above; projects over \$1,000,000 shall be documented on 1391s. In the FEMP program, a system may be defined as "failed or failing" if it is inefficient or technically obsolete. However, if this strategy is used to justify a proposed project, the equipment to be replaced must have been in use for at least three years.
- b. Low Cost/No Cost Projects. These are projects which the Plant Manager can perform using his resources. Documentation shall be as required by the Plant Manager.
- 5.3 <u>Nonfeasible ECOs</u>. All ECOs which the AE has considered but which are not feasible, shall be documented in the report with reasons and justifications showing why they were rejected.
- 6. <u>DETAILED SCOPE OF WORK</u>. See Annex A.
- 7. WORK TO BE ACCOMPLISHED.
- 7.1 Review Previous Studies. Review the previous EEAP study which applies to the specific building, system, or ECO covered by this study. This review should acquaint the AE with the work that has been performed previously. Much of the information the AE may need to develop the ECOs in this study may be contained in the previous study.
- 7.2 <u>Perform a Limited Site Survey</u>. The AE shall obtain all necessary data to evaluate the ECOs or projects by conducting a site survey. However, the AE is encouraged to use any data that may have been documented in a previous study. The AE shall document his site survey on forms developed for the survey, or standard forms, and submit these completed forms as part of the report. All test and/or measurement equipment shall be properly calibrated prior to its use.

- 7.3 Evaluate Selected ECOs. The AE shall analyze the ECOs listed in Annex A. These ECOs shall be analyzed in detail to determine their feasibility. Savings to Investment Ratios (SIRs) shall be determined using current ECIP guidance. The AE shall provide all data and calculations needed to support the recommended ECO. All assumptions and engineering equations shall be clearly stated. Calculations shall be prepared showing how all numbers in the ECO were figured. Calculations shall be an orderly step-by-step progression from the first assumption to the final number. Descriptions of the products, manufacturers catalog cuts, pertinent drawings and sketches shall also be included. A life cycle cost analysis summary sheet shall be prepared for each ECO and included as part of the supporting data.
- 7.4 Combine ECOs Into Recommended Projects. During the Interim Review Conference, as outlined in paragraph 7.5.1, the AE will be advised of the Plant Manager's preferred packaging of recommended ECOs into projects for implementation. Some projects may be a combination of several ECOs, and others may contain only one. These projects will be evaluated and arranged as outlined in paragraphs 5.1, 5.2, and 5.3. Energy savings calculations shall take into account the synergistic effects of multiple ECOs within a project and the effects of one project upon another. The results of this effort will be reported in the Final Submittal per par 7.5.2.
- 7.5 <u>Submittals, Presentations and Reviews</u>. The work accomplished shall be fully documented by a comprehensive report. report shall have a table of contents and shall be indexed. and dividers shall clearly and distinctly divide sections, subsections, and appendices. All pages shall be numbered. Names of the persons primarily responsible for the project shall be included. The AE shall give a formal presentation of the interim submittal to installation, command, and other Government personnel. Slides or view graphs showing the results of the study to date shall be used during the presentation. During the presentation, the personnel in attendance shall be given ample opportunity to ask questions and discuss any changes deemed necessary to the study. A review conference will be conducted the same day, following the presentation. Each comment presented at the review conference will be discussed and resolved or action items assigned. It is anticipated that the presentation and review conference will require approximately one working day. The presentation and review conference will be at the installation on the date agreeable to the Plant Manager, the AE and the Government's representative. The Contracting Officer may require a resubmittal of any document(s), if such document(s) are not approved because they are determined by the Contracting Officer to be inadequate for the intended purpose.
- 7.5.1 Interim Submittal. An interim report shall be submitted for review after the field survey has been completed and an analysis has been performed on all of the ECOs. The report shall indicate the work which has been accomplished to date, illustrate the methods and justifications of the approaches taken and contain

- a plan of the work remaining to complete the study. Calculations showing energy and dollar savings, SIR, and simple payback period of all the ECOs shall be included. The results of the ECO analyses shall be summarized by lists as follows:
- a. All ECOs eliminated from consideration shall be grouped into one listing with reasons for their elimination as discussed in par 5.3.
- b. All ECOs which were analyzed shall be grouped into two listings, recommended and non-recommended, each arranged in order of descending SIR. These lists may be subdivided by building or area as appropriate for the study. The AE shall submit the Scope of Work and any modifications to the Scope of Work as an appendix to the report. A narrative summary describing the work and results to date shall be a part of this submittal. At the Interim Submittal and Review Conference, the Government's and AE's representatives shall coordinate with the Plant Manager to provide the AE with direction for packaging or combining ECOs for programming purposes and also indicate the fiscal year for which the programming or implementation documentation shall be prepared. The survey forms completed during this audit shall be submitted with this report. The survey forms only may be submitted in final form with this submittal. They should be clearly marked at the time of submission that they are to be retained. They shall be bound in a standard three-ring binder which will allow repeated disassembly and reassembly of the material contained within.
- 7.5.2 Final Submittal. The AE shall prepare and submit the final report when all sections of the report are 100% complete and all comments from the interim submittal have been resolved. The AE shall submit the Scope of Work for the study and any modifications to the Scope of Work as an appendix to the submittal. The report shall contain a narrative summary of conclusions and recommendations, together with all raw and supporting data, methods used, and sources of information. The report shall integrate all aspects of the study. The recommended projects, as determined in accordance with paragraph 5, shall be presented in order of priority by SIR. The lists of ECOs specified in paragraph 7.5.1 shall also be included for continuity. The final report and all appendices shall be bound in standard three-ring binders which will allow repeated disassembly and reassembly. The final report shall be arranged to include:
- a. An Executive Summary to give a brief overview of what was accomplished and the results of this study using graphs, tables and charts as much as possible (See Annex B for minimum requirements).
- b. The narrative report describing the problem to be studied, the approach to be used, and the results of this study.

- c. Documentation for the recommended projects (includes LCCA Summary Sheets).
 - d. Appendices to include as a minimum:
 - Energy cost development and backup data Detailed calculations
 - 2)
 - 3) Cost estimates
 - 4) Computer printouts (where applicable)5) Scope of Work

ANNEX A

DETAILED SCOPE OF WORK

- 1. The facility to be studied in this contract is the central steam plant for Area A at Holston Army Ammunition Plant (HSAAP) in Kingsport, Tennessee. Holston Army Ammunition Plant is a government-owned, contractor-operated (GOCO) facility. The operating contractor is the Holston Defense Corporation (HDC). For reasons of safety and security, access to the plant is controlled. Temporary passes will be required for both personnel and vehicle access. Some field work will also be required at Volunteer Army Ammunition Plant near Chattanooga, Tennessee.
 - a. A one-week notice should be given by the AE prior to any visit. This time will be needed to make the necessary arrangements for the visit.
 - b. The AE should submit a list of the equipment and instruments they plan to use prior to their arrival. Because of the nature of HSAAP operations, safety regulations prohibit and restrict the use of some equipment on the installation. Having a list of the equipment to be used beforehand, HSAAP will be better prepared at the entrance interview to address the regulations pertaining to the equipment to be used. This will also facilitate coordination of the inspection and permitting of the equipment.
- 2. The following persons have been designated as points of contact and liaison for all work required under this contract. Mr. Scott Shelton shall be the Installation Representative, and Mr. J. L. Bouchillon shall be the Operating Contractor's Representative.
- 3. Completion and Payment Schedule: The following schedule shall be used as a guide in approving payments on this contract. The final report for this study shall be due not later than 180 days after Notice to Proceed.

MILESTONE	PERCENT OF CONTRACT AMOUNT AUTHORIZED FOR PAYMENT
Completion of Field Work Receipt of Interim Submittal Completion of Interim Presentation & Receipt of Final Report	25 75 Review 85 100

4. Purpose and Background: The purpose of this study is to identify and evaluate the technical and economic feasibility of alternate methods of meeting the steam requirements of the Area A industrial complex. The Area A steam plant was constructed during World War II to serve an industrial complex that produces raw materials used in the manufacture of explosives. There are seven coal-fired boilers which generate steam at 400 psig and 575°F. Each boiler has a full-load capacity of at least

- 100,000 pph. At current production levels, steam requirements can be met by using two boilers; sometimes only one is needed. Future production levels are projected to be even lower, requiring only one boiler to operate at part load. This method of operation would be very inefficient; therefore, HDC would like to evaluate other possibilities for meeting the steam needs of Area A. Following are some points which should be
 - a. Evaluate using a pair of gas-fired package boilers of sufficient capacity at the existing plant. Location will be as directed by HDC; package boiler stacks will be tied into existing plant stack.
 - b. The process and heating needs of Area A are such that it would be preferable to use the existing distribution system rather than using multiple boilers at various sites.
 - c. Existing steam-driven chillers are being replaced with electric. This project should be complete by March 1996. For purposes of this study, assume the project to be complete.
- d. There are two Babcock-Wilcox, natural-gas, packaged water-tube boilers laid away at Volunteer Army Ammunition Plant. They each have a capacity of 150,000 pph at 375 psig. They were installed in 1972, and were last used about 1980. A visual, external inspection was conducted in 1994; a copy of the report is furnished. Can these boilers be used at Area A? Would any repairs or modifications be needed? What would be the cost of relocating these boilers?
- e. To what extent can the existing ancillary equipment (deaerator, feedwater heater, feedwater pumps, etc) in the plant be used with the package boilers? The boilers at Volunteer AAP include ancillary equipment. If these boilers are used, can their ancillary equipment be used also?
- f. Maintenance and operations costs and savings must be included in the evaluation. One of the costs that must be considered is the cost to lay away existing Building 8-A if a gas-fired package boiler is recommended to replace the existing coal-fired boilers. HDC has written plans and procedures that must be followed for lay-away.
- g. HDC currently pays an uninterruptible rate for natural gas due to process requirements; this is not likely to change. However, the package boilers should have dual-fuel (no.2 fuel oil) capability in the event of an emergency. Evaluate adequacy of current DF2 storage capacity, and include cost of additional storage if needed.
- h. Determine changes that would have to be made to the existing air pollution operating permit for the addition of the package boilers, and include costs in evaluation.

- i. Evaluate the possibility of using existing steam turbine drives to operate river water pumps which are presently electrically driven.
- 5. The boilers which are laid away at Volunteer Army Ammunition Plant must be inspected by a member of the National Board of Boiler and Pressure Vessel Inspectors to determine if they are suitable for the intended purpose and if any repairs or modifications will be needed.
- 6. Point of contact for entry to Volunteer Army Ammunition Plant is Mr. Jim Fry. Phone number (615) 855-7109.
- 7. An EEAP Limited Energy Study for Area A and Area B steam plants at HSAAP was completed by EMC Engineers, Inc. in August of 1992. The final report of this study includes a very good physical and operational description and a mathematical model of each plant. The AE is encouraged to read and use the information provided in this report.
- 8. Government-furnished information. The following documents will be furnished to the AE:
 - a. Final Report; LIMITED ENERGY STUDIES, HOLSTON ARMY AMMUNITION PLANT, KINGSPORT, TENNESSEE; August 1992; EMC Engineers, Inc.
 - b. MEMORANDUM, dated 5 October 1994, Subject: Trip Report T.
 - A. 7881 Volunteer Army Ammo Plant.
 - c. Energy Conservation Investment Program (ECIP) Guidance, dated 10 Jan 1994 and the latest revision with current energy prices and discount factors for life cycle cost analysis.
 - d. AR 420-49, Heating, Energy Selection and Fuel Storage, Distribution, and Dispensing Systems.
 - e. AR 415-15, 1 Jan 84, Military Construction, Army (MCA) Program Development
 - f. TM5-800-2, Cost Estimates, Military Construction.
 - g. Tri-Service Military Construction Program (MCP) Index, dated 13 February 1995.
 - h. Boiler plant logs for the Area A steam plant will be made available to the AE as needed.
- 9. A computer program titled Life Cycle Costing in Design (LCCID) is available from the BLAST Support Office in Urbana, Illinois for a nominal fee. This computer program can be used for performing the economic calculations for ECIP and non-ECIP ECOs. The AE is encouraged to obtain and use this computer program. The BLAST Support Office can be contacted at 144 Mechanical Engineering Building, 1206 West Green Street, Urbana,

Illinois 61801. The telephone number is (217) 333-3977 or (800) 842-5278.

10. Direct Distribution of Submittals. The AE shall make direct distribution of correspondence, minutes, report submittals, and responses to comments as indicated by the following schedule:

AGENCY

EXECUTIVE SUMMARIES REPORTS

FIELD NOTES CORRESPONDENCE

Commander Holston Army Ammunition Plant ATTN: SMCHO-EN (Mr Shelton) Kingsport, TN 37660-9982	3	3	1**	1
Commander U S AMC Installation and Service Activity ATTN: AMXEN-C (Mr Nache) Rock Island, IL, 61299-7190	1	1	_	_
Commander U. S. Army Corps of Engineers ATTN: CEMP-ET (Mr Gentil) 20 Massachusetts Avenue NW Washington, DC, 20314-1000	1*	_	-	-
Commander USAED, South Atlantic ATTN: CESAD-EN-TE (Mr Baggette) 77 Forsyth Street, SW Atlanta, GA 30335-6801	1	1	-	_
Commander USAED, Mobile ATTN: CESAM-EN-DM (Battaglia) PO Box 2288 Mobile, AL 36628-0001	2	2	1**	1
Commander U. S. Army Logistics Evaluation Agency ATTN: LOEA-PL (Mr Keath) New Cumberland Army Depot New Cumberland, PA, 17070 - 5007	1*	-	-	_

- Receives Executive Summary of final report only. Field Notes submitted in final form at interim submittal.

ANNEX B

EXECUTIVE SUMMARY GUIDELINE

- 1. Introduction.
- Building Data (types, number of similar buildings, sizes, etc.)
- 3. Present Energy Consumption of Buildings or Systems Studied.
 - o Total Annual Energy Used.
 - o Source Energy Consumption.

Electricity - KWH, Dollars, MBTU

Coal - TONS, Dollars, MBTU, MWH

Natural Gas - THERMS, Dollars, MBTU, MWH

Other - QTY, Dollars, MBTU, MWH

- 4. Energy Conservation Analysis.
 - o ECOs Investigated.
 - o ECOs Recommended.
 - o ECOs Rejected. (Provide economics or reasons)
 - o ECIP Projects Developed. (Provide list) *
 - o Non-ECIP Projects Developed. (Provide list)*
 - o Operational or Policy Change Recommendations.
- * Include the following data from the life cycle cost analysis summary sheet: the cost (construction plus SIOH), the annual energy savings (type and amount), the annual dollar savings, the SIR, the simple payback period and the analysis date.
- 6. Energy and Cost Savings.
 - o Total Potential Energy Savings in MegaBTU per year (and MegaWattHr per year) and first year dollar savings.
 - o Percentage of Energy Conserved.
 - o Energy Use and Cost Before and After the Energy Conservation Opportunities are Implemented.

ANNEX C

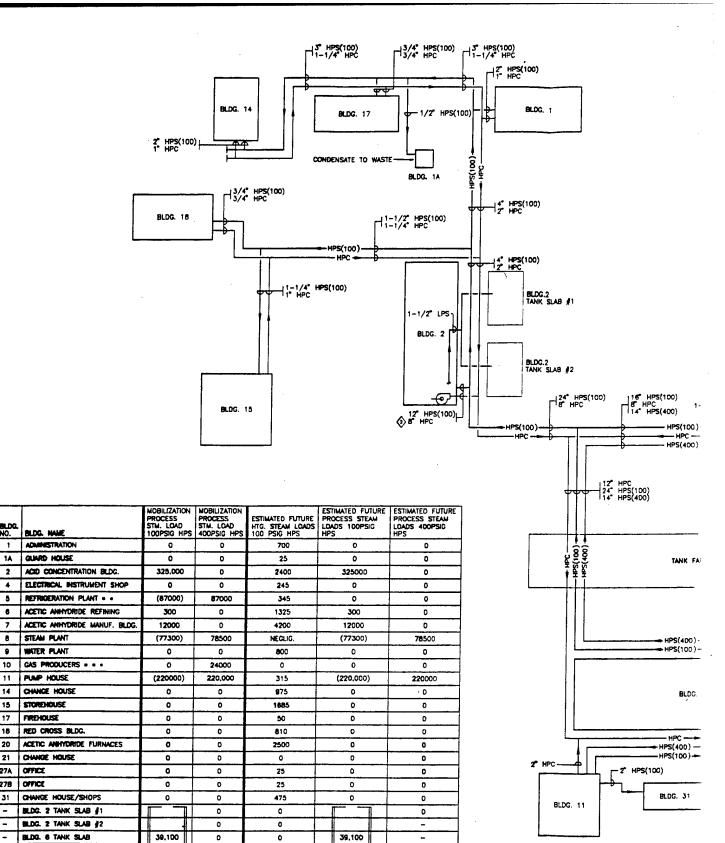
REQUIRED DD FORM 1391 DATA

To facilitate ECIP project approval, the following supplemental data shall be provided:

- a. In title block clearly identify projects as "ECIP."
- b. Complete description of each item of work to be accomplished including quantity, square footage, etc.
- c. A comprehensive list of buildings, zones, or areas including building numbers, square foot floor area, designated temporary or permanent, and usage (administration, patient treatment, etc.).
- d. List references, and assumptions, and provide calculations to support dollar and energy savings, and indicate any added costs.
- (1) If a specific building, zone, or area is used for sample calculations, identify building, zone or area, category, orientation, square footage, floor area, window and wall area for each exposure.
 - (2) Identify weather data source.
- (3) Identify infiltration assumptions before and after improvements.
- (4) Include source of expertise and demonstrate savings claimed. Identify any special or critical environmental conditions such as pressure relationships, exhaust or outside air quantities, temperatures, humidity, etc.
- e. Claims for boiler efficiency improvements must identify data to support present properly adjusted boiler operation and future expected efficiency. If full replacement of boilers is indicated, explain rejection of alternatives such as replace burners, nonfunctioning controls, etc. Assessment of the complete existing installation is required to make accurate determinations of required retrofit actions.
- f. Lighting retrofit projects must identify number and type of fixtures, and wattage of each fixture being deleted and installed. New lighting shall be only of the level to meet current criteria. Lamp changes in existing fixtures is not considered an ECIP type project.

- g. An ECIP life cycle cost analysis summary sheet as shown in the ECIP Guidance shall be provided for the complete project and for each discrete part included in the project. The SIR is applicable to all segments of the project. Supporting documentation consisting of basic engineering and economic calculations showing how savings were determined shall be included.
- h. The DD Form 1391 face sheet shall include, for the complete project, the annual dollar and MBTU (MWH) savings, SIR, simple amortization period and a statement attesting that all buildings and retrofit actions will be in active use throughout the amortization period.
- i. The calendar year in which the cost was calculated shall be clearly shown on the DD Form 1391.
- j. For each temporary building included in a project, separate documentation is required showing (1) a minimum 10-year continuing need, based on the installation's annual real property utilization survey, for active building retention after retrofit, (2) the specific retrofit action applicable and (3) an economic analysis supporting the specific retrofit.
- k. Nonappropriated funded facilities will not be included in an ECIP project without an accompanying statement certifying that utility costs are not reimbursable.
- 1. Any requirements required by ECIP guidance dated 10 Jan 1994 and any revisions thereto. Note that unescalated costs/savings are to be used in the economic analyses.
- m. The five digit category number for all ECIP projects except for Family Housing is 80000. The category code number for Family Housing projects is 71100.

Appendix 4 - Drawings



HTG. ONLY BLOGS. ESTIMATED AT 1258TU/FT2: PROCESS BLDGS ESTIMATED AT 358TU/FT2. ORIGINAL DESIGN INCLUDED BACK PRESSURE STEAM TURBINE DRIVEN REFRIGERATION COMPRESSORS WHICH HAVE BEEN (OR WILL BE) REPLACED BY ELECTRIC DRIVEN EQUIPMENT. GAS PRODUCERS LAST USED IN FEB. 1994.

(7900)



AREA 'A' STEAM



DES. HTG STM. LD 100PSIG

NEGLIG.

VLVS. CL.

BLDG. NO.

1A

27A OFFICE

278 OFFICE

PLDC NAME

ADMINISTRATION

CLIMPO HOLISE

STEAM PLANT

WATER PLANT

PUMP HOUSE

STOREHOUSE

CHANGE HOUSE

RED CROSS BLDG.

CHANGE HOUSE

TANK FARM

HEAT TRACING

TOTAL HEATING

NET TOTAL PRODUCTION

NET TOTAL STM RQD.

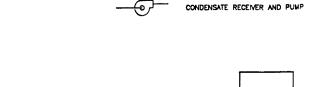
LEGEND

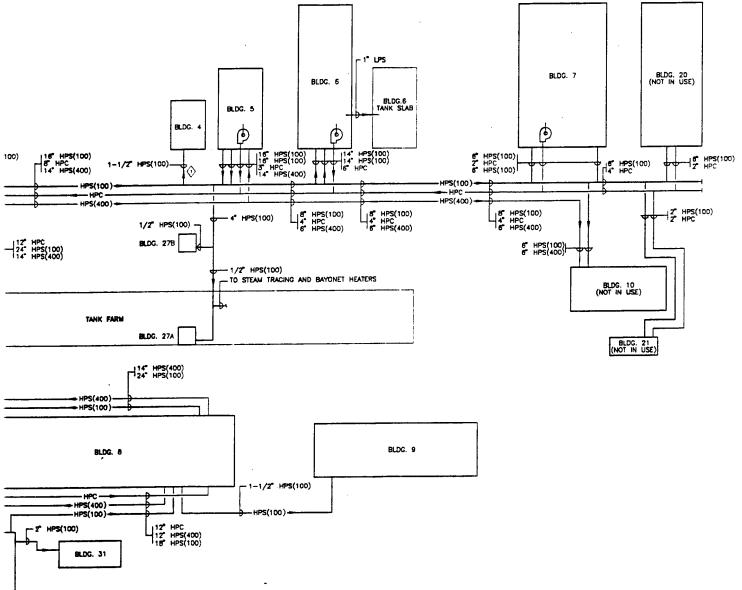
--- HPS(400) ---HIGH PRESSURE STEAM - 400 PSIG. 575'F --- HPS(150)--HIGH PRESSURE STEAM - 150 PSIG. 540°F - HPS(100)-HIGH PRESSURE STEAM - 100 PSIG. 400°F — нрс — HIGH PRESSURE CONDENSATE - UPS ----LOW PRESSURE STEAM - 20 PSIG DIRECTION OF FLOW

DRAWING NOTES

100 PSIG STEAM SUPPLY PIPE REDUCED FROM 1-1/2" TO 3/4" TO FEED BUILDING HEATING.

HIGH PRESSURE CONDENSATE PIPE REDUCED FROM 8" TO 2".

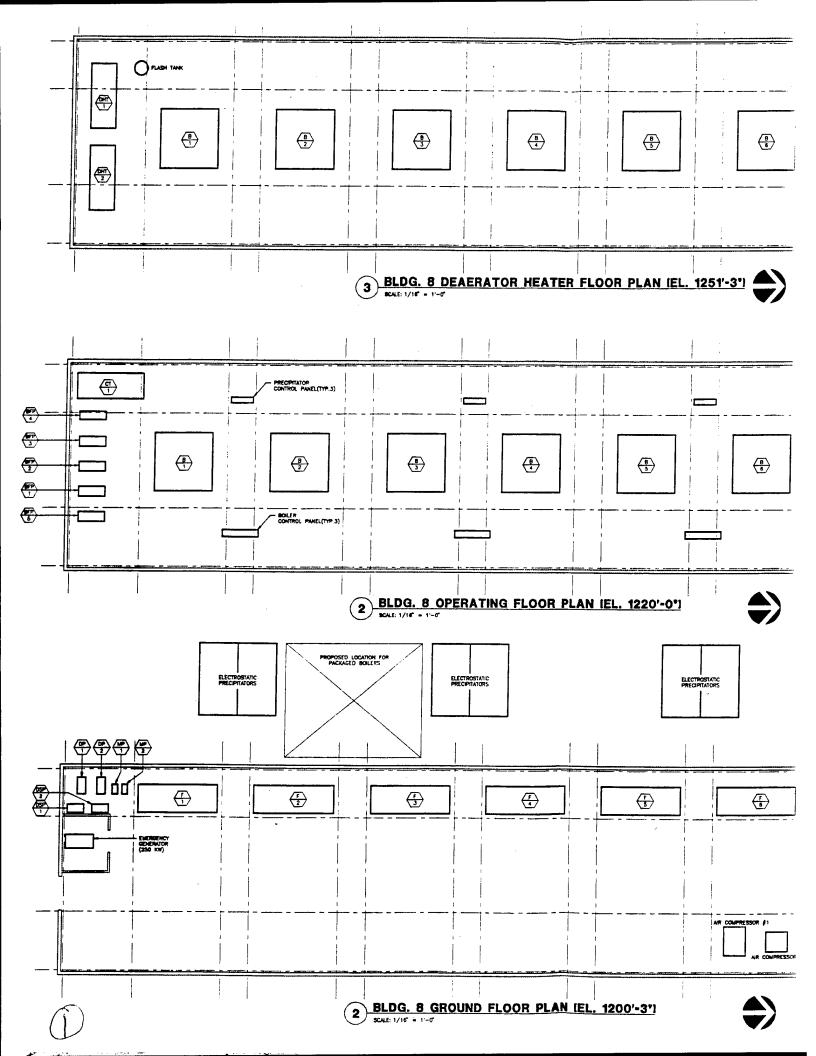


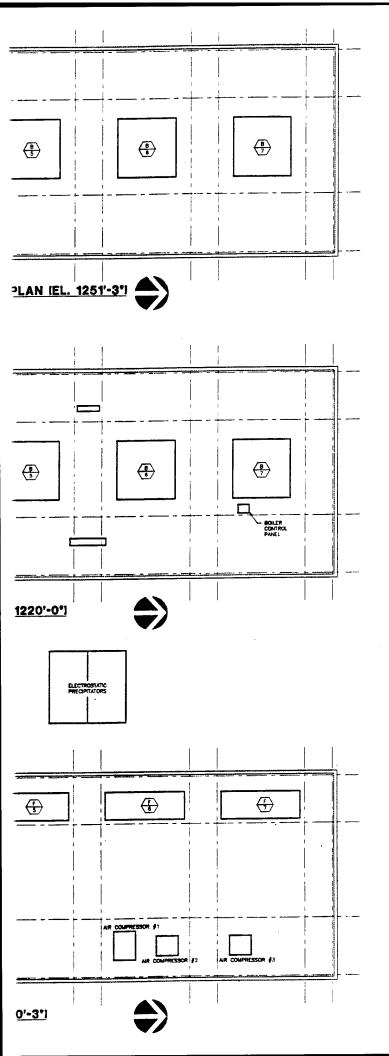


AREA 'A' STEAM & CONDENSATE DISTRIBUTION PIPING DIAGRAM

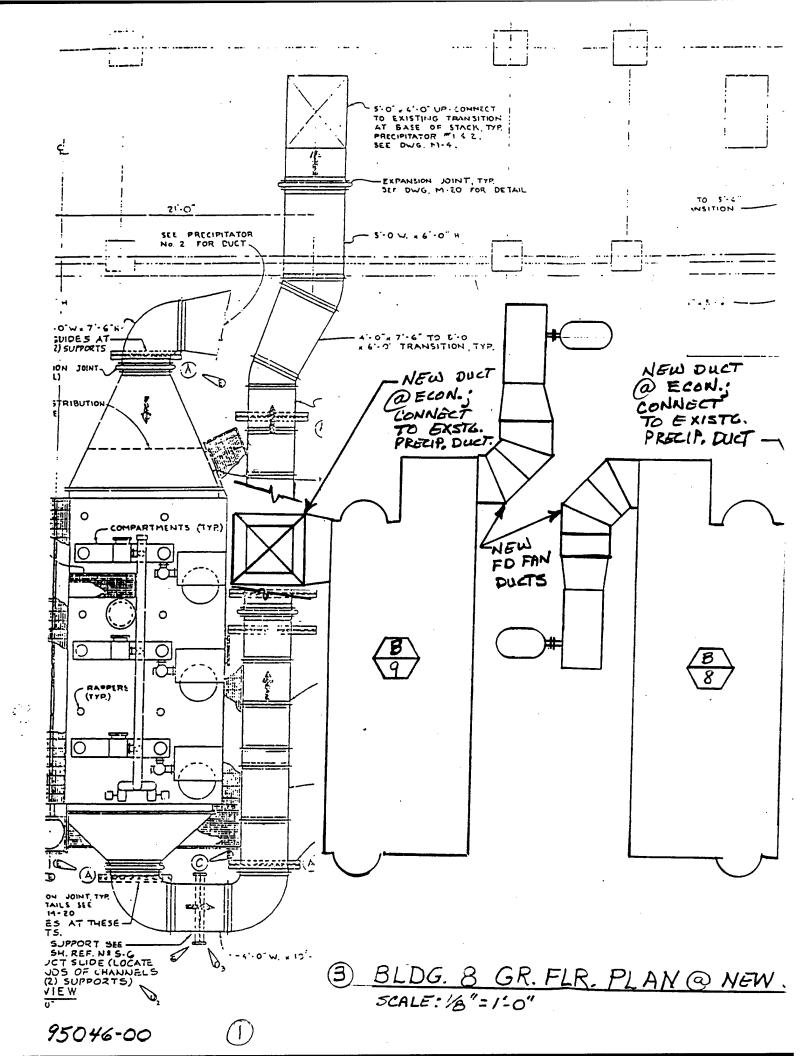
NOTE:
THIS DWG, IS DIAGRAMMATIC IN NATURE AND DOES NOT SHOW EXPANSION LOOPS,
STEAM TRAPS, ISOLATION VALVES, ACTUAL BUILDING SIZES, OR ACTUAL PIPE ROUTING.

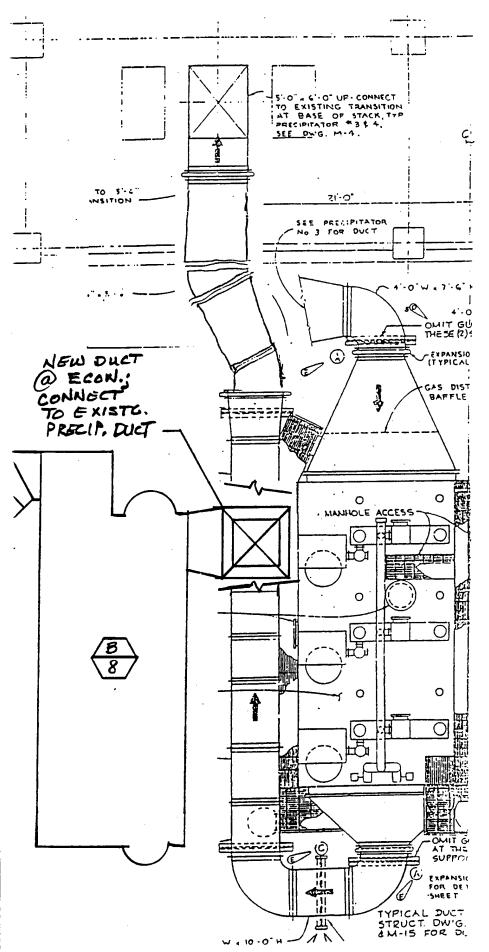








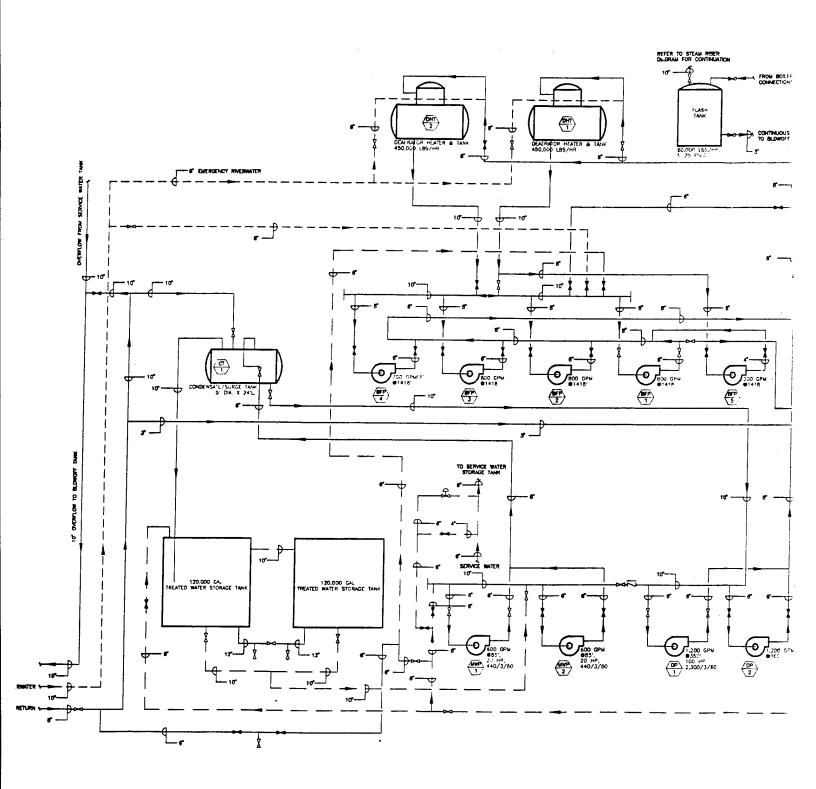


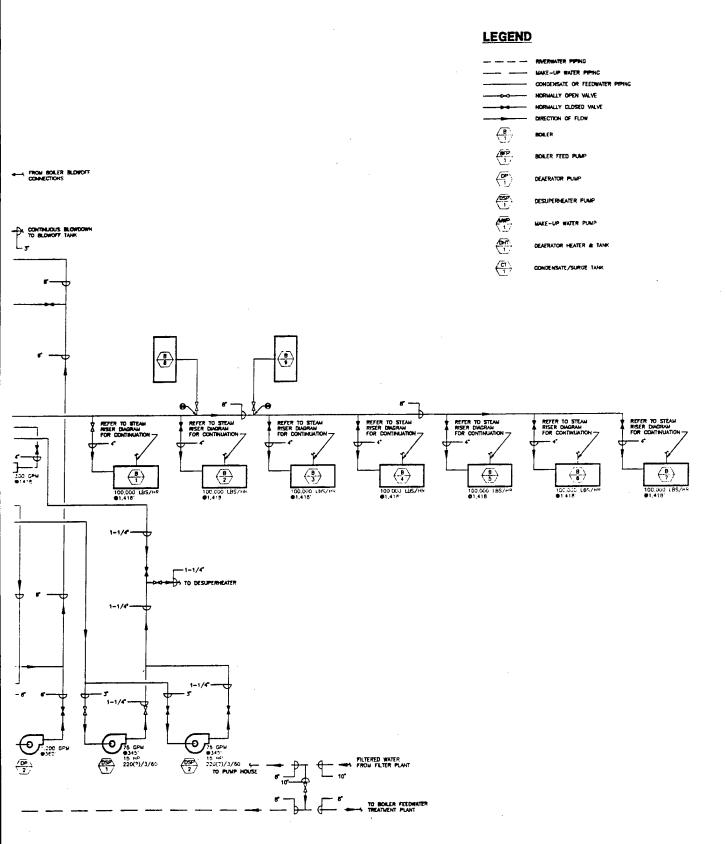




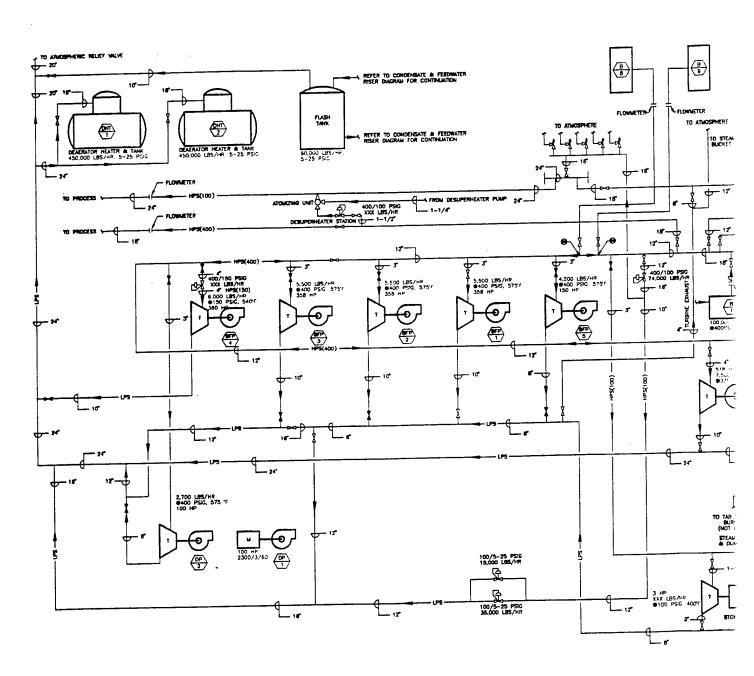
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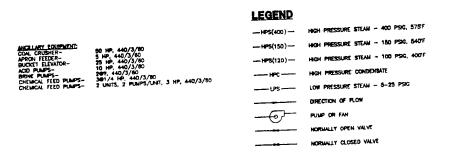


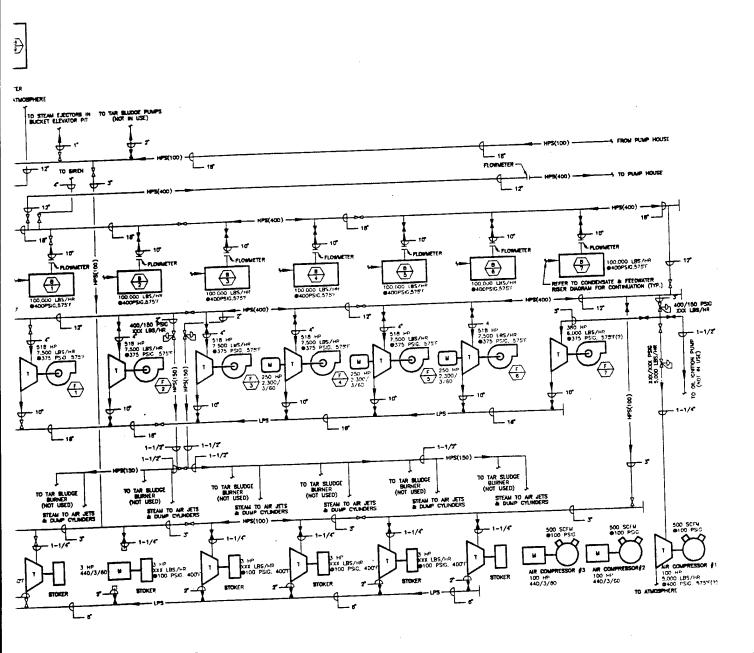




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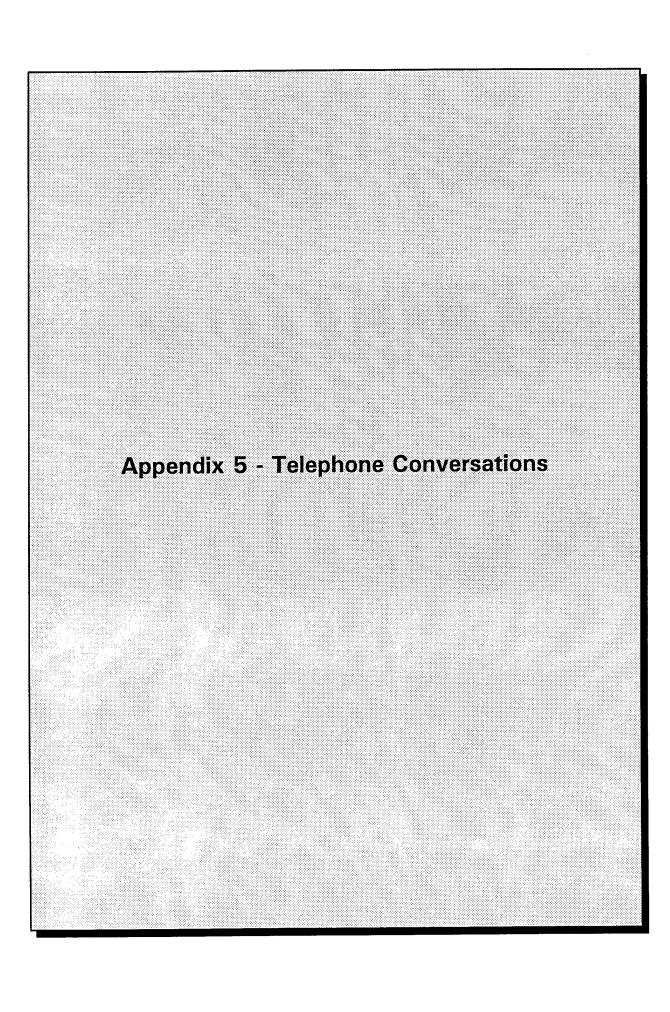














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WAYNO CERNY Conversation With	Routing
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Project Name	Date
Location	Time
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THAN FRIDAY -	
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THOY HAVE A CLE. BR. I	-NOUSTRIAL D-72
ON HAND (RETURN FROM OTHER	e RENTAL) WHICH
HO WILL BUDTE	
WILL ALSO QUOTE ON	A FIRETURA
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LIKE YORK-SHIPLEY.	



THE MIKE	RAMERS	4		
Conversation With ABCO INDUSTRIES			Routing 95096	-00
Representing HOLSTON BOILER			Project Number 10-24-5	75
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Project Name	Date
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FOR SYSTEM INCL. 750T FIRE	
CLEAVER-BROOKS) FOR SEMI-PERI	UANON
INSTAL, INSIDE A GOUT RUDG.	
PRICE FOR D.A. SKIDS	,
TRICE FOR D.IT. DRIDS	

	·

Fax Randy Green your Classified

or call (810 837-7370/ext.3 for more info. at (810)362-0317

Equipment For Rent

TEMPERATURE RENTAL **SPECIALISTS**

- Air Conditioners up to 60 tons
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nwide Availability 24 Hours A Dayl

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L CATEGORIES OF NEW COOLING EQUIPMENT AVAILA-FOR YOUR PROCESS AND COMFORT REQUIREMENT:

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C# SERVIDYNE # 1-800-241-8996

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ile Trailer or Sidd Mounted + 2 to 1,500 Ton Units fioning • Air Handlers • Commercial & Proce #: 800-486-9377; Fax: 713-930-1834 NTS: 800-331-6500; Fax: 410-242-369



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chilter up to 450 tons •Air cooled chilters 20 to 110 tons. Cold air units 10 to 75 tons. •Portable boiler rooms or skid mounted boilers 100 HP to 35,000 Lb/Hr.

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For water, steam and thermal oil. 1/2"-6" in bronze, W cast iron and ductile iron. Electric & pneum. actuators. PAXTON CORPORATION Phone (203) 929-1800 Fax (203) 925-8722

CIRCLE NO. 133

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BELOW WHOLESALE PLOTTERS!!! Hewlett-Packard 7550A, 7440A, Houston instruments DMP-52, calcomp 5902. Omnitech Gencorp (305) 599-

Equipment For Sale

Equipment For Sale/Rent

CHILLERS For Rent and Sale

WHEN KEEPING COOL IS CRITICAL

- ◆ 40-1,500 Tons
- HVAC, Industrial Process
- Engineered Solutions
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- ◆ R-134A, R-22, R717, R123
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REFRIGERANT ANALYSIS: Full service refrigeration chemistry laboratory offers ARI 700 and IRG-2 refrigerant analysis with guaranteed next day results. Preventive maintenance LUBRICANT ANALYSIS for determination of systems contaminants such as acidity, moisture, viscosity, and compressor wear metals. We provide refrigerant sample cylinders. oil test kits, sample cylinder cleaning, detailed sampling instructions and complete shipping information. For technical services or free consultation call INTEGRAL SCIENCES (800)745-8091.

Indoor Air Quality

HEAT PIPES

Decision Makers

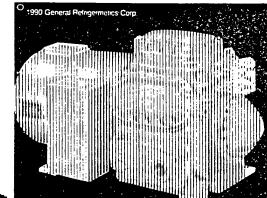
IAO & ENERGY SAVINGS

Dehumidification * Heat Recovery * Ventilation

AMERICAN HEAT PIPES INC. 515 Recker Hwy, * Auburndale, FL 33823 (800)727-6511

CIRCLE NO. 125

Equipment For Sale



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Carrier ·

YORK

Copeland



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EXEC. OFFICE: 19-35 Hazen St., East Elmhurst, N.Y. 11370

1 718 721-3600

86

Kennedy Tank & Mig Co inc Nationwide Boilers Inc Piley Stoker Corp

BOLER SERVICE, RENTAL ABCO Industries inc 100% Clayton Industries Indeck Power Equipment Co Nationwide Boilers inc

LER SERVICE, RETUBING 20 industries inc : A CONTRACTOR Soller & Tank Co Pater Soller Royance Bouler & Tank Co
Babcock & Wilcox
The Bigelow Co
General Electric Company,
Business info Center
Goltens
Indeck Power Equipment Co Kennedy Tank & Mfg Co Inc Nationwide Boilers Inc Riley Stoker Corp

Turnibuil & Sons Ltd

BOILER SERVICE, OTHER ABCO Industries Inc Cooperheat Inc, Heat Tracing Dept General Electric Company, Business Info Center Helmick Corp
Hationwide Boilers Inc
Pillorico Company

BOILER WATER TREATMENT, CHEMICAL SYSTEM

Alken-Murray Corp

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Ca Clark-Cooper Corp Clayton Industries Dearborn Div, W. R. Grace & Co. -exter Corp. Mogul Div

V/ASHLAND, Drew Industrial Div See Catalog Pages J-25—J-28)
The Duriron Co Inc, Filtration Systems Div THE FOXBORO COMPANY (See Ad Pages K-8, K-9) Garratt-Callahan Co GELBER PUMPS INC (See Ad Page 150) Herman Bogot & Co Hydrofio Corp Illinois Water Treatment Co Indeck Power Equipment Co Jamestown Chemical Co Inc Lancy International Inc. Monarch Water Systems, A Div Systech Corp Natco Chemical Co Nationwide Boilers Inc Neptune Chemical Pump Co Olin Corp, Olin Water Svcs PSE International Inc Resources Conservation Co Signet Scientific Co Div TVC inc, TVC Systemms Watcon Inc.

BOILER WATER TREATMENT, CHEMICALS

Alken-Murray Corp Atomergic Chemetals Corp Betz Industrial, Water Mgt Div Of Betz Labs Bowman Distribution, Barnes Group Inc Burman Technical Serv Inc. Water Management Div Calgon Corp, Commercial Div Certified Laboratories, Eastern Div Chargar Corp, Elgene Div Cherned Corporation, Dubois Chemicals Chemical Testing Corp Clayton industries. Dearborn Div, W. R. Grace & Co. Processing Processing Company

See Catalog Pages 425—428)

Dustiane Products Company

See Catalog Pages 425—428) Garratt-Callahan Co.

Jamestown Chemical Co Inc.

32 Plant Engineering Directory

J C Whittam Mfg Co Mitco Inc Naico Chemical Co Nationwide Boilers Inc. Oakite Products Inc Olin Corp, Olin Water Svcs Western Chemical Co. Wright Chemical Corp

BOILER WATER TREATMENT, NON-CHEMICAL SYSTEM

Aqua Dynamics Corp Agua-Tech Inc Cambridge Scientific Ind Clinc Clayton industries Cleaver-Brooks Culligan Intl CX/Oxytech The Duriron Co Inc., Filtration Systems Div Environmental Elements Corp. Graver Co, Graver Water Div Hydro Max Corp, Member Raytec Water Group Kerntune Inc., Superior Water Conditioners Monarch Water Systems, A Div Systech Corp. Nationwide Boilers Inc Osmo Membrane Sys Div, Osmonics Inc Pall Process Filtration Corp, Div Pall Corp Permutit Co Inc Permutit Co Inc
Progressive Equipment Corp Resources Conservation Co Saltech Corp Scale Control Sys.

Water Refining Co Inc. Inclustrial Div
BOILER, BY APPLICATION,
COGENERATION
ABCO Inclustres inc Babook & Wilcox
The Bigloow Co
Cain Industries
C-E Power Systems, CE: Power Systems,
Combustion Engineering Inc
Clayton Industries
Energy Systems, Div Midwesco Inc Federal Boiler Company Henry Vogt Machine Co Herman Bogot & Co Mitsubishi Heavy Indus Americ Montgomery Brothers Inc Olin Corp. Olin Water Svcs Riley Stoker Corp Haley Stokes Corp Solar Turbines Inc, Subs Caterpillar Tractor Co Struthers Wells Corp Struthers Corporation

BOILER, BY APPLICATION, HOT WATER

Vapor Corp, Div of Brunswick

TVC Inc, TVC Systemms United States Filter, Fluid Systems Corp.

Systech Corporation

ABCO Industries Inc. The Bigelow Co Brasch Mfg Co Inc Bryan Steem Corp Burnham Corp, Hydronics Div CAM industries inc Carrier Air Conditioning, Carrier Corp C-E Power Systems, Combustion Engineering Inc CHROMALOX-E L WIEGAND DIV, Emerson Electric Co (See Catalog C/CHR)
Clayton Industries Cleaver-Brooks Columbia Boiler Co Pottstown Edwards Engineering Comp. Federal Boiler Company Fluidyne Engr Corp Fulton Boiler Works Inc Herman Bogot & Co Hydrotherm Indeck Power Equipment Co Industrial Boiler Co Inc The Intl Boiler Works Co. Mitsubishi Heavy Indus Americ Montgomery Brothers Inc. Nationwide Boilers Inc. Olin Corp, Olin Water Svcs Ray Burner Company Raypak Inc . . Reimers Electra Steam Inc Scale Control Sys Slant Fin Corporation Systech Corporation Vapor Corp, Div of Brunswick Weil-McLain, A Marley Co

BOILER, BY APPLICATION, STEAM ABCO Industries inc
Beboock & Wilcox
The Bigelow Co
Brasch Mfg Co Inc
Bryan Steem Corp
Burnhern Corp, Hydronics Div
CAM Industries Inc ABCO industries inc Burnham Corp, Hydronics Div
CAM Industries inc
Carrier Air Conditioning, Carrier Corp
CE-Power Systems,
Combustion Engineering Inc
CHROMALOX-E L WITEGAND DIV,
Emerson Electric Co
(See Catalog C/CIRI)
Clayton Industries
Columbia Boiler Co Pottstown
Electric Steam Generator Corp
Electro-Steam Generator Corp
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Electro-Steam Generator Corp
Futor Boiler Company
Fluidyne Engr Corp
Futton Boiler Works Inc Fluidyne Engr Corp Futton Boiler Works Inc Henry Vogt Machine Co Herman Bogot & Co Hydrotherm Indeck Power Equipment Co Industrial Boiler Co Inc The Intl Boiler Works Co Mitsubishi Heavy Indus Americ
Montgomery Brothers Inc
Nationwide Boilers Inc Nationwide Boilers Inc
Olin Corp, Olin Water Svcs
Ray Burner Company
Reimers Electra Steam Inc
Riley Stoker Corp Remers Electra Steam inc Filey Stoker Corp Scale Control Sys Slant Fin Corporation Systech Corporation Vapor Corp, Div of Brunswick Weil-McLain, A Marley Co

BOILER, BY APPLICATION, OTHER ABCO Industries Inc Cain Industries Federal Boiler Company Federal Boiler Company
Futton Boiler Works Inc
Hydrotherm
The left Beiler Works Co Hydrotherm The Intt Boiler Works Co Systech Corporation

BOILER, BY TYPE, ELECTRIC OR

CAM Industries inc CHROMALOX-E L WIEGAND DIV. Emerson Electric Co (See Catalog C/CHR) (See Catalog C/CFR)
Edwards Engineering Corp
Electric Steam Generator Corp
Fulton Boiler Works Inc Herman Bogot & Co Hynes Electric Heating Co deck Power Equipment Co INDEECO (See Ad Page C-45)
The Intl Boiler Works Co

Montgomery Brothers Inc Olin Corp, Olin Water Svcs Patterson-Kelley Co, Div Harsco Corp Reimers Electra Steam Inc Scale Control Sys Slant Fin Corporation

BOILER, BY TYPE, FIRETUBE

ABCO Industries Inc Rabcock & Wilcox Basic Environmental Englind The Bigelow Co Burnham Corp, Hydronics Div Cleaver-Brooks Columbia Boiler Co Pottstown Energy Controls Inc Federal Boiler Company Herman Bogot & Co Indeck Power Equipment Co Industrial Boiler Co Inc Industrial Combustion, Div of Aqua-Chem John Zink Co, Allegheny International Nationwide Boilers Inc. Olin Corp, Olin Water Svcs Ray Burner Company Scale Control Sys Struthers Wells Corp Systech Corporation
Thermal Transfer Corp Wabash Power Equipment Co 1 300000 100.001 . In large, ord and an engine

BOILER, BY TYPE, FLUIDIZED BED 30 ABCO Industries Inc

258

Babcock & Wilcox
The Bigelow Co
C-E Power Systems,
Combining End Combustion Engineering Inc Section 1997

The Intl Boiler Works Common 2, 170 (1997)

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BOILER, BY TYPE, WASTE HEAT ABCO Industries Inc
Babcock & Wilcox
Basic Environmental Eng Inc The Bigelow Co. Cain Industries
C-E Power Systems.

Combustion Engineering Inc
Cleaver-Brooks
Electro-Steam Generation Cleaver-Brooks
Electro-Steam Generator Corp
Epcon Industrial Systems Inc
Federal Boiler Company
Henry Vogt Machine Co Indeck Power Equipment Co Industrial Boiler Co inc The Intl Boiler Works Co John Zink Co, Allegheny International John Zink Co, Allegheny International Mitsubishi Heavy Indus Americ Olin Corp, Olin Water Svcs Parker Boiler Co RILEY-BEAIRD INC (See Ad Page J-11)

Filey Stoker Corp Simonds Manufacturing Corp Simonds Manufacturing Corp Solar Turbines Inc. Subs Caterpillar Tractor Co Struthers Wells Corp (1997) (1997) (1997) (1997) Thermal Transfer Corp (1997) (1997) (1997)

Vapor Corp. Div of Brunswick BOILER, BY TYPE, WATERTUBE ABCO industries Inc Babcock & Wilcox Basic Environmental Eng Inc
The Bigelow Co Bryan Steam Corp C-E Power Systems, Combustion Engineering Inc Clayton Industries Cleaver-Brooks Columbia Boiler Co Pottstown Henry Vogt Machine Co Herman Bogot & Co Indeck Power Equipment Co.: The Intil Boiler Works Co. John Zink Co, Allegheny International Keeler/Dorr-Oliver Mitsubishi Heavy Indus Americ
Nationwide Boilers Inc Olin Corp, Olin Water Svcs Raypak Inc Riley Stoker Corp Thermal Transfer Corp Vapor Corp, Div of Brunswick Wabash Power Equipment Co

BOILER, BY TYPE, OTHER ABCO Industries Inc Cleaver-Brooks Fulton Boiler Works Inc The Intl Boiler Works Co Slant Fin Corporation Systech Corporation Weil-McLain, A Marley Co

BOLT (SEE "FASTENER")

BOOK (SEE "PUBLICATION. TECHNICAL REFERENCE)

BOOTH, PAINT SPRAYING Alemite Div, Stewart-Warner Corp Binks Manufacturing Co Cambridge Engineering Inc Chemco Mfg Co Inc Columbus Industries Inc G&C Automation Projects Inc GEORGE KOCH SONS INC (See Ad Page 140) Nycoil Company Paasche Airbrush Co Protectaire Systems Co Tri-Dim Filter Com

A Liss & Co Inc. A Control of the Co



Telephone Conversation

Affiliated Engineers SE, Inc. 3300 SW Archer Road Gainesville, FL 32608 (904)376-5500 [FAX 375-3479]

Holston AAP Boiler Study	95046-00	
Project	Project#	
Martin Drinkard	September 18, 1995	
Conversation With	Date	
Norfolk Southern Railroad	1 of ?	
Representing	Page	Typist
August 23, 1995	PDL	
Date & Time of Conversation	Copies	File

RE: Movement of Boiler from Volumteer AAP to Holston AAP

Per Mr. Drinkard, Norfolk Southern is capable of moving the boilers from the Volunteer AAP outside of Chattanooga, TN, to Holston AAP outside of Kingsport, TN. However, there are a couple of areas of difficulty which will have to be worked out if it is decided to move the boilers, as follows:

- Norfolk Southern will only transport the boilers and provide recommendations for proper rigging at time of loading. All handling of the boilers at each end will have to be by others.
 - 2. There is some concern about the use of the sidings at each end of the trip. While Norfolk Southern has the rights to the tracks in Chattanooga, CSX has the rights to the local sidings in the Kingsport area. NOTE: it might be possible to set up a shipment through intermodal (multiple carriers). This might affect the rate slightly.
 - 3. The base rate for transportation is \$3.72 per hundredweight. This results in a transportation cost of \$5208 per boiler or \$10,416 for both. There is no discount for multiple units.
 - 4. If it is decided to ship the boilers, enough notice will have to be provided to arrange for detailed routing and scheduling. NOTE: "Enough notice" was not defined during our conversation.



Raymond F. Parham, P.E. Plumbing/Fire Protection Project Engineer



JIM FRY (615-855-7109)	CO, PDL
Conversation With	Routing - CC
VOLUNTETR AAP, CHATTANOOGA, TO Representing	95046-00 Project Number
HOLLION AMP BOILER STUDY	7/11/95
Project Name	Date
16LSTON, TN	10:15 Am
Location	Time
I PETGUSTED MR FRY'S FAX NUMBER S	WE COULD SONS
THE BOILER INSPECTION AGENTA, ETOWIPMENT	T UST AND REGOUSET
	-
FOR COILER DOCUMENTATION TO HIM.	FAX. NO. 615-855-1205
I INFORMED MR FRY OF OUR INTENDED	> insterior sider
FROM JULY ZH THROUGH JULY 28, 1945 BY	THE BOILER
INSPECTOR AND ABSE'S INSPECTION FROM	JULY 25 TAROUGH
JULY 27,1995-	
0004 27,1113-	
I ALSO INFORMEDS MR FRY THAT THE BOIL	BE INSPECTOR WOULD
LIKE TO PERFORM A PRELIMINARY SURVEY	_
AND WOULD RESOURCE A CAMERA PASS.	
I ASKED FOR DIRECTIONS TO THE VOLUNTEE	TR PLANT (ATTACHED).
THE PLANT IS LOCATED ON THE WORTHEAST	
LODGING IS AUTILLABLE AT THE I-75/SHALL	
	CLEAR 103, EAT
AND THE I-75/BONNIE DAKS DR. EXIT.	
•	
1	
CONTACT MR. PAUL HOLLIS (855-7111) AS ALTER	DATE POINT OF LONTACT
IF MR. FRY UNAVAILABLE.	
Du Porison A FARING 25	
BY: KOBERT A. BARNES P.E.	
HVAL PROJECT ENGINEER	

DIRECTIONS TO VOLUM TEER AAP

COMING FROM ATLANTA ON I-75 GOING TOWARDS

IKNOXVILLE, PASS SHALLOWFORD RD. EXIT (LARDE MALL IN

(HUY 215(?) OR 315 (?))

VICINITY), GET OFF AT BONNIE OAKS DR/, GO UNDERNET

OVERPASS. CONTINUE TO 4-WAY STOP, GO TAROUGH 4-WAY

STOP TO NEXT RED WONT, WHICH SHOULD BE ENTRACE

TO PLANT.



SCOTT SHELTON	
Conversation With HDC	95046-00
Representing HOLSTON BLR/ACID STUDY	Project Number 8 - 3/ - 95
Project Name	Date 4:00
Location	Time
Scott JUST GOT DUT C	OF A MESTING
AND FOUND THE INFO THAT	
HAD COLLECTED ON HIS DES	
ARRIVED). HE SAYS THEIR FA	
15 ALLREADY CLOSED TODAY, A	
MONDAY IS A HOLIDAY, THE BY	
COULD GOT IT TO US WO	
	_
MORNING. THERE ARE ONLY	_
OR TWECIE PAGES, SO HE	LL FAX ITO
	TOTAL TO A CONTROL OF THE CONTROL OF
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By:	



SCOTT SHELTON CO	
Conversation With Holston 95046	
Representing Boilth Study ACID PLNT. Ex. 57 Project Number 8-28	-95
	-/-5
Location Time	
SOME COMING TO SCOTT TODAY (SENT
TO HIM FRIDAY)	
JORRY BOUCHICON HAVING TROUB	Œ
LOCATING PUMP CURVOS.	
I TOLD SCOTT THAT PUMP CUR	2085
PROBABLY ARE NOT AS NECESSARY A	5
PUMP DRIVE TURBING STEAM RA	78.
SCOTT WILL SOND INFO AS SOON	
IT GOTS TO HIM.	
·	· · · · · · · · · · · · · · · · · · ·
· · · · · · · · · · · · · · · · · · ·	
	· .
By: (/ / //)	



SONEE HALL	
Conversation With HDC	95 046 - (D
HOLSTON BOILER STUDY	Project Number 8-22-95
Project Name HOCSTON, TONN.	Date
Location .	Time
I INFORMED SONNER THA	T L COULD
NOT RECONCILE THE AIR/FUE	C RATIO
SHOWN ON PROCESS SCREETS, I	AND WHICH
I RECORDED FOR MY CALCUL	LATIONS I
STATED THAT MY CALCULAT	CONS FOR
50 CFM NATIGAS WOOLD IN.	
LEAST 800 CFM THEORETICAL	
COMBUSTION, WHILE WHAT W	
235 CFM. SONER SAID TH	
BRICK FURNACES HAD A U	
LEAKAGE THROUGH WALLS & T	•
THEM ALL KINDS OF PRO	. .
WILL LOCATE BURNER DE	
AND CALL OR SEND TO M	



SCOTT SHELTON	
Conversation With HOSTON	Routing 95046 - 00
Representing HOLSTON BCR STUDY	Project Number 8 - 7 - 95
Project Name	Date
Location	Time
	_
LOFT MSG. ON VOICE MAIL	THAT I
WAS FOCCOWING UP TO SEE	WHAT
PROGRESS WAS BETWG MADE	ON
ACCUMUCATING MATERIAL WE RE	FOUESTED
BY FAX.	
ASKED HIM TO RETURN	Any CALL.
<u> </u>	
	· · · · · · · · · · · · · · · · · · ·
By:	



615-247-9111 × 3791

	0.5
SCOTT SHOLTON SMCHO-EN	_ <u> </u>
Conversation With HOLS TO N	95046-00
Representing HOLSTON BLR STUDY	Project Number 7- 31-95
Project Name	Date
Location	Time
Localion	THING
ASKED SCOTT IF HE	NEW WHAT
PROGRESS HAD BEEN MAD	•
REQUEST FOR PUMP & TU	
SCOTT SAID HO FIGURED	
MUST HAVE BEEN MADE	·
PEOPLE DURING AESE VIS	
HIM THE REQUEST WAS	
HIM ON 26 JUNE, 1995.	
HE WOULD HAVE TO	
AND SEE WHAT HAPPEN	
HIM ANYTHING HE COULD	
HEZP US DUT WOU	
APPRECIATOD BOCAUSE	
DATA FOR ANALYSIS	
DATA TOIC AIGHT STS.	
(to SD holds	
Tare X To The West	



MR. DOGNAZZI (MSG. MACH.) Conversation With HARTFORI	CLO Routing 95046-00 Protect Number
HOLSTON BOILER STUDY Project Name	Project Number 2-21-95 Date
Location	Time
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ASKED FOR RETURN CALL	-
STATED THAT AGSE WILL @ VARP ON TUES. MORN.	BE ON BOAR
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HUAC PROJECT ENGINEER

AL DOGNAZZI	CO.PDL
Conversation With	Routing
HARTEFORD STEAM BOILER INSPECTION & INSURANCE W.	95046-00
Representing	Project Number
HOLSTON HAP BOILER STUDY	7/14/95
Project Name	Date
HOLSTON, TN	1:55 P4
Location	Time
MR. DOCHAZZI INDUIRED AS TO THE STA	ITUS OF THE PURCHASE
10, 2002.00 11-00100	
ORDER OR OTHER ACKNOWLESSEMON OF HIS	CONTRACT FOR THIS
BOILER IUSPECTION, HE WOULD ACCEPT A	VORBAL ACKNOWLEDGEND
TODAY OR MONDAY TO KOUP THE PROJECT	ON THE HEBEUT
TIMETABLE. I ALSO CONFIRMES LITMER PAUL	- LITTLE OF CARL
2000	
OSBERG AS FUTURE CONTACT PERSONS.	
	-
	-
By: Bob Barues	

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AL DOGNAZZI (404-928-0788)	CO, PDL
Conversation With	Routing
HARTFORD STEAM BOLDR INSPECTION: AND INSURANCE CO.	95046-00 Project Number
HOLSTON DAP BOILER STUDY	7/11/95
Project Name	Date
HOLSTON, TN.	1:20 AM Time
Location	
	,
I CALLED MR DOGNAZZI TO CLARIFY HIS	ITINURARY (REFER
TO FAX DATED JULY 10,1995 FROM HARTFORD).	SPECIFICALLY
I INQUIRED IF OUR PRESENCE WAS REQUIRE	بعد بالا رسم
1995. MR DOGNAZZI ROSPONDES THAT THE	BULK OF THE
TESTING AND INSPECTION WOULD BE PERFORME!	DESTAY WEST
WEDDESDAY AND THURSDAY. I INFORMED MY	DOGNAZZI THAT
NE WOULD PLAN TO CONSUCT OUR PORTION OF	THE FIELD INVESTIGATION
DURING THE TUESDAY THROUGH THURSDAY TIME	FRAME.
MR DOGNATION INFORMED HE HE WOULD LIKE	TO CONSUCT A
	995, AND ASLES
IF WE COULD CONTACT THE APPRIARIE PERLOC	WEL AT VOLVITEER
MAP AND ARRANGE A CAMPARA PASS. I IN	FORMED ANY I
WOULD DO SO AND CONFIRM THE FACT WITH	HM LATER TODAY.

BY: POBER A BARNES, P.E.
HUAC PROJECT ENGINEER



AL DOGNAZZI (404-928-078	3e) <u>co</u>
Conversation With	Routing
HARTFORD STEAM BOILDE INSPE	
Representing	Project Number
16LSTON AAP BOILER STUDY	
Project Name Holston, TN	9:55 AM
Location	Time
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TO HAVE TESTING BUTTON ON	JULY 24, 1995. I WILL START
REQUEST FOR BOILER DAT	A FROM JIM FRY AT VAAP
TODAY.	
	(IMPORTANT MESOS
	IMPORTANT MESSAGE
	FOR RB
V	DATE 7-10 TIME 910 (A.M.)
	4 / 7
	M_Al Dognazzi
	of Hartford Steam Boile
	PHONE 404 928 0788
	D FAX
	O MOBILE
	AREA CODE NUMBER TIME TO CALL
	TELEPHONED PLEASE CALL
	CAME TO SEE YOU WILL CALL AGAIN
	WANTS TO SEE YOU RUSH
	RETURNED YOUR CALL WILL FAX TO YOU
	MESSAGE Hart ford can
	start on 24 or 31
	of July - IV. msg.
	on voice mail as
	to when you want.
	-(11)
	SIGNED
	TOPS FORM 4005
	¥ 2000 0000

270



By: BOB BARENES

Affiliated Engineers SE, Inc. 3300 SW Archer Road Gainesville, FL 32608

2-1 150-21	
CAZL 65D672 6-	Routing
ASSE	95046-00
Representing	Project Number
COE HOLSTON MAP BOILER STUDY	7/7/15
Project Name Holston TN	Date 10:25
Location	Time
CEET ITINGRARY FROM AL DOUNAZZI	SO WE CAN SCHEDULE
OUR 125PECTION,	
COR IFOI BOLIDE,	
GET WFO FROM JIM FRY ON BOILE	P.C
CET DIO : MORE THAT TELLE	23.
	TALL TALL HALL TO C
INFORM PAUL LITTLE RE: SITE INVESTIGATION	TOO IRIP TO VOLUPTEELS
AND ALSO TRIP TO MOLSTON TO FAMILIAN	21ZE HIM WITH
20 a time	
PROJECTS.	

271



NOS WEIGHT (615-756-4517)	
Conversation With	Routing
Waser und	95046-00
Representing	Project Number
COE HULSTON AND BOILLER STUDY	15 28 95
Project Name	Date 7:2 B
CHATTANOOGA E	Z:30 PA Time
Location	ime
CAN CONVERT COAL TO GAS	
THE CHIESE CONT. 12 CAS	
DIXHARDE	
CONTINUOUS ASH ADDER STOKER	
PULVOTUZOS COLL NOT PRACTICAL	
CHS PRACTICAL	
PACKAGED BOILDRS PRACTICAL GOICE	



TOM ROBERTS (404-939-6292)	Routing
Conversation With BABCOCK & WILLOX	95046-00
Representing	Project Number
COE HOLSTON MAP BOILER STUDY	6/28/95
Project Name	Date
1tol5700, TD	
Location	Time
10 0 10 10 10 10 10 10 10 10 10 10 10 10	5-11-11-1
MR. ROBERS WAS NOT AVAILABLE ON 6/28/45.	I WILL CALL
AGAIN 6/29/95	
TOTAL TOTAL	
·	
	•
By: BOB BARNES	



JOHN MANNIUL (617-255-4740)	
Conversation With	Routing
FACTORY MUTUAL ENGINEERING ASSOC.	95046-00
Representing	Project Number
HOLSTOP AAP BOILER STUDY	6/15/45
Project Name	Date
4T, GOTZJOH	Z:20 PM
Location	Time
I LOFT A PHONE MUSSIAGE ON MIR. HA	WILLIAM AUSWIATINIO
= 20. The Prome State Do The Prome	ACTOR A PROPERTY OF
MACHINE TO CALL ME BACK.	
THUMBE IT TO DATE.	
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HAYC GLOJECT ENGINEERS



and of lown	
GARY ANDREWS (817-543-8032)	
Conversation With	Routing
OLD REPUBLIC INSURMCE CO.	95046-00
Representing HOLITON AAP BOILUTE STUDY	Project Number 6/5/95
Project Name	Date
אין, מפונואי	7:28
Location	Time
	TO. HE WILL
ROTURN CALL.	
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BY: BUB BARNUS

HUNC PROJECT ENCINEER



booder ,	
EDOMR WHITTES (617-725-7309)	
Conversation With	Routing
COMMERCIAL UDION INSURANCE CO.	95046-00
Representing	Project Number
HOLSTON AND BILLOR STUDY	6/5/95
Project Name	Date
HOLSTON, TW	11=15 PM
Location	Time
OUT FOR THO RUST OF THE DAY.	I WILL CALL TOMOTOROW
6/6.	
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	and the second second second second second second second second second second second second second second second



ENGAR WHITTLE 617-725-7309	
Conversation With	Routing
COMMISSIAL UNION INSURANCE CO.	95046-00
HOLYTON HAP BOILER STUDY	Project Number _6/2/45
Project Name	Date
HOLSTON, TH	4:30 PM
Location	Time
MR. WHITTLE OUT TILL NORT WERE O	PFICE CLOSED
T WILL CALL BACK NOXT WEEK.	
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10.1.	06- (617-255-	4747	
JOHN MANUIA	(617 = 233		<u></u>
Conversation With			Routing
FACTORY MUTU	AL		95046-00
Representing			Project Number
HOLSTON AAP P	bollor study		6/2/95
Project Name			Date
HOLSTON, TH			4:25 PM
Location			Time
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CALLOD P	LOT MESSAGE	OU AUGUER	ING MACHINE ,
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STENS RUDNICIAN (617-255-4270)	
Conversation With	Routing
FACTORY MUTIM GNOWBER	95046-00
Representing	Project Number
HOUSTON AAP BALFR STUDY	6/2/95 Date
Project Name Holston, Th	4:15 pm
Location	Time
The state of the s	
MR. RUDNICKS RIROMMOND CONTACTING	•
FM RESEARCH LAB NDE	
JOHN MANNING, METALORGICAL CAB	
1151 BOSTON PROVIDENCE TURNA	KU .
NOTWOOD MA 02062	TEL. 617-255-4745
- Jennous Julia Barbe	180. 017 0 30 17 10
· · · · · · · · · · · · · · · · · · ·	
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AL DOGGEZZI	
Conversation With	Routing
HARTFORD STEAM BOILD'S	95046-00
COE HOLSTON AAP POILER STUDY	Project Number 5/26/45
Project Name	Date
KINGS PORT TN	8=30 Am
Location	Time
I ASVINGS MR. DOWNAZZI THAT THE	TESTING AND
INSPECTION OF THE TWO BOILDRES AT VILL	NIETR AAP HAS
EFFU DULMED DE TO CURPS REVIEW OF	THE COST OF THE
TOSTING. WE WILL ASVISE HIM MEXT	WEEK HOW THINGS
ARE OR MEEN'T PROGRESSING AND TRU TO	COME UP WITH
A NEW SCHEDUE FOR TESTING	
• •	

By: BOB BARNES, P.E.



		/ -	7	
Conversation With		(617-255	-4272)	Routing
	TUAL ENGINEER	ING ASSOCIA	7700	95046-00
Representing 1 to LS TOP DANG				Project Number 5/19/95
Project Name HOLSTON, Th)			2=30 PM
Location				Time
Pă	5D-01CK-US			
STEVE RI	UDNICKAS, A	TANAGER	617-25	5-4270
	EXT WEEK			REQUEST
	1100			
	· · · · · · · · · · · · · · · · · · ·			

By: DOB BARNES



GENE HENNESSY (704-362-4499)	
Conversation With TOTAL INSURMICE	Routing 95046-00
Representing 1+0LSTON AAP COILDR STUBY	Project Number 5/14/45
Project Name 1+0LSTON TN	Date 4:00 PM
Location	Time
THEY DON'T BO CONTRACT WORK A	M4401215 ,
The state of the s	

By: BBB BARDUS

HVAC PROJECT ENGINEER



HANK PAULSÓN	(704-522-2932)	
Conversation With		Routing
ROYAL INXURANCE		95046-00
Representing HOLSTON ANP		Project Number 5 9 95
Project Name		Date
Project realie		3:15 PM
Location		Time
CALL		
GENE HONDESSY	CHARLOTTE NC .	704-362-4499
		362-4453
	· · · · · · · · · · · · · · · · · · ·	
n		



TOM ROPERTS 404-939-6292	40
Conversation With	Routing
BABCOCK & WILCOX CO. ATCHITA, GA	95046-00
Representing	Project Number
HOLSTOD AND ARDA "A" BOILER STUDY	5/9/45
Project Name	Date 11-30 Aug
Holston, Th	Time
Location .	14110
t in a constant with the constant of the const	NE TOTAL
I ASKED MR. ROBERTS IF CHANGING T	AC LESITAGE DATES
FORWARD OR BACK I WEEK WOULD	enable him to
PROJECT A PROPOSAL FOR THIS PROJECT.	MR ROBBETS INFORMED
ME THAT THE REMOTE FIELD EDDY CURRE	
THEY OWNED WAS OUT FOR REPAIRS IN	ID WOULD NOT BE
_	IN OUR REDUKT
FOR PROPOSAL. ADDITIONALLY, MR. ROBBETS	ADVILLED ME THAT
SUBCOLTRACTION OUT THE REFEL TESTING	
MAKE HIM COMPETITIVE IN HIS PROPOSI	
TO MAKE A PROPOSAL.	
TO VINCE TO THE TOTAL OF THE TO	
I IN FORMED MR. ROBERTS THAT I WOULD	POSSIBLY BE COUTACTING
HIM IN THE FUTURE IF I HAD ANY OU	
TWO BOILERS AND ANCILLARY EQUIPMENT	PI VOULTEEL RAT
IN CHATTANDOGA, TN.	
:	

By: ROBORT A. BARLIES P. U.
HUAC PROLITE ENGINEER



AL DOGNAZZI (404-928-0788) CO
AL DOGNA 721 (404 - 928 - 5788) Conversation With Routing
HARTFORD STEAM BOILERS INSPECTED EINSPENCE 6, 95046-00
Representing Project Number
HOLSTON AND BOILDR STUDY 4/11/95
Project Name Date
KINGSPORT, TN 4:15 AM
Location
TONY BATAGLIA, MOBILE LORPS OF ENCHOPERS
ULTRASONIC THICKNOSS TISTING
VISUAL IUSPECTON
MAG-PARTICLE TESTING
EDDY CHERENT TESTING OF TUBBS
RESOURCES RECOMMENDED TOSTS of COSTS FOR BULLET INSPECTION.
AL WILL CALL TONY PS: POSSIBLE FRE-INSPORTION TO EVALUATE
PROPOSAL. WILL CALL & ADVISE.
AL DOGNAZZI CALLOD BACK AT 11:00 mm 4/11 TO MOVING 140 HAD
CONSTRUTED TONY BATACLIK AND JIM FIRM AT VOLUNTOUS AMP
MUD HAS TENTATIVE USPECTION SCHOOL LOTS FOR MIN. 4/17/95.

By: KOBERT A BARNOS

NAC PROJECT ENGINEER

Appendix 6 - Entry/Exit Interviews



3300 SW Archer Road Gainesville, Florida 32608 (904) 376-5500 • FAX (904) 375-3479

MEETING NOTES

HOLSTON AAP	CONTRACT NO.: DACA01-94-D-0007	95046-00	
Project		Project #	
Holston, TN		August 22, 1995	
City, State		Date	
Exit Interview		1 of 1	DA
Type of Meeting		Page	Typist
08/18/95			
Meeting Date		Copies	
Present	Representing		
Orville Depew	HDC		
Sonee Hall	HDC		
Carl Osberg	AESE		
Paul Little	AESE		

The purpose of this meeting was to review the items surveyed and discuss probable areas of energy conservation. The following items were discussed.

Observations were made at the Acetic Anhydride manufacturing equipment in building 7. Natural gas and combustion air quantities at one cracking furnace, which was in operation, were obtained: 50 CFM main burner N.G., 5 CFM Pilot N.G., and 235 CFM Air. It was noted that flue gas temperature exiting the furnace is 329°C. The waste heat boilers anufactured by Union Iron Works, were originally selected for conditions existing with producer gas used as fuel. The units are single pass firetube type. It was noted that discussions have previously taken place to address feasibility of incorporating auxiliary burners on these units, but detailed investigation was never completed. A boiler cross sectional drawing was obtained indicating the quantity and size of boiler tubes. Nominal tube length was measured as 15 feet.

At steam plant building 8, Mr. Hall stated that all tar handling equipment and concrete dike/basin will be removed prior to work related to installation of boilers from VAAP, if in fact, those boilers are to be used. Mr. Davenport pointed out the burner port for burning tar, which might make installation of a natural gas burner possible. It was also pointed out that only three sides of the boiler fire box section contain water wall tubes; The wall opposite the tar burner does not contain riser tubes.

Mr. Davenport stated that the river water piping "loop" has now been completed, so that the electric driven pump previously called the "backside" pump is available for any high head system pumping requirements. Mr. Hall indicated that current operations are being met without utilizing turbine driven river water pumps, and this configuration is maintained under conditions requiring less than about 100,000 #/hr boiler plant load.

Mr. Davenport was asked how often the coal bunkers are filled. He stated each bunker capacity is 200 ton, and at present they burn about 70 tons each day.

The above constitutes the writer's understanding of the discussions of this meeting and conclusions reached. Corrections/errors should be noted to the writer within 5 working days.

Ву,

Paul Little P.F.



3300 SW Archer Road			
Gainesville, Florida 32608			
(904) 376-5500 • FAX (904) 375-347	7		

Mike Richarme

Bob Barnes

MEETING NOTES

HOLSTON AAP	CONTRACT NO.: DACA01-94-D-0007	95046-00	
Project	-	Project #	
Holston, TN		June 2, 1995	
City, State		Date	
Exit Interview		1 of 2	MAH
Type of Meeting		Page	Typist
05/25/95		CO, MR	
Meeting Date		Copies	
Present	Representing		
Jerry Bouchillon	HDC		
J.L. "Butch" Jones	HDC		
Sonee Hall	HDC		
George Davenport	HDC		
Max G. Noe	HDC		
D.L. Cretsinger	HDC		
Richard Gillenwater	HDC		
Van Jones	HDC		

The purpose of this meeting was to review the items surveyed and discuss probable areas of energy conservation. The following items were discussed.

1. Bob Barnes briefly reviewed the scope of work for this project and described some of the options available for saving energy for this project. Among the options were the relocation and reuse of one or two existing gas fired boilers at Volunteer Army Ammunition Plant (VAAP) in Chattanooga, TN. Other options included new boilers either at the existing boiler plant or located near the points of use. Reuse of existing feedwater equipment appeared feasible but would be analyzed in detail in the study of this project. Ancillary equipment at VAAP may also be reused but inspection of the equipment would determine the economic feasibility.

AESE

AESE

- 2. The question was raised about how the new boilers would affect the current air permit and environmental concerns. A brief discussion of possible scenarios of equipment, fuels, and siting followed. More definite information would be developed by AESE during the course of the study which would be forwarded to HDC to be evaluated for impact on this project.
- 3. An additional question was raised regarding the interruptability of natural gas supplies and back-up fuels or storage to protect process equipment and product. Jerry Bouchillon will check on the interruptability of natural gas, as the current contract with United Cities Gas Company is for uninterruptable natural gas supply. Fuel oil is not desired by HDC due to storage and environmental concerns. Other possible alternatives might be electrical back-up for critical needs (such as pumps, heating tracing, bayonet heaters, etc.) but duration of interruption needs to be determined as well as identifying systems and components requiring backup.
- 4. As part of the study, Jerry Bouchillon recommended overhead costs be included in operation and maintenance costs. Jerry had previously furnished data on "out-of-pocket costs" for steam to be used as part of the economic analysis for this project.

Project Name:

HOLSTON AAP

Date:

June 2, 1995

Project No.:

95046-00

Page No.:

2 of 2

5. Mike Richarme suggested there could possibly be some cost savings on electricity costs due to power factor billing by the utility company. However, this proved not to be the case as HDC owns and maintains the electrical distribution equipment downstream of the primary metering location and has done a good job correcting power factor conditions and line losses.

The above constitutes the writer's understanding of the discussions of this meeting and conclusions reached. Corrections/errors should be noted to the writer within 5 working days.

By:

AFFILIATED ENGINEERS SE, INC.

Robert A. Barnes, P.E.

HVAC Project Engineer



3300 SW Archer Road Gainesville, Florida 32608 (904) 376-5500 • FAX (904) 375-3479

MEETING NOTES

HOLSTON AAP	CONTRACT NO.: DACA01-94-D-0007	95046-00
Project		Project #
Holston, TN		June 2, 1995
City, State		Date
Entry Interview		1 of 2 MAH
Type of Meeting		Page Typist
05/22/95		RB, MR
Meeting Date		Copies
Present	Representing	
Scott Shelton	SMCHO-EN	
Sonee Hall	HDC	
George Davenport	HDC	
Max G. Noe	HDC	
Carl Osberg	AESE	
Mike Richarme	AESE	
Bob Barnes	AESE	

The purpose of this meeting was to have an entry interview and the following items were discussed.

- Production levels of explosives was 14 million pounds (lbs) in 1994, 7 million lbs projected in 1995, 1. and about 2 million lbs projected for 1996. Production levels beyond 1996 are not available at this time.
- Current plans are to replace steam turbine drives at refrigeration machines in Building 5 to electrical 2. motors.
- Holston Defense Corporation (HDC) is presently investigating the possibility of buying or selling 3. steam from Tennessee Eastman.
- There are no steam lines between Area "A" and Area "B". 4.
- Electric power is supplied to HDC from Kingsport Power at a single substation with a back-up from 5. Appalachian Power (TVA).
- Shelby Jones is presently investigating alternative electric power sources. 6.
- In Building 8, Boiler 7 is currently laid away, and plans are to lay away Boilers 3, 5, and 6. Boilers 1 7. and 2 are used alternately with Boiler 4 inactive but capable of being fired. HDC has an estimate of the cost of boiler lay-up which will be furnished later.
- Process steam requirement is 90 psig and most is used in Building 2.

Project Name:

HOLSTON AAP

Date:

June 2, 1995

Project No.:

95046-00

Page No.:

2 of 2

- 9. Cogeneration is under investigation by HDC as a possible solution to supplying steam for Area "A" but this has been excluded from the AESE Limited Energy Study.
- 10. PCB containing transformers are routinely removed from Holston AAP which has a holding area for temporary storage of transformers prior to their disposal.

The above constitutes the writer's understanding of the discussions of this meeting and conclusions reached. Corrections/errors should be noted to the writer within 5 working days.

By:

AFFILIATED ENGINEERS SE, INC.

Carl L. Osberg, P.E.

Vice President

Appendix 7 - Response to Comments

MOBILE DISTRICT PROJECT REVIEW COMMENTS

DATE:

28 Sept. 1995 | Page 291 of 5

TO: U.S. Army Corps of Engineers Mobile District

Mobile, AL

FROM: Robert S. Woodruff, CESAM-EN-DM PHONE: (334) 694-6074 FAX: (334) 690-2424

PROJECT/FY: FY95 Limited Energy Study for Area "A" Package Boilers

LOCATION: Holston Army Ammunition Plant, Kingsport, TN

TYPE REVIEW: Interim Submittal Review

NO.	PAGE/PAR	COMMENT	RESPONSES TO COMMENT
1.	Exec. Sum. P.2	What is Synergism Analysis?	Interaction of discrete elements of system changes, the combination of which may produce more or less desirable effects than the sum of the individual changes alone. A/E will so state in the report.
2.	Paṛt II P. 6	The fact that the chillers are being converted to electric drive as well as the fact that the existing distribution system is to be reused are "givens" and do not require evaluation.	None.
3.	Part II P. 6	The items outlined on this page are not the same as those stated in the detailed scope of work. These should be identical.	A/E will clarify which of these items were addressed at Entry/Exit Interviews.
4.	Part II P. 8	Item 4) gives the electrical consumption of the steam plant equipment. Does this value come from the actual operating logs?	Assumption based on 1994 Tony Battaglia steam cost calcs.
5.	Part II P. 25	The first paragraph on this page states that no differentiation was made between energy and demand charge for electric service. Because demand charges are really paid for the entire 12 months wouldn't this have an effect on the economics?	Effect is insignificant. Report will be modified explain.
6.	General	Would it be prudent to consider a 30,000 #/HR gas fired boiler not using the existing stacks? That way enough steam would be produced to meet the small demands without having to vent any steam.	Yes.

MOBILE DISTRICT PROJECT REVIEW COMMENTSDATE:28 Sept. 1995Page 2 of 5TO: Affiliated Engineers SE, Inc.FROM: Anthony W. Battaglia, CESAM-EN-DM

PROJECT/FY: FY95 Limited Energy Study for Area "A" Package Boilers

LOCATION: Holston Army Ammunition Plant, Tennessee

TYPE REVIEW: Interim Submittal Review

Gainesville, FL

TYPE				
NO.	PAGE/PAR	COMMENT	RESPONSES TO COMMENT	
1.	General	The conclusions reached by this report appear to be reasonable, and some aspects of the report are quite good; however, in some respects it is incomplete, and there are several areas which need clarification.	None.	
2.	General	Not all of the topics listed in the Detailed Scope of Work have been adequately addressed. The following comments are keyed to the topics listed in the Detailed Scope of Work, paragraph 4., pages A-2 & A-3:		
		Sub-par 4.a., Evaluation of Gas-fired Package Boilers: For the case of the boilers relocated from Volunteer AAP, this has been adequately addressed; but it has not addressed boilers sized to meet the current requirements. This should be added to the evaluation.	A/E will incorporate.	
		Sub-par 4.b., Use of Existing Distribution System: Adequately addressed.	None.	
		Sub-par 4. c., Existing steam-driven chillers replaced with electric: The steam requirement for the chillers must be subtracted from the overall steam requirement; cannot determine how this was accommodated in the calculations. Please clarify.	A/E will clarify.	
		Sub-par 4.d., Inspection of existing boilers at Volunteer AAP: Adequately addressed.	None.	
		Sub-par 4.e., Evaluation of existing ancillary equipment at Volunteer AAP: No clear statement was made regarding this equipment, nor how it would affect the cost/savings. Please include.	A/E will clarify.	
		Sub-par 4.f., Maintenance and Operation Costs: Either this was not adequately addressed or there is some discussion missing. Please include or elaborate.	A/E will elaborate.	
		Sub-par 4.g., Fuel oil storage capacity: No analysis has been provided, please include.	A/E will include.	
		Sub-par 4.h., Air pollution permits: No discussion was included regarding impacts of the proposed changes. Please indicate.	A/E will add statement that no impact is involved.	
		Sub-par 4.i., River water Pumps: There appears to have been a misunderstanding regarding this topic. The scope of work says that the pumps are currently (at the time of the pre-negotiation conference) electrically driven, although each has a steam turbine connected to the same shaft. The study is supposed to evaluate the economics of using the turbines instead of the motors. If there was a change in the method of operation prior to starting the field work, this should have been stated in the report. Please revise as needed.	A/E will clarify.	
3.	General	The AE is commended for proposing additional ECOs as possible solutions to the problem.	None.	
4.	Detailed Narrative General	In the detailed narrative there is some discussion of each case (1 thru 5) investigated; however, it is not detailed enough to really give the reader an understanding of the costs/savings involved. Please expand.	A/E will comply.	

PHONE: (334) 694-2618 FAX: (334) 690-2424

5.	Energy Calcs, General	In the detailed narrative, there is a discussion of the spreadsheet calculations used for determining energy consumption; however, there are no sample calculations to show how the spreadsheet numbers were generated. Please include.	A/E will comply.
6.	LCCAs, General	The LCCA summary Sheets should not be under "Miscellaneous Data". Each sheet should be included with the discussion of the pertinent ECO.	A/E will comply.
7.	Pg 2 & 3	Case 1 & Case 2: These cases appear to be reversed with respect to the river water pumps. See Comment 2, sub-par 4.i., above.	A/E will comply.
8.	Pg 4	The penultimate sentence states that the savings are negative, but makes no attempt to explain the situation. Please clarify.	A/E will amplify.
9.	Pg 6	3rd bullet: Notes replacement of steam driven chillers with electric. Be sure this is included in the base case; see Comment 2, sub-par 4.c., above.	A/E will comply.
10.	Pg 8	Par 5): Reference records (in Appendix, I presume) that were used in determining these costs.	A/E will comply.
11.	Pg 8	Par 9): Have you checked with turbine manufacturers to see if turbines can be operated with saturated steam?	Mollier Charts.
12.	Pg 11	States, "Production levels below 167,000 lb/month have not been evaluated." The graphs provided do not even go as low as 167,000 lb/month. Perhaps they should. Please check and correct as necessary.	Expanded graphs available.
13.	Pg 17	Case 1: See Comment 2, sub-par 4.i.	None.
14.	Pg. 18-22	Figures 8 - 12: The axis for "ANNUAL COST" does not identify "cost of what". The axis for "Lbs/Month" appears should be "Millions of Lb/Month". Please correct.	A/E will correct.
15.	Pg 23 & 24	Table 1 & Table 2 would be easier to follow if they were combined into a foldout or if each case were on a separate table printed horizontally. Please consider.	Reformatted tables available.
16.	Pg 25	First paragraph: States that no attempt was made to differentiate between energy cost and demand cost, but gives no justification for this approach. Usually it is worth while to consider the effects of both. Please discuss.	A/E will include additional evaluation.
17.	Pg 96	LCCA for Case 2: This may change based on Comment 2, but why would there be no coal cost or savings if a change was made from electricity to steam (or vice-versa) for driving the pumps? Please correct as necessary.	Minimum boiler oper. point - steam blown to atmosphere.
18.	Pg 97, 98, & 99	LCCA for Case 3, Case 4, & Case 5: I don't understand the asterisks under "Savings" for natural gas. I would expect there to be a negative number in this location. Please explain.	LCCID format not adjustable calculated value is out of range for this summary sheet.
19.	General	The combustion calculations look very good.	None.
20.	Pg 133	Cost Estimate: Please provide some backup for the lump sum costs for Bailey Motor Co. Control Rehab and for Misc piping, tubing, valves & fittings.	Backup will be provided.
21.	Pg. 134	Please provide some backup for Transporting and for Boiler Startup.	Unintentional omission.
22.	Pg. 136	This is hard to follow. Please include more explanation of details, and improve format.	A/E will comply.
23.	General	In the appendices there are several invoices and other documents which have been highlighted. The highlighted figures become opaque when reproduced; so the copies become essentially useless. Please find a better way to present this information.	A/E will annotate documents.
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24.	Pg 139	Demand charge for natural gas. Will this change with increased use? Please discuss.	Discussion will be provided.
25.	Pg 168	Table: Please indicate units in the column headings (lb/hr)?	A/E will comply.
26.	Pg 170	Label fan & motor.	A/E will comply.
27.	Pg 172	Indicate proposed size of steam lines leaving new boilers.	A/E will comply.
28.	Noted	The following are nit-picky editorial comments:	
	Pg 1	Holston AAP is in Kingsport, TN.	A/E will correct.
	Pg 2	No. 11: "Benefit/Cost" ratios.	A/E will comply.
	Pg 2	Correct spelling of "alternative".	A/E will comply.
	Pg 11	3413 Btu/kWh	A/E will comply.
	Pg 11	"calculations are presented"	A/E will comply.
-	Pg 25	Correct spelling of "differentiate".	A/E will comply.

MOBILE DISTRICT PROJECT REVIEW COMMENTS

DATE:

28 Sept. 1995

Page 295 of 5

TO: U.S. Army Corps of Engineers Mobile District

Mobile, AL

FROM: Jerry Bouchillon (HDC Engineering)

Sonee Hall (HDC Utilities)

PROJECT/FY: FY95 Limited Energy Study for Area "A" Package Boilers

OCATION: Holston Army Ammunition Plant, Kingsport, TN

TYPE REVIEW: Interim Submittal Review

NO.	PAGE/PAR	COMMENT	RESPONSES TO COMMENT
1.	General	This study appears to be a respectable analysis of the subject manner.	
2.	Pg 4	The FINDINGS, ANALYSIS AND RESULTS are not very definitive. What is the meaning of a negative SIR? Why can't the short, candid CONCLUSION of page 25 be put on page 4?	A/E will consider revisions as requested.
3.	General	I would like to see a step-wise sample calculation showing how each of the 12 parts for a given condition (example: Case 3, 0.075 mill #/mo) on Tables 1 and 2 are obtained.	A/E will provide.
4.	General	Please be consistent with units on all tables, text and figures. For example, say, "750,000 #/MO Eq RDX" instead of "0.75 MILL #/MO", etc.	A/E will edit as required.
5.	General	Any analysis involving LCCID of Cases 4 and 5 (using VAAP Boilers) shall include consideration for the cost to layaway Building 8A since this will be a natural consequence of making this change.	Feedwater system, boiler water treatment and deaerator continue in service coal boilers can be laid away.
6.	General	All "units costs" in units of \$/MBtu for the LCCID's (pages 96-99) shall be changed to reflect the unit costs of STEAM generated with these fuels similar to the analysis on page 145 for coal instead of the unit cost of the heating value of the fuels. For example, coal = 3.00 \$/MBtu instead of 1.86 \$/MBtu.	LCCID instructions call for fuel costs and non-energy savings account for remainder.
7.	Pg 96-99	In the LCCID's changes the SIOH and Design Costs to reflect more realistic values. These can be obtained from Tony Battaglia unless you have already done so.	A/E will revise if directed to do so; values shown are program default values.

Appendix 8
Indeck Power Equipment Company
Lease Proposal

INDECK POWER EQUIPMENT COMPANY - 1111 SOUTH WILLS AVENUE - WHEELING, ILLINOIS 600E0-5841



October 25, 1995

Affiliated Engineers S. E., Inc.

Attn: Mr. Paul Little

FAX #:1-904-375-3479

REFERENCE:

YOUR TELEPHONE INQUIRY OF OCTOBER 24, 1995

INDECK PROPOSAL #6421

SUBJECT:

800 HP BOILER AND DEAERATOR RENTAL PROPOSAL

Dear Mr. Little:

Per the above referenced telephone conversation in which we discussed the possible rental of an 800 HP firetube boiler and a duplex packaged deaerating system for a U.S. Government operation in Tennessee, I am pleased to provide the following information for your review, evaluation and further rental consideration.

INDECK POWER EQUIPMENT COMPANY PROPOSES TO FURNISH:

One (1) New 800 HP Donlee Technologies (York-Shipley) 3-pass packaged automatic firetube boiler, Model #596-SPH-800-N/2. This unit will be designed, built and stamped in accordance with the latest edition of the ASME Power Boiler Code, Section I for a design pressure of 150 psig and an operating pressure range of 50-125 psig. The unit will be equipped with a York-Shipley designed and built natural gas and #2 oil fired forced draft, fully modulating burner. The unit will be complete with the manufacturer's standard boiler trim, burner and controls as per the following specification sheets as well as the following recommended optional equipment:

- a. Stack thermometer installed
- b. 2" blowdown valves two quick and one slow opening (shipped loose)
- c. Warrick probe type auxiliary low water cut off, Model #3E1B
- d. 2" Jordan electric modulating feedwater valve with 3-valve bypass
- e. 460 V, 3-phase, 60 Hz main power with a 120 V, single phase control voltage transformer
- f. Single electric location connection with circuit breakers
- g. Three (3) indicating lights (customer to specify function)
- h. Manual reset steam limit control
- i. Manual potentiometer for manual firing rate adjustment



Page 2.

One (1) packaged duplex feedwater deaerating system consisting of a 30,000 PPH horizontal storage tank designed, built and stamped to the ASME Code for 50 psig design pressure and will have 10 minute storage to overflow. The vessel will be complete with make-up water regulating valve with float cage and operating linkage, overflow trap, steam pressure reducing valve, high and low water level switches, sentinel type relief valve, vent valve, water level gauge glass set, steam pressure gauges and two (2) thermometers. The vessel will be mounted on a 4-post structural steel support stand with pads to match the deaerator tank saddles, foundation pads with holes, base plate for pump sets with structural steel horizontal and diagonal support braces. Mounted beneath the vessel will be two (2) centrifugal boiler feedwater pumps, each with a minimum flow rate of 60 gpm at 150 psig pump discharge pressure coupled to drip-proof drive motors requiring 460 V, 3-phase, 60 Hz power. A control panel in a NEMA 1 enclosure will be furnished and include two (2) pump motor starters, pump circuit breakers, pump running lights, high and low water lights with alarm bell and silencing switch, pump selector switch and terminal switch. Duplex suction piping assembly which includes gate valves, flexible connectors, compound gauges and pipe supports. Discharge piping will be supplied with a separate gate and check valve and pressure gauge. The unit will be shop assembled with the horizontal storage tank and some trim removed to facilitate shipping clearances.

Based on a minimum guaranteed rental term of 36 months, a budgetary monthly rental rate for the boiler and deaerator as described above is \$3,800.00.

Delivery of this equipment is approximately 12-14 weeks after receipt of approved contract.

The following two pages are the boiler and burner specifications and should you require additional information on either the boiler or deaerator please feel free to contact me at your convenience.

Thank you for your inquiry and I look forward to working with you further when you have final specifications available for firm pricing.

Very truly yours,

INDECK POWER EQUIPMENT COMPANY

Wayne J. Cerny Vice President

Sales and Rentals

Wayne Kerny

SAMPLE SPECIFICATIONS

HIGH PRESSURE STEAM BOILERS
(150 PSI OR HIGHER)

A. GENERAL

FURNISH (AMERICAN) ONE PACKAGED SCOTCH TYPE STEEL BOILER(S) DESIGNED AND CONSTRUCTED FOR (T50) (150) PSIG STEAM PRESSURE IN ACCORDANCE WITH SECTION I ASME CODE. THE UNIT SHALL BE MOUNTED ON A STEEL FRAME, COMPLETE WITH BURNER AND ALL NECESSARY CONTROLS, AND SHALL BE FACTORY ASSEMBLED AND FIRE TESTED, READY FOR ATTACHMENT OF STEAM SUPPLY AND FEEDWATER LINES, BLOW-OFF PIPING, FUEL LINES, ELECTRICAL CONNECTIONS, AND VENT/BREECHING CONNECTION. THE ENTIRE UNIT SHALL BEAR THE UNDERWRITER'S LABORATORY B LABEL.

THE BOILER SHALL HAVE A CONTINUOUS NOZZLE RATING OF 800 BOILER HORSEPOWER, 27,600 LBS. OF STEAM/HR., AND 26800 MBH GROSS OUTPUT, AND SHALL BE A YORK-SHIPLEY MODEL 596-SPH-800-M2.

B. BOILER DESIGN

THE BOILER SHALL BE OF THE FIRE TUBE TYPE, THREE PASS, DRY-BACK DESIGN. THE BOILER SHALL HAVE (A MINIMUM OF FIVE SQUARE FEET PER BOILER HORSEPOWER OR A TOTAL OF) 4000 SQUARE FEET OF EFFECTIVE FIRESIDE HEATING SURFACE. IT SHALL BE PROVIDED WITH HANDHOLES AND A MANHOLE AS REQUIRED BY ASME CODE.

THE BOILER SHALL BE COVERED ON SIDES AND TOP WITH A MINIMUM OF 2" OF GLASS WOOL INSULATION AND PROTECTED BY A 22 GAUGE SHEET STEEL JACKET. A HEAVY GAUGE STEEL CATWALK SHALL BE INCLUDED AS PART OF THE JACKET ALONG THE TOP LONGITUDINAL CENTERLINE OF THE BOILER SHELL.

THE FURNACE TUBE SHALL BE CENTRALLY LOCATED IN THE BOILER SHELL, AND SHALL BE EQUIPPED WITH A REFRACTORY TARGET RING FOR RESHAPING THE FLAME AT A POINT WHERE IT BEGINS TO SPREAD. ALL REFRACTORY BRICKWORK SHALL BE HIGH TEMPERATURE FIREBRICK AND/OR PRE-CAST REFRACTORY SHAPES LAID IN HIGH TEMPERATURE REFRACTORY CEMENT. THE REAR TURNING CHAMBER SHALL BE LINED WITH HIGH TEMPERATURE PRE-CAST REFRACTORY AND BACKED WITH SEAL WELDED STEEL LINING TO PREVENT FLUE GAS SHORT-CIRCUITING.

THE REAR DOOR SHALL BE DESIGNED IN THREE SECTIONS FOR EASE OF REMOVAL AND TO ALLOW ACCESS TO ANY SECTION OF THE FIRESIDE SURFACE WITHOUT REMOVING THE ENTIRE DOOR. THE LOWER REAR SECTION SHALL BE INSULATED OR REFRACTORY LINED AS REQUIRED. THE REFRACTORY LINED SECTION SHALL BE SUPPORTED BY A HINGED DAVIT ARRANGEMENT. THE FRONT DOOR SHALL BE ONE PIECE OR TWO PIECE, AS REQUIRED BY WEIGHT AND SIZE, AND INSULATED WHERE NECESSARY. THE FRONT DOOR SHALL INCLUDE AN ACCESS OPENING FOR CLEANOUT WITHOUT REQUIRING OPENING OF THE DOOR.

C. TRIM AND CONTROLS

THE BOILER SHALL BE EQUIPPED WITH A COMBINATION WATER COLUMN, PUMP CONTROLLER, AND LOW WATER CUT-OFF WITH ALARM SWITCH; AND WITH WATER GAUGE SET AND GLASS, TRY COCKS, AND WATER COLUMN BLOWDOWN VALVE. IN ADDITION, THE BOILER SHALL BE EQUIPPED WITH A SAFETY LIMIT CONTROL AND A SEPARATE OPERATING LIMIT CONTROL. SAFETY VALVES AND A STEAM PRESSURE GAUGE SHALL BE FURNISHED. ALL THE ABOVE EQUIPMENT SHALL BE FACTORY PIPED AND WIRED IN ACCORDANCE WITH ASME CODE AND U/L REQUIREMENTS.

SAMPLE SPECIFICATIONS

GAS/#2 OIL BURNERS

FA BURNERS - 400 THRU 1000 HP

FOR STEAM-PAK BOILERS

THE BURNER SHALL BE A YORK-SHIPLEY MODEL FA AND SHALL BE DESIGNED FOR FIRING NATURAL GAS OR #2 FUEL OIL, WITH GAS CHARACTERISTICS OF 1000 BTU/CU. FT., SPECIFIC GRAVITY OF ______, AN AVAILABLE GAS SUPPLY PRESSURE OF ______, AND A FIRING RATE OF 33,500 CU. FT./HR. GAS AND _______ GPH OIL. THE OVERALL EFFICIENCY OF THE UNIT, BASED ON FUEL INPUT AND BOILER OUTPUT, SHALL BE NOT LESS THAN 80%.

THE BURNER SHALL BE EXTERNAL MIX GAS AND LOW PRESSURE AIR ATOMIZED OIL TYPE, USING A GAS PORT AND OIL NOZZLE ARRANGEMENT WITH AN AIR SWIRL FOR MAXIMUM COMBUSTION EFFICIENCY. IGNITION SHALL BE ACCOMPLISHED BY A SPARK IGNITED NATURAL GAS PILOT USING A 10,000 VOLT IGNITION TRANSFORMER.

THE PILOT SHALL INCLUDE, IN ADDITION TO THE NOZZLE AND ELECTRODE ASSEMBLY, A SOLENOID GAS VAVLE, GAS PRESSURE REGULATOR WITH 5 PSI MAXIMUM INLET PRESSURE RATING, AND A SHUT-OFF COCK.

THE BURNER SHALL BE ARRANGED FOR FULLY MODULATED FIRING, USING A SINGLE MODULATING MOTOR WITH BUILT IN END SWITCH FOR GUARANTEED LOW FIRE START, A LINKAGE ARRANGEMENT TO GOVERN BOTH AIR SUPPLY AND FUEL SUPPLY.

THE BURNER SHALL INCLUDE A HINGED DOUBLE DOOR FULLY ENCLOSED CONTROL PANEL WITH LATCH, MOUNTED SEPARATELY ON THE BOILER, WITH TERMINAL STRIPS FOR MAIN ELECTRICAL POWER CONNECTION AND FOR ALL WIRING RUNNING OUT OF THE PANEL, A CONTROL CIRCUIT FUSE, AN ON-OFF TOGGLE SWITCH, FUEL CHANGEOVER SWITCH, A YS-7000L MICROCOMPUTER TYPE FLAME CONTROL WITH LEAD SULFIDE SCANNER, ALL MOTOR STARTERS (WHERE SPACE PERMITS), RELAYS, TRANSFORMERS, ETC.

THE BURNER SHALL BE FORCED DRAFT TYPE WITH A BLOWER WHICH FURNISHES ALL NECESSARY AIR FOR COMBUSTION, AND INCLUDES AN AIR INLET SILENCER. THE BLOWER AIR SUPPLY SHALL BE GOVERNED BY THE MODULATING MOTOR LINKAGE CONNECTED TO A DAMPER ON THE BLOWER DISCHARGE. THE BURNER SHALL INCLUDE AN AIR SAFETY INTERLOCK FOR LOW BLOWER AIR. THE BLOWER SHALL BE AN AIR FOIL TYPE AND SHALL BE DIRECTLY DRIVEN BY A 40 HP 3500 RPM MOTOR.

THE BURNER WINDBOX SHALL BE FURNISHED WITH A BOLTED-ON ACCESS PLATE FOR EASY REMOVAL OF THE NOZZLE AND ELECTRODE ASSEMBLY. IN ADDITION, THE ENTIRE BACK PLATE OF THE WINDBOX SHALL BE REMOVABLE FOR EASY ACCESS TO THE OTHER INTERNAL BURNER COMPONENTS.

THE BURNER SHALL INCLUDE A SINGLE OIL NOZZLE WHICH PROVIDES FOR MIXING OF FUEL WITH COMPRESSOR AIR INSIDE THE NOZZLE. OIL FLOW SHALL BE CONTROLLED BY A SINGLE SOLENOID VALVE ON THE NOZZLE SUPPLY LINE, PLUS AN ADJUSTABLE TEARDROP TYPE COMBINATION HIGH FIRE AND METERING VALVE, ACTUATED BY THE MODULATING MOTOR LINKAGE. THE OIL SUPPLY LINE TO THE BURNER SHALL INCLUDE A FILTER UPSTREAM OF THE CONTROL VALVES AND SOLENOID VALVE.

SAMPLE SPECIFICATIONS CONT'D

GAS/#2 OIL BURNERS

BURNERS - 400 THRU 1000 HP CONT'D

FOR STEAM-PAK BOILERS

COMPRESSED AIR FOR THE AIR ATOMIZATION SHALL BE PROVIDED BY A ROTARY VANE TYPE AIR COMPRESSOR, COMPLETE WITH AIR FILTER, RELIEF VALVE, PRESSURE GAUGE, AUTOMATIC GRAVITY FEED LUBRICATOR, OIL ACCUMULATOR, AND BELT DRIVEN WITH AN ADJUSTABLE SHEAVE ARRANGEMENT AND A / HP 1750 RPM MOTOR.

GAS CONTROLS INCLUDE A BUTTERFLY TYPE GAS VOLUME VALVE CONNECTED BY LINKAGE TO THE MODULATING MOTOR, A DOWNSTREAM BLOCK/TEST LUBRICATED PLUG COCK, A MOTORIZED TYPE SAFETY GAS VALVE WITH INTEGRAL PROOF-OF-CLOSURE SWITCH, A PRIMARY MOTORIZED GAS VALVE, AN UPSTREAM SHUT-OFF LUBRICATED PLUG COCK, HIGH AND LOW GAS PRESSURE INTERLOCKS, AND TEST CONNECTIONS DOWNSTREAM OF EACH MOTORIZED VALVE. A NORMALLY OPEN FULL PORTED SOLENOID VENT VALVE SHALL BE INCLUDED BETWEEN THE MOTORIZED GAS VALVES. A MAIN GAS PRESSURE REGULATOR SHALL BE (INCLUDED AND SHIPPED LOOSE) (INSTALLED DOWN-STREAM OF THE MAIN SHUT-OFF-COCK) (FURNISHED BY OTHERS).

ALL MOTORS SHALL BE ARRANGED FOR CONNECTION TO 295 VOLTS, 3 PHASE, 60 HERTZ ELECTRICAL POWER AND THE CONTROL SYSTEM SHALL BE ARRANGED FOR 115 VOLTS, 1 PHASE, 60 HERTZ POWER (USING A CONTROL VOLTAGE TRANSFORMER).

CENTRAL TX COMMERCIAL A/C & HEATING, INC.

7909 Rosson Dr. Austin, Texas 78736-8018 License #: TACLA 002692C 512/288-0822 1-800-338-5429 Fax #288-0941

October 30, 1995

Affiliated Engineers
Attn: Mr. Paul Little
3300 Southwest Archer Road
Gannsville, FL 32608
Fax (904) 375-3479

Central Texas Commercial Air Conditioning and Heating, Inc. is pleased to propose:

- 1) Lease for 800 horse power boiler at 100 PSI, including dearator and feed water pumps. Quote includes the following:
 - * One 800 Hp or two (2) 400 Hp boilers set up to burn natural gas or #2 fuel oil.
 - * Motor for 230/460 volts.
 - * 110 volt control transformer.
 - * Freight to and from job site.
 - Dearator with dual pumps and controls.
 - * Start up after complete installation.
- 2) Installation is not included.
- 3) Licensing and insurance are not included.
- 4) Taxes are not included.
- 5) Terms and Conditions attached

First 12 month lease \$7,800.00/month 2nd year lease cost \$5,800.00/month 3rd year lease cost \$4,900.00/month

If you have any questions please don't hesitate to call.

Best Regards,

Roland R. Hampton, Jr.

Roland R. Hamph Jr.

President

RRH:jm